

**SYNTHESIS, CHARACTERIZATION AND PERFORMANCE OF
ADSORBENTS FOR MERCURY VAPOR REMOVAL**

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SYNTHESIS, CHARACTERIZATION AND PERFORMANCE OF
ADSORBENTS FOR MERCURY VAPOR REMOVAL

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A thesis submitted in fulfilment of the
requirements for the award of the degree of
Doctor of Philosophy (Chemical Engineering)

Faculty of Chemical Engineering
Universiti Teknologi Malaysia

JUNE 2015

Dedicated to my parents, family and my husband for their love and support

ACKNOWLEDGEMENT

First and foremost, I would like to express my greatest gratitude to my supervisor Associate Professor Dr. Hanapi bin Mat for his supervision, strong support, and patience throughout the project period. He was always there to provide everything needed in laboratory and generous with his time spent for the discussions and inputs on the research.

I am very thankful to my sponsor, the Ministry of Education (MOE), Malaysia for provided me the MyPhD scholarship in order to pursue this PhD study.

I would like to thank the members of Advanced Materials and Process Engineering (AMPEN) Research Laboratory and all my friends for their love, sharing the joys and frustrations, supports, patience and understanding. Their views and tips are useful indeed.

Last but certainly not least, I wish to express my deepest gratitude to my lovely parents (Johari Sharudin and Khairulbariah Alang Othman), sisters (Noorkhairiezan and Khairidasheila), Amir Adam and family members for their prayers, loves, continuous moral support and unending encouragement. Thank you so much to them.

ABSTRACT

Mercury pollution is a growing concern due to its toxicity, volatility, and bioaccumulation in the environment. The main and most problematic source of mercury emission comes from the coal-fired power plants and gas processing activities. Hence, mercury needs to be removed and adsorption has been proven to be an excellent method due to easiness of operation and efficiency. In this study, coconut husk such as coconut pith and fiber were used as alternative low-cost adsorbents in exchange to the existing conventional elemental mercury (Hg^0) adsorbents. The potential use of coconut based-adsorbents for elemental mercury removal from gas streams has not yet been fully explored due to lack of research in this regard. This research focused on synthesis and modifications of coconut husk such as surface, carbonization and sulfurization treatments in order to enhance elemental mercury adsorption performance. The adsorbents were characterized using proximate analysis, scanning electron microscope (SEM), Fourier transform infrared (FTIR) spectroscopy, nitrogen adsorption/desorption (NAD), carbon-hydrogen-nitrogen-sulfur (CHNS) analysis and X-ray photoelectron spectroscopy (XPS) measurement. The Hg^0 adsorption experiments were conducted using a conventional flow type packed-bed reactor system with nitrogen as carrier gas. The results show that the chemical, physical, morphological and spectral properties of the adsorbents were greatly influenced by the modification methods used. Adsorbents obtained through carbonization and sulfurization treatments produced the best Hg^0 adsorption capacity. The experimental data exhibited that the increase of thermal carbonization up to 900 °C, resulted in high adsorption capacity of 6067.49 $\mu\text{g/g}$. The sulfurization at lower temperature (i.e. CPS300) resulted in the highest adsorption capacity (26077.69 $\mu\text{g/g}$). Enhancement in Hg^0 adsorption capacity might due to the higher sulfur compounds on the surface which acts as active site towards elemental mercury. The adsorption data revealed that the adsorbent with larger equilibrium adsorption capacity possessed poor adsorption reaction kinetics and diffusion process. This study also revealed that the char adsorbent could sustain Hg^0 adsorption capacity over multiple regeneration cycles. However, sulfurized-char is non-regenerative adsorbent, which can be utilized for longer adsorption process. Finally, the present findings indicate that the coconut husk can be potential low-cost elemental mercury adsorbents by applying appropriate modifications such as carbonization and sulfurization treatments. In addition, the utilization of coconut husks can reduce waste disposal problems and thus improving environmental quality and sustainability.

ABSTRAK

Pencemaran raksa semakin mendapat perhatian disebabkan oleh ketoksidan, kemeruapan, bioakumulasinya dalam alam sekitar. Sumber utama dan paling bermasalah adalah pengeluaran raksa berpunca dari loji kuasa arang batu dan aktiviti-aktiviti pemprosesan gas. Oleh itu, raksa perlu disingkirkan dan penjerapan telah terbukti sebagai proses yang unggul kerana mudah dioperasi dan cekap. Dalam kajian ini, sisa kelapa seperti habuk dan serat sabut kelapa digunakan sebagai alternatif penjerap kos rendah kepada penjerap raksa lazim yang sedia ada. Keupayaan kegunaan penjerap berasaskan kelapa untuk penyingkiran unsur raksa dari aliran gas masih belum diterokai sepenuhnya kerana kekurangan penyelidikan dalam hal ini. Kajian ini tertumpu pada sintesis dan pengubahsuaian sabut kelapa seperti proses rawatan permukaan, pengkarbonan dan pensulfuran bagi meningkatkan prestasi penjerapan unsur raksa. Penjerap dicirikan melalui pengukuran analisis hampiran, mikroskop elektron imbasan (SEM), spektrometer Fourier transformasi inframerah (FTIR), penjerapan/penyahjerapan nitrogen (NAD), analisis karbon-hidrogen-nitrogen-sulfur (CHNS) dan spektroskopi fotoelektron sinar-X (XPS). Ujikaji penjerapan Hg^0 telah dijalankan dengan menggunakan aliran lazim reaktor sistem jenis lapisan terpadat dengan nitrogen sebagai gas pembawa. Hasil kajian menunjukkan bahawa ciri kimia, fizikal, morfologi dan spektrum penjerap banyak dipengaruhi oleh kaedah pengubahsuaian yang digunakan. Penjerap diperoleh melalui rawatan pengkarbonan dan pensulfuran menunjukkan keupayaan penjerapan Hg^0 yang terbaik. Data ujikaji menunjukkan kenaikan terma pengkarbonan sehingga $900\text{ }^\circ\text{C}$ menghasilkan keupayaan penjerapan yang tinggi iaitu $6067.49\text{ }\mu\text{g/g}$. Pensulfuran pada suhu lebih rendah, (misalnya CPS300) menghasilkan keupayaan penjerapan yang paling tinggi ($26077.69\text{ }\mu\text{g/g}$). Peningkatan dalam kapasiti penjerapan Hg^0 mungkin disebabkan oleh sebatian sulfur yang tinggi dipermukaan yang bertindak sebagai tapak aktif terhadap raksa. Data penjerapan mendedahkan bahawa penjerap dengan keseimbangan keupayaan penjerapan yang besar memiliki proses penjerapan kinetik dan resapan yang lemah. Kajian ini juga mendedahkan penjerap arang boleh mengekalkan keupayaan jerapan Hg^0 sepanjang kitaran penjanaan semula berganda. Walau bagaimanapun, penjerap sulfur-arang adalah penjerap tanpa penjanaan semula, yang boleh digunakan untuk proses penjerapan yang panjang. Akhirnya, penemuan ini menunjukkan bahawa sabut kelapa berkeupayaan sebagai penjerap unsur raksa kos rendah dengan menggunakan pengubahsuaian yang sesuai seperti rawatan pengkarbonan dan pensulfuran. Tambahan pula, penggunaan sabut kelapa boleh mengurangkan masalah pembuangan sisa, sehubungan itu memperbaiki kualiti alam sekitar dan kesinambungannya.

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LIST OF SYMBOLS

Hg	-	Mercury
A	-	Mass of air-dry sample (g)
A_c	-	Constant in the Clark model
A_r	-	Arrhenius factor
α	-	Initial adsorption rate in Elovich equation (ng/mg.min)
α_K	-	Khan isotherm model exponent
α_R	-	Redlich-Peterson isotherm constant (1/mg)
α_s	-	Sips isotherm model constant (L/mg)
α_T	-	Toth isotherm constant (L/mg)
B	-	Mass of sample after drying at 105°C (g)
b_k	-	Khan isotherm model constant
b_T	-	Tempkin isotherm constant
C	-	Mass of sample after drying at 950°C (g).
C_e	-	Equilibrium concentration (mg/L)
C_s	-	Saturation concentration of solute (mg/L)
C_o	-	Concentrations ($\mu\text{g}/\text{m}^3$) at time $t = 0$ (min)
C_t	-	Concentrations ($\mu\text{g}/\text{m}^3$) at time $t = t$ (min)
C_{BP}	-	Bypassed concentration ($\mu\text{g}/\text{m}^3$)
C_{BET}	-	BET adsorption isotherm relating to the energy of surface interaction (L/mg)
D	-	Mass of the residue (g)
D_{eff}	-	Effective diffusivity (cm^2/s)
D_{ep}	-	Effective pore diffusion coefficient
$(D_e)_{Ma}$	-	Effective diffusion coefficient of macropore region
$(D_e)_{Mi}$	-	Effective diffusion coefficient of micropore region

D_s	-	Surface diffusion coefficient
E_a	-	Action energy of adsorption (kJ/mol)
ϵ	-	Dubinin-Radushkevich isotherm constant
f	-	Volume fraction of the macropore region
g	-	Redlich-Peterson isotherm exponent
k_0	-	Kinetic rate constant of pseudo-zero order adsorption kinetic (min^{-1})
k_1	-	Kinetic rate constant of pseudo-first order adsorption kinetic (min^{-1})
k_2	-	Kinetic rate constant of pseudo-second order adsorption kinetic ($\text{g}/\mu\text{g}\cdot\text{min}$)
k_d	-	Kinetic rate constant (m^2/min)
k_{id}	-	Intraparticle rate constant ($\text{mg}/\text{g}\cdot\text{min}$)
k_{DR}	-	Dubinin-Radushkevich isotherm constant (mol^2/kJ^2)
k_{TH}	-	Thomas rate constant ($\text{dm}^3/\text{min}\cdot\text{mg}$)
k_{AB}	-	Mass transfer coefficient ($\text{L}/\text{mg}\cdot\text{min}$)
k_{YN}	-	Yoon-Nelson rate constant (min^{-1})
K_F	-	Freundlich isotherm constant (mg/g) (dm^3/g) ⁿ
K_L	-	Langmuir isotherm constant (L/mg)
K_R	-	Redlich-Peterson isotherm constant (L/g)
K_s	-	Sips isotherm model constant (L/g)
K_T	-	Tempkin isotherm equilibrium binding constant (L/g)
K_{TOTH}	-	Toth isotherm constant (mg/g)
m	-	Mass of the adsorbent (g)
m_c	-	Mass of final char produced (g)
m_o	-	Mass of air-dried precursor (g)
n	-	Characteristic constant related to adsorption intensity or degree of favorability of adsorption (Freundlich)
N	-	Number of observations in the experimental
N_o	-	Saturation concentration (mg/L)
p	-	Number of parameters in the regression model
q	-	Adsorption capacity ($\mu\text{g}/\text{g}$)

q_o	-	Maximum solid-phase concentration of the solute (mg/g)
q_{exp}	-	Calculate adsorption capacity ($\mu\text{g/g}$)
q_{calc}	-	Measured adsorption capacity ($\mu\text{g/g}$)
Q	-	Quantity of the mercury adsorbed
q_e	-	Equilibrium adsorption capacity ($\mu\text{g/g}$)
$q_{e,exp}$	-	Experimental equilibrium adsorption capacity ($\mu\text{g/g}$)
$q_{e,theory}$	-	Theoretical equilibrium adsorption capacity ($\mu\text{g/g}$)
q_{Ma}	-	Adsorbed concentration of the macropore zone
q_{Mi}	-	Adsorbed concentration of the micropore zone
q_{max}	-	Saturated monolayer adsorption capacity ($\mu\text{g/g}$)
q_t	-	Adsorption capacity at time t ($\mu\text{g/g}$)
q_s	-	Theoretical isotherm saturation capacity (mg/g)
ρ	-	Bed density
r	-	Constant in the Clark model (min^{-1})
r	-	Distance to the centre of pellet (general rate model)
r_c	-	Critical radius
R	-	Universal gas constant (8.314 J/mol.K)
R^2	-	Coefficient of determination
R_b		Branched pore kinetic model rate constant
R_p	-	Particle radius (cm)
t	-	Time (minute or hour or day)
T	-	Temperature ($^{\circ}\text{C}$ or K)
U_o	-	Superficial velocity (cm/min)
ν	-	Wavenumber (cm^{-1})
\dot{V}	-	Volumetric flow rate (L/min)
(v/v)	-	Volume per volume
wt. %	-	Weight percentage
z	-	Bed height (cm)
β	-	Desorption constant in Elovich equation (mg/ng)
β_s	-	Sips isotherm model exponent
β_w	-	Kinetic coefficient of the external mass transfer (min^{-1})
τ	-	Time required for 50% adsorbate breakthrough

LIST OF ABBREVIATIONS

AB	-	Adsorbent bed
AC	-	Activated carbon
APCD	-	Air pollution control devices
ARE	-	Average relative error
AWs	-	Agricultural wastes
BDDT	-	Brunauer-Deming-Deminng-Teller
BE	-	Binding energy
BET	-	Brunauer-Emmett-Teller
BJH	-	Barret-Joyner-Halenda
BJH	-	Barret–Joyner–Halender
BP	-	Bypass
CAAA	-	The Clean Air Act Amendment
CCA	-	Char, closed, ambient
CCN	-	Char, closed, purging nitrogen
CF	-	Coconut fiber
CFN	-	Char, flow nitrogen
CHNS	-	Carbon, Hydrogen, Nitrogen, Sulfur
CP	-	Coconut pith
D-R	-	Dubinin-Radushkevich
EPA	-	Environmental Protection Agency
ESP	-	Electrostatic precipitators
ETD	-	Everhart-Thornley Detector
FC	-	Fixed carbon
FF	-	Fabric filters

FGD	-	Flue gas desulfurization
FPD	-	Flame photometric detector
FTIR	-	Fourier Transform Infrared Spectroscopy
LFD	-	Large Field Detector
M	-	Moisture
MF	-	Mercury feed
MPSD	-	Marquardt's percent standard deviation
NAD	-	Nitrogen Adsorption/Desorption
NS	-	Nitrogen stream
ppb	-	Parts-per-billion
ppm	-	Parts-per-million
SEM	-	Scanning Electron Microscopy
TCD	-	Thermal conductivity detector
VM	-	Volatile matter
WD	-	Working distance
WHO	-	World Health Organization
XPS	-	X-ray photoelectron spectroscopy

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CHAPTER 1

INTRODUCTION

1.1 Research Background

Mercury is one of the most toxic heavy metals which could contaminate the environment and accumulate in animals and plants (Wang *et al.*, 2009). It is transported in the environment by air and water, as well as by biological organisms through the food-chains. The exposure to high levels of mercury can permanently damage the central nerve system, the brain and kidneys (Merrifield *et al.*, 2004). Mercury may exist in three different forms namely metallic mercury (e.g. Hg^0), inorganic mercury compounds (e.g. HgCl_2), and organic mercury compounds (e.g. MeHg^+) (Pirrone *et al.*, 2010).

Mercury enters the environment by natural processes (e.g. volcanic eruptions, and geothermic activities) and anthropogenic (e.g. coal-fired power plants, metal mining and refining, cement plant, municipal incinerators and wellhead natural gas processing) sources. It is well known that the coal fired power plants are the largest single source in most countries with high mercury emissions which release more than 50 tons of mercury annually (US EPA, 2014). At high temperature in the combustion zone of the boiler, the elemental mercury was released, and oxidized to Hg^{2+} (Wilcox *et al.*, 2012). The Hg^{2+} has tendency to form particulate bound mercury (Hg_p) which has been reported to be efficiently captured by air pollution control devices (APCD), such as electrostatic precipitators (ESP), fabric filters (FF) and flue gas desulfurization (FGD) (Wang *et al.*, 2010; Wilcox *et al.*, 2012). However, it is still difficult to directly remove Hg^0 from flue gas with these APCDs due to its high

volatility and insolubility in water (Padak *et al.*, 2006). The downstream of APCD (stack flue gas) contains major mercury species of Hg^0 and low concentrations of NO_x and SO_2 . The removal of mercury is generally performed by using fixed-bed adsorber system under low dust and low temperature process conditions (≈ 50 to 100°C).

Mercury also presents in natural gas which can cause catastrophic failures of aluminium heat exchangers in gas processing plants (Abu El Ela *et al.*, 2008; Abu El Ela *et al.*, 2008a). It was reported that the mercury concentration in natural gas is between 1 and 200 ng/L (Shafawi *et al.*, 1999) which are sufficiently high to cause both safety and health concerns. The natural gas processing typically consists of fixed-bed adsorbents to remove elemental mercury carried out, for instance, at temperature of $16 - 60^\circ\text{C}$ (El Ela *et al.*, 2008; Eckersley, 2010).

Several techniques have been developed in which adsorption is one of the most effective approaches to remove elemental mercury from gas streams. The solid materials such as activated carbon (Karatza *et al.*, 2013; Ie *et al.*, 2013), silica-based materials (Saman *et al.*, 2015; Johari *et al.*, 2014; Meyer *et al.*, 2007), fly ash (Gao *et al.*, 2013; Xu *et al.*, 2013; Xu *et al.*, 2012) and zeolites (Fan *et al.*, 2012; Chen *et al.*, 2010) have been proved as successful adsorbents for Hg^0 removal by many researchers. However, some limitations towards their applications include their complex preparations, high cost and non-renewable sources. Attempts towards the new precursors such as agricultural residues which are cheaper have recently been explored (Sun *et al.*, 2013).

Agricultural wastes (AWs) have been gaining increasing attention during recent years as new precursors for production of low-cost adsorbents (Chowdury *et al.*, 2011; Johari *et al.*, 2013; Johari *et al.*, 2014; Johari *et al.*, 2015; Lim and Aris, 2013; Song *et al.*, 2013). These agricultural wastes are naturally and abundantly available, in which could obtain for free or at a minimal cost. In addition, the AWs would be attractive for conversion to high added-value product such as adsorbents due to their simple and low-cost preparation process. In addition, their proper utilization may improve the environmental quality and sustainability. The common

AWs such as oil palm (*Elaeis guineensis*), rice (*Oryza sativa L.*) and coconut (*Cocos nucifera L.*) residues have been reported to have a high adsorption capacity of heavy metals from water and wastewaters (Bhatnagar *et al.*, 2010; Ahmad *et al.*, 2011; Chowdhury *et al.*, 2011; Johari *et al.*, 2013; Johari *et al.*, 2014; Lim and Aris, 2013; Song *et al.*, 2013).

Coconut (*Cocos nucifera L.*) is one of the most widely planted tree species in tropical region such as Brazil, India, Philippines, Malaysia and Indonesia. It is known for its great versatility of its parts such as coconut shell, fibers, and pith for commercial and industrial uses. A large amount of coconut processing wastes is also generated and becoming an environmental problems. So far, the coconut wastes have been used for fertilizer, building materials and automotive components (Sulaiman *et al.*, 2010; da Costa Castro *et al.*, 2012; Ucol-Ganiron JR, 2013) or left to decompose on the fields. Thus, the development of high value added product from coconut wastes is essential to solve their disposal problems. Besides, it helps in improving the environment quality and sustainability. In recent years, the use of coconut wastes has been extensively studied in adsorbent preparation for specific applications (Johari *et al.*, 2013; Johari *et al.*, 2014; Anirudhan *et al.*, 2008). For instances, the coconut wastes were reported on the production of carbonaceous adsorbents for the removal of mercury (Johari *et al.*, 2015), dye (Foo and Hameed, 2012; Kavitha and Namasivayam, 2007; Phan *et al.*, 2006), arsenic (Manju *et al.*, 1998), copper (Namasivayam and Kadirvelu, 1997), and chromium (Shen *et al.*, 2012) from water and wastewater. However, there is no research on coconut pith except for coconut shell as elemental mercury adsorbents (Matsumura 1974; Hu *et al.*, 2009).

1.2 Problem Background

Recently, the potential risk of toxic elements emitted from anthropogenic sources has become a public concern. Like other elements, mercury is persistent, cannot be destroyed by combustion or bacterial degradation and eliminated from environment. A great attention has been focused on mercury due to the increasing level of bioaccumulation in the environment and food-chain which can cause

potential risk for human health (Jack, 2010). Among the existing mercury removal systems, adsorption process is attractive for coal combustors and hazardous/municipal waste incinerators for treatment of mercury from both gas and liquid streams.

Several adsorbents have been commercialized for heavy metal removal processes (Sag and Kutsal, 2001; Dias *et al.*, 2007; Shareef, 2009; Park *et al.*, 2010). The carbonaceous adsorbents such as activated carbon has proven in their ability as adsorbents in aqueous and gas phase treatments due to their excellent thermal stability and non-specific adsorption characteristics (Dias *et al.*, 2007). The uses of carbonaceous adsorbents are limited by their non-renewable source of coal and high cost (Granite *et al.*, 2007). In addition, the preparation of carbonaceous adsorbents is complex, the cost is high and the specific surface area is small, limiting on their application. Moreover, they are not easily functionalized with mercury functional groups because of their surfaces are non-polar in nature.

Manchester *et al.* (2008) reported that the sulfur impregnated carbons have high adsorption capacities towards elemental mercury. However, it is too costly and the adsorption kinetics was observed too slow for some important applications. The low-cost methods namely oxidation process have been used for modifying carbon surface using reagents that include molecular oxygen, ozone, hydrogen peroxide, nitric acid, and permanganate. Despite of activated carbon prolific use in adsorption process, the biggest barrier of its application in industries is its high cost and difficulties associated with regeneration (Foo and Hameed, 2009). In order to reduce the adsorbent cost and thus the cost of treatment, the use of low-cost adsorbent precursors such as agricultural wastes namely coconut pith, orange peel, sawdust, rice husk, and baggase pith (Sag and Kutsal, 2001; Dias *et al.*, 2007; Shareef, 2009; Park *et al.*, 2010) have gained considerable researches recently. The agriculture wastes have been widely studied for removal of heavy metals from aqueous solutions. In addition, the processing and transformation of these wastes into charcoal or activated carbon would solve their disposal problems.

Since the last two decades, the development of low-cost adsorbents using lignocellulosic agricultural wastes has gained consideration among research communities. The agricultural wastes would be attractive as precursors for development of adsorbents due to their being abundant and cheap, simple and low-cost preparation process, possessing no waste disposal problems, and contributing to the sustainability of the surrounding environment (Johari et al. 2013; Rahman and Khan, 2007). It was previously proven by several literatures on the potential use of coconut wastes (e.g. desiccated, pith, fiber and shell) as potential low-cost adsorbents (Johari et al. 2013; Sharma et al. 2013; Johari et al. 2014b; Tan et al. 2008; Namasivayam and Sangeetha, 2004; Parab and Sudersanan, 2010; Igwe et al. 2008) from aqueous phase. To my knowledge, the use of coconut waste especially coconut husk as adsorbents for the elemental mercury (Hg^0) removal is still limited, even though it is in abundance and low-cost. Furthermore, the facile treatments of the coconut husk (pith and fiber) for elemental mercury adsorbents has not been thoroughly reported. Thus, with proper treatments via mercerization, bleaching, carbonization and sulfurization can be very promising adsorbents for Hg^0 removal process from gas streams. This study ultimately demonstrated the potential application of coconut husk (fiber and coconut pith) as precursors for elemental mercury adsorbent synthesis since they are expected to be good and relatively inexpensive adsorbent precursors and thus cheaper than the existing adsorbents.

1.3 Objectives

Based on the research background and the problem statement identified, the objectives of this study are as follows:

- i. To synthesize and characterize the coconut husk as an elemental mercury adsorbents
- ii. To investigate the elemental mercury adsorption process of coconut-based adsorbents

- iii. To study the elemental mercury adsorption performances of selected adsorbent.

1.4 Scopes of the Studies

In this study, the coconut husk such as coconut pith (CP) and coconut fiber (CF) was selected as precursor for elemental mercury (Hg^0) adsorbent. The synthesis was carried out by mercerization, bleaching, carbonization and sulfurization treatments. The carbonization treatment was done in different environment conditions, meanwhile the sulfurization was conducted at various temperatures and sulfur ratios. The pristine and treated coconut husk adsorbents obtained were characterized by proximate analysis (moisture, volatile matter, and ash content), scanning electron microscopy (SEM), nitrogen adsorption/desorption (NAD), X-ray photoelectron spectroscopy (XPS) analysis, Fourier transform infrared (FTIR), and CHNS elemental analysis.

The adsorption capability of the coconut husk adsorbents was measured using fabricated Hg^0 adsorption rig at fixed experimental conditions ($[\text{Hg}^0] = 200 \pm 20 \mu\text{g}/\text{m}^3$, bed temperature = 50°C , nitrogen flow rate = $50 \text{ mL}/\text{min}$, mass of adsorbent = 50mg). The Hg^0 adsorption experimental data were analyzed using the existing isotherm (i.e. Langmuir, Freundlich, and Temkin) and kinetic (i.e. pseudo-zero order, pseudo-first order, pseudo-second order, Elovich and Fick's intraparticle diffusion) models. These adsorption model analyses were carried out towards understanding the mechanism of the Hg^0 adsorption process.

The adsorbent with highest adsorption capacity was selected for further Hg^0 adsorption performances. Several experimental conditions such as initial mercury concentrations (i.e. $100 - 500 \mu\text{g}/\text{m}^3$) and adsorbent bed temperatures (i.e. $50 - 200^\circ\text{C}$) were performed. In addition, the adsorption and desorption were also studied via thermal desorption method in order to evaluate the regenerability of the adsorbents and thus the mechanism of desorption process.

1.5 Thesis Outline

Chapter 1 presents the general introduction of the elemental mercury adsorption problems and the utilization of agricultural wastes as high value added products. The problem backgrounds of the study are reviewed in Section 1.2, which contain on the effect of elemental mercury emission to the environment and the limitations of the existing adsorbents. The objective and scopes of this study are presented in Sections 1.3 and 1.4. Chapter 2 deals with critical review of mercury in the environment, development of numerous agricultural wastes as mercury adsorbents and theory of adsorption process. In Sections 2.1 and 2.2, the mercury overviews include the mercury toxicity and the adsorbent development for elemental mercury removal process. The review in Section 2.3 is intended to provide the evident those agricultural wastes (i.e. coconut husk), which is inexpensive and abundantly available, could be the potential adsorbents for the heavy metals removal. A mathematical model is presented in Section 2.5 including adsorption isotherm, kinetic and packed-bed column performances in term of engineering aspects of adsorption process.

Chapter 3 discusses about the research methodology, which comprises of research materials and experimental procedures for synthesis, characterization, and Hg^0 adsorption and desorption measurements. The selection of precursors and methods of synthesis are justified. The experiment conducted using lab-scale mercury adsorption rig in order to collect the experimental data. Chapter 4 presents the results and discussions of adsorbent synthesis and characterizations, evaluation of Hg^0 adsorption process onto the adsorbents and Hg^0 adsorption performances of the selected adsorbents. In Section 4.2, the findings based on the adsorbent preparation using coconut husk as precursor and adsorbent characterizations are discussed. In addition, the experimental data obtained from Hg^0 adsorption is used to analyze the validity of adsorption models and the assumptions made describing the mechanism of the adsorbent towards adsorption process. Chapter 5 is a summary of the research findings on the elemental mercury removal by coconut-based adsorbents and recommendations for extending in the future work. This is followed by list of references cited in the thesis.

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