

PREPARATION AND CHARACTERIZATION OF POLYLACTIC ACID
MODIFIED POLYVINYLIDENE FLUORIDE HOLLOW FIBER MEMBRANES
WITH ENHANCED WATER FLUX AND ANTIFOULING RESISTANCE

NUR SYUHADHA BINTI MOHAMAD ASERI

A thesis submitted in fulfilment of the
requirements for the award of the degree of
Master of Philosophy

School of Chemical and Energy Engineering
Faculty of Engineering
Universiti Teknologi Malaysia

DECEMBER 2019

DEDICATION

This thesis is dedicated to my father, who taught me that the best kind of knowledge is to learn by yourself. It is also dedicated to my mother, who taught me that even the most difficult task can be accomplished if it is done one step at a time.

ACKNOWLEDGEMENT

In preparing this thesis, I was in contact with many people, researchers, academicians and practitioners. They have contributed towards my understanding and thoughts. In particular, I wish to express my sincere appreciation to my main supervisor, Assoc. Prof. Dr. Lau Woei Jye, for his encouragement, guidance, critics and motivation. I am also very thankful to my co-supervisors - Dr. Hasrinah Binti Hasbullah and Assoc. Prof. Dr. Goh Pei Sean for their guidance, advices and motivation. Without their continued support and interest, this thesis would not have been the same as presented here.

I am also indebted to Universiti Teknologi Malaysia (UTM) for funding my Master study. Librarians at UTM also deserve special thanks for their assistance in supplying the relevant literatures.

My fellow postgraduate friends should also be recognised for their support. My sincere appreciation also extends to others who have provided assistance at various occasions. Their views and tips are useful indeed. Unfortunately, it is not possible to list all of them in this limited space. I am grateful to my entire family members.

ABSTRACT

Although ultrafiltration (UF) membranes have gained considerable attention in water separation and purification process, most of the materials used for commercial UF membranes fabrication are not able to degrade/decompose easily and tend to cause severe environmental problem when they are discarded. In view of this, an environmentally friendly hydrophilic polymeric material - polylactic acid (PLA) has been considered in this work, aiming to reduce not only the environmental impacts caused by the existing membranes but also to improve membrane water flux and antifouling resistance. In this study, the effects of PLA quantity and air gap (during spinning process) on the morphology and liquid separation performance of polyvinylidene fluoride (PVDF) hollow fiber membranes were investigated. The membrane properties were characterised using scanning electron microscope, atomic force microscope, Fourier transform infrared spectrometer, tensile tester and contact angle goniometer before filtration experiment was conducted. Results showed that the incorporation of low quantity of PLA (with PLA/PVDF weight ratio of ≤ 1.0) could significantly improve the membrane water flux from ~ 30 to $376.7 \text{ L/m}^2 \cdot \text{h} \cdot \text{bar}$ without compromising rejection (95–97%). More importantly, the PLA-modified PVDF membranes required a much lower temperature to decompose which minimizes environmental impacts. Owing to the improved surface hydrophilicity (lower water contact angle), the PLA-modified PVDF membranes also exhibited a higher flux recovery rate than that of pure PVDF membrane, revealing the improved antifouling resistance against bovine serum albumin. The findings of this work demonstrated that biodegradable PLA has the potential to modify the characteristics of UF membranes, leading to an enhanced water treatment process.

ABSTRAK

Walaupun membran ultrafiltrasi (UF) telah banyak mendapat perhatian dalam proses pemisahan dan penulenan air, kebanyakan bahan yang digunakan untuk fabrikasi membran UF komersial tidak dapat diuraikan dengan mudah dan cenderung menyebabkan masalah alam sekitar yang teruk apabila dibuang. Berdasarkan pandangan ini, bahan polimer hidrofilik yang mesra alam - asid polilaktik (PLA) telah dipertimbangkan dalam kerja ini, bertujuan untuk mengurangkan bukan sahaja kesan alam sekitar yang disebabkan oleh membran yang sedia ada tetapi juga untuk memperbaiki fluks air membran dan rintangan antikotoran. Dalam kajian ini, kesan kuantiti PLA dan sela udara (semasa proses berputar) pada morfologi dan prestasi pemisahan cecair membran gentian berongga polivinilidena fluorida (PVDF) telah disiasat. Sifat-sifat membran dicirikan dengan menggunakan mikroskop elektron imbasan, mikroskop daya atomik, spektrometer infra-merah jelmaan fourier, penguji tegangan dan goniometer sudut sentuhan sebelum filtrasi dijalankan. Keputusan menunjukkan bahawa penggabungan kuantiti kecil PLA (dengan nisbah berat PLA / PVDF ≤ 1.0) dapat meningkatkan fluks air membran dari ~ 30 hingga 376.7 L/m².h.bar tanpa menjejaskan penolakan (95-97%). Lebih penting lagi, membran PLA-terubahsuai PVDF memerlukan suhu yang lebih rendah untuk mengurai yang mana meminimumkan kesan alam sekitar. Oleh kerana peningkatan hidrofilik permukaan yang lebih baik (sudut sentuhan air yang lebih rendah), membran PLA-terubahsuai PVDF juga mempamerkan kadar perolehan fluks yang lebih tinggi daripada membran PVDF tulen, mendedahkan rintangan antikotoran yang lebih baik terhadap albumin serum lembu. Penemuan kerja ini menunjukkan bahawa PLA boleh biodegradasi berpotensi untuk digunakan untuk mengubah ciri-ciri membran UF, yang membawa kepada peningkatan proses rawatan air.

TABLE OF CONTENTS

	TITLE	PAGE
	DECLARATION	ii
	DEDICATION	iii
	ACKNOWLEDGEMENT	iv
	ABSTRACT	v
	ABSTRAK	vi
	TABLE OF CONTENTS	vii
	LIST OF TABLES	xi
	LIST OF FIGURES	xii
	LIST OF ABBREVIATIONS	xiv
	LIST OF SYMBOLS	xvi
CHAPTER 1	INTRODUCTION	1
	1.1 Research Background	1
	1.2 Problem Statements	2
	1.3 Research Objective	4
	1.4 Scopes of the Study	5
	1.5 Significance of Study	5
CHAPTER 2	LITERATURE REVIEW	7
	2.1 Water Sources	7
	2.2 Disinfection by Products	8
	2.3 Basic Principle of Membrane Technology	10
	2.3.1 Separation Mechanism	12
	2.3.2 Fabrication Technique	15
	2.3.3 Membrane Configuration	17
	2.4 Membrane Fouling	20
	2.5 Ultrafiltration Membrane	21
	2.6 Single Polymer	22

2.7	Polymeric Membrane Blended with Secondary Polymer	23
2.8	Potential of Biodegradable Polymer as Additive for Membrane Preparation	25
2.8.1	Advantages of Biodegradable Polymer	25
2.8.2	Application of Polylactic Acid as a Membrane	26
CHAPTER 3	RESEARCH METHODOLOGY	29
3.1	Research Design	29
3.2	Materials Selection	31
3.2.1	Main Polymer	31
3.2.2	Solvent	31
3.2.3	Additives	32
3.3	Hollow Fiber Membrane Fabrication	33
3.4	Membrane Characterization	36
3.4.1	Fourier-Transform Infrared (FTIR) Spectrometry	36
3.4.2	Thermogravimetric Analysis (TGA)	36
3.4.3	Scanning Electron Microscopy (SEM)	36
3.4.4	Atomic Force Microscopy (AFM)	37
3.4.5	Mechanical Strength Analysis	37
3.4.6	Hydrophilicity and Membrane Porosity Analysis	37
3.5	Membrane Performance Evaluation	38
3.5.1	Anti-fouling Performance	40
3.5.2	Leachability Test of PLA	41
3.5.3	River Water Analysis	41
CHAPTER 4	RESULTS AND DISCUSSION	43
4.1	Effect of PLA and Air gap on the Properties of PVDF Hollow Fiber Membrane	43
4.1.1	FTIR Analysis	43
4.1.2	Membrane Thermal Degradation	45
4.1.3	Morphology of PVDF/PLA Hollow Fiber Membrane	46
4.1.4	AFM Analysis	50
4.1.5	Mechanical Analysis of PVDF/PLA Membranes	51
4.1.6	Surface Wettability studies of PVDF Membrane	53

4.2	Filtration Performance	54
4.2.1	Permeability Performance of PVDF/PLA Membranes	54
4.2.2	Performance of Natural Organic Matter	55
4.2.3	Anti-Fouling Performance of Membranes	56
4.2.4	Separation Efficiency of Membrane for River Water Treatment	58
CHAPTER 5	CONCLUSIONS AND RECOMMENDATIONS	61
5.1	Conclusions	61
5.2	Recommendations	61
REFERENCES		63
LIST OF PUBLICATION		73

LIST OF TABLES

TABLE NO.	TITLE	PAGE
Table 2.1	Classification of membrane process in water and wastewater filtration	11
Table 2.2	Classification of pore size from International Union of Pure and Applied Chemistry (1985)	14
Table 2.3	Application of UF membranes	21
Table 2.4	Performance of polymeric membrane embedded with other polymers	24
Table 3.1	Composition and viscosity of dope solution	33
Table 4.1	Overall porosity and pore size of membranes	48
Table 4.2	Summary results of flux recovery rate of resultant membrane	55

LIST OF FIGURES

FIGURE NO.	TITLE	PAGE
Figure 2.1	Point source and non-point sources	8
Figure 2.2	Water treatment plant	9
Figure 2.3	Basic diagram of membrane separation system	13
Figure 2.4	Schematic diagram of isotropic and anisotropic membrane	15
Figure 2.5	Illustration of different membrane morphologies caused of different precipitation rate	16
Figure 2.6	A plate and frame module diagram	17
Figure 2.7	Exploded view and cross-section drawing of spiral-wound module	18
Figure 2.8	Two types of hollow fibre modules, (a) shell-side feed and (b) bore-side feed	19
Figure 3.1	Experimental stages of this research study	29
Figure 3.2	Chemical structure of PVDF	30
Figure 3.3	Chemical structure of n-methyl-pyrrolidone	31
Figure 3.4	Chemical structure of PLA	31
Figure 3.5	Chemical structure of PVP	32
Figure 3.6	Schematic diagram of dry/wet inversion spinning technique	34
Figure 3.7	Schematic diagram of hollow fiber membrane module	34
Figure 3.8	Schematic diagram of cross flow ultrafiltration system	38
Figure 4.1	FTIR spectra of PVDF membranes modified by PLA at different PVDF/PLA ratio	42
Figure 4.2	TGA analysis of PVDF membranes modified by PLA at different PVDF/PLA ratio	43
Figure 4.3	SEM images of cross-sectional structural of hollow fiber membrane	46
Figure 4.4	SEM outer surface images of membrane	47
Figure 4.5	3D AFM outer surface images of membrane	49

Figure 4.6	Stress-strain curves of resultant hollow fiber membranes	50
Figure 4.7	Graph of percent elongation and young modulus of PVDF and PVDF/PLA hollow fiber membranes	50
Figure 4.8	Water contact angle of PVDF and PVDF/PLA hollow fiber membranes at different air gap	51
Figure 4.9	Pure water flux performance of PVDF membrane with and without PLA modification at different air gap	52
Figure 4.10	Performance of fabricated hollow fiber membrane for HA rejection at different air gap	53
Figure 4.11	Flux versus time for the PVDF and PVDF-PLA membranes tested at 1 bar during three steps	54
Figure 4.12	Extended flux profiles for the PVDF and PVDF-PLA membranes tested at 1 bar using 1500 mg/L BSA solution for three cycles of operation	55
Figure 4.13	Separation efficiency of PVDF membrane with and with PLA material	56

LIST OF ABBREVIATIONS

AFM	-	Atomic Force Microscopy
BSA	-	Bovine Serum Albumin
COD	-	Chemical Oxygen Demand
DBPs	-	Disinfection by Products
DER	-	Dope Extrusion Rate
DOM	-	Dissolved Organic Matter
DON	-	Dissolved Organic Nitrogen
EG	-	Ethylene Glycol
FRR	-	Flux Recovery Rate
FTIR	-	Fourier Transform Infrared
GC-MS	-	Gas Chromatography–Mass Spectrometry
HA	-	Humic Acid
HAAs	-	Haloacetic Acids
HANs	-	Halocetonitriles
HPLC	-	High Performance Liquid Chromatography
ID	-	Inner Diameter
MF	-	Microfiltration
MW	-	Molecular Weight
MWCO	-	Molecular Weight Cut Off
NCI	-	National Cancer Institute
NF	-	Nanofiltration
NIPS	-	Nonsolvent Induce Phase Separation
NMP	-	N-Methyl-Pyrrolidone
NOM	-	Natural Organic Matter
OD	-	Outer Diameter
PAN	-	Polyacrylonitrile
PD	-	Polydopamine
PE	-	Polyethylene
PEG	-	Polyethylene Glycol
PEI	-	Polyetherimide

PES	-	Polyethersulfone
PHEMA	-	Poly(2-hydroxyethyl methacrylate)
PI	-	Polyimide
PLA	-	Poly(lactic acid)
PP	-	Polypropylene
PPO	-	Polypropylene Oxide
PSF	-	Polysulfone
PTFE	-	Polytetrafluoroethylene
PU	-	Poly(urethane)
PVDF	-	Poly(vinylidene fluoride)
PVP	-	Poly(vinylpyrrolidone)
PWF	-	Pure Water Flux
PWP	-	Pure Water Permeation
RO	-	Reverse Osmosis
SEM	-	Scanning Electron Microscopy
TGA	-	Thermogravimetric Analysis
THMs	-	Trihalomethanes
TIPS	-	Thermal Induced Phase Separation
TOC	-	Total Organic Carbon
UF	-	Ultrafiltration
US	-	United States
USEPA	-	United State Environmental Protection Agency
UV-Vis	-	Ultraviolet Visible
WTP	-	Water Treatment Plant
XA	-	Xanthan Gum

LIST OF SYMBOLS

β	-	Beta
$^{\circ}\text{C}$	-	Celcius
$^{\circ}\text{C}/\text{min}$	-	Celcius Per Minute
ρ	-	Density
l	-	Thickness
$<$	-	Less Than
$>$	-	More Than
μm	-	Micrometer
μL	-	Microlitre
ΔP	-	Operating Pressure
$\%$	-	Percent
ε	-	Porosity
A	-	Effective area
$(\text{C}_3\text{H}_4\text{O}_2)_n$	-	Polylactic acid
CO_2	-	Carbon Dioxide
C_p	-	Concentration of permeate
C_f	-	Concentration of feed
cm	-	centimetre
cP	-	Centipoises
Da	-	Dalton
g	-	Gram
g/mol	-	Gram Per Mole
H_2O	-	Water
h	-	Hour
J_w	-	Flux Pure Water
K	-	Kelvin
L	-	Litre
L/min	-	Litre Per Minute
m	-	Mass of Hollow Fiber Membrane
ml	-	Millilitre

ml/min	-	Millilitre Per Minute
mm	-	Millimetre
mm/min	-	Millimetre Per Minute
mg	-	Milligram
mg/L	-	Milligram Per Litre
min	-	Minute
MPa	-	Mega Pascal
m ²	-	Meter Square
m ³ /s	-	Meter Cube Per Second
n	-	Number of Unit
nm	-	Nanometre
<i>n</i>	-	Water Viscosity
ppm	-	Part Per Millions
psig	-	Pound Per Square in Gauge
R	-	Rejection
r	-	Mean Pore Radius
t	-	Filtration Time
v	-	Volume
wt.%	-	Percent Weight

CHAPTER 1

INTRODUCTION

1.1 Research Background

Drinking water is essential to human life. Drinking water resources are mainly from rivers or water bodies that enter water treatment plant (WTP) before distribution. WTPs are designed to treat contaminants that exist in water bodies such as natural organic matter (NOM) and ammonia. These compounds are found in the water body or soil in the upstream of water bodies. Mostly they are from plantation or aquatic plants that flow in water bodies by precipitation, underground flow and flood.

However, there are some problems in existing WTP where the presence of free chlorine content that is used as a disinfectant is found to react with residual NOMs. This reaction process has been found to have a tendency to form disinfection by-products (DBPs) such as trihalomethanes, haloacetic acids and other halogenated organics. DBPs are carcinogens and direct exposure may lead to cancers, miscarriages and nervous system complications [1–4].

The increasing soil erosion and flood from unplanned construction and rapid economic development on the other hand had also increased the amount of NOMs, causing problems to the existing WTP [5]. Certainly, up to date, some of the existing WTPs are not able to eliminate these DBPs to a satisfactory level, thus an advanced treatment process is needed [6].

At present, the development of membrane technologies has attracted attention in the field of water treatment process. Ultrafiltration (UF) membranes in particular are used for removal of large particles. Although UF membranes have gained considerable attention in water separation and purification process, most of the

materials used for commercial UF membranes fabrication are not able to degrade/ decompose easily and tend to cause severe environmental problems when they are discarded. In view of this, an environmentally friendly hydrophilic polymeric material - polylactic acid (PLA) has been considered in this work, aiming to reduce not only the environmental impacts caused by the existing membranes but also to improve membrane water flux and antifouling resistance.

1.2 Problem Statements

Natural organic matter (NOM) found in the water environment is ubiquitous and chemically complex organic compound. A study showed that NOM is one of the main pollutants in drinking water production mainly because of the generation of disinfection by-products (DBPs) such as trihalomethanes (THMs) and haloacetic acids (HAAs) when NOM interacts with chlorine in water [7]. Direct exposure to the DBPs can cause cancers, miscarriages and nervous system complications [1–3]. Therefore, effective removal of NOM is a significant and challenging research topic in the current development of water purification. Humic acid (HA) is the major species in NOM and accounts for 50–90% of the total freshwater organic matters [2,3]. Scientists always considered HA as a model compound in the studies of water treatment process using membrane-based technology [1–3].

UF membrane process receives a wider attention compared to other membrane technologies such as reverse osmosis (RO), nanofiltration (NF) and microfiltration (MF) due to its good balance between water flux and rejections against colloids, macromolecules and suspended particles [8–12]. One of the main polymeric materials that is widely used for the commercial UF membranes fabrication is polyvinylidene fluoride (PVDF). Compared to polysulfone (PSF) and polyethersulfone (PES), PVDF offers greater thermal stability and mechanical property as well as outstanding chemical and oxidation resistance [8,11,13–15]. However, PVDF is not made of biodegradable material and requires longer time to achieve complete degradation upon dump site disposal [16]. In view of this, it is a

great significance if a novel membrane material is able to be developed using biodegradable polymer.

Biodegradable materials can be broken down by microorganisms, producing harmless compounds for nature. These kinds of materials have already been widely used in food packaging, daily necessities, containers, and medical instruments [13,16]. Among the biodegradable materials, polylactic acid (PLA, formula: $(C_3H_4O_2)_n$) - a polymer produced from natural sources like corn is widely reported in the literature [13,16]. Statistics from the SCOPUS reveal that there are more than 3,000 papers reporting the use of PLA for various applications over the past 10 years (2007–2018). PLA is possibly degraded in soil, compost or human body. In a composting environment the PLA is hydrolyzed into smaller molecules, e.g., oligomers, dimers and monomers after 45–60 days at 50–60°C. These smaller molecules are then degraded into CO_2 and H_2O by microorganisms in compost [17,18].

Incorporation of hydrophilic biopolymer like xanthan gum (XA) into PES membrane had been previously reported for HA removal. The modified PES membrane was reported to exhibit enhanced water permeability (24.8 $L/m^2 \cdot h \cdot bar$) with HA rejection above 80% [19]. Similar to XA, PLA which is also a hydrophilic biopolymer has potential to be used for membrane modification. Previous studies have investigated the potential of using PLA and its derivatives for membrane fabrication. For instance, PLA/poly(lactic acid)-block-poly(2-hydroxyethyl methacrylate) (PLA–PHEMA) membranes with high PLA–PHEMA contents exhibited enhanced hydrophilicity, water permeability and anti-fouling resistance [20]. Upon addition of 15 wt% PLA–PHEMA, the water flux of the resultant membrane was reported to be about 236 $L/m^2 \cdot h \cdot bar$ with bovine serum albumin (BSA) clearance as low as 0.31 mL/min [20]. Shen *et al.* [21] on the other hand reported that the incorporation of PLA-based copolymer could improve the hydrophilicity of membrane by decreasing water contact angle from around 80° to 60°, leading to enhanced water permeability and greater antifouling properties.

Previous studies have shown that hydrophilic PLA could be used to modify the properties of PSF nanofiber membrane with respect to pore dimension [22] and oil sorption capacity [23], but using PLA as additive for asymmetric UF membrane fabrication has yet to be reported in the literature. It must be pointed out that the membranes made of pure PLA are not likely to be used for pressure-driven process owing to the poor mechanical properties of PLA film [16-17]. Thus, PLA can only be considered as additive to modify the existing membranes.

In view of this, the main objective of this work was to modify PVDF-based hollow fiber membrane using biodegradable PLA, aiming to produce environmentally friendly membranes with enhanced water flux and antifouling properties for water treatment process.

1.3 Research Objective

Based on the above-mentioned problems, the main objectives of this work were:

- 1) To characterize PVDF/PLA blend hollow fiber membranes with different properties by varying PLA:PVDF ratio in dope solution and air gap during spinning process.
- 2) To evaluate filtration performance of PVDF/PLA blend membrane as advanced treatment process in purifying water source containing organic foulants.

1.4 Scopes of the Study

In order to achieve the objectives of this research, the following scopes are outlined:

- 1) Preparing a spinning solution made of different ratio of PLA/PVDF ratio (0, 0.3, 1, 2 and 3) with the presence of 5 wt% polyvinylpyrrolidone (PVP).
- 2) Fabricating hollow fiber membrane via spinning technique by varying air gap from zero to 8 cm using the dope solutions prepared.
- 3) Characterizing membrane properties using Fourier transform infrared (FTIR), scanning electron microscopy (SEM), contact angle measurement, atomic force microscope (AFM) analysis, thermogravimetric analysis (TGA), tensile machine and goniometer contact angle.
- 4) Evaluating PLA/PVDF hollow fiber membrane performance with respect to pure water flux, humic acid rejection and antifouling properties using bovine serum albumin (BSA) as foulant.
- 5) Investigating PLA leaching from the PVDF membranes by analyzing the water solution using total organic carbon (TOC) analyzer
- 6) Assessing performance of PLA/PVDF hollow fiber membrane towards river water treatment by measuring river water flux and reduction of turbidity, conductivity and chemical oxygen demand (COD).

1.5 Significance of Study

The significance of the current research was to develop a more environmentally friendly UF membrane for water application using biodegradable polymer - PLA. Besides being environmentally friendly, the PVDF-based hollow fiber membrane embedded with PLA as secondary polymer also exhibited greater water flux without compromising HA rejection. More importantly, the PLA-modified PVDF membranes required much lower temperature to decompose which minimizes environmental impacts. Owing to the improved surface hydrophilicity (lower water

contact angle), the PLA-modified PVDF membranes also exhibited higher flux recovery rate than that of pure PVDF membrane, revealing the improved antifouling resistance against bovine serum albumin.

REFERENCES

1. N.A.A. Hamid, A.F. Ismail, T. Matsuura, A.W. Zularisam, W.J. Lau, E. Yuliwati, M.S. Abdullah, Morphological and separation performance study of polysulfone/titanium dioxide (PSF/TiO₂) ultrafiltration membranes for humic acid removal, *Desalination*. 273 (2011) 85–92.
2. G. Amy, J. Cho, Interactions between natural organic matter (NOM) and membranes: Rejection and fouling, *Water Sci. Technol.* 40 (1999) 131–139.
3. J. Wang, W.Z. Lang, H.P. Xu, X. Zhang, Y.J. Guo, Improved poly(vinyl butyral) hollow fiber membranes by embedding multi-walled carbon nanotube for the ultrafiltrations of bovine serum albumin and humic acid, *Chem. Eng. J.* 260 (2015) 90–98.
4. A.W. Zularisam, A.F. Ismail, R. Salim, Behaviours of natural organic matter in membrane filtration for surface water treatment — a review, *Desalination* 194 (2006) 211–231.
5. J. Tian, H. Liang, J. Nan, Y. Yang, S. You, G. Li, Submerged membrane bioreactor (sMBR) for the treatment of contaminated raw water, *Chemical Energy Engineering*, 148 (2009) 296–305.
6. T. Wintgens, M. Gallenkemper, T. Melin, Endocrine disrupter removal from wastewater using membrane bioreactor and nanofiltration technology, *Desalination*, 146 (2002) 387–391.
7. S. Xia, M. Ni, Preparation of poly(vinylidene fluoride) membranes with graphene oxide addition for natural organic matter removal, *J. Memb. Sci.* 473 (2014) 54–62.
8. M. Sri Abirami Saraswathi, R. Kausalya, N.J. Kaleekkal, D. Rana, A. Nagendran, BSA and humic acid separation from aqueous stream using polydopamine coated PVDF ultrafiltration membranes, *J. Environ. Chem. Eng.* 5 (2017) 2937–2943.
9. J. Lee, S. Jeong, Y. Ye, V. Chen, S. Vigneswaran, T.O. Leiknes, Z. Liu, Protein fouling in carbon nanotubes enhanced ultrafiltration membrane: Fouling mechanism as a function of pH and ionic strength, *Sep. Purif. Technol.* 176 (2017) 323–334.

10. G.S. Lai, M.H.M. Yusob, W.J. Lau, R.J. Gohari, D. Emadzadeh, A.F. Ismail, P.S. Goh, A.M. Isloor, M.R. Arzhandi, Novel mixed matrix membranes incorporated with dual-nanofillers for enhanced oil-water separation, *Sep. Purif. Technol.* 178 (2017) 113–121.
11. C.S. Ong, W.J. Lau, P.S. Goh, B.C. Ng, T. Matsuura, A.F. Ismail, Effect of PVP Molecular Weights on the Properties of PVDF-TiO₂ Composite Membrane for Oily Wastewater Treatment Process, *Sep. Sci. Technol.* 49 (2014) 2303–2314.
12. M.S. Muhamad, M.R. Salim, W.J. Lau, Z. Yusop, A review on bisphenol A occurrences , health effects and treatment process via membrane technology for drinking water, *Env. Sci Pollut Res.* 23 (2016) 11549-11567.
13. R. Fryczkowski, B. Fryczkowska, W. Biniaś, J. Janicki, Morphology of fibrous composites of PLA and PVDF, *Compos. Sci. Technol.* 89 (2013) 186–193.
14. S. Simone, A. Figoli, A. Criscuoli, M.C. Carnevale, A. Rosselli, E. Drioli, Preparation of hollow fibre membranes from PVDF/PVP blends and their application in VMD, *J. Memb. Sci.* 364 (2010) 219–232.
15. M.N. Subramaniam, P.S. Goh, W.J. Lau, B.C. Ng, A.F. Ismail, AT-POME colour removal through photocatalytic submerged filtration using antifouling PVDF-TiO₂ nanocomposite membrane, *Sep. Purif. Technol.* 191 (2018) 266–275.
16. Z. Xue, Z. Sun, Y. Cao, Y. Chen, L. Tao, K. Li, L. Feng, Q. Fu, Y. Wei, Superoleophilic and superhydrophobic biodegradable material with porous structures for oil absorption and oil-water separation, *RSC Adv.* 3 (2013) 23432–23437.
17. Y. Tokiwa, B.P. Calabia, Biodegradability and biodegradation of poly (lactide), *Appl. Microbiol Biotechnol.* 72 (2006) 244–251.
18. C. Vasile, D. Pamfil, M. Râpă, R.N. Darie-niță, C. Mitelut, E.E. Popa, P.A. Popescu, M. Cristina, M.E. Popa, Study of the soil burial degradation of some PLA/CS biocomposites *Cornelia, Compos. Part B Eng.* 142 (2018) 251-262.
19. R. Sathish Kumar, G. Arthanareeswaran, D. Paul, J.H. Kweon, Effective removal of humic acid using xanthan gum incorporated polyethersulfone membranes, *Ecotoxicol. Environ. Saf.* 121 (2015) 223–228.

20. L. Zhu, F. Liu, X. Yu, L. Xue, Poly(Lactic Acid) Hemodialysis Membranes with Poly(Lactic Acid)-block-Poly(2-Hydroxyethyl Methacrylate) Copolymer As Additive: Preparation, Characterization, and Performance, *ACS Appl. Mater. Interfaces.* 7 (2015) 17748–17755.
21. P. Shen, K. Tu, C. Yang, J. Li, R. Du, Preparation of anti-fouling poly (lactic acid) (PLA) hollow fiber membranes via non-solvent induced phase separation, *Advanced Material Science*, 884-885 (2014) 112–116.
22. L.G. Liu, J.H. He, Solvent evaporation in a binary solvent system for controllable fabrication of porous fibers by electrospinning, *Therm. Sci.* 21 (2017) 1821–1825.
23. L. Liu, Z. Lin, J. Niu, D. Tian, J. He, Electrospun polysulfone/poly(lactic acid) nanoporous fibrous mats for oil removal from water, *Adsorpt. Sci. Technol.* 37 (2019) 5-6, 438-450.
24. H.C. Chen, C.H. Tsai, M.C. Yang, Mechanical properties and biocompatibility of electrospun polylactide/poly(vinylidene fluoride) mats, *J. Polym. Res.* 18 (2011) 319–327.
25. W. Xie, J. Li, T. Sun, W. Shang, W. Dong, M. Li, F. Sun, Hydrophilic modification and anti-fouling properties of PVDF membrane via in situ nanoparticle blending, *Environ. Sci. Pollut. Res.* 25 (2018) 25227–25242.
26. E. Corcoran, C. Nellesmann, E. Baker, R. Bos, D. Osborn, H. Savelli, Sick water? The central role of wastewater management in sustainable development, 2010.978-82-7701-075-5.
27. D. Pimentel, B. Berger, D. Filiberto, M. Newton, B. Wolfe, S. Clark, E. Poon, E. Abbett, S. Nandagopal, *Water Resources : Agricultural and Environmental Issues*, 54 (2004) 909–918.
28. R.A. Kraemer, K. Choudburry, E. Kampa, *Protecting Water Resources: Pollution Prevention*, *Int. Conf. Freshw.* (2001).
29. C.N. Ukwe, C.A. Ibe, *Ocean & Coastal Management A regional collaborative approach in transboundary pollution management in the guinea current region of western Africa*, *Ocean Coast. Manag.* 53 (2010) 493–506.
30. M. La Farre', S. Pe'rez, L. Kantiani, D. Barcelo', Fate and toxicity of emerging pollutants, their metabolites and transformation products in the aquatic environment, *TrAC Trends in Analytical Chemistry*, 27 (2008) 991–1007.

31. M.K. Hill, *Understanding Environmental Pollution* Third edition, (2010).
32. H.F. Hemond, E.J. Fechner, *Chemical Fate and Transport in the Environment* Chemical Fate and Transport in the Environment, 3rd Edition, 2015.
33. A. Maartens, P. Swart, E.P. Jacobs, Feed-water pretreatment : methods to reduce membrane fouling by natural organic matter, 163 (1999) 51–62.
34. P. Westerhoff, H. Mash, Dissolved organic nitrogen in drinking water supplies : a review , *Journal Water Supply:Research and Technology. Aqua.* 51 (2002) 415-448.
35. T. Bond, M.R. Templeton, N. Graham, Precursors of nitrogenous disinfection by-products in drinking water — A critical review and analysis, *J. Hazard. Mater.* 235–236 (2012) 1–16.
36. R.W. Baker, *Membrane technology and applications*, 3rd Edition, 2012.
37. W. Chu, N. Gao, Y. Deng, M.R. Templeton, D. Yin, *Bioresource Technology* Impacts of drinking water pretreatments on the formation of nitrogenous disinfection by-products, *Bioresour. Technol.* 102 (2011) 11161–11166.
38. A.D. Shah, S.W. Krasner, C. Fen, U. Von Gunten, W.A. Mitch, Trade-Off s in Disinfection Byproduct Formation Associated with Precursor Preoxidation for Control of N -Nitrosodimethylamine Formation, 46 (2012) 4809-4818.
39. A.D. Shah, W.A. Mitch, A Critical Review of Nitrogenous Disinfection Byproduct Formation Pathways, (2012) 119–131.
40. N. Ozaki, K. Yamamoto, Hydraulic effects on sludge accumulation on membrane surface in crossflow filtration, 35 (2001) 3137–3146.
41. J. Tian, Y. Xu, Z. Chen, J. Nan, G. Li, Air bubbling for alleviating membrane fouling of immersed hollow- fi ber membrane for ultra fi ltration of river water, *Desalination.* 260 (2010) 225–230.
42. F. Meng, H. Zhang, F. Yang, L. Liu, Characterization of Cake Layer in Submerged Membrane Bioreactor, *Enviironmental Sci. Technol.* (2007) 4065–4070.
43. S. Chae, H. Yamamura, B. Choi, Y. Watanabe, Fouling characteristics of pressurized and submerged PVDF (polyvinylidene fluoride) microfiltration membranes in a pilot-scale drinking water treatment system under low and high turbidity conditions, *Desalination.* 244 (2009) 215–226.
44. A. Bottino, C. Capannelli, A. Del Borghi, M. Colombinob, Water treatment for drinking purpose : ceramic microfiltration application, *Desalination.* 141

- (2001) 75–79.
45. J. Lee, B. Park, J. Kim, S. Bin Park, Effect of PVP , Lithium Chloride , and Glycerol Additives on PVDF Dual-Layer Hollow Fiber Membranes Fabricated Using Simultaneous Spinning of TIPS and NIPS, 23 (2015) 291–299.
 46. L.E. Fratila-apachitei, M.D. Kennedy, J.D. Linton, I. Blume, J.C. Schippers, Influence of membrane morphology on the flux decline during dead-end ultrafiltration of refinery and petrochemical waste water, J. Memb. Sci. 182 (2001) 151–159.
 47. A.L. Zydney, C.K. Colton, A concentration polarization model for the filtrate flux in cross-flow microfiltration of particulate suspensions for the filtrate flux in cross-flow, Chem. Eng. Commun. (2007) 37–41.
 48. V. Urbain, R. Benoit, Membrane bioreactor : A New Treatment Tool, Am. Water Work. Assoc. 5 (1996) 75–86.
 49. M. Cheryan, N. Rajagopalan, Membrane processing of oily streams . Wastewater treatment and waste reduction, Jpurnal Membr. Sci. 151 (1998) 13-28.
 50. B. Ladewig, M.N.Z. Al-Shaeli, Fundamentals of Membrane Bioreactors, (2017) 13–38.
 51. H. Strathmann, Introduction to Membrane Science and Technology, Wiley-VCH. (2011). 544.
 52. J. Lee, B. Park, J. Kim, S. Bin Park, Effect of PVP, lithium chloride, and glycerol additives on PVDF dual-layer hollow fiber membranes fabricated using simultaneous spinning of TIPS and NIPS, Macromol. Res. 23 (2015) 291–299.
 53. G.R. Guillen, Y. Pan, M. Li, E.M. V Hoek, Preparation and characterization of membranes formed by nonsolvent induced phase separation: A review, Ind. Eng. Chem. Res. 50 (2011) 3798–3817.
 54. R.W. Baker, Membrane technology and applications, 2nd Edition 2012.
 55. X. Zhu, M. Elimelech, Fouling of Reverse Osmosis Membranes by Aluminum Oxide Colloids, Journal Environmental Engineering. 121 (1997) 884.
 56. A.F. Viero, G.L. Sant, A. Jr, R. Nobrega, The use of polyetherimide hollow fibres in a submerged membrane bioreactor operating with air backwashing
The use of polyetherimide hollow fibres in a submerged membrane bioreactor

- operating with air backwashing, 302 (2007) 127-135.
57. W.S. Ang, M. Elimelech, Protein (BSA) fouling of reverse osmosis membranes : Implications for wastewater reclamation, 296 (2007) 83–92.
 58. C.Y. Tang, Y. Kwon, J.O. Leckie, Fouling of reverse osmosis and nanofiltration membranes by humic acid — Effects of solution composition and hydrodynamic conditions, 290 (2007) 86–94.
 59. C.S. Ong, W.J. Lau, P.S. Goh, B.C. Ng, Desalination and Water Treatment Preparation and characterization of PVDF – PVP – TiO₂ composite hollow fiber membranes for oily wastewater treatment using submerged membrane system, *Desalin. Water Treat.* 1-11 (2013) 1944-3986.
 60. M.F.A. Goosen, S.S. Sablani, H. Al-Hinai, S. Al-Obeidani, R. Al-Belushi, D. Jackson, Fouling of Reverse Osmosis and Ultrafiltration Membranes : A Critical Review, *Separation Sci. Technol.* 10 (2010) 2261–2297.
 61. G. Guven, A. Perendeci, A. Tanyolac, Electrochemical treatment of deproteinated whey wastewater and optimization of treatment conditions with response surface methodology, *J. Hazard. Mater.* 157 (2008) 69–78.
 62. 1991 Mulder, *Basic Principle of membrane technology*, 119 (1997) 8580–8584.
 63. Y. Shui, L. Yan, C. Bao, L. Jiang, Treatment of oily wastewater by organic – inorganic composite tubular ultrafiltration (UF) membranes, *Desalination.* 196 (2006) 76–83.
 64. D. Hou, J. Wang, D. Qu, Z. Luan, C. Zhao, X. Ren, Preparation of hydrophobic PVDF hollow fiber membranes for desalination through membrane distillation, *Water Sci. Technol.* (2009) 1219–1226.
 65. F. Wicaksana, A.G. Fane, V. Chen, Fibre movement induced by bubbling using submerged hollow fibre membranes, 271 (2006) 186–195.
 66. G. Guglielmi, D. Chiarani, S.J. Judd, G. Andreottola, Flux criticality and sustainability in a hollow fibre submerged membrane bioreactor for municipal waste water treatment, *Journal Environmental Engineering.* 289 (2007) 241–248.
 67. J. Jin, M. Song, Chitosan and Chitosan – PEO Blend Membranes Crosslinked by Genipin for Drug Release, *J. Appl. Polym. Sci.* 102 (2005) 436-444.
 68. A. Witek, A. Kotuniewicz, B. Kurczewski, Simultaneous removal of phenols and Cr³⁺ using micellar-enhanced ultrafiltration process. *Desalination.* 191

- (2006) 111–116.
69. F. Saravia, C. Zwiener, F.H. Frimmel, Interactions between membrane surface, dissolved organic substances and ions in submerged membrane filtration. *Desalination*. 192 (2006) 280–287.
 70. X.H. Cao, M. Qiu, A.W. Qin, C.J. He, H.F. Wang, Effect of Additive on the Performance of PVDF Membrane via Non-Solvent Induced Phase Separation, *Mater. Sci. Forum*. 789 (2014) 240–248.
 71. W. Li, X. Tan, T. Luo, Y. Shi, Y. Yang, L. Liu, Preparation and characterization of electrospun PLA/PU bilayer nanofibrous membranes for controlled drug release applications, *Integr. Ferroelectr*. 179 (2017) 104–119.
 72. K. V. Kurada, S. De, Modeling of solution thermodynamics: A method for tuning the properties of blend polymeric membranes, *J. Memb. Sci.* 540 (2017) 485–495.
 73. A. Roy, S. De, Extraction of steviol glycosides using novel cellulose acetate phthalate (CAP) – Polyacrylonitrile blend membranes, *J. Food Eng.* 126 (2014) 7–16.
 74. N.M. Mokhtar, W.J. Lau, B.C. Ng, A.F. Ismail, D. Veerasamy, Treatment Preparation and characterization of PVDF membranes incorporated with different additives for dyeing solution treatment using membrane distillation, *Desalin. Water*. 8 (2014) 37–41.
 75. N. Said, H. Hasbullah, A.F. Ismail, M. Nidzhom, Z. Abidin, P. Sean, M.H. Dzarfah, The effect of air gap on the morphological properties of PSf / PVP90 membrane for hemodialysis application, *Chem. Eng. Trans.* 56 (2017) 1591–1596.
 76. F.H. and M.A. N. Abdali, A. Marjani, Fabrication of PVA coated PES/PVDF nanocomposite membrane embedded with in-situ formed magnetite nanoparticles for removal of metal ions from aqueous solutions, *New J. Chem.* 14 (2017) 1–11.
 77. A. Anvari, A. Azimi, Y. Fatemeh, PVDF / PAN Blend Membrane : Preparation, Characterization and Fouling Analysis, *J. Polym. Environ.* 25 (2016) 1348-1358.
 78. H. Abdallah, R. Taman, D. Elgayar, H. Farag, Antibacterial blend Polyvinylidene Fluoride / Polyethyleneimine membranes for salty oil emulsion separation, *Journal of Polymer*. 108 (2018) 542-553.

79. S. Zereshki, A. Figoli, S.S. Madaeni, S. Simone, J.C. Jansen, M. Esmailinezhad, E. Drioli, Poly(lactic acid)/poly(vinyl pyrrolidone) blend membranes: Effect of membrane composition on pervaporation separation of ethanol/cyclohexane mixture, *J. Memb. Sci.* 362 (2010) 105–112.
80. A. Moriya, P. Shen, Y. Ohmukai, T. Maruyama, H. Matsuyama, Reduction of fouling on poly(lactic acid) hollow fiber membranes by blending with poly(lactic acid)-polyethylene glycol-poly(lactic acid) triblock copolymers, *J. Memb. Sci.* 415–416 (2012) 712–717.
- 81 R. Jamshidi Gohari, W.J. Lau, T. Matsuura, A.F. Ismail, Effect of surface pattern formation on membrane fouling and its control in phase inversion process, *J. Memb. Sci.* 446 (2013) 326–331.
82. A. Iulianelli, C. Algieri, L. Donato, A. Garofalo, F. Galiano, G. Bagnato, A. Basile, A. Figoli, New PEEK-WC and PLA membranes for H₂ separation, *Int. J. Hydrogen Energy.* 34 (2017) 22138-22148.
83. W.N.R. Jami'an, H. Hasbullah, F. Mohamed, W.N. Wan Salleh, N. Ibrahim, R. Rasit Ali, Biodegradable Gas Separation Membrane Preparation by Manipulation of Casting Parameters, *Chem. Eng. Trans.* 43 (2015) 1–6.
84. L. Marbelia, M.R. Bilad, I.F.J. Vankelecom, Gradual PVP leaching from PVDF/PVP blend membranes and its effects on membrane fouling in membrane bioreactors, *Sep. Purif. Technol.* 213 (2019) 276–282.
85. X. Lu, Y. Peng, H. Qiu, X. Liu, L. Ge, Anti-fouling membranes by manipulating surface wettability and their anti-fouling mechanism, *Desalination.* 413 (2017) 127–135.
86. R.F. Bonan, P.R.F. Bonan, A.U.D. Batista, D.E.C. Perez, L.R.C. Castellano, J.E. Oliveira, E.S. Medeiros, Poly(lactic acid)/poly(vinyl pyrrolidone) membranes produced by solution blow spinning: Structure, thermal, spectroscopic, and microbial barrier properties, *J. Appl. Polym. Sci.* 134 (2017) 1–9.
87. R. Fryczkowski, B. Fryczkowska, W. Binia's, J. Janicki, Morphology of fibrous composites of PLA and PVDF, *Compos. Sci. Technol.* 89 (2013) 186–193.
88. J.P. Mofokeng, A.S. Luyt, T. Tábi, J. Kovács, Comparison of injection moulded, natural fibre-reinforced composites with PP and PLA as matrices, *J. Thermoplast. Compos. Mater.* 25 (2012) 927–948.

89. A. Chisom, H. Wang, Q. Zhang, Y. Zhuang, K. Hassan, C. Ying, H. Yang, W. Xu, Structure and thermal properties of porous polylactic acid membranes prepared via phase inversion induced by hot water droplets, *Polymer (Guildf)*. 141 (2018) 62–69.
90. K. Wang, A.A. Abdalla, M.A. Khaleel, N. Hilal, M.K. Khraisheh, Mechanical properties of water desalination and wastewater treatment membranes, *Desalination*. 406 (2016) 190-205.
91. Y. Li, H. Shimizu, Toughening of polylactide by melt blending with a biodegradable poly(ether)urethane elastomer, *Macromol. Biosci*. 7 (2007) 921–928.
92. W.J. Lau, A.F. Ismail, S. Firdaus, Car wash industry in Malaysia : Treatment of car wash effluent using ultrafiltration and nanofiltration membranes Car wash industry in Malaysia : Treatment of car wash effluent using ultrafiltration and nanofiltration membranes, *Sep. Purif. Technol*. 104 (2013) 26–31.

LIST OF PUBLICATION

1. **N.S. Aseri, W.J. Lau, P.S. Goh, H. Hasbullah, N.H. Othman, A.F. Ismail,** Preparation and characterization of polylactic acid-modified polyvinylidene fluoride hollow fiber membranes with enhanced water flux and antifouling resistance, *J. Water Process Eng.* 32 (2019) 100912. (Impact factor: 3.173)