

POLICY ENHANCEMENT FRAMEWORK FOR ENERGY GENERATION  
FROM PALM OIL MILL EFFLUENT USING LIFE CYCLE MULTI CRITERIA  
ANALYSIS

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## ABSTRACT

One of the most challenging problems in palm oil industry in Malaysia is the management of palm oil mill effluent (POME). Majority of the palm oil mills treat POME using anaerobic ponding system, which is not environmentally friendly as large amount of generated greenhouse gases is not captured but released to the atmosphere. Therefore, it is crucial to ensure a sustainable practise of closed anaerobic digestion system in the palm oil industry. This study was mainly aimed to provide evidence-based policy enhancement for POME treatment to energy generation. For this, life cycle assessment (LCA) was carried out to assess environmental impacts and life cycle cost-benefit analysis to assess the economic aspects focusing on two commercially available POME treatment technologies which are covered lagoon bio-digester (CLB, representing 36 palm oil mills with covered lagoon system) and continuous stirred tank reactor (CSTR, representing majority of the 54 palm oil mills employing closed tank system). Based on the output of life cycle analysis and interviews with palm oil mill management, thirteen possible solutions for policy enhancement were suggested. Possible solutions were ranked by experts and weighting were assigned to the possible solutions by using analytical hierarchy process, which were then used for policy enhancement. In terms of LCA, the global warming potential and acidification potential for CSTR were  $-4.48 \text{ kg CO}_2 \text{ eq/kWh}$  and  $-2.21 \text{ kg SO}_2 \text{ eq/kWh}$ , respectively, while for CLB the values were  $-4.09 \text{ kg CO}_2 \text{ eq/kWh}$  and  $-0.15 \text{ kg SO}_2 \text{ eq/kWh}$ . Both technologies produced a negative result, which equates to a net environmental benefit. However, both systems had a negative impact in terms of eutrophication potential. The CSTR nevertheless achieved a better eutrophication potential result of  $0.048 \text{ kg PO}_4^{3-} \text{ eq/kWh}$  than the CLB with  $0.054 \text{ kg PO}_4^{3-} \text{ eq/kWh}$ . With respect to life cycle cost (LCC), CSTR has a higher LCC of RM 2.60 million/year compared to CLB with LCC value of RM 2.29 million/year. In terms of cost-benefit, CSTR has a higher net present value (NPV) of RM 2.21 million/year, higher return on investment (ROI) of 11.80% and shorter payback period (PP) of 8.5 years compared to the CLB system with NPV of RM 0.91 million/year, ROI of 7.79% and PP of 12.8 years. ‘Provide detailed environmental guidelines’ followed by ‘standardise technical guidelines for biogas installation’ and ‘cover open pond wall using lining’ were the top three possible solutions to be considered in order to improve the existing policy for the POME treatment for energy generation. Future researchers may wish to consider social aspects related to job creation, safety and health of workers besides environmental and economic aspects. As a whole, this study allows policy makers to understand the current situation faced by palm oil mill managers and the rankings of possible solutions, offering important inputs for consideration in policy development for the treatment of POME for energy generation.

## ABSTRAK

Salah satu masalah yang paling mencabar dalam industri minyak kelapa sawit di Malaysia ialah pengurusan kilang kumbahan minyak kelapa sawit (POME). Kebanyakan kilang kumbahan minyak kelapa sawit merawat POME dengan menggunakan sistem pengoloman anaerobik yang tidak mesra alam kerana sebahagian besar gas rumah hijau yang terjana tidak diperangkap tapi terbebas ke atmosfera. Oleh itu, adalah penting untuk memastikan amalan lestari sistem pencernaan anaerobik tertutup dalam industri kelapa sawit. Tujuan utama kajian ini adalah untuk mengemukakan bukti bagi pengukuhan dasar untuk rawatan POME terhadap penjana tenaga. Dengan itu, penilaian kitaran hidup (LCA) untuk menilai impak terhadap alam sekitar dan analisis kos-faedah kitaran hidup untuk menilai aspek ekonomi yang tertumpu kepada dua teknologi rawatan POME yang didapati secara komersial, iaitu pencerna biogas lagun tertutup (CLB, diwakili 36 kilang minyak kelapa sawit menggunakan sistem lagun tertutup) dan reaktor tangki teraduk selanjara (CSTR, diwakili majoriti 54 kilang minyak kelapa sawit menggunakan sistem tangki tertutup), telah dijalankan. Berdasarkan hasil analisis kitaran hidup dan temu ramah bersama pihak pengurusan kilang kelapa sawit, tiga belas penyelesaian munasabah bagi pengukuhan dasar telah dicadangkan. Penyelesaian munasabah dinilai oleh pakar dan pemberat diberikan pada penyelesaian munasabah tersebut dengan menggunakan proses hierarki analisis, yang kemudian digunakan dalam pengukuhan dasar. Daripada aspek LCA, potensi pemanasan global dan potensi pengasidan bagi CSTR masing-masing ialah  $-4.48 \text{ kg CO}_2 \text{ eq/kWh}$  dan  $-2.21 \text{ kg SO}_2 \text{ eq/kWh}$ . Bagi CLB, potensi pemanasan global ialah  $-4.09 \text{ kg CO}_2 \text{ eq/kWh}$  dan potensi pengasidan ialah  $-0.15 \text{ kg SO}_2 \text{ eq/kWh}$ . Kedua-dua teknologi memperolehi keputusan negatif menunjukkan bahawa ianya setara dengan keuntungan persekitaran bersih. Namun begitu, kedua-dua sistem mempunyai impak negatif dari segi potensi eutrofikasi. Walau bagaimanapun, CSTR telah mencapai keputusan potensi eutrofikasi yang lebih baik iaitu  $0.048 \text{ kg PO}_4^{3-} \text{ eq/kWh}$  berbanding CLB iaitu  $0.054 \text{ kg PO}_4^{3-} \text{ eq/kWh}$ . Berdasarkan kos kitaran hidup (LCC), CSTR mempunyai nilai LCC yang lebih tinggi iaitu RM 2.60 juta/tahun berbanding CLB iaitu dengan nilai LCC sebanyak RM 2.29 juta/tahun. Dari segi kos-faedah, CSTR mempunyai nilai kini bersih (NPV) yang lebih tinggi iaitu sebanyak RM 2.21 juta/tahun, pulangan pelaburan yang lebih tinggi (ROI) iaitu sebanyak 11.80 % dan tempoh bayar balik (PP) yang lebih pendek iaitu 8.5 tahun berbanding sistem CLB dengan nilai NPV sebanyak RM 0.91 juta/tahun, ROI sebanyak 7.79% dan PP selama 12.8 tahun. ‘Menyediakan garis panduan alam sekitar yang terperinci’ diikuti dengan ‘menyeragamkan garis panduan teknikal untuk pemasangan biogas’ dan ‘menutup dinding kolam terbuka menggunakan pelapik’ adalah tiga penyelesaian yang paling munasabah untuk dipertimbangkan bagi menambah baik dasar sedia ada untuk rawatan POME bagi penjana tenaga. Penyelidik masa hadapan boleh mempertimbangkan aspek sosial berkaitan penciptaan pekerjaan dan kesihatan pekerja selain aspek ekonomi dan alam sekitar. Secara keseluruhannya, kajian ini boleh memberikan peluang kepada para pembuat dasar untuk memahami situasi semasa yang dihadapi oleh pengurus kilang kelapa sawit dan pemeringkatan penyelesaian yang munasabah, dengan memberikan input penting untuk dipertimbangkan dalam pembangunan dasar bagi rawatan POME untuk penjana tenaga.

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## LIST OF ABBREVIATIONS

|        |   |   |
|--------|---|---|
| AD     | - | Anaerobic digestion                           |
| AHP    | - | Analytical hierarchy process                  |
| AOP    | - | Advanced oxidation process                    |
| AP     | - | Acidification potential                       |
| AS-GMP | - | Assessment System Genetically Modified Plants |
| BA     | - | Break-Even analysis                           |
| B.E.P  | - | Break-Even point                              |
| BOD    | - | Biological oxygen demand                      |
| BPMSG  | - | Business Performance Management Singapore     |
| C&D    | - | Construction and demolition                   |
| CBA    | - | Cost benefit analysis                         |
| CDM    | - | Clean Development Mechanism                   |
| CI     | - | Consistency index                             |
| CLB    | - | Covered lagoon bio-digester                   |
| COD    | - | Chemical oxygen demand                        |
| COLT   | - | Combination of open lagoon technology         |
| CPO    | - | Crude palm oil                                |
| CR     | - | Consistency ratio                             |
| CSTR   | - | Continuous stirred tank reactor               |
| CT     | - | Carbon trading                                |
| DALY   | - | Disability adjusted life year                 |
| DG     | - | Distributed generation                        |
| DOE    | - | Department of Environment                     |
| DOSH   | - | Department of Occupational Safety and Health  |
| EFB    | - | Empty fruit bunch                             |
| EGSB   | - | Expanded granular sludge bed reactor          |
| EP     | - | Eutrophication potential                      |
| EPP    | - | Entry Point Projects                          |
| EQA    | - | Environmental Quality Act                     |
| ETSs   | - | Emission trading systems                      |

|       |   |  |
|-------|---|--|
| FBR   | - | Fluidised bed reactor                      |
| FDI   | - | Foreign direct investment                  |
| FFB   | - | Fresh fruit bunch                          |
| FiT   | - | Feed-in Tariff                             |
| FU    | - | Functional unit                            |
| GHG   | - | Greenhouse gas                             |
| GMM   | - | Geometric means method                     |
| GITA  | - | Green Investment Tax Allowance             |
| GITE  | - | Green Investment Tax Exemption             |
| GTFS  | - | Green Technology Financing Scheme          |
| GWP   | - | Global warming potential                   |
| HRT   | - | Hydraulic retention time                   |
| IRB   | - | Inland Revenue Board                       |
| IRR   | - | Internal rate of return                    |
| ITA   | - | Investment Tax Allowance                   |
| ITE   | - | Income tax exemption                       |
| JKR   | - | Jabatan Kerja Raya                         |
| KAU   | - | Korean allowance units                     |
| KETS  | - | Korea emission trading system              |
| kWh   | - | Kilowatt-hour                              |
| LCA   | - | Life cycle assessment                      |
| LCC   | - | Life cycle costing                         |
| LCCBA | - | Life cycle cost benefit analysis           |
| LCI   | - | Life cycle inventory                       |
| LCIA  | - | Life cycle impact assessment               |
| LUC   | - | Land use change                            |
| MCDM  | - | Multi Criteria Decision Making             |
| MGTC  | - | Malaysia Green Technology Corporation      |
| MIDA  | - | Malaysian Investment Development Authority |
| MMBtu | - | One million British Thermal Units          |
| MOP   | - | Multi Objective Programming                |
| MPOB  | - | Malaysian Palm Oil Board                   |
| MSW   | - | Municipal Solid Waste                      |



|        |   |   |
|--------|---|---|
| Mtoe   | - | Millions of tonnes of oil equivalent                  |
| MW     | - | Megawatts   |
| NKEA   | - | National Key Economic Area                            |
| NPV    | - | Net present value                                     |
| NVivo  | - | Qualitative data management software                  |
| O&G    | - | Oil and grease  |
| OLR    | - | Organic loading rate                                  |
| POME   | - | Palm oil mill effluent                                |
| POMs   | - | Palm oil mills  |
| PP     | - | Payback period  |
| PV     | - | Photovoltaic  |
| RE     | - | Renewable energy                                      |
| RI     | - | Random index  |
| RM     | - | Ringgit Malaysia                                      |
| ROI    | - | Return on investment                                  |
| RSPO   | - | Roundtable on Sustainable Palm Oil                    |
| SEDA   | - | Sustainable Energy Development Authority              |
| SPSS   | - | Statistical Package for Social Sciences               |
| SS     | - | Suspended solids                                      |
| SSCM   | - | Sustainable supply chain management                   |
| TN     | - | Total nitrogen  |
| TNB    | - | Tenaga Nasional Berhad                                |
| TS     | - | Total solids  |
| UASB   | - | Upflow anaerobic sludge blanket                       |
| UASFF  | - | Upflow anaerobic sludge fixed film                    |
| UFF    | - | Upflow fixed film                                     |
| UNFCCC | - | United Nations Framework Convention on Climate Change |
| USD    | - | United States Dollar                                  |
| WAMM   | - | Weighted arithmetic means method                      |
| WC     | - | Water consumption                                     |
| ZCB    | - | Zero carbon building                                  |

## LIST OF SYMBOLS

|                             |   |  |
|-----------------------------|---|--|
| $B_{o,ww}$                  | - | Methane production per kg COD digester                     |
| $^{\circ}\text{C}$          | - | Degree Celsius   |
| $C_i$                       | - | Electricity  |
| $\text{CFE}_{ww}$           | - | Digester efficiency  |
| $\text{CH}_4$               | - | Methane  |
| $\text{CO}_2$               | - | Carbon dioxide   |
| $D_r$                       | - | dumping rate   |
| $\text{EF}_{\text{CO}_2}$   | - | Grid displacement  |
| $\text{EW}_r$               | - | earth works rate   |
| $\text{GWP}_{\text{CH}_4}$  | - | Global warming potential                                   |
| $\text{H}_2$                | - | Hydrogen   |
| h/d                         | - | hour per day   |
| $\text{m}^3/\text{hr}$      | - | cubic meter per hour                                       |
| $\text{MCF}_{ww,digestate}$ | - | Digestate POME   |
| $\text{MCF}_{ww,anaerobic}$ | - | Recovery/combustion utilisation                            |
| mg/L                        | - | milligram per litre  |
| N                           | - | Nitrogen   |
| $\text{NH}_3\text{-N}$      | - | Ammoniacal nitrogen  |
| $\text{PO}_{\text{COD}}$    | - | Phosphate equivalence factor (in terms of COD)             |
| $\text{PO}_{\text{tn}}$     | - | Phosphate equivalence factor (in terms of TN)              |
| r                           | - | interest rate  |
| $\text{SO}_2$               | - | Sulphur dioxide  |
| $\text{SO}_{ww}$            | - | $\text{SO}_2$ equivalence factor (acidification potential) |
| t                           | - | tonne  |
| $\lambda_{\text{max}}$      | - | Largest eigenvalue   |

## LIST OF APPENDICES

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# CHAPTER 1

## INTRODUCTION

### 1.1 Introduction

In this chapter, an introduction about this study is made where the background of study is described to give a general overview of the study. Then, the problem that this study is focusing on is leading to the presentation of the goal of the study and the research objectives. The scope of this study is described to reflect the boundary of what was considered, and information is given on how this study was conducted. The significance of the study is discussed to highlight the importance and contribution to society. At the end of this chapter, the layout of the thesis is briefly discussed.

### 1.2 Background of the Study

Renewable energy (RE) is emphasised globally as a new unlimited source of power due to its potential to contribute to economic and sustainable development (Kaplan, 2015). For a long period of time, the majority of countries have depended on fossil fuels including coal, diesel and natural gas as the main sources of electricity generation. Decades of excessive exploitation of these non-renewable resources cause not only pollution but also contribute towards global warming and climate change. Renewable resources are then prioritised in line with the realisation of rapidly diminishing resources, only they are not being taken up fast enough to cater for such unrelenting consumption. In addition, RE offers major economic opportunities, especially in the elimination of energy poverty (Vidadili et al., 2017). RE is a vital underpinning to the development of sustainability as well as helping to overcome the global environmental and energy crisis.

Biomass is one of the emerging credible fuel resources. Bioethanol and biodiesel are some of the biomass energy sources which have been commercialised in some countries of the world (Ohimain and Izah, 2017). Oil palm processing feedstock is the most notable feedstock for biomass energy, and can be used for the production of bioproducts like bioelectricity, bio-hydrogen, biodiesel, bioethanol, briquette, bio-methanol, biogas (Ohimain and Izah, 2014a, b), bio-butanol, briquette and bio-oil. Biofuels reduce the utilisation of fossil fuels and reduce carbon dioxide (CO<sub>2</sub>) emissions as biofuels are carbon neutral (Hanaki and Portugal-Pereira, 2018). Biogas is a renewable, colorless, combustible and relatively odourless inflammable (Igoni et al., 2007; 2008).

In Malaysia, 5.8 million hectares (MPOB, 2018a) of land are covered by oil palm plantations and there are approximately 450 palm oil mills (POMs) in operation (Oshedale et al., 2016). Each oil palm tree produces 8 to 15 fresh fruit bunches (FFBs) annually (Yasin et al., 2017). Oil extracted from these FFBs consists of 10% of the whole dry matter of the palm, while the remaining 90% is palm oil biomass (Sue and Pantzaris, 2017), comprising empty fruit bunches (EFBs), palm oil mill effluent (POME), palm kernel shells, mesocarp fibres and palm oil trunks and fronds (Abdulrazik et al., 2017; Loh, 2017a). Both POME and EFBs are generated in huge quantities of 67% and 22%, respectively for every one tonne (t) of FFB (Loh, 2017a; Saelor et al., 2017). POME is a non-toxic, thick, viscous liquid waste that can cause damage if it is directly released into the environment as it is a highly polluting wastewater (Kamyab et al., 2018). POME has high organic content. An anaerobic treatment method is thus most suitable POME treatment method because such a method is more efficient (Choong et al., 2018). Anaerobic digestion (AD) is currently considered the most environmentally friendly biological treatment process because the waste subjected to AD can be converted into value-added products such as bio-energy (Li et al., 2019).

POME has a high organic content making a highly polluting effluent (MPOB, 2014). It has been a great challenge and it is critical to have a proper management system for handling the abundance of POME (Choong et al., 2018). However, more than 80% of POMs have been using a low cost ponding system which is a conventional

system to treat POME (Oshegale et al., 2016). Another serious threat to the environment from the conventional system is the escaping greenhouse gases (GHGs) as a result of applying this treatment method, in addition to the large land area required (Choong et al., 2018). Thus, sustainable management of POME is crucial for the development of a cleaner palm oil industry (Choong et al., 2018) as to meet the requirement of environmental quality.

The current conventional system to treat the POME is inefficient due to the failure to comply with the standard discharge limit set by the Department of Environment (DOE) in many cases. This scenario leads to disruption of the water ecosystem (Iskandar et al., 2018). Khadaroo et al. (2019) agrees that POME has been identified as one of the most challenging waste products to dispose of in the palm oil industry due to its high organic content. Thus, identifying and using a proper disposal method is critically important. Efficient treatment can enable POME to supply useful products like biogas and A grade biosolids used in fertilisers (Khadaroo et al., 2019), which offer important new options and income streams from what would otherwise be waste.

Biogas production is one of the best ways to manage POME by-product particularly in developing countries (Hanafiah et al., 2017). Other countries around the world including Malaysia are shifting towards RE substituting the depleting and polluting fossil fuel sources. Ensuring the sustainability of biogas production from POME is the utmost important as Malaysia is one of the biggest producers and exporters of palm oil biomass sources for biogas generation (Aziz, Hanafiah and Gheewala, 2019). If biogas is captured from POME, there are two benefits: RE recovery and direct GHG emission reduction (Ohimain and Izah, 2017). Also, it is crucial to implement biogas facilities in all POMs in accordance with the Palm Oil National Key Economic Areas programme plans to implement eight core Entry Point Projects (EPPs) where EPP 5 particularly targets to ensure all POMs in Malaysia to have biogas facilities installed by 2020 (NKEA, 2014).

### 1.3 Problem Statement

POME has huge amount of essential fatty acids, inorganic nutrients, nitrogenous compound and more which will pollute the water and is particularly harmful to aquatic communities upon discharging POME into waterways (Iskandar et al., 2018; Santosa, 2008). Currently, 80% of Malaysia's POMs employ either anaerobic ponding systems or open digester tanks to treat the POME (Oshegale et al., 2016). These treatment methods generate a large amount of GHGs comprising CO<sub>2</sub> and methane that are not captured but rather, escape into the atmosphere (Khadaroo et al., 2019; Choong et al., 2018). A more environmentally-friendly alternative is the biogas plant. However, only 90 POMs have a complete biogas plant out of 450 POMs in Malaysia (Oshegale et al., 2016). Figure 1.1 shows the current utilisation of the biogas generated from the treatment of POME in POMs in Malaysia. It is clear from the figure that most of the biogas is flared (58%), while the second highest utilisation of biogas is for electricity generation (27%) which is sold to the grid. It is also apparent from the figure that it is critical to encourage sustainable practices in managing POME (Raman et al., 2019). Thus, this study compared two different POME treatment technologies which are: covered lagoon bio-digester (CLB) representing 36 mills employing covered lagoon system (Foo and Aziz, 2019) and continuous stirred tank reactor (CSTR), representing the majority of the 54 mills employing a closed tank system (Oshegale et al., 2016).

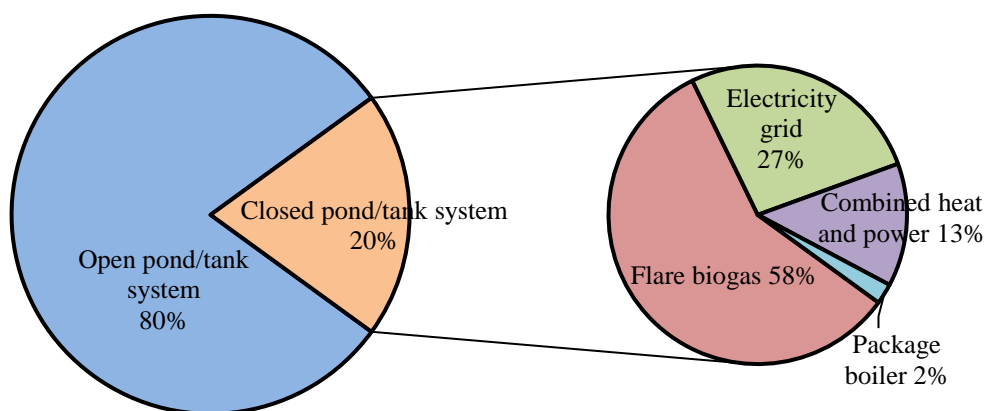


Figure 1.1 Current utilisation of biogas in POMs (Source: Oshegale et al., 2016)

Additionally, lack of support from the relevant authorities and government on related RE technology adoption in the current market has resulted in slow growth of biogas plant development in Malaysia. High risks of implementing new RE technology and a long payback period (PP) have reduced the interest of the stakeholders to finance RE projects, which eventually makes the RE technology not commercially viable in Malaysia (Yien et al., 2015). Thus, it is crucial to encourage a sustainable practise of a closed AD system of converting POME to renewable biogas which is then converted to electricity (Choong et al., 2018).

Malaysia pledged to reduce its GHG emission by 45% in 2030 based on the Nationally Determined Contribution of Malaysia (INDC, 2015). However, there is not any carbon trading to encourage the implementation of RE technologies as the first five-year commitment period for certified emission reductions credit in the Kyoto Protocol ended in 2012 and second international agreement regarding carbon reductions is yet to be implemented (UNFCCC, 2018). Apart from that, the feed-in tariff (FiT) scheme introduced by the Sustainable Energy Development Authority (SEDA), given to the installation of the biogas technology, differs according to the facilities' capacity. In addition, an extra bonus is given to facilities employing local technology, as well as for achieving high efficacy in electricity generation (Wong et al., 2015). Such policy regulations never seem to be attractive to POM owners who expect a high, fixed FiT price. Other than that, natural gas which is the main contributor of primary energy production in Malaysia is given as much as 71-77% subsidy by the Government of Malaysia on its selling price (Chatri et al., 2018). Simultaneously, POM owners expect the Malaysian Government to be able to provide a subsidy in the form of incentives for investment in electricity transmission to grid or to set up the biogas facilities. Currently, there is investment tax allowance (ITA) and an interest subsidy provided for the installation of biogas facilities where the application for ITA seems to be complicated. However, there is not any subsidy or incentives provided for the investment made to encourage the RE generation. This clearly shows that there is a need to enhance the current policy with sufficient evidence on POME treatment for energy generation to attract investors and foster the contribution of renewables in the energy mix.



Building from the policy context outlined above, this study seeks to identify possible solutions that could provide recommendations for the development of a relevant policy on the treatment of POME for energy generation. Policy plays an important role to ensure this study has a positive impact on society. The policy enhancement emerging from the study has the following characteristics:

1. It considers both environmental and economic aspects of the POME treatment process for energy generation;
2. It considers the output of life cycle studies and interviews with POM management who then suggested the possible solutions for policy enhancement based on the current scenario;
3. It considers the opinions of experts who ranked the possible solutions according to current regulations and practices set by the relevant authorities;
4. It acts as an initiative and evidence-based policy enhancement to encourage the implementation of biogas facilities in the remaining POMs with no biogas facilities and upcoming biogas plant projects.

#### **1.4 Research Goal and Scope**

The main goal of this study is to provide evidence-based policy suggestions for energy generation from POME. It delivers policy suggestions taking into consideration the output of LCA, life cycle cost-benefit analysis (LCCBA), interviews with POM management and a survey with experts for two types of energy generation POME treatment technologies for energy generation, enabling policy makers to improve the existing policy and encourage investors to implement biogas facilities in all POMs.

### **1.4.1 Research Objectives**

The specific objectives are as follows:

1. To establish an inventory of inputs and outputs for two types of treatment technologies of electricity generation from POME.
2. To assess the potential environmental impacts for two types of treatment technologies of electricity generation from POME using LCA approach.
3. To evaluate the economic feasibility for two types of treatment technologies of electricity generation from POME using LCCBA.
4. To utilise the findings from LCA, LCCBA and conduct interview with the palm oil mill management for the suggestion of possible solutions for policy enhancement.
5. To rank the possible solutions through a survey with experts and assign weights using multi criteria analysis to suggest prioritised solutions towards policy enhancement of electricity generation from POME.

### **1.4.2 Research Scope**

This study covered two different POME treatment technologies from POM 1 and POM 2, respectively for energy generation. The two POME treatment technologies compared are: CLB and CSTR system. Out of the 90 POMs with biogas facilities, 36 mills are employing the CLB system while the remaining 54 mills using the tank system, most commonly the CSTR system. Thus, CLB and CSTR systems would represent the scenarios of POMs employing biogas facilities. As for data inventory, inputs and outputs for two different processing routes are based on the software database and industrial data from POM 1 and POM 2. The boundary of the study is based on gate-to-gate (POME to electricity generation) for two types of processing route.

In order to quantify the potential environmental impacts for different treatment technologies of electricity generation from POME, potential impacts available in CML 2001 method, a life cycle impact assessment (LCIA) methodology was used, with specific and related impacts assessed. The collected inventory data is modelled using LCA software (Gabi 8). The LCIA shows the values possessed for each different impact which enable easy assessment of generating electricity for the life cycle stages including the full gate-to-gate system boundary. The economic feasibility is evaluated using LCCBA approach which consist of both life cycle cost (LCC) and cost benefit analysis (CBA). LCC comprises the capital cost and operational cost while CBA includes additional economic factors such as return on investment, PP, net present value and Break-Even analysis (BA) which is necessary to evaluate the desirability and feasibility of a process.

An interview with eleven POM management from five POMs were conducted where a list of possible solutions was derived using the output of LCA (environmental hotspots) and LCCBA (economic outputs) as an evidence for policy enhancement of POME treatment for energy generation. The limited number of interviewees was one of the limitations of this study as it was difficult to engage with relevant stakeholders due to slow responses (or mostly no response at all). It is also important to note that if a higher number of POMs responded positively to invitations to participate in interviews, a wider range of solutions may have been identified. Then, a survey listing all the possible solutions was conducted with experts. The possible solutions were analysed and assigned weights using an AHP method. Prioritised solutions towards policy enhancement in this study can be used to guide policy makers to take into consideration the aspects which need improving in the existing policy, as well as to encourage investors to implement biogas facilities in remaining POMs with no biogas facilities and upcoming biogas plant projects.

## **1.5 Research Significance**

Global warming issues are having an adverse impact on the environment. Substituting fossil fuels with renewable resources such as biomass will reduce the environmental impacts, which will help to overcome the environmental crisis. Also, growing demand for electricity generation has increased the necessity to further venture into renewable resources to substitute depleting fossil fuel resources. Apart from environmental issues, economic aspects like longer payback period (PP) upon investing into new RE technology reduces the interest of investors to confidently venture into RE sector. Thus, this study used LCA and LCCBA to assess and compare environmental and economic aspects as well as interviews with POM management and surveys with experts considering two major POME treatment technologies applied in the palm oil industry.

The importance of this study is its contribution in providing an evidence-base for a case study of POME treatment for energy generation, in order to enhance policy decision making. It is crucial to improve the existing policy as it currently fails to portray RE (particularly biogas) as an attractive alternative for the country to move forward as it ventures into RE. In this study, the evidence could encourage policy makers to take into account certain elements in the midst of improving the existing policy, as well as encouraging investors to implement biogas technologies for the remaining POMs with no biogas facilities in Malaysia, taking into account environmental and economic dimensions.

## **1.6 Thesis Layout**

Chapter 1 discussed the background and problem statement of this study. Research goal, objectives, scope and significance of this study were also discussed in Chapter 1.

Chapter 2 discusses all the relevant areas of literature covered in this study. In this chapter, a policy review on energy, POME, characteristics of POME, available treatment technologies of POME, LCA, LCCBA, and previous studies on evidence-based policy are discussed. Lastly, the types of sustainability models are discussed where AHP is discussed in depth.

Chapter 3 presents the research methodology of this study. The overall flow of this study is explained followed by the description of the study site. The data collection methods for life cycle studies as well as the equation involved for emission calculations, and costing calculations are discussed in detail. Lastly, the process flow towards setting the list of possible solutions for policy enhancement through interviews with POM management, a survey with experts and the AHP method to assign weighting for the possible solutions are also explained.

As for Chapter 4, the results and discussions of this study are discussed. Under this chapter, the output of LCA for two different POME treatment technologies are compared and evaluated. Lastly, a sensitivity analysis conducted is presented and critically reflected upon in order to overcome the hotspot of environmental impact.

Chapter 5 further considers economic aspects, which include both LCC and CBA (LCCBA) for the two different POME treatment technologies that are compared. A sensitivity analysis to overcome the hotspot of the economic aspects issue is set out. Lastly, BA to determine minimum annual production of electricity to ensure the company operates at gain is presented.

Chapter 6 sets out the list of possible solutions suggested by the POM management based on the output of life cycle studies which were ranked through a survey with experts. The possible solutions are assigned weights using an AHP. This caters to the policy enhancement of this study based on the final output of the AHP analysis. Lastly, based on the results analysed from this study, conclusions and recommendations for future study and limitations of this study are identified and discussed in Chapter 7.

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