ENZYMATIC CONVERSION STRATEGIES OF STARCH TO MALTOOLIGOSACCHARIDES BY MALTOGENIC AMYLASE AND CYCLODEXTRIN GLUCANOTRANSFERASE

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ABSTRACT

nature, Bacillus lehensis G1 utilizes extracellular cyclodextrin glucanotransferase (CGTase) to degrade starch into cyclodextrins (CDs). This is followed by hydrolysis of CDs by intracellular maltogenic amylase (MAG1) into glucose, maltose and maltooligosaccharides (MOS). The MOS are potential prebiotic for human consumption. In industries, amylases are used to produce MOS from starch. However, the conversion of starch directly to MOS using MAG1 has several limitations such as low specificity towards starch compared to β -cyclodextrin (β -CD) and low productivity of MOS. In order to overcome these drawbacks, two strategies involving optimization of reaction parameters using statistical method and synergism of enzyme mixture approach, were applied. In this study, the optimization of enzymatic reaction parameters for enhanced MOS production by MAG1 using soluble starch as a substrate was performed. In the first strategy, the effects of reaction parameters (enzyme loading, substrate loading, temperature, reaction time and pH) on MOS yield was investigated using one-factor-at-a-time (OFAT) method and 2⁵⁻¹ fractional factorial design. Based on the 2⁵⁻¹ fractional factorial design results, three parameters namely substrate loading, reaction time and pH were found to have a significant effect and was used in central composite design under response surface methodology (RSM). The MOS production was successfully optimized by the RSM. Under the optimized conditions (0.25 % (w / v) of substrate loading, 0.5 h of reaction time and pH 7.45) by RSM, the MOS yield was 107.29 mg/g of substrate which was 1.3-fold higher compared to the value after OFAT analysis which was only 84.87 mg / g of substrate. In the second strategy, the synergistic effect of MAG1 and CGTase for improving the MOS production process had also been studied using two different approaches which were asynchronous and synchronous methods. asynchronous method, the cyclization and hydrolysis reaction of CGTase and MAG1, were carried out in two separated steps respectively. Whereas, for the synchronous method, the two enzymes were added simultaneously and became a one-pot enzymatic The results from the studies conducted show the capability of the synchronous method was capable to convert the soluble starch (1.5 % (w / v)) into MOS with higher yield than the asynchronous method. The optimum conditions were obtained when MAG1 loading to CGTase loading in 3 U: 7 U ratio, with the reaction temperature of 40 °C and pH 7.0. Based on these optimum conditions, the total yield of MOS attained was 307.86 mg/g of substrate after 2 h, which was 2.1-fold higher than the asynchronous method (146.78 mg / g) and 2.9-fold higher compared to the reaction of MAG1 alone. The used of CGTase and MAG1 synchronously enable the direct conversion of soluble starch to higher yield of MOS.

ABSTRAK

Secara semulajadi, Bacillus lehensis G1 menggunakan enzim siklodekstrin glukanotransferase (CGTase) di luar sel untuk menukarkan kanji kepada siklodekstrin (CD). Diikuti dengan hidrolisis CD oleh amilase maltogenik (MAG1) di dalam sel menjadi glukosa, maltosa dan maltooligosakarida (MOS). MOS adalah prebiotik yang berpotensi untuk kegunaan manusia. Didalam industri, amilase digunakan untuk menghasilkan MOS daripada kanji. Walau bagaimanapun, penukaran kanji secara langsung kepada MOS menggunakan MAG1 mempunyai beberapa kekangan seperti pengkhususan yang rendah terhadap kanji berbanding β-siklodekstrin (β-CD) dan produktiviti MOS yang rendah. Untuk mengatasi kelemahan ini, dua strategi yang melibatkan pengoptimuman pembolehubah tindakbalas dengan menggunakan kaedah statistik dan pendekatan sinergi campuran enzim, telah digunakan. Dalam kajian ini, pengoptimuman terhadap pembolehubah tindakbalas enzimatik bagi meningkatkan penghasilan MOS oleh MAG1 dengan menggunakan kanji boleh larut sebagai substrat telah dilakukan. Dalam strategi yang pertama, kesan pembolehubah tindakbalas (muatan enzim, muatan substrat, suhu, masa tindakbalas dan pH) terhadap penghasilan MOS telah dikaji menggunakan kaedah satu-faktor-pada-satu-masa (OFAT) dan reka bentuk pemfaktoran pecahan 2⁵⁻¹. Berdasarkan kepada keputusan reka bentuk pemfaktoran pecahan 2⁵⁻¹, tiga pembolehubah iaitu muatan substrat, masa tindakbalas dan pH didapati mempunyai kesan yang ketara dan digunakan dalam reka bentuk komposit berpusat di bawah kaedah sambutan permukaan (RSM). Penghasilan MOS berjaya dioptimumkan dengan RSM. Di bawah keadaan yang dioptimakan (0.25 % (w / v) muatan substrat, 0.5 jam masa tindakbalas dan pH 7.45) oleh RSM, hasil MOS adalah 107.29 mg / g substrat yang mana 1.3 kali lebih tinggi berbanding dengan nilai selepas analisis OFAT iaitu hanya 84.87 mg/g substrat. Dalam strategi yang kedua, kesan sinergistik MAG1 dan CGTase dalam memperbaiki proses penghasilan MOS juga telah dikaji dengan menggunakan dua pendekatan yang berbeza iaitu kaedah tidak serentak dan serentak. Bagi kaedah tidak serentak, tindakbalas pensiklikan dan hidrolisis CGTase dan MAG1, masing-masing telah dijalankan dalam dua langkah berasingan. Manakala, untuk kaedah serentak, kedua-dua enzim telah ditambah secara serentak dan menjadi tindakbalas enzimatik satu bekas. Hasil daripada kajian yang telah dijalankan menunjukkan kemampuan kaedah serentak mampu menukarkan kanji boleh larut (1.5 % (w/v)) kepada MOS dengan hasil yang lebih tinggi daripada kaedah tidak serentak. Keadaan optima diperolehi apabila muatan MAG1 kepada muatan CGTase dalam nisbah 3 U: 7 U, dengan suhu tindakbalas 40 °C dan pH 7.0. Berdasarkan keadaan optima ini, hasil keseluruhan MOS yang dicapai adalah 307.86 mg / g substrat selepas 2 jam, iaitu 2.1 kali ganda lebih tinggi daripada kaedah tidak serentak (146.78 mg/g) dan 2.9 kali ganda lebih tinggi berbanding tindakbalas oleh MAG1 sahaja. Penggunaan CGTase dan MAG1 secara serentak membolehkan penukaran kanji boleh larut terus kepada hasil MOS yang lebih tinggi.

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LIST OF ABBREVIATIONS AND SYMBOLS

A₆₀₀ - absorbance at optical density of 600 nm

Asp or D - Aspartic acid

B. lehensis - Bacillus lehensis

B. licheniformis - Bacillus licheniformis

B. stearothermophilus - Bacillus stearothermophilus

BSA - bovine serum albumin

C - carbon

CGTase - Cyclodextrin glucanotransferase

CD - cyclodextrin

E. coli - Escherichia coli

EC - Enzyme Commission

g - gram

G. thermoleovorans - Geobacillus thermoleovorans

GH - Glycosyl Hydrolase

Glu or E - glutamic acid

h - hour

H - hydrogen

HPLC - high-performance liquid chromatography

IPTG - isopropyl β-D-1-thiogalactopyranoside

kDa - kilodalton

l - liter

L. gasseri - Lactobacillus gasseri

LB - Luria-Bertani

m - mili
M - molar
M1 - glucose
M2 - maltose

M3 - maltotriose

M4 - maltotetraose

M5 - maltopentaose

M6 - maltohexaose

M7 - maltoheptaose

MAG1 - maltogenic amylase from Bacillus lehensis G1

mg - milligram
min - minute
ml - milliliter

MW - molecular weight

NEB - New England Biolabs

nm - nanomete
O - oxygen
OH - hydroxyl

PMSF - phenylmethylsulfonyl fluoride

rpm - revolutions per minute

s - second

SDS - sodium dodecyl sulphate

SDS-PAGE - sodium dodecyl sulfate-polyacrylamide gel

sp - species U - unit

UV - ultraviolet

V - volt

w/v- weight per volumew/w- weight per weight

 α - alpha

 α -CD - α - cyclodextrin

 β - beta

 β -CD - β -cyclodextrin $^{\circ}$ C - degree celcius

γ - gamma

γ- CD - γ-cyclodextrin

μ - micro

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CHAPTER 1

INTRODUCTION

1.1 Background

Starch is a polysaccharide that resulted from the photosynthesis process of green plants. Starch is the most abundant form of storage in cereals, legumes and mainly tubers. In the plant, the starch is stored within the cells as partially crystalline granules (Englyst *et al.*, 2006). According to Van Der Maarel *et al.* (2002), starch also can be used to produce glucose, maltose, dextrin, maltooligomer mixture and oligosaccharides, by chemically or enzymatically. Nowadays, the use of enzymes for catalyzing various biochemical reactions is more preferable than chemical such as acid because it is safer and environmental-friendly. Since the starch is naturally existed in a form of an insoluble starch granules, therefore, most of the research on starch degrading enzyme, has been conducted on gelatinized starch, which is starch granules was heating in water to produce starch solution (Taniguchi and Honnda, 2009).

Glucan-1,4-α-maltohydrolase (EC 3.2.1.133) is usually known as maltogenic amylase. It is an amylolytic enzyme from glycosyl hydrolase family 13 (GH 13). It is one of the maltooligosaccharide- forming amylase (MFAse) enzyme used in the commercial production of maltose and novel oligosaccharides for food and pharmaceutical applications. In addition to hydrolysis, maltogenic amylase also known to have transglycosylation ativity to produce sugar molecules with various lengths. Maltogenic amylase exhibits broad substrates specificity toward cyclodextrins (CDs), starch and pullulan and favours CDs as a substrate (Kim *et al.*, 1999).

Oligosaccharides have potential benefits for human health and diverse applications in improving physicochemical properties of foods. Conventionally, the oligosaccharides were synthesized using chemical such as acid. However, later the use of enzymes for oligosaccharides production is more preferable than chemical because it is safer, environmental-friendly, low cost and give high yield. Glycoside hydrolases and glycosyltransferases have been used, but glycoside hydrolase enzymes are favoured due to cheap and easy-to-get saccharides, such as starch as their substrates.

However, excessive hydrolysis could be one of the drawback resulting in low yield of oligosaccharides. The control of the reaction condition will affect the reaction and product yield. Furthermore, less substrate specificity of starch would also results in the low yield of oligosaccharides. Over a decade, interest in oligosaccharides is growing and research are being carried out to improve the production of oligosaccharides. The development for synergism of enzyme mixture is an alternative for enhancing the production of oligosaccharides. Previous findings such as Kuriki *et al.* (1993) and Lee *et al.* (2002a) have provided a guidance for improving the direct conversion of starch to achieve the objective of the current study.

1.2 Problem Statement

To date, numerous enzymes are being discovered and some are available commercially to degrade starch for producing oligosaccharides. Thus, the use of enzymes is almost completely replace chemical techniques for synthesizing oligosaccharides in the industry. Glycoside hydrolase enzyme is preferred to be employed over the glycosyltransferase enzyme. However, the low production of maltooligosaccharides (MOS) by maltogenic amylase (MAG1) from starch is the major obstacle. Various strategies have been employed to overcome the problem, including the control of thermodynamic equilibrium of the enzyme reaction by manipulating the range of parameters used in reaction mixture (Abdul Manas *et al.*, 2014). However, no statistical study on the influence of reaction conditions for improving MOS production by maltogenic amylase has been reported to date. Enzyme

mixture approach has also become a recently practice to improve the production of oligosaccharides (Li *et al.*, 2017). The substrate specificity of MAG1 towards CD compared to starch also can be a significant drawback for direct conversion of starch into MOS. Therefore, the synergistic enzyme of MAG1 and cyclodextrin glucanotransferase (CGTase) is expected to enhanced the direct conversion or used of starch for MOS production.

1.3 Research Objectives

The objective of this research is to improve the production of MOS by MAG1 from soluble starch via optimization of reaction parameters using statistical method and synergism of enzyme mixture approach.

1.4 Scopes of the Study

This study focusses on the improvement of the production of MOS by appropriate strategies. Therefore, the following scopes were outlined to achieve the objective:

- (a) Expression of MAG1 and CGTase in *Escherichia coli* expression system and purification using AKTAprime plus purification system.
- (b) Determination of the significant ranges of reaction parameters (enzyme loading, substrate loading, reaction time, temperature and pH) on MOS production using a one-factor-at-a-time (OFAT) method and screening of the reaction conditions (enzyme loading, substrate loading, reaction time, temperature and pH) affecting MOS production by Fractional Factorial Design (FFD). Optimization of the reaction conditions (substrate loading, reaction time and pH) by central composite design (CCD) towards the achievement of highest MOS yield.

(c) Screening of the reaction parameters (pH, substrate loading, CGTase loading and reaction time) on β-CD production through OFAT in the first step of the asynchronous method. Screening of the reaction parameters (MAG1 loading and reaction time) on MOS production via OFAT in the second step of the asynchronous method. Screening of the reaction parameters (temperature, MAG1: CGTase ratio, substrate loading and reaction time) on MOS production by OFAT in the synchronous method.

1.5 Novelties of the Study

The novelties of the study are as follows:

- 1. The optimization of reaction conditions for the enhanced MOS yield by maltogenic amylase from *Bacillus lehensis* G1 using statistical tool has not been reported.
- 2. To the best of our knowledge, this is the first report on direct conversion of starch using the synergistic action of maltogenic amylase and CGTase from *B*. *lehensis* G1 to improve the production of MOS.

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LIST OF PUBLICATIONS

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APPENDIX A

Medium and Buffers Preparation

Medium Preparation for E. coli Culturing

Luria-Bertani (LB) Medium/Agar

Composition: 1 % (w/v) tryptone, 0.5 % yeast extract, 0.5 % NaCl and 1.5 % agar.

For 1 liter LB medium/agar:

- 1) The following ingredients were dissolved in 950 ml distilled water: 10 g tryptone, 5 g yeast extract, 5 g NaCl and 15 g agar. For LB medium, agar was excluded.
- 2) The pH of the solution was adjusted to 7.5 using 5 M NaOH solution. Distilled water was added to bring the volume to 1 liter.
- 3) The solution was autoclaved for 15 min at 121 °C.
- 4) When the solution has cooled to ~ 55 °C, antibiotic was added appropriately. For LB agar, the solution was poured into the petri dish and left to solidify. Plates were stored at 4 °C.

Ampicillin Stock Solution

Composition: 100 mg/ml ampicillin.

For 10 ml ampicillin stock solution:

- 1) The ampicillin powder was weighed to 1 g and dissolved in 10 ml distilled water.
- 2) The solution was filtered using a sterile $0.2 \mu m$ nylon syringe filter and keep in a sterile vial.
- 3) The solution was stored in -20 °C and thawed prior to use.

IPTG Stock Solution

Composition: 0.1 M IPTG.

For 10 ml IPTG stock solution:

- 1) The IPTG powder was weighed to 0.24 g and dissolved in 10 ml distilled water.
- 2) The solution was filtered using a sterile $0.2~\mu m$ nylon syringe filter and keep in a sterile vial.
- 3) The solution was stored in -20 °C and thawed prior to use

Buffers for Molecular Works

50X TAE Electrophoresis Buffer

Composition: 2M Tris base, 50 mM EDTA

For 1 liter 50X TAE electrophoresis buffer:

1) The following ingredients were dissolved in distilled water: 242 g Tris base,

57.1 ml glacial acetic acid and 100 ml 0.5 M EDTA (pH 8.0).

2) Distilled water was added to bring the volume to 1 liter.

3) The solution was diluted to 1X prior to use by mixing 20 ml of 50X TAE

buffer with 980 ml distilled water.

EDTA Solution

Composition: 0.5 M EDTA (pH 8.0).

For 500 ml EDTA solution:

1) EDTA was weighed to 93.05 g and put into 350 ml distilled water.

2) The solution was mixed vigorously using a magnetic stirrer and the pH was

adjusted to 8.0 by titrating 5 M NaOH solution. The EDTA powder will

only soluble in solution when the pH reaches 8.0.

3) Distilled water was added to bring the volume to 500 ml.

RNAase A Stock Solution

Composition: 10 mg/ml RNAase A.

For 10 ml RNAase A stock solution:

1) The RNAase A powder was weighed to 0.1 g and dissolved in 10 ml distilled

water.

2) The solution was filtered using a sterile 0.2 µm nylon syringe filter and keep

in a sterile vial.

3) The solution was stored in -20 °C and thawed prior to use.

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TE Buffer

Composition: 10 mM Tris-HCl pH 8.0, 0.1 mM EDTA pH 8.0.

The solution was autoclaved and stored at room temperature

Lysozyme Stock Solution

Composition: 50 mg/ml lysozyme.

For 10 ml 50 mg/ml lysozyme:

- 1) The lysozyme powder was weighed to 0.5 g and dissolved in 10 ml distilled water.
- 2) The solution was filtered using a sterile 0.2 μm nylon syringe filter and keep in a sterile vial.
- 3) The solution was stored in -20 °C and thawed prior to use.

Transformation and Storage Solution (TSS)

Composition: 10% (w/v) polyethyleneglycol (PEG), 5% (v/v) dimethyl sulfoxide (DMSO), 50 mM MgCl2

Preparation:

- 1) The components were weighed and pipetted accordingly and dissolved in LB medium at final pH of 6.5.
- 2) The solution was autoclaved and stored at 4 °C

Buffers for Protein Analysis

50 mM Potassium Phosphate Buffer

Table A1 Preparation of 100 ml of 50 mM potassium phosphate buffer at 25 °C

pН	Volume of 1 M	Volume of 1 M	Volume of distilled	
	K ₂ HPO ₄ (ml)	KH ₂ PO ₄ (ml)	water (ml)	
6.0	8.5	91.5	100.0	
7.0	61.5	38.5	100.0	
8.0	94.0	6.0	100.0	

50 mM Glycine - NaOH Buffer

For 100 ml preparation of 50 mM glycine-NaOH buffer.

- 1) 0.38 g of glycine was weighed and dissolved in distilled water.
- 2) The pH was titrated to desired pH (9.0 and 10.0) using 5 M NaOH.
- 3) Distilled water was added to 100 ml.

Binding Buffer/ Buffer A (Ni²⁺ Affinity Chromatography)

Composition: 20 mM phosphate, 0.5 M NaCl, pH 7.4

For 1 liter preparation of binding buffer:

- 1) 3.12 g of NaH2PO4.2H2O and 29.22 g of NaCl was weighed.
- 2) The powder was dissolved in distilled water by stirring.
- 3) After the powder was completely dissolved, the pH was adjusted to 7.5 using 5 M NaOH or 5 M HCl.
- 4) Distilled water was added to 1 liter.
- 5) The solution was degassed using vacuum filter prior to use for the protein purification.

Elution Buffer/ Buffer B (Ni²⁺ Affinity Chromatography)

Composition: 20 mM phosphate, 0.5 M NaCl, 0.5 M imidazole, pH 7.4

For 500 ml preparation of elution buffer:

- 1) 1.56 g of NaH2PO4.2H2O, 14.62 g of NaCl and 17.02 g of imidazole was weighed.
- 2) The powder was dissolved in distilled water by stirring.
- 3) After the powder was completely dissolved, the pH was adjusted to 7.5 using 5 M NaOH or 5 M HCl.
- 4) Distilled water was added to 500 ml.
- 5) The solution was degassed using vacuum filter prior to use for the protein purification.

Polyacrylamide Stacking Gel (SDS-PAGE)

Composition: 5% polyacrylamide in Tris-HCl pH 6.8.

For 5 ml preparation of stacking gel:

- 1) 0.83 ml of 30% acrylamide mix solution, 0.63 ml of 1.0 M Tris-HCl (pH 6.8) stock solution and 0.05 ml of 10% SDS stock solution was dissolved in 3.4 ml distilled water.
- 2) 0.05 ml of 10% ammonium persulfate and 0.005 ml TEMED were added prior to polymerization.

Polyacrylamide Resolving Gel (SDS-PAGE)

Composition: 12% polyacrylamide in Tris-HCl pH 8.8.

For 15 ml preparation of resolving gel:

- 1) 6.0 ml of 30% acrylamide mix solution, 3.8 ml of 1.5 M Tris-HCl (pH 8.8) stock solution and 0.15 ml of 10% SDS stock solution was dissolved in 4.9 ml distilled water.
- 2) 0.15 ml of 10% ammonium persulfate and 0.006 ml TEMED were added prior to polymerization.

Polycrylamide Mix Stock Solution

Composition: 30% (w/v) Acrylamide, 0.8 (w/v) Bis-acrylamide

Ammonium Persulfate Stock Solution

Composition: 10% ammonium persulfate.

For 2 ml preparation of ammonium persulfate stock solution:

- 1) 0.2 g ammonium persulfate was weighed and dissolved in 2 ml distilled water.
- 2) The solution was kept in 4 °C.

Note: Stable for months in a capped tube in refrigerator.

5X Tris-glycine Electrophoresis Buffer (SDS-PAGE)

For 1 liter preparation of 5X Tris-glycine electrophoresis buffer:

- 1) 15.1 g of Tris-base, 72.0 g of glycine and 5.0 g of SDS were weighed.
- 2) The powder mixture was dissolved in 1 liter distilled water.
- 3) The solution was diluted to 1X before use.

2X SDS – Gel Loading Buffer (SDS-PAGE)

Composition: 100 mM Tris-HCl (pH 6.8), 4% SDS, 0.2% bromophenol blue, 20% glycerol, 200 mM DTT

For 50 ml preparation of 2X SDS – gel loading buffer:

- 1) 0.6055 g of tris base, 2 g of SDS and 0.1 g bromophenol blue were weighed.
- 2) 10 ml glycerol was pipetted and all components were dissolved in distilled water.
- 3) The pH was adjusted to 6.8 and distilled water was added to 50 ml.
- 4) DTT was freshly added to final concentration prior to loading the protein sample.

Staining Solution A

Composition: 50% ethanol, 10% acetic acid.

For 500 ml preparation of staining solution A:

- 1) 263 ml of 95% ethanol and 50 ml of acetic acid glacial were measured and dissolved in distilled water.
- 2) Distilled water was added to 500 ml.

Staining Solution B

Composition: 5% ethanol, 7.5% acetic acid.

For 500 ml preparation of staining solution B:

- 1) 26.3 ml of 95% ethanol and 37.5 ml of acetic acid glacial were measured and dissolved in distilled water.
- 2) Distilled water was added to 500 ml.

Coomassie Blue Solution

Composition: 0.25% coomassie blue

For 50 ml preparation of coomassie blue solution:

- 1) 0.125 g coomassie blue was weighed and dissolved in 50 ml ethanol.
- 2) The solution was kept in a dark bottle at room temperature.

Gel Filtration Buffer

Composition: 50mM NaH2PO4, 0.15 M NaCl, pH 7.4

For 1 liter preparation of gel filtration buffer.

- 1) 6.90 g of NaH2PO4.H2O and 8.77 g of NaCl were weighed and dissolved in distilled water.
- 2) The pH was adjusted to 7.5 using 5 M NaOH or 5 M HCl.
- 3) Distilled water was added to 1 liter.
- 4) The solution was degassed using vacuum filter prior to use for the protein purification.

DNS Reagent

For 500 ml preparation of DNS reagent:

- 1) 5 g dinitrosalicylic acid was weighed and dissolved in 300 ml distilled water in a tin foil-covered beaker.
- 2) 8 g NaOH was weighed and gradually added into the DNS solution and stirred to dissolve.
- 3) 150 g Rochelle salt (sodium potassium tartarate) was weighed and slowly added into the mixture solution and stirred until dissolved at temperature between 40-100 °C.
- 4) Distilled water was added to 500 ml and the solution was kept in a dark bottle at room temperature.

APPENDIX B

Example of Experimental Data Calculation

Maltogenic Amylase Activity Calculation (DNS Assay)

One unit (U) of enzyme activity is defined as the amount of enzyme required to produce 1 μ mol maltose per min under the optimum conditions.

Unit activity per volume enzyme (U/ml) was calculated using the equation below:

Activity,
$$U/ml = \frac{A_{575,enzyme} - A_{575,control}}{A575/\mu mol\ maltose \times 10 \min \times 0.1 ml} \times DF_{enzyme} \times DF_{assay}$$

Where,

 $A_{575, enzyme}$: the absorbance of assay with the enzyme read at 575 nm

 $A_{575, control}$: the absorbance of assay without the enzyme read at 575 nm

 $A_{575}/\mu mol\ maltose$: standard curve equation of maltose

10 min : incubation time

0.1 ml : volume of the enzyme used in the assay

 DF_{enzyme} : dilution factor of the enzyme used for the assay

 DF_{assay} : dilution factor of the enzyme in the assay

Standard deviation = $\sqrt{\sum \frac{(x-\overline{x})^2}{n}}$

Where,
$$x = \text{sample}$$

 $\bar{x} = \text{mean sample}$
 $n = \text{number of sample}$

An example of activity calculation is shown below:

Given,

 $A_{575, enzyme} = 0.136, 0.117, 0.115$ (triplicate readings)

 $A_{575, control} = 0.000, 0.000, 0.000$ (triplicate readings)

 $A_{575}/\mu mol\ maltose = 0.6028$ (from the standard curve)

 $DF_{enzyme} = 100$

 DF_{assay} = 5 (0.1 ml enzyme in 0.5 ml assay volume)

Therefore,

Activity
$$_{1} = \frac{0.136 - 0.000}{0.6028 \times 10 \text{ min} \times 0.1 ml} \times 100 \times 5 = 112.81 \text{ U/ml}$$

Activity
$$_2 = \frac{0.117 - 0.000}{0.6028 \times 10 \min \times 0.1 ml} \times 100 \times 5 = 97.05 \ U / ml$$

Activity
$$_3 = \frac{0.115 - 0.000}{0.6028 \times 10 \min \times 0.1 ml} \times 100 \times 5 = 95.39 \ U / ml$$

Activity mean =
$$\frac{112.81 + 97.05 + 95.39}{3} = 101.75 \ U / ml$$

Standard deviation =
$$\sqrt{\frac{(112.81 - 101.75)^2}{3} + \frac{(97.05 - 101.75)^2}{3} + \frac{(95.39 - 101.75)^2}{3}} = 7.85$$

Enzyme activity = 101.75 ± 7.85 U/ml

Cyclodextrin Glucanotransferase Activity Calculation

 $A {=} \left(\%OD \; decrease \times Y_p \!\!\times D_f \!\!\times\!\! 10^3\right) / \left(MW \!\!\times t_i\right)$

Where,

A = Enzyme activity (U/ml or μ mol/ml) of protein sample

%OD decrease = [(ODcontrol-ODsample)/ ODcontrol] × 100%

 Y_p = mg of β-CD equivalent to 100% OD decrease of the standard curve

 D_f = Dilution factor

MW = Molecular weight of β-CD, 1135

 t_i = Time of incubation

Example of calculation:

% OD decrease:

 OD_{550} for control (in triplicate) = (1.438+1.424+1.438)/3 = 1.433

 OD_{550} for sample (in triplicate) = (1.225+1.226+1.205)/3 = 1.219

Hence, % OD decrease = $[(1.433-1.219)/1.433] \times 100\% = 14.9\%$

Y_p:

When y = 100, y = 66.712x + 6.8336 (refer Figure E1)

100 = 66.712x + 6.8336

x = 1.4

Hence, $Y_p = 1.4$

D_f:

Sample taken for assay = $100 \mu l$

Hence, Df = 10

$$MW \ of \ \beta\text{-CD} = 1135 \ g/mol$$

$$t_i = 10 \ min$$

Therefore, CGTase activity of the sample is:

$$\mathbf{A} = [(14.9)(1.4)(10)(103)]/[(1135)(10)]$$
$$= \underline{18.4 \text{ U/ml}}$$

Protein Concentration Calculation (Bradford Assay)

Protein concentration was calculated using the equation below:

Protein concentration,
$$mg/ml = \frac{A_{595}}{A_{595}/mg \ ml^{-1}BSA} \times DF$$

Where,
$$A_{595}$$
 = the absorbance of Bradford assay read at 575 nm $A_{595}/mg \ ml^{-1} \ BSA$ = standard curve equation of BSA DF = dilution factor of the protein

An example of activity calculation is shown below:

Given,

$$A_{595}$$
 = 0.107, 0.132, 0.112
 $A_{595}/ mg ml^{-1} BSA$ = 0.2815
 DF = 10

Therefore,

Protein concentration
$$_1 = \frac{0.107}{0.2815} \times 10 = 3.80 \ mg / ml$$

Protein concentration
$$_2 = \frac{0.132}{0.2815} \times 10 = 4.69 \ mg / ml$$

Protein concentration
$$_3 = \frac{0.112}{0.2815} \times 10 = 3.98 \ mg / ml$$

Protein concentration mean =
$$\frac{3.80 + 4.69 + 3.98}{3} = 4.16 \ mg / ml$$

Standard deviation =
$$\sqrt{\frac{(3.80 - 4.16)^2}{3} + \frac{(4.69 - 4.16)^2}{3} + \frac{(3.98 - 4.16)^2}{3}} = 0.38$$

Protein concentration = $4.16 \pm 0.38 \, mg/ml$

APPENDIX C

Standard Curves

DNS Assay

Table C1 Absorbance at OD of 575 nm for maltose standards

[Maltose], mM	Maltose mass, µmol	Abs	Average		
0	0	0	0	0	0
1	0.5	0.228	0.223	0.227	0.226
2	1.0	0.536	0.530	0.542	0.536
3	1.5	0.849	0.868	0.884	0.867
4	2.0	1.169	1.181	1.190	1.180
5	2.5	1.538	1.496	1.539	1.524
6	3.0	1.815	1.832	1.847	1.831
7	3.5	2.109	2.117	2.137	2.121
8	4.0	2.418	2.431	2.430	2.426

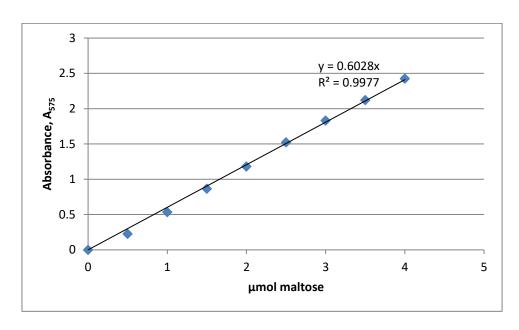


Figure C1 $\,$ The standard curve of absorbance, A_{575} versus maltose mass, μmol

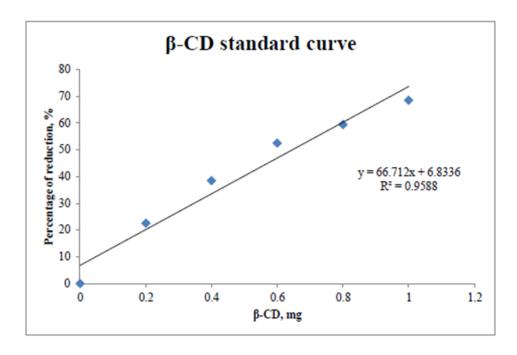


Figure C2 β -CD standard curve for the calculation of CGTase assay

Bradford Assay

Table C3 Absorbance at OD of 595 nm for BSA standards

[BSA], mg/ml	A	Average		
2.0	0.516	0.586	0.594	0.565
1.4	0.403	0.407	0.426	0.412
1.2	0.333	0.341	0.345	0.340
1.0	0.171	0.283	0.294	0.249
0.8	0.214	0.243	0.213	0.223
0.6	0.172	0.168	0.183	0.174
0.4	0.101	0.115	0.113	0.110
0.2	0.057	0.057	0.051	0.055

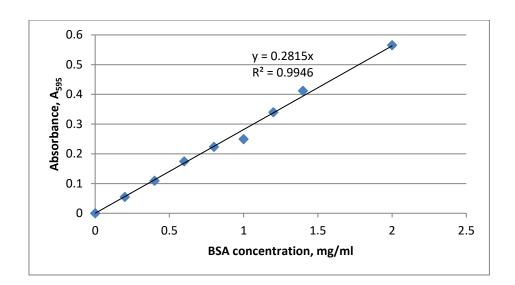


Figure C3 $\,$ The standard curve of absorbance, A_{595} versus BSA concentration, mg/ml

APPENDIX D

Example of Peaks from HPLC Analysis (Standard)

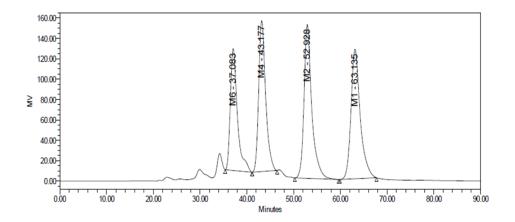


Figure D1 Peaks from standard curve of glucose (M1), maltose (M2), maltotetraose (M4) and maltohexaose (M6) with concentration of 5 mg/ml

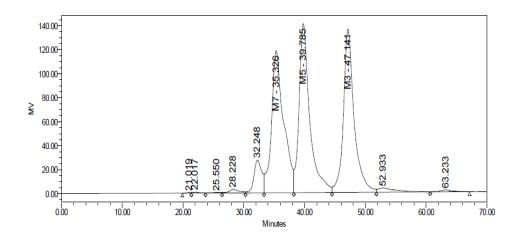


Figure D2 Peaks from standard curve of maltotriose (M3), maltopentaose (M5) and maltoheptaose (M7) with concentration of 5 mg/ml

APPENDIX E

Standard Operational Procedures for Instruments

AKTA Prime

- 1. Distilled water, binding buffer, elution buffer and 20% ethanol were prepared and degassed by vacuum filter using 0.2 μm nylon filter.
- 2. The AKTAPrime and computer were switched on and the PrimeView program was opened.
- 3. Both lines A and B were put in a bottle containing distilled water.
- 4. The system was washed using distilled water by running the 'System Wash' program (Template >Application template>System wash method).
- 5. After the system wash has finished, the flow rate was increased by using manual run (Manual run> Set flow rate 0.5 ml/min> Pressure limit 0.3 MPa> Start run).
- 6. The column was connected to the system via wet connection (drop to drop). Connections were checked for any leakage.
- 7. The flow rate was increased to 5 ml/min. The column was washed by allowing five column volume of distilled water to flow. The flow was end by pressing the 'End' button.
- 8. Line A was put into binding buffer and line B was put into elution buffer.
- 9. The system was washed using buffer by running the 'System Wash' program.
- 10. The column was equilibrated by allowing two column volume of binding buffer to flow using 'Manual Run'. The flow was end by pressing the 'End' button.
- 11. The program for running the desired protein purification was selected and all parameters were set.
- 12. The sample loop was connected to the system and the loop was washed using binding buffer.

- 13. The sample was filtered through a 0.2 µm nylon syringe filter and loaded into the sample loop. Any bubbles in the syringe containing the samples were removed prior to sample loading.
- 14. The fraction collectors were filled in with collection tubes.
- 15. The appropriate method was run.
- 16. After finish, both lines A and B were put in distilled water.
- 17. The system was washed using distilled water by running the 'System Wash' method.
- 18. The column was washed by allowing five column volume of distilled water to flow. The flow was end by pressing the 'End' button.
- 19. Steps 16 to 18 were repeated with 20% ethanol.
- 20. The flow rate was set to 0.5 ml/min by 'Manual Run'.
- 21. The bottom part of the column was detached from the system followed by the top.
- 22. The line was re-connected to the UV detector. Hit End.
- 23. The AKTAPrime and computer were switched off.

Always set pressure limit to 0.3MPa to protect your column from damage.

High Performance Liquid Chromatography (Waters)

- 1. Column and guard column were attached to the appropriate lines.
- 2. Deionized water was degassed using vacuum filter and the probe was inserted into the water.
- 3. The degasser, pump and detector were switched on.
- 4. The computer was switched on and the Breeze software was opened.
- 5. The line for the flow of the mobile phase was set to 100%.
- 6. Pump prime was carried out using a syringe.
- 7. The pump valve was pushed to the right and pump purge was started.
- 8. Method was set by opening a new method in the Breeze software.
- 9. The system was equilibrated for a few seconds to recognize the new set method.
- 10. The flow rate was increased to 0.05 ml/min and pressure was observed. After the pressure was stable, the flow rate was increased gradually. Connecting lines were checked for any leakage.
- 11. When the flow rate reached half of the desired flow rate, the oven was switched on.
- 12. The flow rate was increased gradually until the desired flow rate was reached.
- 13. After flow rate and temperature reached the set up conditions, detector was purged until the reading was stable (until +0000 reading was shown on the detector's screen).
- 14. The detector was unpurged.
- 15. The system was equilibrated until a stable baseline was achieved.
- After finished equilibration, standards and samples can be injected into the column.