PREPARATION, CHARACTERIZATION AND MECHANISTIC STUDY ON TRANSESTERIFICATION OF REFINED USED COOKING OIL FOR BIODIESEL PRODUCTION USING ZINC AND CALCIUM OXIDES-BASED CATALYSTS

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Dedicated to my beloved parents,
Sulaiman Ahmad and Foziah Jusoh @ Mohd Yusoff,
to my siblings, family and family in law,
for the continuos support and prayers.

To my dearest husband, Mohamad Helmi Bin Abd Mubin,
to my loving daughter, Nur Aleesa,
my source of strength,
thanks for always being there for me.

To my friends,
thank you so much,
for their patience, support, love and encouragement.
May Allah bless all of you...

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In the name of Allah S.W.T, the Most Gracious and the Most Merciful,

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ABSTRACT

Environmental concerns in fossil fuel depletion intensified the search for alternative fuel from renewable resources. Biodiesel is commonly produced by transesterification of vegetable oil in the presence of homogeneous catalyst. These catalysts, however, dissolve into the vegetable oil and large amount of water is required to clean the biodiesel that can cause saponification. Previously, extensive studies have been conducted on alkaline earth metal oxides such as calcium and magnesium oxides with manganese, iron, zirconium and cerium as the dopants. This research thus focused on the use of heterogeneous base catalysts that are easily separated and environmentally friendly for the biodiesel production. Zinc and calcium oxides-based supported on alumina were used as catalysts for the transesterification reaction of refined used cooking oil due to their highly basic characteristic. In order to improve the catalytic activity, the bimetallic and trimetallic oxides catalysts with copper, nickel, chromium and titanium as their co-catalysts were investigated. All the alumina supported catalysts were prepared by wetness impregnation method. The screening of biodiesel production using synthesized catalysts was monitored by gas chromatography-flame ionization detector (GC-FID). The two most potential catalysts were selected for the optimization and characterization study. Cu/Zn/γ-Al₂O₃ catalyst calcined at 800°C with 10:90 wt.% dopant ratio to based and 3 times of alumina coating, exhibited the highest biodiesel production (89.50%) at mild reaction conditions (65°C, 10 wt.% catalyst loading, 1:20 oil:methanol mole ratio and 2 hours of reaction time). Cr/Ca/γ-Al₂O₃ catalyst calcined at 700°C with 10:90 wt.% dopant ratio to based and 3 times number of alumina coating gave 86.64% of biodiesel production at 65°C, 6 wt.% catalyst loading, 1:18 oil:methanol mole ratio and 3 hours of reaction time. The physicochemical properties of the potential catalysts were accomplished using nitrogen analysis (NA) and CO2-temperature programmed desorption (CO₂-TPD) that indicated high surface area (>140 m²/g) and high basicity (>3 mmol/g). X-ray diffraction (XRD) and field emission scanning electron microscopy (FESEM) analysis showed the polycrystalline structure with small particles sizes (<50 nm). Energy dispersive X-ray (EDX) spectroscopy, X-ray fluorescence (XRF), transmission electron microscopy (TEM) and X-ray photoelectron spectroscopy (XPS) analyses confirmed the existence of Al, O, Zn, Cu, Ca and Cr species in each potential catalyst. The optimization of catalyst preparation conditions and biodiesel production parameters were verified by response surface methodology (RSM) method and they were in good agreement with the experimental values. The mechanistic study on both potential catalysts follows the Langmuir-Hinshelwood (LH) model which involves the initial adsorption of reactants molecules on active sites of the catalyst surface. The specification analysis of produced biodiesel utilizing Cu/Zn/γ-Al₂O₃ and Cr/Ca/γ-Al₂O₃ catalysts showed that the refined used cooking oil has potential to be used in large-scale biodiesel production using reaction conditions found in the present study.

ABSTRAK

Kebimbangan alam sekitar dalam kekurangan bahan api fosil telah meningkatkan pencarian bahan bakar alternatif dari sumber yang boleh diperbaharui. Biodiesel biasanya dihasilkan melalui transesterifikasi minyak sayuran dengan kehadiran mangkin homogen. Mangkin ini, walau bagaimanapun, terlarut di dalam minyak sayuran dan sejumlah besar air diperlukan untuk membersihkan biodiesel yang boleh menyebabkan saponifikasi. Sebelum ini, kajian menyeluruh telah dijalankan ke atas oksida logam alkali bumi seperti kalsium dan magnesium oksida dengan mangan, ferum, zirkonium dan serium sebagai dopan. Dengan itu, kajian ini memberi tumpuan kepada penggunaan mangkin bes heterogen yang mudah dipisahkan dan mesra alam untuk penghasilan biodiesel. Mangkin berasaskan zink oksida dan kalsium oksida berpenyokong alumina telah digunakan sebagai mangkin untuk tindak balas transesterifikasi minyak masak terpakai yang ditapis disebabkan oleh ciri kebesannya yang tinggi. Untuk meningkatkan aktiviti pemangkinan, mangkin oksida dwilogam dan trilogam dengan kuprum, nikel, kromium and titanium sebagai ko-mangkinnya telah disiasat. Kesemua mangkin berpenyokong alumina telah disediakan dengan kaedah pengisitepuan basah. Penyaringan penghasilan biodiesel menggunakan mangkin yang disintesis telah dipantau menggunakan kromatografi gas-pengesan pengionan nyala (GC-FID). Dua mangkin yang paling berpotensi telah dipilih bagi kajian pengoptimuman dan pencirian. Mangkin Cu/Zn/γ-Al₂O₃ yang dikalsinkan pada 800°C dengan nisbah dopan terhadap bahan asas 10:90 wt.% dan 3 kali salutan alumina telah menunjukkan penghasilan biodiesel tertinggi (89.50%) pada keadaan tindak balas sederhana (65°C, muatan mangkin 10 wt.%, nisbah mol minyak:metanol 1:20 and 2 jam masa tindak balas). Mangkin Cr/Ca/γ-Al₂O₃ yang dikalsinkan pada 700°C dengan nisbah dopan terhadap bahan asas 10:90 wt.% dan 3 kali salutan alumina memberikan penghasilan biodiesel 86.64% pada 65°C, muatan mangkin 6 wt.%, nisbah mol minyak:metanol 1:18 dan 3 jam masa tindak balas. Sifat fisikokimia mangkin berpotensi tersebut telah dikaji menggunakan analisis nitrogen (NA) dan penyahjerapan pengaturcaraan CO₂ (CO₂-TPD) yang menunjukkan luas permukaan yang tinggi (>140 m²/g) dan kebesan yang tinggi (>3 mmol/g). Pembelauan sinar-X (XRD) dan analisis mikroskopi electron pengimbas pemancaran medan (FESEM) menunjukkan struktur polihablur dengan saiz zarah yang kecil (<50 nm). Analisis spektroskopi serakan tenaga sinar-X (EDX), pendarfluor sinar-X (XRF), mikroskopi elektron penghantaran (TEM) and spektroskopi fotoelektron sinar-X (XPS) mengesahkan kewujudan spesies Al, O, Zn, Cu, Ca dan Cr di dalam setiap mangkin yang berpotensi. Pengoptimuman keadaan persediaan mangkin dan parameter penghasilan biodiesel telah disahkan melalui kaedah permukaan gerak balas (RSM) dan ia menunjukkan persetujuan yang baik dengan nilai eksperimen. Kajian mekanistik ke atas kedua-dua mangkin yang berpotensi adalah mengikuti model Langmuir-Hinshelwood (LH) yang melibatkan penjerapan awal molekul reaktan pada tapak aktif permukaan mangkin. Analisis spesifikasi bagi biodiesel yang dihasilkan menggunakan mangkin Cu/Zn/y-Al₂O₃ and Cr/Ca/y-Al₂O₃ menunjukkan bahawa minyak masak terpakai yang ditapis berpotensi untuk digunakan dalam penghasilan skala besar biodiesel menggunakan keadaan tindak balas yang ditemukan dalam kajian ini.

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LIST OF ABBREVIATIONS AND SYMBOLS

ANOVA - Analysis of Variance

ATR-FTIR - Attenuated Total Reflection-Fourier Transform Infrared

BBD - Box-Behnken Design

BET - Brunauer-Emmet-Teller

CO₂-TPD - Temperature Programmed Desorption

Cu Kα - X-ray diffraction from Copper K energy levels rate of

conversion (percentage)

FAME - Fatty Acid Methyl Ester

FESEM - Field Emission Scanning Electron Microscope

EDX Energy Dispersive X-Ray

FTIR - Fourier Transform Infrared Spectroscopy

GC-FID - Gas Chromatography-Flame Ionization Detector

JCPDS - Joint Committee on Powder Diffraction Standard

NA Nitrogen Adsorption

RSM - Response Surface Methodology

TGA-DTA - Thermogravimetry Analysis-Differential Thermal

Analysis

TEM - Transmission Electron Microscopy

XPS - X-Ray Photoelectron Spectroscopy

XRD - X-Ray Diffraction

XRF - X-Ray Fluorescence

α - Alpha

γ - Gamma

θ - Half angle of diffraction beam

λ - Wavelength

% - Percentage

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CHAPTER 1

INTRODUCTION

1.1 Background of Study

The world was facing an acute energy crisis due to the fact that high energy demand from the fossil fuels such as coal, petroleum and natural gas at present and compete with the feedstocks requirement for chemical industries. The demand of these non-renewable sources of energy which are getting consumed by us at an extraordinary rate is increasing rapidly. Since 1850's, petroleum has been the most main fuel and energy source which is about 90% of vehicular fuels need are met by oil. Petroleum also is becoming as raw material for many chemical products including pharmaceuticals, solvents, fertilizers, pesticides, plastics and others. In any case, there has been increasing concern about an energy crisis caused by potential petroleum depletion since petroleum is non-renewable.

The need for increased energy security and concern about high oil costs drove researchers to seek for renewable and sustainable energy sources to overcome the reliance on petroleum. Besides, the effect of gas emissions from fossil fuels and the environmental is another factor to seek for green and ecologically benign fuels. Emissions of carbon dioxide, CO₂ to the atmosphere from the combustion of fossil fuels have ended up a worldwide concern due to the related climate change, which has unfavorable impacts on human society. In order to overcome this crisis in depending on a fossil fuels, increasing the renewable energy capacity that can reduces greenhouse gases emissions is very important. As stated by Anuar and Abdullah, (2016), the renewable energy should ensure a cleaner environment that can

reduce the impact of any future energy crisis on fossil fuel-constrained economies. Attention continues to be focused on biomass-derived fuels or known as biofuels for energy production. One of the liquid biofuels considered for this application is biodiesel.

1.2 Biodiesel

Biodiesel has become the world's attention as one of a very promising alternative energy as a substitute for fossil diesels because it has similar properties to fossil diesels. Biodiesel is the most commonly used liquid biofuels in the transport sector, representing about 82% of biofuels production in European Union (Mardhiah *et al.*, 2017). The advantages of the biodiesel compared with the conventional fossil diesels are their renewability, biodegradability, non-toxicity and low exhaust emissions due to the free of sulphur and aromatics in biodiesel (Hassan and Rahman, 2017). In this 21st century, biodiesel has experienced a major surge worldwide due to these advantages. Figure 1.1 shows the global biodiesel production from 2000 to 2016 in 1000 metric tons of oil equivalent. Meanwhile, Figure 1.2 illustrates Malaysia biodiesel production and consumption by year. From this statistic in 2016, biodiesel production amounted to approximately 82 billion metric tons of oil equivalent worldwide.

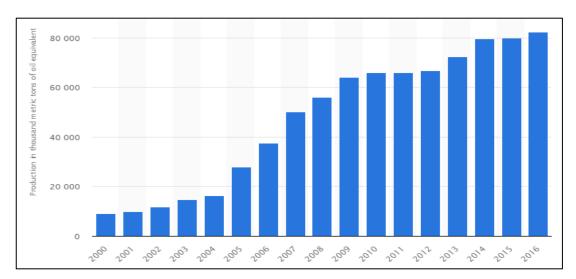


Figure 1.1 Global biodiesel production from 2000 to 2016 in 1000 metric tons of oil equivalent from The Statistics Portal (Hajjari *et al.*, 2017)

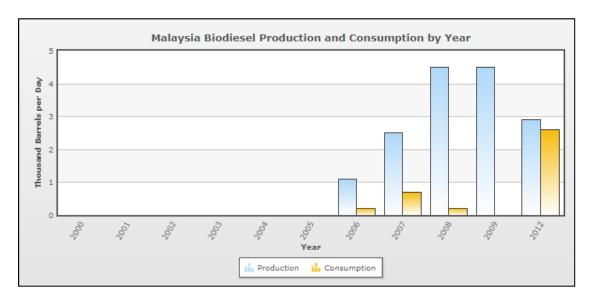


Figure 1.2 Malaysia biodiesel production and consumption by year from United States Energy Information Administration (Mahmudul *et al.*, 2017)

The name of biodiesel (bio-means life (Greek) and diesel from Rudolf diesel/petro-diesel) has been given from transesterification of vegetable oil that use as a diesel fuel and renewable nature. Technically, the term "biodiesel" refers to mixtures of fatty acid alkyl esters (FAAE) produced by transesterification of vegetable oils or animal fats with alcohols or via esterification of free fatty acids (FFA) with alcohols. Transesterification is a process where triglyceride reacts with an alcohol such as methanol to give methyl ester of fatty acids (FAME) and glycerol. The overall transesterification reaction is presented by the stoichiometric equation shown in Figure 1.3.

$$\begin{array}{c} H_2C \\ HC \\ HC \\ O \\ H_2C \\ O \\ H_2C \\ O \\ R_2 + 3 \\ CH_3 \\ OH \\ R_3 \\ R_1, R_2, R_3 = Alkyl \\ Group \\ \hline \\ \textbf{Triglycerides} \\ \textbf{Methanol} \\ \end{array}$$

Figure 1.3 Generalized schematic representation of transesterification reaction

Biodiesel can be produced from variety of feedstocks including soybean, cottonseed, palm, peanut, rapeseed, sunflower and rice bran from vegetable oils with tallow, chicken fat and fish oils from animal fats as well as waste cooking oil and grease. Biodiesel is commonly used in conventional compression-ignition engines without any modifications, either in pure form or blended with petro-diesel. According to Knothe and Razon, (2017), the similarity in fuel properties between biodiesel and petro-diesel was the reason of the direct application of biodiesel in diesel engines. Table 1.1 listed the fuel properties of biodiesel compared to petro-diesel. Based on Table 1.1, biodiesel possess viscosity much closer to the petro-diesel and it has higher flash point, higher lubricity and smaller carbon footprint (Agarwal *et al.*, 2017). Therefore, this research had focused on producing biodiesel with similar fuel properties as petro-diesel via transesterification of refined used cooking oil.

Table 1.1: The American Society for Testing Materials (ASTM) standards for petro-diesel and biodiesel fuel properties

Fuel properties specification	Petro-diesel	Biodiesel
Standard	ASTM D975	ASTM D6751
Composition	HC (C10-C21)	FAME (C12-C22)
Kinematic viscosity @ 40°C (mm²/s)	1.9-4.1	1.9-6.0
Specific gravity (g/mL)	0.85	0.88
Flash point (°C)	60 to 180	100 to 190
Cloud point (°C)	-15 to 5	-3 to 12
Pour point (°C)	-35 to -15	-15 to 16
Water content, vol.%	0.05	0.05
Carbon content, wt.%	87	77
Hydrogen content, wt.%	13	12
Oxygen content, wt.%	0	11
Sulphur content, wt.%	0.05	0.05
Cetane number	40 to 55	48 to 60

1.3 Catalysis in Biodiesel Production

Catalysis plays an important role in numerous industrial processes which incorporates food production, energy production, chemical production and environmental protection. Basically, the catalyst is needed in any of the reaction in order to increase the rate performance of the process. In this transesterification reaction, both acid and base catalysts can be used to enhance the biodiesel production. Lately, much research has been reported relating to the development of heterogeneous catalysts for transesterification of various vegetable oils with methanol (Baskar and Aiswarya, 2016; Verma and Sharma, 2016).

Many researchers have pointed out the drawback related with the use of homogeneous catalysts in biodiesel production (Pukale *et al.*, 2015; Abdullah *et al.*, 2017). Conventional biodiesel production had used base-catalyzed homogeneous reaction such as sodium hydroxide and potassium hydroxide and the process are illustrated in Figure 1.4. This requires various operating procedures in order to recover the catalyst for further use. The large amount of water and energy was needed for washing and drying the biodiesel product, thus it will form soap as unwanted by-product.

Therefore, there is currently a shift toward the development of industrial processes for biodiesel production using solid catalysts. The major benefit of using heterogeneous catalysts is that no polluting by-products are formed and the catalysts do not mix with biodiesel. Furthermore, the heterogeneous catalyst would reduce the extra operating costs from the catalyst neutralization, product washing and continual replacement of catalyst, thus producing higher purity of biodiesel. There is no requirement for catalyst neutralization since the solid catalyst could easily be removed from the reaction mixture by simple filtration. Figure 1.5 represents a typical heterogeneously base-catalyzed biodiesel process. Meanwhile, Table 1.2 depicts the comparison of homogeneous and heterogeneous catalyzed transesterification reaction.

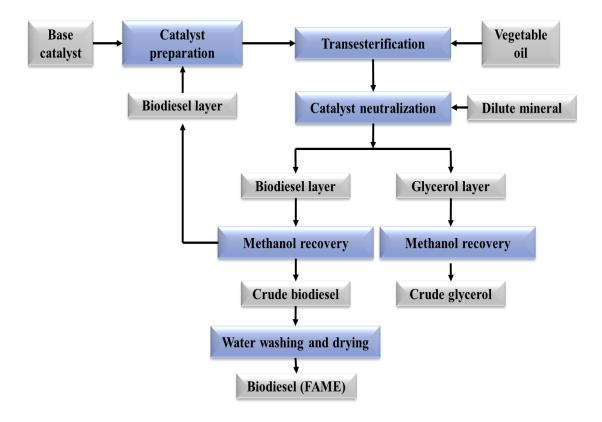


Figure 1.4 A typical homogeneous base-catalyzed biodiesel process

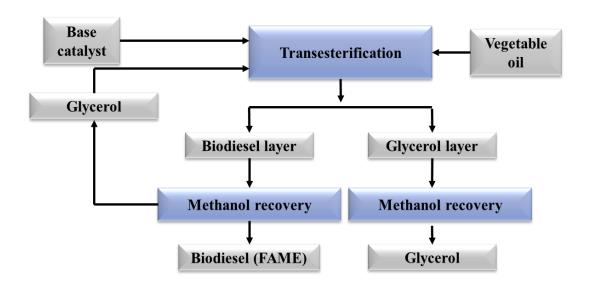


Figure 1.5 A typical heterogeneous base-catalyzed biodiesel process

Table 1.2: Comparison of homogeneous and heterogeneously catalyzed transesterification

Factors	Homogeneously	Heterogeneously
	catalysis	catalysis
Reaction rate	Fast and high conversion	Fast and high conversion
After treatment	Catalyst cannot be	Can be recovered
	recovered, must be	
	neutralized	
Processing methodology	Limited use of continuous	Continuous fixed
	methodology	operation is possible
Presence of water/ free	Sensitive	Not sensitive
fatty acids		
Catalyst reuse	Not possible	Possible
Cost	Comparatively costly	Potentially cheaper

Physicochemical properties of solid base catalyst are dependent on their preparation methods, pretreatment process and the way of handling the catalyst itself. There are numbers of preparation methods for producing solid base catalyst such as co-precipitation method (Lee *et al.*, 2015), hydration dehydration method (Mijan *et al.*, 2015), sol gel (Mohadesi *et al.*, 2014) and chemical vapor deposition (CVD) methods (You *et al.*, 2017). Physicochemical properties such as morphology, surface area, particle size and basicity normally could influence the catalytic activity. The importance of solid base catalysts has come to be known for their environmental friendly qualities. Much significant progress has been made over the past two decades in catalytic materials and solid base-catalyzed reactions (Hattori, 2001).

Typically, metal oxides are identified as the most significant and extensively used as catalyst. As described by Hattori, (2015), metal oxides had both proton and electron transfer abilities, thus can be used in redox catalysis as well as acid-base reactions. A strong basic strength can be formed after a high temperature treatment applied in order to obtain a carbonate free metal oxide surface. Surface defect which can be detected using surface area analysis display the significant sites for

heterogeneous catalysis that can change the reactivity of any reaction (Aransiola *et al.*, 2014). Hence, the higher the surface area indicates higher reactivity.

Alkaline earth metal oxides such as calcium oxide, CaO possess a rock-salt structure with alternating metal cations and oxygen anions. An alkaline earth metal oxide exposing more of electron rich planes, thus give a greater number of defect sites (Marinković *et al.*, 2016). From alkaline earth metal oxide group, CaO has been widely used as a catalyst in the transesterification reaction due to its high basicity, low solubility in organic solvents and low price. On the other hand, zinc oxide, ZnO is a cheap, re-usable, stable and environmentally catalyst that used in many catalytic reactions. Nanoparticles of ZnO comprises a good optical, electrical and chemical properties. Furthermore, ZnO is one of the most extensively studied materials due to its outstanding optoelectronic properties with potential applications in many different fields of technology (Downs *et al.*, 2017). ZnO is generally used as catalyst support and it has been established that impregnation with alkaline metals gives a good basic solid catalyst for the transesterification of vegetable oils (Alba-Rubio *et al.*, 2010).

Despite of high catalytic activity by using single metal oxides catalyst in biodiesel production, the addition of dopants offers a route to achieve better performance due to the increased surface basic properties. There is a demand to develop desirable solid base catalysts from mixed metal oxide with a high activity. The important use of transition metals as co-catalysts are the ability to be in a variety of oxidation state, interchange between the oxidation states and formation of complexes with the reagents. The availability and lower costs are additional factors for the consideration.

Supporting metal oxides on high surface area materials is another alternative of increasing their stability as catalysts and reducing the cost in preparing the catalysts. The high surface area of supported material allows good dispersion of the catalytically active metal and easily recovered after the reaction (Matsubu *et al.*, 2017). Furthermore, supports are a good way of minimizing in mass transfer limitations for heterogeneous catalysts in liquid phase reaction by providing greater

accessibility through the existence of pores. Gamma aluminium oxide (γ -Al₂O₃) has been widely used as a support of active species in industrial processes due to its high thermal stability and surface area of 300 m²/g, mesopore size of 5 to 15 nm, pore volume of 0.60 cm³/g and ability to be shaped into pallets (Evangelista *et al.*, 2016).

Therefore, in this study, the modification with more active substance in order to prepare a base heterogeneous catalyst was introduced in biodiesel production due to the simplifications in the existing process. To the best of our knowledge, the utilization of wetness impregnation method to synthesize zinc and calcium oxides based catalyst with addition of transition metals (Cr, Ti, Ni, Cu) as co-catalysts in alumina supported for the transesterification of biodiesel has not been revealed yet.

1.4 Response Surface Methodology (RSM)

RSM is a collection of mathematical and statistical techniques based on the fit of a polynomial equation to the experimental data. It describes the behavior of a data set with the objective of making statistical previsions. RSM can be applied when a response of interest is influenced by several independent variables. The main objective of RSM application is to optimize the levels of independent variables in order to achieve the best system performance.

Toward this objective, linear or square polynomial function is employed to describe the experimental design and thus, explored the modeling for the optimization. The stages in the application of RSM as an optimization technique are as follows: (1) the selection of the independent variables from the screening studied; (2) the choice of the experimental design and carrying out according to the experimental matrix; (3) the mathematic-statistical analysis through the fit of a polynomial function; (4) the evaluation of the model's fitness; (5) the verification of the predicted value from experimental design and (6) the determination of the optimum values for each variable.

RSM has been successfully applied in the study on optimization of biodiesel production from rapeseed oil, soybean oil, cotton seed oil and other vegetable oils (Silva *et al.*, 2011; Dwivedi and Sharma, 2015; Kostić *et al.*, 2016; Onukwuli *et al.*, 2017; Baskar *et al.*, 2018). However, there is no literature reported on the optimization of the transesterification reaction from refined used cooking oil over potential catalyst in this research. Therefore, RSM modelling coupled with Box-Behnken design was used to determine the optimum catalyst conditions and biodiesel production parameters that could lead to the maximum biodiesel yield.

1.5 Mechanistic Study

In heterogeneous catalysis, adsorption of reactants and desorption of products take place on the surface of a solid catalyst. Two hypotheses have been proposed for solid acid catalyzed transesterification reaction mechanisms which are Eley–Rideal (ER) and Langmuir-Hinshelwood (LH), represent the foundation of modern heterogeneous transesterification mechanisms. According to the ER mechanism, it is performed by a direct pickup of species from the surface by a liquid phase molecule. Meanwhile, in the LH mechanism, there are three main steps that occurred on the catalyst surface which are adsorption of reactants, surface reaction and desorption of products. Therefore, this present study might provide an understanding on the mechanism of heterogeneous base-catalyzed transesterification reaction.

1.6 Problem Statement

Concerns about greenhouse gas emissions, global warming and limitation of crude oil resources have encouraged researchers to develop an alternative fuel. The depleting fossil oil reserves give big influence in the interest in finding alternative source of energy. In order to overcome those problems and to further enhance the awareness of the environment, the biomass has become the global attention as one of a great promising substitute and sustainable energy. Biodiesel derived from

renewable resources such as vegetable oil or animal fats is expected to be one of the biomass-base alternative fuel to substitute the diesel oil.

Conventional biodiesel production is commercially synthesized in the presence of homogeneous base catalysts mainly alkali-metal hydroxides and methoxides (NaOH, KOH and NaOCH₃) as reported by Konwar *et al.*, (2014). However, it should be noted that this conventional process has several drawbacks. This requires various operating and capital costs downstream arising from the inability to recover the catalyst. Particularly, these catalysts are sensitive to the presence of water and free fatty acid (FFA). Homogeneous base catalyst dissolved into the vegetable oil or animal fat. Thus, large amount of water is required for washing purpose. On the other hand, the presence of water leads to the soap formation. As a result, the saponification could lower the biodiesel quality and makes the biodiesel production becomes difficult, time consuming, expensive and complicated.

Moreover, the acid-catalyzed transesterification process typically uses hydrochloric acid and phosphoric acid as catalysts. However, the reaction process needed longer time, higher oil to methanol ratio, higher reaction temperature and pressure (Veljković et al., 2015; Melero et al., 2015). As the acid catalysts are more corrosive, it is not preferable due to the large operation costs in industrial process. Furthermore, several solid base catalysts have been investigated transesterification including alkaline earth oxides, alkaline earth metal oxides, rare earth oxides, basic zeolite, hydrotalcites and organic base catalysts (Hattori, 2015). Despite showing higher activity than acid catalysts, solid base catalyst was unfavorable for feedstock containing high free fatty acids. These catalysts deactivate faster in the presence of air and moisture, thus free fatty acids would react with the catalyst forming soap. Therefore, in this study, base heterogeneous catalytic reaction was introduced in biodiesel production under mild reaction conditions. The process of heterogeneous base-catalyzed transesterification is expected to be effective as it can reduce the extra operating costs and gives minimal impact into the environment.

This research work focused on the mixed metal oxides catalyst with the incorporation of transition metal as co-catalysts supported on alumina for the transesterification in biodiesel production. The supported catalyst can be used in direct applications for the automotive and petroleum industries due to its stability and reusability (Wefers, 1990; Zabeti *et al.*, 2009). The advantage of this mixed metal oxides can be traced to a favorable combination of its textural properties such as surface area, pore size distribution, pore volume and its base characteristics which are related to surface chemical composition and phase composition (Teo *et al.*, 2014; Joshi *et al.*, 2015). The use of mixed metal oxides would reduce the leaching properties and the reaction time in the biodiesel production as proved by Wong *et al.*, (2015).

Previous studies by Wang *et al.*, (2007) and Patil *et al.*, (2010) reported a two-step catalytic transesterification of biodiesel process. However, the two-step method faces the problem in catalyst removal and time consuming, thus would increase the cost of biodiesel production. In order to overcome this situation, single step transesterification reaction using heterogeneous mixed metal oxides catalyst was introduced. In addition, another factor that affect the cost of biodiesel production is based on the raw materials that used as a feedstock. Most of the biodiesel is widely produced from the costly edible oils like soybean oil, sunflower oil, rapeseed oil and rice bran oil (Baskar and Aiswarya, 2016; Arora *et al.*, 2014; Anuar and Abdullah, 2016). However, the application of such feedstocks in biodiesel production could maximize competition between demand of vegetable oils with human consumption. This research had introduced refined used cooking oil as an alternative feedstock which has not been investigated.

1.7 Aim and Objectives of Study

The main aim of this research is to develop the most effective catalyst in the transesterification of refined used cooking oil to biodiesel under mild conditions. Thus, the objectives of this research are:

- To synthesize zinc and calcium oxides-based catalysts supported on alumina with different series of dopants.
- ii) To test and measure the catalytic activity of the prepared catalysts in the transesterification of refined used cooking oil by using gas chromatography-flame ionization detector (GC-FID).
- iii) To characterize the potential prepared catalysts using various analytical technique in order to understand the physicochemical properties of the catalysts.
- iv) To optimize the catalyst preparation parameters and biodiesel production conditions using response surface methodology (RSM)-Box-Behnken design (BBD).
- v) To postulate the mechanism over potential catalysts.
- vi) To verify the fuel properties of synthesized biodiesel according to ASTM D6751 and EN14214 standards.

1.8 Scope of Study

This research was emphasized on base-catalyzed transesterification of biodiesel from refined used cooking oil by using alumina supported zinc (Zn) and calcium (Ca) with addition of nickel (Ni), copper (Cu), titanium (Ti) and chromium (Cr) as co-catalysts. Three types of catalysts including monometallic, bimetallic and trimetallic oxides catalysts were synthesized via wetness impregnation method. Then, the catalytic activity of the prepared catalysts was tested and monitored by using gas chromatography (GC-FID). From the screening stages, the both potential catalysts from each based were optimized on different calcination temperatures, dopant ratios to based and number of alumina coatings and further validated by response surface methodology (RSM) via Box-Behnken design (BBD).

Next, the both potential catalysts were characterized in order to explore its physicochemical properties. The surface characteristics of the prepared catalysts were analyzed using nitrogen adsorption (NA). X-Ray diffraction (XRD) was used

to determine the degree of crystallinity, particle shape and sizes for the prepared catalysts. X-ray photoelectron spectroscopy (XPS), energy dispersive X-ray (EDX), X-ray Fluorescence (XRF) and transmission electron microcopy (TEM) were used to study the chemical state and the elemental composition of the catalysts. The surface morphology was examined using field emission scanning electron microscopy (FESEM), while CO₂-TPD was used to measure the basicity and basic site distributions of the catalysts. Thermogravimetric analysis—differential thermal analysis (TGA-DTA) was conducted to study the weight loss of the catalyst with change of temperature.

From the characterization analysis, the both potential catalysts were further investigated in the optimization of biodiesel parameters including percentage catalyst loadings, oil to methanol ratios and reaction times and verified by RSM. The both potential catalysts were also studied on reusability and reliability testing as well as regeneration activity under optimum conditions. The mechanistic study of transesterification reaction on the catalyst surface was conducted via attenuated total reflection-Fourier transform infrared (ATR-FTIR) and the product was analyzed using GC-FID. Lastly, the verification of fuel properties on product was examined according to ASTM D6751 and EN14214 standards.

1.9 Significance of Study

The harmful effect of global warming, depletion of fossil fuel resources and the rising numbers of environmental related problems had become the main factors that contribute to the global transformation in the development of biodiesel. The used of biodiesel as a source of fuel offers several advantages including renewable and sustainable resources, non-toxic and environmental friendly where it reduces the emission of CO₂ and hazardous compound such as aromatic, sulfur, particulate matter and NO_x. Hence, the use of biodiesel will significantly reduce the effect of global warming and utilizes a green chemistry concept. Generally, biodiesel displays good oil qualities with higher cetane number and higher combustion efficiency. In addition, no sulfur content in biodiesel provides greater lubricity than conventional

diesel fuel, thus improves the durability of the engine. The advantage of biodiesel production from this study is easily to operate because it only required to process at low temperature in order to give optimum performance.

In addition, the application of a heterogeneous or solid catalyst has gained interest in the biodiesel production. The catalysts are not dissolved in the reaction mixture which made it easier to be separated from the product. On top of that, the base heterogeneous catalyst has several advantages including reusability, easier operational procedures, effortless catalyst separation and reduction of environmental pollutions. All the materials in the fabrication of the catalyst are cheap, stable and easily available. The catalysts are safe to handle because it can be used at low reaction temperature.

Accordingly, the novelties of this research study are as follows:

- 1. The development of highly basic metal oxide catalysts from alkaline earth metal (Ca) and transition metal (Zn) as based catalysts with the use of alumina beads as a support in order to increase the stability of the catalyst. The addition of second and third metal as co-catalysts were carried out in order to increase the performance on transesterification for biodiesel production.
- 2. The invention of a simple method that only required low temperature for the biodiesel production from refined used cooking oil.
- 3. The optimization on the catalyst preparation conditions and biodiesel production parameters over two potential catalysts by using response surface methodology (RSM) via Box-Behnken design (BBD).
- 4. The mechanistic study on the catalyst surface of triglyceride model substitution using attenuated total reflection-Fourier transform infrared (ATR-FTIR).

REFERENCES

- Abbas, A.S. and Rowaida, N.A. (2013). Kinetic study and simulation of oleic acid esterification over prepared NaY zeolite catalyst. *Iraqi Journal of Chemical and Petroleum Engineering*. 14(4): 35-43.
- Abd-Elkader, O. and Deraz, N.M. (2013). Synthesis and characterization of new copper based nanocomposite. *International Journal of Electrochemical Science*. 8: 8614-8622.
- Abdullah, S.H.Y.S, Hanapi, N.H.M., Azid, A., Umar, R., Juahir, H., Khatoon, H. and Endut, A. (2017). A review of biomass-derived heterogeneous catalyst for a sustainable biodiesel production. *Renewable and Sustainable Energy Reviews*. 70: 1040-1051.
- Agarwal, A.K., Gupta, J.G. and Dhar, A. (2017). Potential and challenges for large-scale application of biodiesel in automotive sector. *Progress in Energy and Combustion Science*. 61: 113-149.
- Alba-Rubio, A.C., Santamaría-González, J., Mèrida-Robles, J.M., Moreno-Tost, R., Martín Alonso, D., Jimènez-López, A. and Maireles-Torres, P. (2010). Heterogeneous transesterification processes by using CaO supported on zinc oxide as basic catalysts. *Catalysis Today*. 149: 281-287.
- Albuquerque, M.C.G., Azevedo, D.C.S., Cavalcante Jr., C.L., Santamaría-González, J., Mérida-Robles, J.M., Moreno-Tost, R., Rodríguez-Castellón, E., Jiménez-López, A. and Maireles-Torres, P. (2009). Transesterification of ethyl butyrate with methanol using MgO/CaO catalysts. *Journal of Molecular Catalysis A: Chemical.* 300: 19-24.
- Al-Gaashani, R., Radiman, S., Daud, A.R., Tabet, N. and Al-Douri, Y. (2013). XPS and optical studies of different morphologies of ZnO nanostructures prepared by microwave methods. *Ceramics International*. 39: 2283-2292.
- Al-Jaberi, S.H.H., Rashid, U., Al-Doghachi, F.A.J., Abdulkareem-Alsultan, G. and Yap, Y.H.T. (2017). Synthesis of MnO-NiO- SO₄²⁻/ZrO₂ solid acid catalyst

- for methyl ester production from palm fatty acid distillate. *Energy Conversion and Management*. 139: 166-174.
- Alves, C.T., Oliveira, A.S., Carneiro, S.A.V., Santos, R.C.D., Melo, S.A.B.V., Andrade, H.M.C., Marques, F.C. and Torres, E.A. (2012). Transesterification of waste frying oils using ZnAl₂O₄ as heterogeneous catalyst. *Procedia Engineering*. 42: 1928-1945.
- Anuar, M.R. and Abdullah, A.Z. (2016). Challenges in biodiesel industry with regards to feedstock, environmental, social and sustainability issues: A critical review. *Renewable and Sustainable Energy Reviews*. 58: 208-223.
- Aransiola, E.F., Ojumu, T.V., Oyekola, O.O., Madzimbamuto, T.F., Omoregbe, D.I.O.I. (2014). A review of current technology for biodiesel production: State of the art. *Biomass and Bioenergy*. 61: 276-297.
- Aronniemi, M., Sainio, J. and Lahtinen, J. (2005). Chemical state quantification of iron and chromium oxides using XPS: the effect of the background subtraction method. *Surface Science*. 578: 108-123.
- Arora, A.K., Sunil, R.M.P., Mandal, T., Christopher, J., Puri, S.K. and Gupta, A.A. (2014). An effective heterogeneous catalyst from waste material for the biodiesel production. *Journal of Surface Science and Technology*. 30(1): 45-58.
- Arumugam, A. and Ponnusami, V. (2014). Biodiesel production from *Calophyllum inophyllum* oil using lipase producing *Rhizopus oryzae* cells immobilized within reticulated foams. *Renewable Energy*. 64: 276-282.
- Ashraful, A.M., Masjuki, H.H., Kalam, M.A., Fattah, I.M.R., Imtenan, S., Shahir, S.A. and Mobarak, H.M. (2014). Production and comparison of fuel properties, engine performance, and emission characteristics of biodiesel from various non-edible vegetable oils: A review. *Energy Conversion and Management*. 80: 202-228.
- Asri, N.P., Savitri, S.D., Suprapto, Budikarjono, K. and Roesyadi, A. (2012). Development of heterogeneous alumina supported base catalyst for biodiesel production. *International Proceedings of Chemical, Biological and Environmental Engineering*. 46: 116-121.
- Avhad, M.R. and Marchetti, J.M. (2015). A review on recent advancement in catalytic materials for biodiesel production. *Renewable and Sustainable Energy Reviews*. 50: 696-718.

- Ayetor, G.K., Sunnu, A. and Parbey, J. (2015). Effect of biodiesel production parameters on viscosity and yield of methyl esters: *Jatropha curcas, Elaeis guineensis and Cocos nucifera*. *Alexandria Engineering Journal*. 54: 1285-1290.
- Aziz, H.A., Aroua, M.K., Yusoff, R., Abas, N.A. and Idris, Z. (2017). Optimization of transesterification of palm-based methyl palmitate and triethanolamine towards maximum di-esteramine content. *Biocatalysis and Agricultural Biotechnology*. 10: 352-359.
- Bakar, W.A.W.A., Ali, R. and Toemen, S. (2012). Catalytic methanation reaction over supported nickel–ruthenium oxide base for purification of simulated natural gas. *Science Iran.* 19: 525-345.
- Bancquart, S., Vanhove, C., Pouilloux, Y. and Barrauult, J. (2001). Glycerol transesterification with methyl stearate over solid basic catalysts relationship between activity and basicity. *Applied Catalysis A: General.* 218: 1-11.
- Baskar, G. and Aiswarya, R. (2016). Trends in catalytic production of biodiesel from various feedstocks. *Renewable and Sustainable Energy Reviews*. 57: 496-504.
- Baskar, G. and Soumiya, S. (2016). Production of biodiesel from castor oil using iron (II) doped zinc oxide nanocatalyst. *Renewable Energy*. 98: 101-107.
- Baskar, G., Gurugulladevi, A., Nishanthini, T, Aiswarya, R. and Tamilarasan, K. (2017). Optimization and kinetics of biodiesel production from Mahua oil using manganese doped zinc oxide nanocatalyst. *Renewable Energy*. 103: 641-646.
- Baskar, G., Selvakumari, A.E. and Aiswarya, R. (2018). Biodiesel production from castor oil using heterogeneous Ni doped ZnO nanocatalyst. *Bioresource Technology*. 250: 793-798.
- Bazant, P., Kuritka, I., Munster, L. and Kalina, L. (2015). Microwave solvothermal decoration of the cellulose surface by nanostructured hybrid Ag/ZnO particles: a joint XPS, XRD and SEM study. *Cellulose*. 22: 1275-1293.
- Bazargan, A., Kostić, M.D., Stamenković, O.S., Velijković, V.B. and McKay, G. (2015). A calcium oxide-based catalyst derived from palm kernel shell gasification residues for biodiesel production. *Fuel.* 519-525.
- Benjapornkulaphong, S., Ngamcharussrivichai, C. and Bunyakiat, K. (2009). Al₂O₃-supported alkali and alkali earth metal oxides for transesterification of palm kernel oil and coconut oil. *Chemical Engineering Journal*. 145: 468-474.

- Bertagnolli, C., Uhart, A., Dupin, J.C., Silva, M.G.C., Guibal, E. and Desbrieres, J. (2014). Biosorption of chromium by alginate extraction products from *Sargassum filipendula*: Investigation of adsorption mechanisms using X-ray photoelectron spectroscopy analysis. *Bioresource Technology*. 164: 264-269.
- Bet-Moushoul, E., Farhadi, K., Mansourpanah, Y., Nikbakht, A.M., Molaei, R. and Forough, M. (2016). Application of CaO-based/Au nanoparticles as heterogeneous nanocatalysts in biodiesel production. *Fuel.* 164: 119-127.
- Biesinger, M.C., Payne, B.P., Grosvenor, A.P., Lau, L.W.M., Gerson, A.R. and Smart, R.S.C. (2011). Resolving surface chemical states in XPS analysis of first row transition metals, oxides and hydroxides: Cr, Mn, Fe, Co and Ni. *Applied Surface Science*. 257: 2717-2730.
- Boubakri, A., Hafiane, A. and Bouguecha, S.A.T. (2013). Application of response surface methodology for modeling and 3 optimization of membrane distillation desalination process. *Journal of Industrial and Engineering Chemistry*. 20: 3163-3169.
- Boz, N. and Kara, M. (2009). Solid base catalyzed transesterification of canola oil. *Chemical Engineering Communications*. 196(1): 80-92.
- Brito, A., Borges, M.E. and Otero, N. (2007). Zeolite Y as a heterogeneous catalyst in biodiesel fuel production from used vegetable oil. *Energy & Fuels*. 21: 3280-3283.
- Cannilla, C., Bonura, G., Rombi, E., Arena, F. and Frusteri, F. (2010). Highly effective MnCeOx catalysts for biodiesel production by transesterification of vegetable oils with methanol. *Applied Catalysis A: General*. 382: 158-166.
- Cao, F., Chen, Y., Zhai, F., Li, J., Wang, J., Wang, X., Wang, S. and Zhu, W. (2008). Biodiesel production from high acid value waste frying oil catalyzed by superacid heteropolyacid. *Biotechnology and Bioengineering*. 101(1): 93-100.
- Carabineiro, S. A. C., Silva, A. M. T., Drazic, G., Tavares, P. B. and Figueiredo. (2010). Effect of chloride on the sinterization of Au/CeO₂ catalysts. *Catalysis Today*. 154 (3-4): 293-302.
- Cheirslip, B. and Louhasakul, Y. (2013). Industrial wastes as a promising renewable source for production of microbial lipid and direct transesterification of the lipid into biodiesel. *Bioresource Technology*. 142: 329-337.

- Chen, C.L., Huang, C.C., Tran, D.T. and Chang, J.S. (2012). Biodiesel synthesis via heterogeneous catalysis using modified strontium oxides as the catalysts. *Bioresource Technology*. 113: 8-13.
- Chen, M., Wang, X., Yu, Y.H., Pei, Z.L., Bai, X.D., Sun, C., Huang, R.F. and Wen, L.S. (2000). X-ray photoelectron spectroscopy and auger electron spectroscopy studies of Al-doped ZnO films. *Applied Surface Science*. 158: 134-140.
- Contreras, J.L., Fuentes, G.A., Zeifert, B. and Salmones, J. (2009). Stabilization of supported platinum nanoparticles on γ-alumina catalysts by addition of tungsten. *Journal of Alloys and Compounds*. 483: 371-373.
- Correia, L.M., Saboya, R.M.A., Campelo, N.S., Cecilia, J.A., Rodriguez-Castellon, E., Cavalcante Jr, C.L. and Vieira, R.S. (2014). Characterization of calcium oxide catalysts from natural sources and their application in the transesterification of sunflower oil. *Bioresource Technology*. 151: 207-213.
- Correia, L.M., Sousa Campelo, N., Novaes, D.S., Cavalcante Jr., C.L., Cecilia, J.A., Rodríguez-Castellón, E. and Vieira, R.S. (2015). Characterization and application of dolomite as catalytic precursor for canola and sunflower oils for biodiesel production. *Chemical Engineering Journal*. 269: 35-43.
- Crist, B.V. (2005). Commercially pure binary oxides and a few common carbonates and hydroxides. *Handbooks of Monochromatic XPS Spectra*. 2: 43-66.
- D'Cruz, A., Mangesh, G., Kulkarni, L.C.M. and Ajay, K.D. (2007). Synthesis of biodiesel from canola oil using heterogeneous base catalyst. *Journal of the American Oil Chemists' Society*. 84(10): 937-943.
- Dai, Y.M., Wu, J.S., Chen, C.C. and Chen, K.T. (2015). Evaluating the optimum operating parameters on transesterification reaction for biodiesel production over a LiAlO₂ catalyst. *Chemical Engineering Journal*. 280: 370-376.
- Dalibor, M.M., Stanković, M.V., Veličković, A.V., Avramović, J.M., Cakić, M.D. and Veljković, V.B. (2015). The synthesis of CaO loaded onto Al₂O₃ from calcium acetate and its application in transesterification of the sunflower oil. *Advanced Technologies*. 4(1): 26-32.
- Das, J., Pradhan, S.K., Sahu, D.R., Mishra, D.K., Sarangi, S.N., Nayak, B.B., Verma, S. and Roul, B.K. (2010). Micro-Raman and XPS studies of pure ZnO ceramics. *Physica B*. 405: 2492-2497.

- Dawood, S., Ahmad, M., Ullah, K., Zafar, M. and Khan, K. (2018). Synthesis and characterization of methyl esters from non-edible plant species yellow oleander oil, using magnesium oxide (MgO) nano-catalyst. *Materials Research Bulletin*. 101: 371-379.
- Degirmenbasi, N., Coskun, S., Boz, N. and Kalyon, D.M. (2015). Biodiesel synthesis from canola oil via heterogeneous catalysis using functionalized CaO nanoparticles. *Fuel.* 153: 620-627.
- Delfort, B., Pennec, D.L. and Lendresse, C. (2006). Process for transesterification of vegetable oils or animal oils by means of heterogeneous catalysts based on zinc orbismuth, titanium and alumnium. *United States Patent*. US 7,151,187 B2.
- Dharma, S., Masjuki, H.H., Ong, H.C., Sebayang, A.H., Silitonga, A.S., Kusumo, F. and Mahlia, T.M.I. (2016). Optimization of biodiesel production process for mixed *Jatropha curcas–Ceiba pentandra* biodiesel using response surface methodology. *Energy Conversion and Management*. 115: 178-190.
- Dhawane, S.H., Bora, A.P., Kumar, T. and Halder, G. (2017). Parametric optimization of biodiesel synthesis from rubber seed oil using iron doped carbon catalyst by Taguchi approach. *Renewable Energy*. 105: 616-624.
- Djebaili, K., Mekhalif, Z., Boumaza, A. and Djelloul, A. (2015). XPS, FTIR, EDX, and XRD analysis of Al₂O₃ scales grown on PM2000 alloy. *Journal of Spectroscopy*. 15: 1-16.
- Do, S.H., Jo, Y.H., Park, J.Y. and Hong, S.H. (2014). As³⁺ removal by Ca–Mn–Fe₃O₄ with and without H₂O₂: Effects of calcium oxide in Ca–Mn–Fe₃O₄. *Journal of Hazardous Materials*. 280: 322-330.
- Downs, E.E., Ao, S.S., Siegel, R.W. and Schadler, L.S. (2017). Transition metal doping of amorphous silica particles. *Journal of Nanoparticles Research*. 19: 337-341.
- Dwivedi, G. and Sharma, M.P. (2015). Application of Box–Behnken design in optimization of biodiesel yield from *Pongamia* oil and its stability analysis. *Fuel*. 145: 256-262.
- Embong, N.H., Maniam, G.P., Rahim, M.H.A., Lee, K.T. and Huisingh, D. (2016). Utilization of palm fatty acid distillate in methyl esters preparation using SO₄²⁻/TiO₂-SiO₂ as a solid acid catalyst. *Journal of Cleaner Production*. 116: 244-248.

- Evangelista, J.P.C, Gondim, A.D., Souza, L.D. and Araujo, A.S. (2016). Alumina-supported potassium compounds as heterogeneous catalysts for biodiesel production: A review. *Renewable and Sustainable Energy Reviews*. 59: 887-894.
- Ezebor, F., Khairuddean, M., Abdullah, A.Z. and Boey, P.L. (2014). Oil palm trunk and sugarcane baggase derived solid acid catalysts for rapid esterification of fatty acids and moisture-assisted transesterification of oils under pseudo-infinite methanol. *Bioresource Technology*. 157: 254-262.
- Fang, D., Zhao, J., Liu, S., Zhang, L., Ren, W. and Zhang, H. (2015). Relationship between Cr-Al interaction and the performance of Cr-Al₂O₃ catalysts for isobutane dehydrogenation. *Modern Research in Catalysis*. 4: 50-58.
- Farooq, M., Ramli, A. and Naeem, A. (2015). Biodiesel production from low FFA waste cooking oil using heterogeneous catalyst derived from chicken bones. *Renewable Energy*. 76: 362-368.
- Fu, B.S., Gao, L., Niu, L., Wei, R. and Xiao, G. (2009). Biodiesel from waste cooking oil via heterogeneous superacid catalyst SO₄²-/ZrO₂. *Energy & Fuels*. 23: 569-572.
- Fu, Q. and Bao, X. (2015). Catalysis on a metal surface with a graphitic cover. *Chinese Journal of Catalysis*. 36: 517-519.
- Furusawa, T., Watanabe, M., Kadota, R., Matsumoto, T., Sato, M. and Suzuki, N. (2015). Methanolysis of rapeseed oil to fatty acid methyl esters using microencapsulated CaO and TiO₂-supported chromium oxide under light irradiation. *Fuel Processing Technology*. 140: 125-131.
- Furuta, S., Matsuhashi, H. and Arata, K. (2006). Biodiesel fuel production with solid amorphous-zirconia catalysis in fixed bed reactor. *Biomass and Bioenergy*. 30: 870-873.
- Gan, J. and Yuan, W. (2013). Operating condition optimization of corncob hydrothermal conversion for bio-oil production. *Applied Energy*. 103:350-357.
- Gaudin, P., Fioux, P., Dorge, S., Nouali, H., Vierling, M., Fiani, E., Molière, M., Brilhac, J.F. and Patarin, J. (2016). Formation and role of Cu⁺ species on highly dispersed CuO/SBA-15 mesoporous materials for SO_x removal: An XPS study. *Fuel Processing Technology*. 153: 129-136.

- Ghazali, W.N.M.W., Mamat, R., Masjuki, H.H. and Najafi, G. (2015). Effects of biodiesel from different feedstocks on engine performance and emissions: A review. *Renewable and Sustainable Energy Reviews*. 51: 585-602.
- Granados, M.L., Poves, M.D.Z., Alonso, D.M., Mariscal, R., Galisteo, F.C., Moreno-Tost, R., Santamaria, J. and Fierro, J.L.G. (2007). Biodiesel from sunflower oil by using activated calcium oxide. *Applied Catalysis B: Environmental*. 73: 317-326.
- Guan, Q., Shang, H., Liu, J., Gu, J., Li, B., Miao, R., Chen, Q. and Ning, P. (2016). Biodiesel from transesterification at low temperature by AlCl₃ catalysis in ethanol and carbon dioxide as cosolvent: Process, mechanism and application. *Applied Energy*. 164: 380-386.
- Gui, M.M., Lee, K.T. and Bhatia, S. (2008). Feasibility of edible oil vs. non-edible oil vs. waste edible oil as biodiesel feedstock. *Energy*. 3: 1646-1653.
- Guldhe, A., Moura, C.V.R., Singh, P., Rawat, I., Moura, E.M., Sharma, Y. and Bux, F. (2017). Conversion of microalgal lipids to biodiesel using chromium-aluminum mixed oxide as a heterogeneous solid acid catalyst. *Renewable Energy*. 105: 175-182.
- Guo, F., Peng, Z.G., Dai, J.Y. and Xiu, Z.L. (2010). Calcined sodium silicate as solid base catalyst for biodiesel production. *Fuel Process Technology*. 91: 322-328.
- Hajduk, S., Dasireddy, V.D.B.C, Likozar, B., Dražić, G. and Orel, Z.C. (2017). COxfree hydrogen production via decomposition of ammonia over Cu–Zn-based heterogeneous catalysts and their activity/stability. *Applied Catalysis B: Environmental*. 211: 57-67.
- Hajjari, M., Tabatabaei, M., Aghbashlo, M. and Ghanavati, H. (2017). A review on the prospects of sustainable biodiesel production: A global scenario with an emphasis on waste-oil biodiesel utilization. *Renewable and Sustainable Energy Reviews*. 72: 445-464.
- Hameed, B.H., Lai, L.F. and Chin, L.H. (2009). Production of biodiesel from palm oil (*Elaeis guineensis*) using heterogeneous catalyst: An optimized process. *Fuel Processing Technology*. 90: 606-610.
- Hasan, M.M. and Rahman, M.M. (2017). Performance and emission characteristics of biodiesel-diesel blend and environmental and economic impacts of biodiesel production: A review. *Renewable and Sustainable Energy Reviews*. 74: 938-948.

- Hasni, K., Ilham, Z., Dharma, S. and Varman, M. (2017). Optimization of biodiesel production from *Brucea javanica* seeds oil as novel non-edible feedstock using response surface methodology. *Energy Conversion and Management*. 149: 392-400.
- Hassan, M.H. and Kalam, M.A. (2013). An overview of biofuel as a renewable energy source: development and challenges. *Procedia Engineering*. 56: 39-53.
- Hattori, H. (2001). Solid base catalysts: generation of basic sites and application to organic synthesis. *Applied Catalysis A: General*. 222: 247-259.
- Hattori, H. (2015). Solid base catalysts: fundamentals and their applications in organic reactions. *Applied Catalysis A: General*. 504: 103-109.
- He, B.B., Singh, A.P. and Thompson, J.C. (2007). A novel continuous-flow reactor using reactive distillation for biodiesel production. *Applied Catalysis A: General*. 49: 107-112.
- Hsin, T.M., Chen, S., Guo, E., Tsai, C.H., Pruski, M. and Lin, V.S.Y. (2010).
 Calcium containing silicate mixed oxide-based heterogeneous catalysts for biodiesel production. *Topics in Catalysis*. 53: 746-754.
- Huang, Y., Yuan, Y., Zhou, Z., Liang, J., Chen, Z. and Li, G. (2014). Optimization and evaluation of chelerythrine nanoparticles composed of magnetic multiwalled carbon nanotubes by response surface methodology. *Applied Surface Science*. 292: 378-386.
- Huaping, Z., Zongbin, W., Yuanxiong, C., Ping, Z., Shijie, D., Xiaohua, L. and Zongqiang, M. (2006). Preparation of biodiesel catalyzed by solid super base of calcium oxide and its refining process. *Chinese Journal of Catalysis*. 27(5): 391-396.
- Issariyakul, T. and Dalai, A. K. (2012). Comparative kinetics of transesterification for biodiesel production from palm oil and mustard oil. *The Canadian Journal of Chemical Engineering*. 90(2): 342-350.
- Istadi, I., Mabruro, U., Kalimantini, B.A., Buchori, L. and Anggoro, D.D. (2016). reusability and stability tests of calcium oxide based catalyst (K₂O/CaO-ZnO) for transesterification of soybean oil to biodiesel. *Bulletin of Chemical Reaction Engineering & Catalysis*. 11(1): 34-39.

- Istadi, I., Prasetyo, S.A. and Nugroho, T.S. (2015). Characterization of K₂O/CaO-ZnO catalyst for transesterification of soybean oil to biodiesel. *Procedia Environmental Sciences*. 23: 394-399.
- Jacobson, K., Gopinath, R., Meher, L.C. and Dalai, A.K. (2008). Solid acid catalyzed biodiesel production from waste cooking oil. *Applied Catalysis B: Environmental*. 85: 86-91.
- Jain, S. and Sharma, M.P. (2010). Kinetics of acid base catalyzed transesterification of *Jatropha curcas* oil. *Bioresource Technology*. 101: 7701-7706.
- Jeon, H., Kim, D.J., Kim, S.J. and Kim, J.H. (2013). Synthesis of mesoporous MgO catalyst templated by a PDMS–PEO comb-like copolymer for biodiesel production. *Fuel Process Technology*. 116: 325-331.
- Jitputti, J., Kitiyanan, B., Rangsunvigit, P., Bunyakiat, K., Attanatho, L. and Jenvanitpanjakul, P. (2006). Transesterification of crude palm kernel oil and crude coconut oil by different solid catalysts. *Chemical Engineering Journal*. 116: 61-66.
- Joshi, G., Rawat, D.S., Lamba, B.Y., Bisht, K.K., Kumar, P., Kumar, N. and Kumar, S. (2015). Transesterification of *Jatropha* and *Karanja* oils by using waste egg shell derived calcium based mixed metal oxides. *Energy Conversion and Management*. 96: 258-267.
- Kasatkin, I., Kurr, P., Kniep, B., Trunschke, A. and Schlögl, R. (2007). Role of lattice strain and defects in copper particles on the activity of Cu/ZnO/Al₂O₃ catalysts for methanol synthesis. *Angewandte Chemie*. 119:7465-7468.
- Kawashima, A., Matsubara, K. and Honda, K. (2009). Acceleration of catalytic activity of calcium oxide for biodiesel production. *Bioresource Technology*. 100: 696-700.
- Kazemian, H., Turowec, B., Siddiquee, M.N. and Rohani, S. (2013). Biodiesel production using cesium modified mesoporous ordered silica as heterogeneous base catalyst. *Fuel.* 103: 719-724.
- Kloprogge, J.T. and Wood, B.J. (2017). X-ray photoelectron spectroscopic and Raman microscopic investigation of the variscite group minerals: Variscite, strengite, scorodite and mansfieldite. *Spectrochimica Acta Part A: Molecular and Biomolecular Spectroscopy.* 185: 163-172.
- Knothe, G. and Razon, L.F. (2017). Biodiesel fuels. *Progress in Energy and Combustion Science*, 58: 36-59.

- Komintarachat, C. and Chuepeng, S. (2009). Solid acid catalyst for biodiesel production from waste used cooking oils. *Journal of the American Chemical Society*. 48: 9350-9353.
- Konwar, L.J., Boro, J. and Deka, D. (2014). Review on latest developments in biodiesel production using carbon-based catalysts. *Renewable and Sustainable Energy Reviews*. 29: 546-564.
- Korkut, I. and Bayramoglu, M. (2016). Ultrasound assisted biodiesel production in presence of dolomite catalyst. *Fuel.* 180: 624-629.
- Kostić, M.D. Bazargan, A., Stamenković, O.S., Veljković, V.B. and McKay, G. (2016). Optimization and kinetics of sunflower oil methanolysis catalyzed by calcium oxide-based catalyst derived from palm kernel shell biochar. *Fuel.* 163: 304-313.
- Kwon, E.E., Jeon, E.C., Yi, H. and Kim, S. (2014). Transforming duck tallow into biodiesel via noncatalytic transesterification. *Applied Energy*. 116: 20-25.
- Kwong, T.L. and Yung, K.F. (2015). Heterogeneous alkaline earth metal—transition metal bimetallic catalysts for synthesis of biodiesel from low grade unrefined feedstock. *RSC Advances*. 5. 83748-83756.
- Kwong, T.L. and Yung, K.F. (2016). One-step production of biodiesel through simultaneous esterification and transesterification from highly acidic unrefined feedstock over efficient and recyclable ZnO nanostar catalyst. *Renewable Energy*. 90: 450-457.
- Lee, H.V. and Yap, Y.H.T. (2015). Optimization study of binary metal oxides catalyzed transesterification system for biodiesel production. *Process Safety and Environmental Protection*. 94: 430–440
- Lee, H.V., Juan, J.C. and Yap, Y.H.T. (2015). Preparation and application of binary acid-base CaO-La₂O₃ catalyst for biodiesel production. *Renewable Energy*. 74: 124-132.
- Lee, H.V., Juan, J.C., Yap, Y.H.T. and Ong, H.C. (2016). Environment-friendly heterogeneous alkaline-based mixed metal oxide catalysts for biodiesel production. *Energies*. 9: 611-622.
- Li, E. and Rudolph, V. (2008). Transesterification of vegetable oil to biodiesel over MgO-functionalized mesoporous catalysts. *Energy & Fuels*. 22: 145-149.

- Li, P.P., Lang, W.Z., Xia, K., Luan, L., Yan, X. and Guo, Y.J. (2016). The promotion effects of Ni on the properties of Cr/Al catalysts for propane dehydrogenation reaction. *Applied Catalysis A: General.* 522: 172-179.
- Liu, F and Zhang, Y. (2011). Controllable growth of "multi-level tower" ZnO for biodiesel production. *Ceramics International*. 37: 3193-3202.
- Liu, X., Xiong, J. and Liang, L. (2015). Investigation of pore structure and fractal characteristics of organic rich Yanchang formation shale in central China by nitrogen adsorption/desorption analysis. *Journal of Natural Gas Science and Engineering*. 22: 62-72.
- Ljupković, R.B., Mićić, R.D., Tomić, M.D., Radulović, N.S., Bojić, A.L. and Zarubica, A.R. (2014). Significance of the structural properties of CaO catalyst in the production of biodiesel: An effect on the reduction of greenhouse gas emissions. *Hemijska Industrija*. 68(4): 399-412.
- Lu, Y., Zhang, Z., Xu, Y., Liu, Q. and Qian, G. (2015). CaFeAl mixed oxide derived heterogeneous catalysts for transesterification of soybean oil to biodiesel. *Bioresource Technology*. 190: 438-441.
- Lupan, O., Cretu, V., Postica, V., Ababii, N., Polonskyi, O., Kaidas, V., Schütt, F., Mishra, Y.K., Monaico, E., Tiginyanu, I., Sontea, V., Strunskus, T., Faupel, F. and Adelung, R. (2016). Enhanced ethanol vapour sensing performances of copper oxide nanocrystals with mixed phases. *Sensors and Actuators B*. 224: 434-448.
- Macedo, C.C.S., Abreu, F.R., Tavares, A.P., Alves, M.B., Zara, L.F., Rubim, J.C. and Suarez, P.A.Z. (2006). New heterogeneous metal-oxides based catalyst for vegetable oil transesterification. *Journal of the Brazilian Chemical Society*. 17(7): 1291-1296.
- Madhuvilakku, R. and Piraman, S. (2013). Biodiesel synthesis by TiO₂–ZnO mixed oxide nanocatalyst catalyzed palm oil transesterification process. *Bioresource Technology*. 150: 55-59.
- Mahlambi, M.M., Mishra, A.K., Mishra, S.B., Krause, R.W., Mamba, B.B. and Raichur, A.M. (2012). Synthesis and characterization of carbon-covered alumina (CCA) supported TiO₂ nanocatalysts with enhanced visible light photodegradation of *Rhodamine B. Journal of Nanoparticle Research*. 14: 790-801.

- Mahmudul, H.M., Hagoq, F.Y., Mamat, R., Adam, A.A., Ishak, W.F.W. and Alenezi, R. (2017). Production, characterization and performance of biodiesel as an alternative fuel in diesel engines A review. *Renewable and Sustainable Energy Reviews*. 72: 497-509.
- Maneerung, T., Kawi, S., Dai, Y. and Wang, C.H. (2016). Sustainable biodiesel production via transesterification of waste cooking oil by using CaO catalysts prepared from chicken manure. *Energy Conversion and Management*. 123: 487-497.
- Mansir, N., Teo, S.H., Rashid, U. and Yap, Y.H.T. (2018). Efficient waste *Gallus domesticus* shell derived calcium-based catalyst for biodiesel production. *Fuel*. 67-75.
- Mao, B.H., Chang, R., Shi, L., Zhuo, Q.Q., Rani, S., Liu, X.S., Tyo, E.C., Vajda, S., Wang, S.D. and Liu, Z. (2014). A near ambient pressure XPS study of subnanometer silver clusters on Al₂O₃ and TiO₂ ultrathin film supports. *Physical Chemistry Chemical Physics*. 16: 26645-26652.
- Mardhiah, H.H., Ong, H.C. Masjuki, H.H., Lim, S. and Lee. H.V. (2017). A review on latest developments and future prospects of heterogeneous catalyst in biodiesel production from non-edible oils. *Renewable and Sustainable Energy Reviews*. 67: 1225-1236.
- Marinković, D.M., Stanković, M.V., Veličković, A.V., Avramović, J.M., Miladinović, M.R., Stamenković, O.O., Veljković, V.B. and Jovanović, D.M. (2016). Calcium oxide as a promising heterogeneous catalyst for biodiesel production: Current state and perspectives. *Renewable and Sustainable Energy Reviews*. 56: 1387-1408.
- Matsubu, J.C., Zhang, S, De-Rita, L., Marinkovic, N.S., Chen, J.G., Graham, G.W., Pan, X. and Christopher, P. (2017). Adsorbate-mediated strong metal-support interactions in oxide-supported Rh catalysts. *Nature Chemistry*. 9: 120-127.
- Mazaheri, H., Ong, H.C., Masjuki, H.H., Amini, Z., Harrison, M.D., Wang, C.T., Kusumo, F. and Alwi, A. (2018). Rice bran oil based biodiesel production using calcium oxide catalyst derived from *Chicoreus brunneus* shell. *Energy*. 144: 10-19.
- Melero, J.A., Bautista, F., Morales, G., Iglesias, J. and Vázquez, R.S. (2010).
 Biodiesel production from crude palm oil using sulfonic acid-modified mesostructured catalysts. *Chemical Engineering Journal*. 161: 323-331.

- Melero, J.A., Bautista, L.F., Morales, G., Iglesias, J. and Vazquez, R.S. (2015). Acid-catalyzed production of biodiesel over arenesulfonic SBA-15: Insights into the role of water in the reaction network. *Renewable Energy*. 75: 425-432.
- Meng, Y.L., Wang, B.Y., Li, S.F., Tian, S.J. and Zhang, M.H. (2013). Effect of calcination temperature on the activity of solid Ca/Al composite oxide-based alkaline catalyst for biodiesel production. *Bioresource Technology*. 128: 305-309.
- Mijan, N.A., Lee, H.V. and Yap, Y.H.T. (2015). Synthesis and catalytic activity of hydration—dehydration treated clamshell derived CaO for biodiesel production. *Chemical Engineering Research and Design*. 102: 368-377.
- Mirzaei, A.A., Galavy, M., Beigbabaei, A. and Eslamimanesh, V. (2007). Preparation and operating conditions for cobalt cerium oxide catalysts used in the conversion of synthesis gas into light olefins. *Journal of the Iranian Chemical Society*. 4(3): 347-363.
- Mohadesi, M., Hojabri, Z. and Moradi, G. (2014). Biodiesel production using alkali earth metal oxides catalysts synthesized by sol-gel method. *Biofuel Research Journal*. 1: 30-33.
- Mohamad, M. and Ngadi, N. (2014) Effect of TiO₂ Mixed CaO catalyst in palm oil transesterification. *Applied Mechanics & Materials*. 695: 319-322.
- Mootabadi, H., Salamatinia, B., Bhatia, S. and Abdullah, A.Z. (2010). Ultrasonic-assisted biodiesel production process from palm oil using alkaline earth metal oxides as the heterogeneous catalysts. *Fuel.* 89: 1818-1825.
- Mousavi, S.M. and Panahi, P.N. (2013). Modeling and optimization of NH 3 -SCR performance of MnO x / γ -alumina nanocatalysts by response surface methodology. *Journal of the Taiwan Institute of Chemical Engineers*. 69: 68-77.
- Mousavi, S.M. and Panahi, P.N. (2016). Modeling and optimization of NH 3-SCR performance of MnOx/γ-alumina nanocatalysts by response surface methodology. *Journal of the Taiwan Institute of Chemical Engineers*. 69: 68-77.
- Moushoul, E.B., Farhadi, K., Mansourpanah, Y., Nikbakht, A.M., Molaei, R. and Forough, M. (2016). Application of CaO-based/Au nanoparticles as heterogeneous nanocatalysts in biodiesel production. *Fuel.* 164: 119-127.

- Mukenga, M., Muzenda, E., Jalama, K. and Meijboom, R. (2012). Biodiesel production from soybean oil over TiO₂ supported nano-ZnO. *World Academy of Science, Engineering and Technology*. 64: 949-953.
- Musa, I.A. (2016). The effects of alcohol to oil molar ratios and the type of alcohol on biodiesel production using transesterification process. *Egyptian Journal of Petroleum*. 25: 21-31.
- Niju, S., Begum, K.M.M.S. and Anantharaman. (2016). Enhancement of biodiesel synthesis over highly active CaO derived from natural white bivalve clam shell. *Arabian Journal of Chemistry*. 9: 633-639.
- Noh, H.M., Benito, A. and Alonso, G. (2016). Study of the current incentive rules and mechanisms to promote biofuel use in the EU and their possible application to the civil aviation sector. *Transportation Research Part D*. 46: 298-316.
- Noiroj, K., Inatrapong, P., Luengnaruemitchai, A. and Jai-In, S. (2009). A comparative study of KOH/Al₂O₃ and KOH/NaY catalysts for biodiesel production via transesterification from palm oil. *Renewable Energy*. 34: 1145-1150.
- Okoye, P.U., Abdullah, A.Z. and Hameed, B.H. (2017). Stabilized ladle furnace steel slag for glycerol carbonate synthesis via glycerol transesterification reaction with dimethyl carbonate. *Energy Conversion and Management*. 133: 477-485.
- Olutoye, M.A. and Hameed, B.H. (2011). Synthesis of fatty acid methyl ester from used vegetable cooking oil by solid reusable MG₁XZn₁+XO₂ catalyst. *Bioresources Technology*. 102: 3819-3826.
- Olutoye, M.A., Wong, C.P., Chin, L.H. and Hameed, B.H. (2014). Synthesis of FAME from the methanolysis of palm fatty acid distillate using highly active solid oxide acid catalyst. *Fuel Processing Technology*. 124: 54-60.
- Olutoye, M.A., Wong, S.W., Chin, L.H., Amani, H., Asif, M. and Hameed, B.H. (2016). Synthesis of fatty acid methyl esters via the transesterification of waste cooking oil by methanol with a barium-modified montmorillonite K10 catalyst. *Renewable Energy*. 86: 392-398.
- Onukwuli, D.O., Emembolu, L.N., Ude, C.N., Aliozo, S.O. and Menkiti, M.C. (2017). Optimization of biodiesel production from refined cotton seed oil and its characterization. *Egyptian Journal of Petroleum*. 26: 103-110.

- Pachatouridou, E., Papista, E., Iliopoulou, E.F., Delimitis, A., Goula, G., Yentekakis, I.V., Mamellos, G.E. and Konsolakis, M. (2015). Nitrous oxide decomposition over Al₂O₃ supported noble metals (Pt, Pd, Ir): Effect of metal loading and feed composition. *Journal of Environmental Chemical Engineering*. 3: 815-821.
- Park, Y.M., Lee, D.W, Kim, D.K., Lee, J. and Lee, K.Y. (2008). The heterogeneous catalyst system for the continuous conversion of free fatty acids in used vegetable oils for the production of biodiesel. *Catalysis Today*. 131: 238-243.
- Patel, A., Brahmkhatri, V. and Singh, N. (2013). Biodiesel production by esterification of free fatty acid over sulfated zirconia. *Renewable Energy*. 51: 227-233.
- Patil, P., Deng, S., Rhodes, J.I. and Lammers, P.J. (2010). Conversion of waste cooking oil to biodiesel using ferric sulfate and supercritical methanol processes. *Fuel.* 89: 360-364.
- Patil, P.D. and Deng, S. (2009). Optimization of biodiesel production from edible and non-edible vegetable oils. *Fuel*. 88:1302-1306.
- Poosumas, J., Ngaosuwan, K., Quitain, A.T. and Assabumrungrat, S. (2016). Role of ultrasonic irradiation on transesterification of palm oil using calcium oxide as a solid base catalyst. *Energy Conversion and Management*. 120: 62-70.
- Prasad, L. and Agrawal, A. (2012). Experimental investigation of performance of diesel engine working on diesel and neem oil blends. *Carbon*. 86: 78-92.
- Puhan, S., Jegan, R., Balasubbramanian, K. and Nagarajan, G. (2009). Effect of injection pressure on performance, emission and combustion characteristics of high linolenic linseed oil methyl ester in a DI diesel engine. *Renewable Energy*. 34:1227-1233.
- Pukale, D.D., Maddikeri, G.L., Gogate, P.R., Pandit, A.B. and Pratap, A.P. (2015). Ultrasound assisted transesterification of waste cooking oil using heterogeneous solid catalyst. *Ultrasonics Sonochemistry*. 22: 278-286.
- Purova, R., Narasimharao, K., Ahmed, N.S.I., Al-Thabaiti, S., Al-Shehri, A., Mokhtar, M. and Schwieger, W. (2016). Pillared HMCM-36 zeolite catalyst for biodiesel production by esterification of palmitic acid. *Journal of Molecular Catalysis A: Chemical*. 406: 159-167.
- Ramachandran, K., Sivakumar, P., Suganya, T. and Renganathan, S. (2011).

 Production of biodiesel from mixed waste vegetable oil using an aluminium

- hydrogen sulphate as a heterogeneous acid catalyst. *Bioresources Technology*. 102: 7289-7293.
- Ramli, A. and Farooq, M. (2015). Optimization of process parameters for the production of biodiesel from waste cooking oil in the presence of bifunctional γ-Al₂O₃-CeO₂ supported catalysts. *Malaysian Journal of Analytical Sciences*. 19(1): 8-19.
- Ramu, S., Lingaiaha, N., Prabhavathi, B.L.A., Devi, R.B.N., Prasadb, I. and Suryanarayanaa, P.S. (2004). Esterification of palmitic acid with methanol over tungsten oxide supported on zirconia solid acid catalysts: Effect of method of preparation of the catalyst on its structural stability and reactivity. *Applied Catalysis A: General*. 276: 163-168.
- Rashid, U. and Anwar, F. (2008). Production of biodiesel through optimized alkaline-catalyzed transesterification of rapeseed oil. *Fuel.* 87: 265-273.
- Rashid, U., Anwar, F. and Knothe, G. (2009). Evaluation of biodiesel obtained from cottonseed oil. *Fuel Processing Technology*. 90: 1157-1163.
- Rashtizadeh, E., Farzaneh, F. and Talebpour, Z. (2014). Synthesis and characterization of Sr₃Al₂O₆ nanocomposite as catalyst for biodiesel production. *Bioresources Technology*. 154: 32-37.
- Reddy, C.R.V., Oshel, R. and Verkase, J.G. (2006). Room-Temperature Conversion of Soybean Oil And Poultry Fat To Biodiesel Catalyzed By Nanocrystalline Calcium Oxides. *Energy & Fuels*. 20: 1310-1314.
- Reddy, N., Bera, P., Reddy, V.R., Sridhara, N., Dey, A., Anandan, C. and Sharma, A.K. (2014). XPS study of sputtered alumina thin films. *Ceramics International*. 40: 11099-11107.
- Rosid, S.J.M., Bakar, W.A.W.A. and Ali, R. (2014). Physicochemical study of supported cobalt-lanthanum oxide-based catalysts for Co₂/H₂ methanation reaction. *Clean Technologies Environmental Policy*. 17: 627-636.
- Rubio-Caballero, J.M., Santamaría-González, J., Mérida-Robles, J., Moreno-Tost, R., Alonso-Castillo, M.L., Vereda-Alonso, E., Jiménez-López, A. and Maireles-Torres, P. (2013). Calcium zincate derived heterogeneous catalyst for biodiesel production by ethanolysis. *Fuel.* 105: 518-522.
- Rubio-Caballero, J.M., Santamaría-González, J., Mèrida-Robles, J., Moreno-Tost, R., Jimènez-López, A. and Maireles-Torres, P. (2009). Calcium zincate as

- precursor of active catalysts for biodiesel production under mild conditions. *Applied Catalysis B: Environmental.* 91: 339-346.
- Said, N.H., Ani, F.N. and Said, M.F.M. (2015). Review of the production of biodiesel from waste cooking oil using solid catalysts. *Journal of Mechanical Engineering and Sciences*. 8: 1302-1311.
- Sani, Y.M., Daud, W.M.A.W, Aziz, A.R.A. (2014). Activity of solid acid catalysts for biodiesel production: A critical review. *Applied Catalysis A: General*. 470: 140-161.
- Santiago-Torres, N., Romero-Ibarra, I.C. and Pfeiffer, H. (2014). Sodium zirconate (Na₂ZrO₃) as a catalyst in a soybean oil transesterification reaction for biodiesel production. *Fuel Process Technology*. 120: 34-39.
- Santos, F.F.P., Malveira, J.Q., Cruz, M.G.A. and Fernandes, F.A.N. (2009). Production of biodiesel by ultrasound assisted esterification of *oreochromis niloticus* oil. *Fuel.* 5. 30-35.
- Saraf, S. and Thomas, B. (2007). Influence of feedstock and process chemistry on biodiesel quality. *Process Safety and Environmental Protection*. 85. 360-364.
- Sener, M., Reddy, D.H.K. and Kayan, B. (2014). Biosorption properties of pretreated sporopollenin biomass for lead (II) and copper (II): Application of response surface methodology. *Ecological Engineering*. 68:200-208.
- Serio, M.D., Ledda, M., Cozzolino, M., Minutillo, G., Tesser, R. and Santacesaria, E. (2006). Transesterification of soybean oil to biodiesel by using heterogeneous basic catalysts. *Industrial & Engineering Chemistry Research*. 45: 3009-3014.
- Shan, R., Zhao, C., Lv, P., Yuan, H. and Yao, J. (2016). Catalytic applications of calcium rich waste materials for biodiesel: Current state and perspectives. *Energy Conversion and Management*. 127: 273-283.
- Shehata, F., Abdelhameed, M., Fathy, A. and Elmahdy, M. (2011). Preparation and characteristics of Cu-Al₂O₃ nanocomposite. *Open Journal of Metal.* 1: 25-33.
- Shukri, N.M., Jaafar, J., Bakar, W.A.W.A. and Majid, Z.A. (2015). Optimization of basic catalyst with ammoniated polyethylene glycol for the removal of naphthenic acid from petroleum crude oil by Box–Behnken design. *Clean Technologies and Environmental Policy*. 17: 2387-2400.

- Silva, G.F., Camargo, F.L. and Ferreira, A.L.O. (2011). Application of response surface methodology for optimization of biodiesel production by transesterification of soybean oil with ethanol. *Fuel Processing Technology*. 92: 407-413.
- Singh, A.K. and Fernando, S.D. (2008). Transesterification of soybean oil using heterogeneous catalysts. *Energy Fuel*. 22(3): 2067-2069.
- Singh, B., Gulde, A., Rawat, I. and Bux, F. (2014). Towards a sustainable approach for development of biodiesel from plant and microalgae. *Renewable and Sustainable Energy Reviews*. 29: 216-245.
- Stamenkovic, O.S., Rajkovic, K., Velickovic, A.V., Milic, P.S. and Veljkovic, V.B. (2013). Optimization of base-catalysed ethanolysis of sunflower oil by regression and artificial neural network models. *Fuel Processing Technology*. 114: 101-108.
- Su, M., Yang, R and Li, M. (2013). Biodiesel production from hempseed oil using alkaline earth metal oxides supporting copper oxide as bi-functional catalysts for transesterification and selective hydrogenation. *Fuel.* 103: 398-407.
- Suryaputra, W., Winata, I., Indraswati, N. and Ismadji, S. (2013). Waste capiz (*Amusium cristatum*) shell as a new heterogeneous catalyst for biodiesel production. *Renewable Energy*. 50: 795-799.
- Svintsitskiy, D.A., Kardash, T.Y., Stonkus, O.A., Slavinskaya, E.M., Stadnichenko, A.I., Koscheev, S., Chupakhin, A.P. and Boronin, A.I. (2013). In Situ XRD, XPS, TEM, and TPR study of highly active in CO oxidation CuO nanopowders. *The Journal of Physical Chemistry C*. 117: 14588-14599.
- Tan, H., Hedhill, M.N., Wang, Y., Zhang, J., Li, K., Sioud, S., Al-Talla, Z.A., Amad, M.H., Zhan, T., Talla, O.E. and Hanc, Y. (2013). One-pot synthesis of Cu/ZnO/ZnAl₂O₄ catalysts and their catalytic performance in glycerol hydrogenolysis. *Catalysis Science & Technology*. 3: 3360-3370.
- Tan, Y.H., Abdullah, M.O., Hipolito, C.N. and Yap, Y.H.T. (2015). Waste ostrichand chicken-eggshells as heterogeneous base catalyst for biodiesel production from used cooking oil: Catalyst characterization and biodiesel yield performance. *Applied Energy*. 160: 58-70.
- Tangy, A., Pulidindi, I.N. and Gedanken, A. (2016). SiO₂ beads decorated with SrO nanoparticles for biodiesel production from waste cooking oil using microwave irradiation. *Energy Fuels*. 30: 3151-3160.

- Tarakc, M.I.S. and Ilgen, O. (2018). Esterification of oleic acid with methanol using Zr(SO₄)₂ as a heterogeneous catalyst. *Chemical Engineering Technology*. 4: 845-852.
- Tarigan, J.B., Prasoko, H.T., Siahaan, D. and Kaban, J. (2017). Rapid biodiesel production from palm kernel through in situ transesterification reaction using CaO as catalyst. *International Journal of Applied Chemistry*. 13(3): 631-646.
- Teixeira, L.S.G., Assis, J.C.R., Mendonça, D.R., Santos, I.T.V., Guimarães, P.R.B., Pontes, L.A.M. and Teixeira, J.S.R. (2009). Comparison between conventional and ultra-sonic preparation of beef tallow biodiesel. *Fuel Processing Technology*. 90: 1164-1166.
- Teo, S.H., Rashid, U. and Yap, Y.H.T. (2014). Biodiesel production from crude *Jatropha Curcas* oil using calcium based mixed oxide catalysts. *Fuel.* 136: 244-252.
- Teo, S.H., Rashid, U., Choong, S.Y.T. and Yap, Y.H.T. (2017). Heterogeneous calcium-based bimetallic oxide catalysed transesterification of *Elaeis guineensis* derived triglycerides biodiesel production. *Energy Conversion and Management*. 141: 20-27.
- Teo, S.H., Yap, Y.H.T and Ng, F.L. (2014). Alumina supported/unsupported mixed oxides of Ca and Mg as heterogeneous catalysts for transesterification of *Nannochloropsis sp.* microalga's oil. *Energy Conversion and Management*. 88: 1193-1199.
- Tickell, J. (2006). Biodiesel America: How to achieve energy security, free America from middle-east oil dependence and make money growing fuel. *Yorkshire Press*. 16-50.
- Toemen, S., Bakar, W.A.W.A. and Ali, R. (2014). Investigation of Ru/Mn/Ce/Al2O3 catalyst for carbon dioxide methanation: Catalytic optimization, physicochemical studies and RSM. *Journal of the Taiwan Institute of Chemical Engineers*. 45: 2370-2378.
- Tonetto, G.M. and Marchetti, J.M. (2010). Transesterification of soybean oil over Me/Al₂O₃ (Me = Na, Ba, Ca, and K) catalysts and monolith K/Al₂O₃-cordierite. *Topics in Catalysis*. 53: 755-762.
- Tseng, H.H., Lin, H.Y., Kuo, Y.F. and Su, Y.T. (2010). Synthesis, characterization, and promoter effect of Cu-Zn/Al₂O₃ catalysts on NO reduction with CO. *Chemical Engineering Journal*. 160: 13-19.

- Umdu, E.S. and Seker, E. (2012). Transesterification of sunflower oil on single step sol–gel made Al₂O₃ supported CaO catalysts: Effect of basic strength and basicity on turnover frequency. *Bioresource Technology*. 106: 178-181.
- Umdu, E.S., Tuncer, M. and Seker, E. (2009). Transesterification of *Nannochloropsis oculata* microalga's lipid to biodiesel on Al₂O₃ supported CaO and MgO catalysts. *Bioresource Technology*. 100: 2828-2831.
- Uzun, B.B., Kılıç, M., Özbay, N., Pütün, A.E. and Pütün, E. (2012). Biodiesel production from waste frying oils: Optimization of reaction parameters and determination of fuel properties. *Energy*. 44: 347-351.
- Vahid, B.R. and Haghighi, M. (2016). Urea-nitrate combustion synthesis of MgO/MgAl₂O₄ nanocatalyst used in biodiesel production from sunflower oil: Influence of fuel ratio on catalytic properties and performance. *Energy Conversion and Management*. 126: 362-372.
- Veljković, V.B., Banković-Ilić, I.B. and Stamenković, O.S. (2015). Purification of crude biodiesel obtained by heterogeneously-catalyzed transesterification. *Renewable and Sustainable Energy Reviews*. 49: 500-516.
- Verma, P. and Sharma, M.P. (2016). Review of process parameters for biodiesel production from different feedstocks. *Renewable and Sustainable Energy Reviews*. 62: 1063-1071.
- Viriya-empikul, N., Krasae, P., Nualpaeng, W., Yoosuk, B. and Faungnawakij, K. (2012). Biodiesel production over Ca-based solid catalysts derived from industrial wastes. *Fuel.* 92: 239-244.
- Vujicic, D., Comic, D., Zarubica, A., Micic, R. and Boskovic, G. (2010). Kinetics of biodiesel synthesis from sunflower oil over CaO heterogeneous catalyst. *Fuel.* 9: 2054-2061.
- Vyas, A.P., Subrahmanyam, N. and Patel, P.A. (2009). Production of biodiesel through transesterification of jatropha oil using KNO₃/Al₂O₃ solid catalyst. *Fuel.* 88: 625-628.
- Wachs, I.E. (2013). Catalysis science of supported vanadium oxide catalysts. *Dalton Transactions*. 42: 11762-11769.
- Wan, Z. and Hameed, B.H. (2011). Transesterification of palm oil to methyl ester on activated carbon supported calcium oxide catalyst. *Bioresource Technology*. 102(3): 2659-2664.

- Wan, Z. and Hameed, B.H. (2014). Chromium–tungsten–titanium mixed oxides solid catalyst for fatty acid methyl ester synthesis from palm fatty acid distillate. *Energy Conversion and Management*. 88: 669-676.
- Wang, D.W. and Su, D. (2014). Heterogeneous nanocarbon materials for oxygen reduction reaction. *Energy & Environmental Science*. 7: 576-591.
- Wang, J., Xing, S., Huang, Y., Fan, P., Fu, J., Yang, G., Yang, L. and Lv, P. (2017). Highly stable gasified straw slag as a novel solid base catalyst for the effective synthesis of biodiesel: Characteristics and performance. *Applied Energy*. 190: 703-712.
- Wang, J., Yang, L., Luo, W., Yang, G., Miao, C., Fu, J., Xing, S., Fan, P., Lv, P. and Wang, Z. (2017). Sustainable biodiesel production via transesterification by using recyclable Ca₂MgSi₂O₇ catalyst. *Fuel.* 196: 306-313.
- Wang, Y., Ou, S., Liu, P. and Zhang, Z. (2007). Preparation of biodiesel from waste cooking oil via two-step catalyzed process. *Energy Conversion Management*. 48: 184-188.
- Wefers, K. (1990). Alumina Chemicals: Science and Technology Handbook. *The American Ceramic Society*. 13-20.
- Winayanuwattikun, P., Kaewpiboon, C., Piriyakananon, K., Tantong, S., Thakernkarnkit, W., Chulalaksananukul, W. and Yongvanich, T. (2008). Potential plant oil feedstock for lipase-catalyzed biodiesel production in Thailand. *Biomass and Bioenergy*, 32: 1279-1286.
- Wong, Y.C., Yap, Y.H.T, Ramli, I. and Tee, H.S. (2015). Biodiesel production via transesterification of palm oil by using CaO–CeO₂ mixed oxide catalysts. *Fuel*. 162: 288-293.
- Wu, X. and Leung, D.Y.C. (2011). Optimization of biodiesel production from camelina oil using orthogonal experiment. *Applied Energy*. 88: 3615-3624.
- Xie, W. and Zhao, L. (2014). Heterogeneous CaO–MoO₃–SBA-15 catalysts for biodiesel production from soybean oil. *Energy Conversion and Management*. 79: 34-42.
- Xie, W., Peng, H. and Chen, L. (2006). Transesterification of soybean oil catalyzed by potassium loaded on alumina as a solid-base catalyst. *Applied Catalysis A: General*. 300: 67-74.

- Xie, W.L. and Li, H.T. (2006). Alumina-supported potassium iodide as a heterogeneous catalyst for biodiesel production from soybean oil. *Catalysis A: Chemistry*. 255: 1-9.
- Xin, L., Ping, N., Hao, L., Xian, S.Z., Cai, W.Y., Hui, Z.J., Su, T.X., Zhi, W.M. and Lin, Z.Q. (2016). Probing NH₃-SCR catalytic activity and SO₂ resistance over aqueous-phase synthesized Ce-W@TiO2 catalyst. *Journal of Fuel Chemistry and Technology*. 44(2): 225-231.
- Yadav, M., Singh, V and Sharma, Y.C. (2017). Methyl transesterification of waste cooking oil using a laboratory synthesized reusable heterogeneous base catalyst: Process optimization and homogeneity study of catalyst. *Energy Conversion and Management*. 148: 1438-1452.
- Yan, J., Wu, G., Guan, N., Li, L., Li, X. and Cao, X. (2013). Understanding the effect of surface/bulk defects on the photocatalytic activity of TiO₂: Anatase versus rutile. *Physical Chemistry Chemical Physics*. 15(26): 10978–10988.
- Yang, F., Ning, Z. and Liu, H. (2014). Fractal characteristics of shales from a shale gas reservoir in the Sichuan Basin, China. *Fuel*. 115: 378-384.
- Yang, Z. and Xie, W. (2007). Soybean oil transesterification over zinc oxide modified with alkali earth metals. *Fuel Processing Technology*. 88: 631-638.
- Yap, Y.H.T., Teo, S.H., Rashid, U., Islam, A., Hussien, M.Z. and Lee. K.T. (2014). Transesterification of *Jatropha curcas* crude oil to biodiesel on calcium lanthanum mixed oxide catalyst: Effect of stoichiometric composition. *Energy Conversion and Management*. 88: 1290-1296.
- Yatish, K.V., Lalithamba, H.S., Suresh, R., Arun, S.B. and Kumar, P.V. (2016). Optimization of scum oil biodiesel production by using response surface methodology. *Process Safety and Environmental Protection*. 102: 667-672.
- Yin, X., Ma, H., You, Q., Wang, Z. and Chang, J. (2012). Comparison of four different enhancing methods for preparing biodiesel through transesterification of sunflower oil. *Applied Energy*. 91: 320-325.
- Yoo, S.J., Lee, H.S., Veriansyah, B., Kim, J. Kim, J.D. and Lee, Y.W. (2010). Synthesis of biodiesel from rapeseed oil using supercritical methanol with metal oxide catalysts. *Bioresource Technology*. 101: 8686-8689.
- Yoshikawa, K., Sato, H., Kaneeda, M. and Kondo, J.N. (2014). Synthesis and analysis of CO₂ adsorbents based on cerium oxide. *Journal of CO₂ Utilization*. 8: 34-38.

- You, Y., Mayyas, M., Xu, S., Mansuri, I., Gaikwad, V., Munroe, P., Sahajwalla, V. and Joshi, R.K. (2017). Growth of NiO nanorods, SiC nanowires and monolayer graphene via a CVD method. *Green Chemistry*. 19: 5599-5607.
- Zabeti, M., Daud, W.M.A.W. and Aroua, M.K. (2009). Activity of solid catalysts for biodiesel production: A review. *Fuel Process Technology*. 90: 770-777.
- Zahrani, S.M.A., Elbashir, N.O., Abasaeed, A.E. and Abdulwahed, M. (2001). Catalytic performance of chromium oxide supported on Al₂O₃ in oxidative dehydrogenation of isobutane to isobutene. *Industrial & Engineering Chemistry Research*. 40: 781-784.
- Zhao, L., Qiu, Z., and Stagg-Williams, S.M. (2013). Transesterification of canola oil catalyzed by nanopowder calcium oxide. *Fuel Processing Technology*. 114: 154-162.
- Zhu, Y.M. and Shi, L. (2014). Zn promoted Cu–Al catalyst for hydrogenation of ethyl acetate to alcohol. *Journal of Industrial and Engineering Chemistry*. 20: 2341-2347.
- Zhu., C. and Liu, X. (2013). Optimization of extraction process of crude polysaccharides from Pomegranate peel by response surface methodology. *Carbohydrate Polymers*. 92: 1197-1202.