

MODELING AND OPTIMIZATION OF SPINNING CONDITIONS FOR
POLYETHERSULFONE HOLLOW FIBER MEMBRANE FABRICATION
USING NON-DOMINATED SORTING GENETIC ALGORITHM-II

NOOR ADILA BINTI ALUWI SHAKIR

UNIVERSITI TEKNOLOGI MALAYSIA

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NOOR ADILA BINTI ALUWI SHAKIR

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To my beloved mother and father

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ABSTRACT

Optimization of spinning conditions plays a key role in the development of high performance asymmetric hollow fiber membranes. However, from previous studies, in solving these spinning condition optimization problems, they were handled mostly by using an experimentation that varied one of the independent spinning conditions and fixed the others. The common problem is the preparation of hollow fiber membranes that cannot be performed effectively due to inappropriate settings of the spinning conditions. Moreover, complexities in the spinning process have increased where the interaction effects between the spinning conditions with the presence of multiple objectives also affect the optimal spinning conditions. This is one of the main reasons why very little work has been carried out to vary spinning conditions simultaneously. Hence, in order to address these issues, this study focused on a non-dominated sorting genetic algorithm-II (NSGA-II) methodology to optimize the spinning conditions during the fabrication of polyethersulfone (PES) ultrafiltration hollow fiber membranes for oily wastewater treatment to maximize flux and rejection. Spinning conditions that were investigated were dope extrusion rate (DER), air gap length (AGL), coagulation bath temperature (CBT), bore fluid ratio (BFR), and post-treatment time (PT). First, the work was focused on predicting the performance of hollow fiber membranes by considering the design of experiments (DOE) and statistical regression technique as an important approach for modeling flux and rejection. In terms of experiments, a response surface methodology (RSM) and a central composite design (CCD) were used, whereby the factorial part was a fractional factorial design with resolution V and overall, it consisted of a combination of high levels and low levels, center points, as well as axial points. Furthermore, the regression models were generated by employing the Design Expert 6.0.5 software and they were found to be significant and valid. Then, the regression models obtained were proposed as the objective functions of NSGA-II to determine the optimal spinning conditions. The MATLAB software was used to code and execute the NSGA-II. With that, a non-dominated solution set was obtained and reported. It was discovered that the optimal spinning conditions occurred at a DER of 2.20 cm³/min, AGL of 0 cm, CBT of 30 °C, BFR (NMP/H₂O) of 0/100 wt.%, and PT of 6 hour. In addition, the membrane morphology under the influence of different spinning conditions was investigated via a scanning electron microscope (SEM). The proposed optimization method based on NSGA-II offered an effective way to attain simple but robust solutions, thus providing an efficient production of PES ultrafiltration hollow fiber membranes to be used in oily wastewater treatment. Therefore, the optimization results contributed by NSGA-II can assist engineers and researchers to make better spinning optimization decisions for the membrane fabrication process.

ABSTRAK

Pengoptimuman keadaan pintalan memainkan peranan penting dalam pembangunan membran gentian geronggang asimetrik yang berprestasi tinggi. Walaubagaimanapun, dari kajian lepas, kebanyakan masalah pengoptimuman keadaan pintalan telah diselesaikan menggunakan uji kaji yang hanya mengubah satu keadaan pintalan dan menetapkan keadaan yang lain. Masalah yang kerap berlaku adalah proses pembuatan membran gentian geronggang tidak dapat dijalankan dengan berkesan disebabkan tetapan keadaan pintalan yang kurang sesuai. Tambahan pula, proses pintalan semakin kompleks, di mana interaksi antara keadaan pintalan dengan kehadiran pelbagai objektif juga memberi kesan kepada pengoptimuman keadaan pintalan. Ini merupakan salah satu sebab utama mengapa kurang penyelidikan dilakukan untuk mengkaji keadaan pintalan secara serentak. Untuk menangani isu ini, kajian ini menggunakan metodologi algoritma genetik tidak terdominasi-II (NSGA-II) untuk mengoptimumkan keadaan pintalan dalam pembuatan membran gentian geronggang ultrapenurasan polietersulfon (PES) untuk rawatan air sisa berminyak bagi memaksimumkan fluk dan kadar buangan. Keadaan pintalan yang dikaji adalah kadar penyemperitan dop (DER), ketinggian sela udara (AGL), suhu takungan pengentalan (CBT), nisbah bendalir liang (BFR) dan masa pasca-rawatan (PT). Pertama, kajian ini meramalkan prestasi membran gentian geronggang menggunakan reka bentuk eksperimen (DOE) dan teknik regrasi statistik bagi pemodelan fluk dan kadar buangan. Dari segi eksperimen, kaedah sambutan berpusat (RSM) dan mod reka bentuk komposit pusat (CCD) digunakan, yang mana bahagian faktor adalah reka bentuk faktor pecahan dengan resolusi V, dan keseluruhannya, ia terdiri daripada gabungan tahap tinggi dan tahap rendah, titik tengah dan mata paksi. Perisian Design Expert 6.0.5 telah menghasilkan model regrasi dan model didapati penting dan sah. Kemudian, model regrasi yang diperolehi dicadangkan sebagai fungsi objektif NSGA-II untuk menentukan keadaan pintalan optimum. Perisian MATLAB digunakan untuk mengekod dan melaksanakan NSGA-II. Satu set penyelesaian tidak dominasi telah diperolehi dan dilaporkan. Didapati bahawa keadaan pintalan optimum berlaku pada DER 2.20 cm³/min, AGL 0 cm, CBT 30 °C, BFR (NMP/H₂O) 0/100 wt.% dan PT 6 jam. Tambahan pula, morfologi membran di bawah pengaruh keadaan berputar berbeza disiasat menggunakan mikroskop elektron pengimbas (SEM). Cadangan kaedah pengoptimuman berdasarkan NSGA-II menawarkan satu cara yang berkesan untuk memperoleh penyelesaian yang mudah tetapi teguh bagi pembuatan membran gentian geronggang ultrapenurasan PES yang digunakan dalam rawatan air sisa berminyak secara cekap. NSGA-II memberi penyelesaian pengoptimuman yang dapat membantu jurutera dan penyelidik membuat keputusan pengoptimuman pintalan secara lebih baik dalam proses pembuatan membran.

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LIST OF ABBREVIATIONS

ABC	-	Artificial bee colony algorithm
ACO	-	Ant colony optimization
AGL	-	Air gap length
AI	-	Artificial intelligence
ANN	-	Artificial neural network
ANOVA	-	Analysis of variance
BFT	-	Bore fluid temperature
BFR	-	Bore fluid ratio
BFFR	-	Bore fluid flow rate
BSA	-	Bovine serum albumin
CA	-	Cellulose acetate
CBT	-	Coagulation bath temperature
CCD	-	Central composite design
DCMD	-	Direct contact membrane distillation
DER	-	Dope extrusion rate
DOE	-	Design of experiments
DP	-	Dynamic programming
DT	-	Dope temperature
EA	-	Evolutionary algorithm
GA	-	Genetic algorithm
GFR	-	Gas flushing rate
GUI	-	Graphical user interface
HMWC	-	High molecular weight component
HQ	-	Hydroquinone
HT	-	High throughput

ID	-	Inner diameter
LMWC	-	Low molecular weight component
LP	-	Linear programming
MATLAB	-	Matrix laboratory
MED	-	Multiple effect distillation
MF	-	Microfiltration
MINLP	-	Mixed-integer non-linear programming
MOEA	-	Multi-objective evolutionary algorithm
MOGA	-	Multi-objective genetic algorithm
MOP	-	Multi-objective optimization problem
MPDA	-	m-Phenylenediamine
MWCO	-	Molecular weight cut-off
NF	-	Nanofiltration
NLP	-	Non-linear programming
NMP	-	<i>N</i> -methyl-2-pyrrolidone
NP	-	Non-deterministic polynomial
NPF	-	Number of Pareto front
NPGA	-	Niched Pareto genetic algorithm
NSGA	-	Non-dominated sorting genetic algorithm
NSGA-II	-	Non-dominated sorting genetic algorithm-II
OD	-	Outer diameter
P	-	Post-treatment
PAES	-	Pareto-archieved evolution strategy
PAI	-	Polyamide-imide
PAN	-	Polyacrylonitrile
PBI	-	Polybenzimidazole
PDMS	-	Polydimethylsiloxane
PE	-	Polyethylene
PEEKWC	-	Modified poly(ether ether ketone)
PEI	-	Polyetherimide
PEG	-	Poly(ethylene) glycol
PES	-	Polyethersulfone
PI	-	Polyimide
PLGA	-	Poly(lactic-co-glycolic acid)

PP	-	Polypropylene
PRESS	-	Predicted residual sum of squares
PSF	-	Polysulfone
PSO	-	Particle swarm optimization
PT	-	Post-treatment time
PU	-	Polyurethane
PVDF	-	Polyvinylidene fluoride
PVDF-HFP	-	Poly (vinylidene fluoride-co-hexafluoropropylene)
PVP	-	Polyvinylpyrrolidone
PWP	-	Pure water permeability
RDGA	-	Rank-density based genetic algorithm
RH	-	Relative humidity
RO	-	Reverse osmosis
RSM	-	Response surface methodology
RT	-	Residence time
RWGA	-	Random weighted genetic algorithm
SA	-	Simulated annealing
SEM	-	Scanning electron microscope
SEPPI	-	Solidification of emulsified polymer solutions via phase inversion
SPEA	-	Strength Pareto evolutionary algorithm
SS	-	Spinneret size
ST	-	Spinneret temperature
TBAB	-	Tetrabutylammonium bromide
TMP	-	Transmembrane pressure
TS	-	Take-up speed
UF	-	Ultrafiltration
VEGA	-	Vector evaluated genetic algorithm

LIST OF SYMBOLS

A	-	Surface area of hollow fiber membrane
C_f	-	Concentration of solute area of feed
C_p	-	Concentration of solute area of permeate
D	-	Outer diameter of hollow fiber membrane
$F_j(x)$	-	Function of flux
$F_r(x)$	-	Function of rejection
$i_{distance}$	-	Crowding distance
i_{rank}	-	Non-domination rank
J	-	Flux
L	-	Liter
l	-	Effective length of hollow fiber membrane
n	-	Number of hollow fiber membrane in module
N_p	-	Population size
P_c	-	Probability of crossover
P_m	-	Probability of mutation
P_t	-	Population
P^*	-	Pareto optimal set
PF^*	-	Pareto front
Q	-	Water flux reading
Q_t	-	Population after selection, crossover and mutation
R	-	Rejection
R_t	-	Combined population
t	-	Time
T_s	-	Tournament size

V	-	Permeate volume
w	-	Pseudo-weight
ΔP	-	Difference of pressure between feed area and permeation area
σ	-	Standard deviation
Ω	-	Decision space
∞	-	Infinity
\prec_n	-	Crowded comparison operator
\mathbb{R}^n	-	Decision variable space
\mathbb{R}^k	-	Objective function space

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CHAPTER 1

INTRODUCTION

1.1 Background of the Research

At present, the global oil demand is rising due to the rapid development of many industries, such as automobile and high fuel consumption for manufacturing industries. As a consequence, massive volumes of oily wastewater have been produced from the oil purifier industry (Agustin *et al.*, 2008; Ong *et al.*, 2015). Since oily wastewater consists of various hazardous hydrocarbon compositions, chemical elements and heavy metals prior to discharging them to receiving water body, it needs to be treated. However, biological, chemical, and physical treatments are incapable of completely separating the oil molecules from water and the process necessitates a huge area for operation (El-Naas *et al.*, 2009).

Therefore, in order to overcome this issue, membrane separation has become one of the most effective and demanding techniques used to fulfill demands in numerous industrial processes based on separation (Gryta *et al.*, 2001). The ability of this membrane technology in separating multi-component compositions into two or more preferred outputs has allowed it to become a more popular choice, considering its potentials and benefits. The advances made by Loeb and Sourirajan in 1960s in

high-flux asymmetric membranes have led to further development of membrane separation techniques. Since then, this technology has attracted much attention and support for research. In the last thirty years, membrane filtration was not economically realistic, however, with the advanced technological revolutions of new substances, procedures, and targets, membrane technology has been recognized as a very successful and commercially attractive choice for separation and purification system (Wiesner and Chellam, 1999). Thus, the membrane filtration technology offers a promising avenue of study and innovation to provide better solutions for sufficient supply of clear water in fulfilling human, environmental, and industrial demands. Nevertheless, in the development of high performance membranes, several aspects need to be considered, such as membrane process, membrane module, and membrane material, in order to provide some basic understanding of the membrane formation mechanism.

There are numerous membrane separation processes are available. One of the membrane processes that have experienced rapid growth during the past few years is ultrafiltration. Typically, ultrafiltration membranes are used for the separation of very tiny suspended molecules and dissolved macromolecules from mixtures by utilizing asymmetric membranes, which possess the size of pores ranging from 0.01 to 0.1 μm . These membranes are normally conducted in a tangential stream mode where the flow of feed solution that sweeps tangentially passes through an upstream surface of membranes (Chaturvedi *et al.*, 2001). Besides, ultrafiltration has the widest diversity of application in numerous industries compared to other membranes processes since it is a separation technology that possesses high efficiency and low energy consumption (Nunes and Peinemann, 2006).

In addition, materials used for the membranes cover a broad range, from organic polymeric to inorganic substances. In fact, many studies have been carried out in the last few years to enhance membranes performance, as well as to search for new membrane materials and techniques to fabricate high performance membranes. Polymeric membranes have been well-established in most areas of industrial applications due to the significant development by Loeb and Sourirajan in 1960s for

their finding to fabricate asymmetric membrane structures. In addition, membrane separation processes using polymeric membranes have been quite marketable. In this study, polyethersulfone (PES) had been chosen as the prime material (polymer) because of its easier accessibility and processing, good characteristics of selectivity, as well as permeability and strong mechanical properties (Li *et al.*, 2004). Besides, PES is classified as an amorphous glassy and hydrophilic polymer in the sulfone group and it is appropriate to be utilized in ultrafiltration separation process through dry-wet inversion process. Also, the ultrafiltration membranes fabricated from PES polymer displayed a broad range of pH and temperature resistance (Wang *et al.*, 2010).

The membrane module is another critical aspect to contemplate as the process productivity and performance depend on it. Among membrane modules, hollow fiber configuration is more favorable for industrial applications mainly due to its huge membrane packing density, which permits it to have a high membrane area in a little tool (Darvishmanesh *et al.*, 2011). In addition, in comparison to flat sheet and spiral wound modules, the hollow fiber module is the preferred option for modules in filtration process as it possesses several good benefits, which are greater productivity due to strong mechanical properties, a very flexible module, and easy handling (Khayet *et al.*, 2012; Qin and Chung, 1999). These excellent features cause hollow fiber membranes irresistible from the industrial viewpoint. Moreover, at present, hollow fiber membranes are extensively applied in many areas especially in membrane separation areas, such as distillation, nanofiltration, reverse osmosis, and many more.

On the other hand, phase inversion spinning technique has been universally accepted as a standard technique for fabricating commercial membranes. It is also referred to as a process where spinning solution is transfigured from liquid to solid state. It is widely used and has become a favored technique to fabricate asymmetric hollow fiber membranes. In short, an operation of phase inversion spinning technique starts when a spinning solution is submerged and solidified in the coagulation bath. Throughout the process, the solvent and non-solvent in the

spinning solution are exchanged. As a result, it produces a property structure of the asymmetric membrane, which comprises of a dense top layer and porous sublayer (Jung *et al.*, 2004). In this research, asymmetric PES ultrafiltration hollow fiber membranes would be fabricated according to the dry-wet phase inversion spinning technique.

In the current state-of-the-art, many researchers are involved in developing, exploring, and expanding high performance membranes. Generally, membrane performance can be classified in terms of two basic attributes, which are membrane productivity (flux) and extent of separation (rejection of various feed components). Flux and rejection are closely related to both the inner and outer skin layers. When inner and outer surfaces possess an open structure, the pure water permeation flux increases, whereas rejection decreases accordingly (Aminudin *et al.*, 2013). In common, membranes with the highest flux and rejection are necessary and can be classified as a high performance membrane, where normally, efforts to maximize one attribute will decrease the other (Qin *et al.*, 2000; Sourirajan and Matsuura, 1985). Hence, the challenge of this research is to maximize membrane performance by enhancing the separation productivity through improving both flux and rejection.

1.2 Problem Statement

In the fabrication of hollow fiber membranes via dry-wet spinning technique, spinning conditions will dominate the properties of hollow fiber membranes in terms of morphology and separation performances. Besides, a lot of efforts have been made to study the relationship between membrane characteristics and spinning parameters. So far, numerous studies have reported varied effects of the spinning conditions like composition of dope solution, concentration of dope solution, air gap length and many more concerning the hollow fiber membranes performances. Nevertheless, not much has been said regarding the simultaneous effect of the parameters (i.e. dope

extrusion rate, air gap length, coagulation bath temperature, bore fluid ratio and post-treatment time), which are yet to be investigated on the performance of hollow fiber membranes.

On top of that, the optimization of preparation settings of membranes fabrication plays a key role in membranes performance (Yi *et al.*, 2010). Determining an optimal solution by using an appropriate optimization method is quite challenging for researchers. Moreover, the complexities in the spinning process have increased where the interaction effects between the spinning conditions also contribute to finding the optimal spinning conditions. It must be pointed out that from previous studies in solving these spinning condition optimization problems, they were handled mostly by using an experimentation that involved changing one of the spinning conditions while maintaining the others at fixed levels. Moreover, from previous studies, there were many researchers who used the parameter-by-parameter optimization method to optimize the spinning conditions in fabricating hollow fiber membranes and it was based on trial and error investigations. Furthermore, the complexity of membrane preparation problems, as numerous parameters are involved, is one of the main reasons why very little work has been done to vary all these spinning parameters simultaneously (Chung *et al.*, 2002; Xu and Qusay, 2004). For instance, Chung *et al.* (2002), Chung *et al.* (1998), Ismail *et al.* (2006), and Qin *et al.* (2000) varied the dope extrusion rate factor only and fixed other factors in fabricating PES ultrafiltration hollow fiber membranes. Meanwhile, Chung and Hu (1997), Kapantaidakis *et al.* (2002), Khayet (2003), and Qin *et al.* (2001) varied the air gap length only and fixed other factors during membrane fabrication. In addition, there were several researchers who varied two and more factors of these spinning conditions by using the parameter-by-parameter optimization technique. Apparently, the drawbacks of this classical approach are that it needs a lot of experimental work and time, does not consider any interaction between the spinning conditions during the spinning process, and displays lower capability in optimization. Thus, it takes tremendous effort to obtain the best optimal spinning conditions. Even though traditional optimization techniques have the ability of considering several parameters at the same time, they still fail to acquire the relationship equation that links the varied parameters and the outcomes, and besides, it is not easy to discover the

optimal parameters combination and optimal response value in the entire area. Furthermore, one of the common problems is that the hollow fiber membrane spinning process cannot be performed effectively due to the inappropriate settings of the spinning conditions (Khayet *et al.*, 2012). In general, most researchers have sought for the most appropriate settings of spinning process using a small number of experiments by keeping all conditions fixed and only varying one condition in a small range as it is more practical to be performed (Chung *et al.*, 2000).

These shortcomings of the classical method can be solved by using the response surface methodology (RSM), in which all parameters are varied simultaneously by using a set of experimental trials. By applying RSM, many spinning condition parameters can be investigated at the same time and the number of experimental trials can be minimized in comparison to the optimization technique based on trial and error attempts (Khayet *et al.*, 2012). In other words, RSM offers more benefits than the familiar conventional optimization method. RSM is faster and reliable, more informative, as well as involves a small number of experiments that save time and operation costs. Nevertheless, the spinning condition optimization problems are indeed challenging and the complexity further increases with the presence of multiple objectives.

From the above discussion, these problems are inherently multi-faceted and involve spinning conditions at various levels, which necessitate multiple objectives to be satisfied. The membranes that possess the highest flux and rejection are classified as high performances membranes (Aminudin *et al.*, 2013; Sourirajan and Matsuura, 1985). Normally, efforts to maximize the flux will have to decrease the rejection. Also, this problem could be categorized as a non-deterministic polynomial (NP)-hard problem. Therefore, multi-objective optimization is one such tool that can come in handy to solve these spinning optimization problems. Hence, a non-dominated sorting genetic algorithm-II (NSGA-II) approach is proposed for solving the spinning problem. NSGA-II is a commonly used global search algorithm due to its outstanding global search ability (Li *et al.*, 2015). Fundamental understanding in optimizing spinning conditions in membrane fabrication is still in its early stage and

not many researchers have reported the application of NSGA-II in optimizing spinning conditions in the PES ultrafiltration hollow fiber membrane fabrication. Thus, a crucial task in exploiting and optimizing novel, robust, and high performance membranes is thus to carry out further dynamic search approaches that quickly focus on the most potential optimal spots within the parameter space. As a result, it increases the possibility of discovering the membrane, which possesses the best separation performance (Vandezande *et al.*, 2009).

Thus, the present study in spinning conditions optimization is required to be undertaken in two stages: (i) modeling of input-output and in-process spinning parameter relationship, and (ii) determination of optimal spinning conditions. The spinning conditions considered dominantly affecting the preparation of PES ultrafiltration hollow fiber membranes are the dope extrusion rate (DER), air gap length (AGL), coagulation bath temperature (CBT), bore fluid ratio (BFR) and post-treatment time (PT). Particularly, design of experiments (DOE) (including central composite design (CCD) and response surface methodology (RSM)) integrated with the NSGA-II methodology are used for these purposes in the development of PES ultrafiltration hollow fiber membranes. Regression models are constructed based on DOE to model the spinning conditions during the fabrication of these membranes via phase inversion spinning technique. Then, these models are expressed as a fitness function of NSGA-II with the objective of maximizing the membrane performance in terms of flux and rejection. The optimization of spinning condition parameters that affect the membrane performance will be explored by using NSGA-II.

1.3 Research Questions

This research is primary to seek answers for these two major questions.

- (i) Which parameters or factors affect membrane performance in terms of flux and rejection?
- (ii) What are the optimal spinning conditions for PES ultrafiltration hollow fiber membranes fabrication?

1.4 Objective of the Research

The objectives of this research are to produce both high flux and rejection of PES ultrafiltration hollow fiber membranes by optimizing the spinning conditions in membrane fabrication. Based on the problems and research questions discussed in the previous sections, the objectives of this study are given as follows:

- (i) To determine the significant spinning parameters and their relationship using DOE. Additionally, the microstructures of PES ultrafiltration hollow fiber membranes are also investigated by using a scanning electron microscope (SEM).
- (ii) To optimize the spinning conditions used in the fabrication of PES ultrafiltration hollow fiber membranes by using the NSGA-II method.

1.5 Scope of the Research

To achieve the objectives of this research, some guidelines should be followed. Several main scopes for this study have been recognized as guidelines in order to optimize the spinning conditions in membrane fabrication as well as to produce high performance PES ultrafiltration hollow fiber membranes.

- (i) The spinning process conditions investigated cover those from the dope formulation stage until the post-treatment process.
- (ii) PES as a polymeric material is used in the dope formulation.
- (iii) Flux and rejection rate are used to characterize the membrane performance.
- (iv) Synthesized oily wastewater is used to characterize the separation performance.
- (v) DOE is used to develop the predicted regression models to show the relationships between the spinning conditions and membrane performance.
- (vi) NSGA-II is used to find the optimal spinning conditions.
- (vii) The MATLAB version 7.9.0529 (R2009b) is used to implement the NSGA-II optimization process.

1.6 Significance of the Research

The recent development of PES ultrafiltration hollow fiber membranes via NSGA-II has highlighted several advantages from this study. Most notably, it helps to provide an efficient spinning process, which makes the fabrication of membranes to become more effective and productive, as well as requiring small investment, energy consumption, and operating cost. The process also becomes an economical

approach and yields a good quality product, while relatively the PES ultrafiltration hollow fiber membranes with desired properties can be obtained. Thus, the knowledge acquired from this study will boost the future researches on membranes development, especially in the spinning process, to further provide better understanding in treating oily wastewater with a combination of various spinning conditions.

Removal of oily wastewater using the ultrafiltration process is very much crucial to contribute towards the availability of sustainable water supply system. The membrane separation is a good performance separation where the separation is based on a size of molecular, with low energy consumption, thus requiring small operating cost compared to the traditional techniques. Since PES is the most promising membrane to treat oily wastewater, this study developed the PES ultrafiltration hollow fiber membranes, while the membrane performances were evaluated in terms of flux and rejection. The impact of this study is important since the PES ultrafiltration hollow fiber membranes fabricated offers prospect of higher productivity and selectivity, as well as prominent boost in membrane performance. Indirectly, this research can help manufacturers to produce high performance membranes, which can contribute to provide fresh water resources and good quality treated water in regions around the world.

Lastly, the findings obtained from this research had been used to determine the optimal setting of the spinning process during membrane fabrication by presenting a new practical NSGA-II methodology for optimization of the spinning process. The emphasis of this study is to offer engineers or decision makers a preferred solution within a short period of time. Requirements and specifications from them can help and lead to choose the best solution. If they desire higher flux or any specific rejections, the appropriate combinations of spinning conditions can be selected accordingly. Thus, NSGA-II stimulates to enhance the production rate of membranes, besides, reducing spinning operation time that saves a lot of costs.

1.7 Structure of the Thesis

This thesis consists of seven chapters. The first chapter introduces the technology of membranes especially in membrane fabrication and its importance in separation and purification systems. It also includes the problem statement, research questions, objectives, scope and significance of the study. Chapter 2 gives a comprehensive overview of the studies conducted on membranes in many aspects especially in membrane manufacturing systems. It reviews the various issues of the usage of NSGA-II for optimizing the spinning conditions in membranes fabrication and its applications. Additionally, the notion and procedures of NSGA-II for solving problems are discussed. Chapter 3 presents the materials and methods as well as detailed procedures of each experiment conducted. Chapter 4 explains the development of the spinning regression models based on the DOE and statistical regression technique. Chapter 5 discusses the optimization process in solving the models using NSGA-II. Chapter 6 analyzes the results of the experimental studies. The last chapter gathers the conclusions of this study and the recommendations for future work.

(ACO), simulated annealing (SA), etc.

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