

NANOCOMPOSITE ULTRAFILTRATION MEMBRANE INCORPORATING  
ZINC-IRON OXIDE PHOTOCATALYST FOR DECOLOURISATION OF  
TREATED PALM OIL MILL EFFLUENT

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## **DEDICATION**

This thesis is dedicated to my mother, who taught me that the best kind of knowledge to have is that which is learned for its own sake. It is also dedicated to my friends, who taught me that even the largest task can be accomplished if it is done one step at a time.

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## ABSTRACT

Palm oil mill effluent (POME) is brownish, high organic loading effluent produced by palm oil industry. Conventionally used biological treatment has successfully reduced the biochemical oxygen demand of POME below 25 ppm, which is considered as clean effluent. However, chemical oxygen demand (COD) and colour of the aerobically treated palm oil mill effluent (AT-POME) are still high. Therefore, tertiary treatment such as membrane processes are used to further polish AT-POME in order to reduce its COD and colour to meet discharge standard. However, fouling becomes severe issue in restricting the membrane lifespan and usage in this application. This work aimed to develop hybrid photocatalytic membranes with self-cleaning properties to mitigate the membrane fouling and also photodegrades the chemical compounds in AT-POME. First, coupled zinc-iron oxide (ZIO) was synthesized from its precursor, i.e. zinc nitrate and iron (III) nitrate through solution combustion by varying the molar ratio between zinc and iron (ranging from 1:1 to 1:4 with respect to zinc to iron ratio). Second, the optimum molar ratio of ZIO was calcined at temperature ranging from 400°C to 800°C. Third, the self-synthesised ZIO was incorporated into polyvinylidene fluoride (PVDF) polymer matrix to produce mixed matrix photocatalytic ultrafiltration membrane (MMMs) for decolourisation of AT-POME. Five membranes were formulated by varying ZIO from 0.0 wt % to 2.0 wt%. The fabricated membranes were subjected to physico-chemical analysis, i.e. field emission scanning electron microscope, energy dispersive X-ray spectroscopy, X-ray diffraction, Brunauer-Emmett-Teller, ultraviolet-visible-near infrared, absorption test, filtration process, photodegradation test to identify the self-cleaning properties, separation performance and fouling mitigation properties. Based on the experimental results, ZIO with 1:4 zinc to iron ratio was the optimum ZIO which provided large surface area (30.9130 m<sup>2</sup>/g), lowest band gap energy (2.07 eV), high photocatalytic activity (achieved 35% of mineralisation in 6.5 hours and 100% degradation in 3.5 hours). On the other hand, as calcination temperature increased, the particle size of ZIO increased gradually. This phenomenon led to the decrease of surface area of ZIO that reduced its performance in absorption and photodegradation of organic compounds. The results demonstrated that calcination temperature of 500°C was the optimum temperature to provide the highest photodegradation. For the MMMs, as the ZIO loading increased, the porosity decreased, and surface negativity increased. However, when higher loading of ZIO was used, the mechanical strength of the membrane structure deteriorated and cannot withstand long-term operation. Therefore, the optimum loading was identified as 0.5 wt% ZIO in which the membrane achieved 75% colour removal efficiency with flux of 20 – 25 LMH (L.m<sup>-2</sup>.hr<sup>-1</sup>). Furthermore, the self-fabricated MMMs photocatalytic ultrafiltration (UF) membrane possess the high flux recovery after ultraviolet and visible light cleaning, i.e. 92.3% and 90.3%, respectively. The addition of ZIO in polymeric matrix enabled the photodegradation of colour pigments in AT-POME. After 16 hours of operation, the colour of AT-POME reduced by 8%. In a nutshell, PVDF/ZIO photocatalytic UF membrane had successfully decolourised AT-POME and reduced its COD.

## ABSTRAK

Efluen minyak kelapa sawit (POME) merupakan efluen berwarna perang dan mempunyai kandungan bahan organik yang tinggi yang dibebaskan dari kilang kelapa sawit. Secara lazimnya, rawatan biologi digunakan untuk merawat POME supaya keperluan oksigen biokimia di bawah 25 ppm, yang dikatakan sebagai efluen bersih. Walaubagaimanapun, keperluan oksigen kimia (COD) dan warna bagi efluen minyak kelapa sawit selepas rawatan anaerobik (AT-POME) masih tinggi. Jadi, rawatan tertier seperti proses membran digunakan untuk merawat AT-POME supaya COD dan warnanya dapat dikurangkan supaya mencapai tahap piawai. Pengotoran membran menjadi isu yang mengehendkan penggunaan proses membran dalam aplikasi ini. Kajian ini bertujuan untuk menghasilkan membran fotopemangkinan hibrid dengan ciri pencucian sendiri untuk meringankan pengotoran membran fotopemangkinan serta menguraikan sebatian organik dalam AT-POME. Pertama, zink-ferum oksida (ZIO) berganding diolah dengan menggunakan zink nitrat dan ferum (III) nitrat sebagai prekursor melalui kaedah pembakaran larutan dengan mengubah nisbah molar antara zink dengan ferum (julat dari 1:1 ke 1:4). Kedua, nisbah molar ZIO optimum dikalsinat pada suhu 400°C hingga 800°C. Ketiga, ZIO ditambah ke dalam matriks polimer polivinilidene difluorida (PVDF) untuk menghasilkan membran ultraturusan fotopemangkinan matriks bercampur (MMMs) untuk penyahwarnaan AT-POME. Lima membran diformulasi dengan mengubah kandungan ZIO dari 0.0 wt% ke 2.0 wt%. Membran yang dihasilkan dikaji dari segi analisis fisiko-kimia seperti mikroskop elektron imbasan pancaran medan, spektroskopi dispersif tenaga sinar-X, belauan sinar-X, Brunauer-Emmett-Teller dan ultraungu-nampak-dekat inframerah, ujian penyerapan, ujian penurasan dan ujian fotopemangkinan untuk menentukan keupayaan membran untuk pembersihan sendiri, penurasan dan pengurangan pengotoran membran. Daripada keputusan eksperimen, ZIO dengan nisbah 1:4 zink kepada ferum merupakan ZIO optimum yang menunjukkan luas permukaan yang besar (30.9130 m<sup>2</sup>/g), tenaga sela jalur yang rendah (2.07 eV), aktiviti fotopemangkinan yang tinggi (35% mineralisasi dalam 6.5 jam dan 100% degradasi dalam 3.5 jam). Di samping itu, peningkatan suhu kalsinasi menyebabkan saiz partikel ZIO bertambah. Fenomena ini menyebabkan penurunan luas permukaan ZIO dan menurunkan prestasi penyerapan dan fotodegradasi sebatian organik. Keputusan eksperimen menunjukkan suhu 500°C adalah suhu kalsinasi optimum yang memberikan fotodegradasi yang tertinggi. Untuk MMMs, apabila ZIO bertambah, keliangan dan cas permukaan semakin negatif. Walaubagaimanapun, semakin tinggi kandungan ZIO yang digunakan, kekuatan mekanikal bagi struktur membran termusnah dan tidak dapat menahan operasi jangka masa panjang. Oleh itu, optimal telah ditentukan iaitu 0.5 % berat ZIO di mana membran mencapai 75 % penyahwarnaan dengan flux 20 – 25 LMH (L.m<sup>-2</sup>.j<sup>-1</sup>). Selain itu, MMMs fotopemangkinan ultraturusan menunjukkan perolehan fluks yang tinggi selepas pencucian ultraungu dan cahaya nampak, iaitu masing-masing 92.3 % dan 90.3 %. Penambahan ZIO dalam matriks PVDF dapat menguraikan pigmen warna dalam AT-POME. Selepas 16 jam operasi, warna AT-POME diturunkan sebanyak 8 %. Kesimpulannya, membran ultraturusan fotopemangkinan PVDF/ZIO telah berjaya menyahwarnakan AT-POME dan mengurangkan CODnya.

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## LIST OF ABBREVIATIONS

ABE	–	Acetone-butanol-ethanol
AC	–	Activated carbon
ADMI	–	American Dye Manufacturers Institute
AFM	–	Atomic force microscopy
AN	–	Ammoniacal nitrogen
AOPs	–	Advanced oxidation processes
AT-POME	–	Aerobically treated palm oil mill effluent
BET	–	Brunauer-Emmett-Teller analysis
BOD	–	Biochemical oxygen demand
BPA	–	Bis-phenol A
CPO	–	Crude palm oil
CNT	–	Carbon nanotube
COD	–	Chemical oxygen demand
CV	–	Crystal violet
DOE	–	Department of Environment
EDX	–	Energy dispersive X-ray analysis
EFB	–	Empty fruit bunch
FESEM	–	Field emission scanning electron microscope
4-HBZ	–	Para-hydrobenzoic acid
HPLC	–	High performance liquid chromatography
HRT	–	Hydraulic retention time
HS	–	Helmholts-Smoluchowski
JAS	–	National Environment Agency/ Department of Environment
MB	–	Methyl blue
MMMs	–	Mixed matrix membranes
MR	–	Methyl red
MWCO	–	Molecular weight cut off
NF	–	Nanofiltration
NMP	–	N-methyl-2-pyrrolidone
OECD	–	Organisation for Economic Co-operation and Development



OMW	–	Olive oil mill wastewater
PEG	–	Polyethylene glycol
PHA	–	Polyhydroxyalkanoates
POME	–	Palm oil mill effluent
PVDF	–	Polyvinylidene fluoride
PVP	–	Polyvinylpyrrolidone
PWP	–	Pure water permeation
RO	–	Reactive orange 16
SCA	–	Static contact angle
SRT	–	Solid retention time
SS	–	Suspended solids
TN	–	Total nitrogen
TOC	–	Total organic carbon
TS	–	Total solids
TSS	–	Total suspended solids
TVS	–	Total volatile solids
UF	–	Ultrafiltration
UV	–	Ultraviolet
UV-Vis-NIR	–	Ultraviolet-visible-near infrared spectrophotometer
WWF	–	World Wildlife Fund
XRD	–	X-ray diffraction
ZIO	–	Coupled zinc-iron oxide

## LIST OF SYMBOLS

°C	–	Degree Celsius
L	–	Litre
LMH	–	Litre per meter square per hour
m	–	meter
mg	–	miligram
ppm	–	Part per million
%	–	Percent

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# CHAPTER 1

## INTRODUCTION

### 1.1 Research Background

Oil palm (*Elaeis guineensis*) is one of the most versatile crops in the tropical region, notably in Malaysia and Indonesia. As reported by World Wildlife Fund (WWF), more than 65 per cent of all vegetable oil traded internationally is palm oil. Also, this number is expected to be increased double by 2020 [1]. In Malaysia, the palm oil production grows 12 per cent annually based on the statistics by United States Department of Agriculture [2]. Despite the benefits of palm oil industries to the social and economic growth, the processing of oil palm generates huge quantity of solid waste and wastewater. The solid waste of palm oil mill includes empty fruit bunch (EFB) and kernel seed. These wastes can be used to produce energy through combustion. Besides, some studies showed that the EFB can be used as the culture medium for microorganism growth. The wastewater from palm oil mill is known as palm oil mill effluent (POME) which is a brownish liquid with unpleasant smell and low pH. The POME is known as one of the major water pollutants in Malaysia due to its high organic content [3, 4]. These organic substances that loaded into source water may cause the eutrophication and eventually cause death of the aquatic organisms. The colour pigment presents in the aerobically or anaerobically treated POME (AT-POME) which arise from the biodegradation of lignocellulosic compound in POME. The brown colour pigment majorly come from tannin, lignin and carotene [5]. These colour pigment prevent the use of AT-POME in the palm oil extraction process because it colourises the pipeline and reduces the lifetime of the pipe. The conventional handling method of these AT-POME is discharge into point and source water instead of reusing it into the process line. AT-POME is dark brownish in colour. In fact, the darkness of the AT-POME is higher than POME due to the degradation of lignocellulose product and carotenoid compound in the POME into lignin and tannin. This will further

increase the acidity, turbidity and colour of the AT-POME. This restrict the reclamation of the treated POME for further reuse.

Generally, there are several technologies available for the removal of colour and COD from POME. For instance, ion exchange [6], coagulation [7], adsorption [8], and membrane processes [9]. Coagulation is a process that uses chemicals to destabilize the impurities (especially macromolecules and suspended solids) in POME. Coagulation has been proven to be capable to remove the suspended impurities that contribute to the high COD and dark brown colour of POME [7]. For instance, Zahrim et al. [10] showed that the use of dual-coagulants, i.e. ferric chloride-anionic polyacrylamide managed to achieve higher than 90% colour removal in POME treatment. The attractiveness of coagulation process is its simplicity in design and operation, low energy consumption and high versatility. However, coagulation process alone could not attain complete decolourization and treatment of POME due to its failure to remove dissolved organic substances in POME. In order to achieve higher removal of colour and reduction of COD, adsorption has been proposed for POME treatment. Adsorption process utilizes adsorbents (with the most widely used is activated carbon) to adsorb and capture the dissolved organic impurities in wastewater for decolourization purpose [11]. Mohammed et al. [8] reported that the use of activated carbon adsorbent could reduce the colour intensity of POME with removal efficiency of 96.46%. Though the high decolourization efficiency is quite encouraging, the widespread of adsorption for POME treatment and decolourization has not been well accepted by industry due to the high expenditure associated with the regeneration of activated carbon for reuse and the replacement cost of spent activated carbon. On the other hand, membrane technologies such as NF and RO could be used to remove both suspended and dissolved organic substances in POME [9]. Both NF and RO membranes could reduce the COD down to less than 10 mg/L and colour intensity to less than 5 Pt.Co. The performance of membrane technologies is very convincing yet it is not employed in POME treatment due to membrane fouling issue, where impurities will deposit on the membrane surface and block the passage of water from passing through the membrane. Hence, unless membrane fouling could be resolved or minimized, the fouling issue will continue to hinder the application of membrane in POME treatment and decolourization.

Another emerging technology for colour removal is photocatalysis [12]. Photocatalyst is a semiconductor nanoparticle that can generate electrons and holes through the excitation by solar or light energy. Photocatalyst can photodegrade most of the organic molecules into less hazardous molecules. Thus, it is widely applied in wastewater and water treatment. However, using photocatalyst directly will cause the suspension of nanoparticles in the treated solution. This requires additional unit operation to recover the nanoparticles for the subsequent usage. Therefore, the footprint of the plant will increase, and more construction and maintenance cost will be involved. In order to enhance the photocatalysis, nanosized photocatalyst has been normally used. However, it is very tedious to separate nanoparticles with low cost process.

In order to harness the advantages of both membrane technology and photocatalysis, also to mitigate their undesired limitations, nanocomposite ultrafiltration (UF) membrane with photocatalytic properties is developed. UF membrane is a membrane technology that is able to separate macromolecule of  $10^3$  to  $10^6$  Da. Therefore, UF can give relatively high flux with lower operating pressure. Yet, UF cannot remove colour pigment since they are too small. Therefore, a new configuration of UF that incorporate with photocatalytic nanoparticles is fabricated to overcome this limitation. Nanoparticles with photocatalytic properties are incorporated into membrane matrix to enhance its hydrophilicity and also render photocatalytic properties to achieve the synergistic effects.

In this study, nanocomposite UF membrane with coupled zinc-iron oxide nanoparticles was fabricated to enhance the AT-POME colour removal. The coupled zinc-iron oxide nanoparticles (ZIO) were synthesised by solution combustion technique. The nanoparticles were then incorporated with the polymer dope solution to form a flat sheet membrane via phase inversion process. The resultant photocatalytic nanocomposite membrane demonstrates the ability of self-cleaning, prolonged operation duration and also enhanced performance in colour removal of AT-POME.

## 1.2 Problem Statements

The high pollutant content of the POME hampers the direct discharge into the water source. Therefore, proper and systematic treatments are highly desired to prevent the pollution of water by the palm oil waste. However, the conventional treatment method, i.e. biological degradation method is ineffective for colour removal. This is due to the dependency of the microorganism on the weather and environment. Besides, the biodegradation of lignocellulosic compounds produces tannin and lignin that increase the brownness of AT-POME [13]. This raises the public concern about the level of toxicity or pollutant in the AT-POME. Besides, the build-up of brown colour pigment restricts the reclamation of AT-POME in palm oil industry. Thus, membrane-based separation holds very promising potential to address this issue as this technology can be used to reclaim the water for the plant reuse and reduce the chemical oxygen demand (COD) significantly.

NF has been widely used in decolourization of wastewater [9, 14, 15]. The major drawback of the process is utilization of high pressure and low permeation rate, i.e. approximate 11.3 LMH [16, 17]. Therefore, it is not feasible for the palm oil industry to handle high output rate of AT-POME. Thus, UF with bigger pore size need to be customized so that it can cope the AT-POME production rate. Another drawback of NF process is the high fouling tendency. The foulant (i.e. colour pigment) tends to block the pore on the membrane and reduce the flux drastically. Therefore, nanocomposite membrane is an attractive candidate to solve these problems. Photocatalysts can serve as nanoparticles that alter the membrane physical properties and also act as antifouling agent. Ideally, photocatalyst in the membrane matrix can work in two ways, which are photodegrade foulant that block the membrane pores and photodegrade the colour pigment in the AT-POME that close to the membrane surface. This can further enhance the membrane separation efficiency by mitigating the fouling problem.

In this study, UF with near NF properties can be incorporated with bimetallic photocatalyst to filter the AT-POME. The photocatalyst in polymeric matrix can tailor the surface charge of membrane so that the desired charge can be obtained. Besides,

the photocatalyst that embedded into the membrane can give self-cleaning property to the membrane and extend its lifespan. Furthermore, when the photocatalytic membrane is irradiated under visible light, it can carry out photocatalysis and filtration simultaneously. Thus, recycle of photocatalyst can be easily achieved. Figure 1.1 shows the working mechanism of membrane with photocatalyst. Upon excited by UV light source,  $\text{TiO}_2$  photocatalyst will produce hydroxyl radicals from water molecules. These hydroxyl radicals will then degrade the organic impurities (either present on the membrane surface or suspended close to the membrane surface) into harmless compounds such as  $\text{CO}_2$  and  $\text{H}_2\text{O}$ . This can help to minimize membrane fouling propensity and enhance the separation efficiency since membrane blocking issue by impurities will be mitigated through photocatalytic degradation. The photodegradation of the colour pigment in the AT-POME can dilute the brownish colour of the AT-POME and reduce the concentration of colour pigment in AT-POME so that the membrane separation can be carried out easily. Another advantage of embedding photocatalyst in the membrane matrix is that it can avoid the secondary treatment of photocatalyst in heterogenous system. Membrane serves as the binder or holder of the photocatalyst to enable the recycle and reuse of the photocatalyst for long term usage.

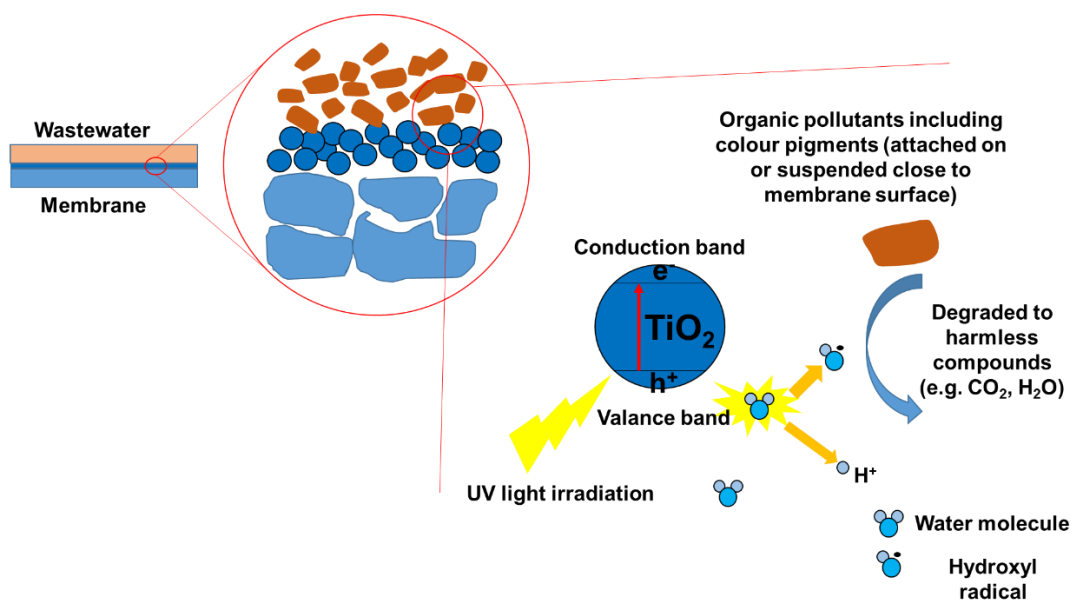


Figure 1.1 Working mechanism of membrane embedded with photocatalyst [12]

The rate of photocatalysis are depending on the concentration of photogenerated holes and electrons and their rate of recombination. Currently,



titanium dioxide has been employed as commercial photocatalyst as its high photocatalytic activity. However, the use of titanium dioxide requires high photoenergy, thus, it can only be activated by ultraviolet (UV) light. Therefore, photocatalytic reactor must be properly enclosed to prevent the exposure of ultraviolet light to operator. Reducing the band gap energy of photocatalyst can be one of the methods to shift the activation light from ultraviolet to visible region. But, this will indirectly increase the rate of recombination between the photoexcited holes and electrons. This phenomenon could result in the low photocatalytic activity. Hence, bimetallic oxide photocatalyst is developed to solve these two mentioned problems above. By constructing bimetallic oxide with different characteristics, a p-n junction can be formed. p-n junction will help to hold the photoexcited holes and electrons at its respective matrixes. As a result, the rate of recombination could be minimised.

### **1.3 Objectives of Study**

The main focus of this study is to develop a photocatalytic nanocomposite membrane for AT-POME colour removal. In order to achieve this main goal, several sub-objectives have been identified:

- (i) To synthesize and characterize coupled zinc-iron oxide (ZIO) photocatalyst that can be activated in both UV and visible light range.
- (ii) To fabricate and characterize nanocomposite UF membrane which embedded with ZIO.
- (iii) To evaluate the performance of the photocatalytic nanocomposite UF membrane which embedded with different loading of ZIO in terms of AT-POME colour removal efficiency, flux, anti-fouling properties, photodegradation and separation performance of the nanocomposite UF membrane.
- (iv) To study the photocatalytic properties of hybrid membrane.

## 1.4 Scopes of Study

The objective of this study can be accomplished by the following scopes:

- (i) Characterising the average particle size of AT-POME with commercial NF and UF membranes.
- (ii) Synthesising ZIO with different zinc to iron molar ratio 1:1, 1:2, 1:3 and 1:4 via solution combustion method using zinc nitrate and iron (III) nitrate as precursor
- (iii) Studying the effect of zinc to iron molar ratio to the reduction in band gap energy and AT-POME photocatalytic activity.
- (iv) Synthesising ZIO with optimum molar ratio by varying calcination temperature ranging from 400°C to 800°C.
- (v) Studying the effect of calcination temperature to the surface area of coupled ZIO and its absorption capacity.
- (vi) Fabricating nanocomposite UF membrane by polyvinylidene fluoride (PVDF) (18.0 wt%), polyvinylpyrrolidone (PVP) (1.0 wt%), lithium chloride (LiCl) (0.5 wt%), ZIO (0.0 – 2.0 wt%) and n-methyl-2-pyrrolidone (NMP) (78.5 – 80.5 wt%).
- (vii) Studying the effect of ZIO loading to the morphology of membrane by field emission scanning electron microscope (FESEM), atomic force microscope (AFM) and X-ray diffraction (XRD).
- (viii) Evaluating the performance of photocatalyst ZIO in terms of photodegradation in visible and UV light.
- (ix) Evaluating the performance of photocatalysis via COD, colour removal and total organic carbon (TOC) analysis.
- (x) Investigating the self-cleaning properties of nanocomposite UF membrane by membrane-flux recovery ratio over 4 hours continuous operation in 4 cycles.
- (xi) Studying the effect of ZIO loading to the membrane performance via pure water permeation, colour removal of AT-POME and fouling analysis.

## **1.5 Significance of Study**

This study aims to decolourise brownish AT-POME which is high in COD, colour and TOC. Therefore, through the well study and the control of the synthesis parameters, it is believed that the ZIO is able to photodegrade colour pigment and other organic substances in AT-POME to produce clear water. Besides, ZIO oxide is believed can move the activation photon of photocatalyst from UV light region to visible light region. Thus, photocatalytic reaction can be easily activated with the presence of natural light (i.e. sunlight).

Besides, this is the first attempt by incorporating bimetallic oxide into polymeric membrane matrix to produce mixed matrix photocatalytic membrane. By developing such nanocomposite photocatalytic membrane, the photocatalysis and UF of AT-POME can be carried out simultaneously. Thus, the efficiency of decolourization will greatly improve and mitigate the water pollution problems. Furthermore, the treated AT-POME which is free from colour pigment can be reclaimed into the palm oil mill for other purposes. This will further enhance the water sustainability in plant and help to mitigate the excessive water use. In a broader text, water shortage problem can be mitigated.

## **1.6 Thesis Outline**

This thesis consists of 5 chapters which are introduction, literature review, methodology, results and discussion and conclusion and recommendation. Besides, raw data for the membrane performance results are attached in the appendices. The thesis was written based on UTM Thesis Manual 2018.

Chapter 1 discussed the problem statement of the current AT-POME treatment for the colour removal and some drawback of the technologies used currently. Besides, objectives and scopes of the research are mentioned. Chapter 2 discussed the literature review which are the recent development for POME and AT-POME treatment,

advanced oxidation processes and membrane technologies used in decolourisation. Chapter 3 discussed the research methodology for the study and chemical and analysis used to determine the performance of the membrane. Chapter 4 discussed the results based on the experimental and analysis. Chapter 5 concluded the research based on the quantitative and qualitative of the experimental results.

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## APPENDIX I

### Raw data for Experiment of Nanocomposite UF membrane incorporating ZIO (PWP, COD Removal and Colour Removal)

#### (a) Pure water permeation

Sample	Flux (mL)					Time (min)	Pressure (bar)	PWP (LMH)	PWP (LMH Bar)	Std Dev
	1	2	3	Average	Std Dev.					
M0	4.10	4.10	4.00	4.07	0.05	2.00	1.00	85.92	85.92	1.00
M0.1	5.40	5.20	5.30	5.30	0.08	1.00	1.00	223.94	223.94	3.45
M0.5	4.00	3.90	4.00	3.97	0.05	1.00	1.00	167.61	167.61	1.99
M1.0	3.80	3.80	3.90	3.83	0.05	1.00	1.00	161.97	161.97	1.99
M2.0	3.00	2.90	3.00	2.97	0.05	1.00	1.00	125.35	125.35	1.99
MZ	2.80	2.70	2.80	2.77	0.05	10.00	5.00	11.69	2.34	0.20
MF	4.90	5.00	4.90	4.93	0.05	30.00	1.00	6.95	6.95	0.07

#### (b) AT-POME permeation

Sample	Flux (mL)	Time (min)	Pressure (bar)	PWP (LMH)
M0	7.5	10	1	31.69
M0.1	9.8	10	1	41.41
M0.5	9.5	10	1	40.14
M1.0	9.8	10	1	41.41
M2.0	7.5	10	1	31.69
MZ	2.6	10	5	10.99
MF	3.1	30	1	4.37

#### (c) Colour and COD removal efficiency

Sample	ADMI Rejection (%)	COD Rejection
M0	59.25	51.37
M0.1	64.46	60.77
M0.5	69.53	60.16
M1.0	66.35	61.14
M2.0	70.97	62.73
MZ	59.32	48.66
MF	53.77	47.39

**(d) Colour and COD removal efficiency**

		<b>COD</b>	<b>COD REDUCTION</b>	<b>TOC</b>	<b>TOC REDUCTION</b>	<b>ADMI</b>	<b>ADMI REDUCTION</b>
		<b>ppm</b>	<b>%</b>	<b>ppm</b>	<b>%</b>		<b>%</b>
	<b>AT-POME</b>	468		160.8		2770	
<b>ABSORBENT (0.5 WT%)</b>	<b>ZIO (1:1) 500C</b>	328	29.91	117.5	26.93	1923	30.58
	<b>ZIO (1:2) 500C</b>	343	26.71	110.5	31.28	1643	40.69
	<b>ZIO (1:3) 500C</b>	321	31.41	105.8	34.20	1538	44.48
	<b>ZIO (1:4) 400C</b>	310	33.76	110.5	31.28	1348	51.34
	<b>ZIO (1:4) 500C</b>	335	28.42	111.1	30.91	1506	45.63
	<b>ZIO (1:4) 600C</b>	301	35.68	114.6	28.73	1894	31.62
	<b>ZIO (1:4) 700C</b>	375	19.87	117.2	27.11	2062	25.56
	<b>ZIO (1:4) 800C</b>	373	20.30	123.4	23.26	2056	25.78