

**SUPERCRITICAL CARBON DIOXIDE EXTRACTION OF CASTOR OIL SEED**

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A thesis submitted in fulfilment of the  
requirements for the award of the degree of  
Doctor of Philosophy (Chemical Engineering)

Faculty of Chemical Engineering  
Universiti Teknologi Malaysia

OCTOBER 2015

*To Allah (SWT), my beloved mother and father*

## ACKNOWLEDGEMENT

In the name of Allah the beneficent and the most merciful; Praise be to Allah (SWT), peace and blessing of Allah be upon our the most choicest and last prophet Muhammad (S.A.W), his family, companions and all those who follow his footsteps, Ameen.

I am heartily grateful to my supervisor and co supervisors of this program Dr. Agus Arsad and Dr Muhammad Abbas Ahmad Zaini whose encouragement, guidance and support from the initial to the final level enabled me to develop an understanding in the area. I thank them for sharing their valuable time and for giving helpful information to complete this PhD program. May Allah (SWT) reward them with good life here and in the hereafter. I would also like to thank my family members, especially to my father and mother for their total support, commitment, encouragement and their upbringing, may almighty Allah reward them with Aljanah Firdausi. I have to thank my wife and children for their moral support during this program. Also to my brothers, colleagues and friends that have given their full support and encouragement during this program and thesis preparation, I thank you very much. My deepest thanks go to Dr. Mohd Azizi Che Yunus, Zuhaili Idham, Salman Zhari, Syafiq Hazwan, Fahim Rithwan, Yian and Nina all of the group members of Centre of Lipids Engineering and Applied Research of Universiti Teknologi Malaysia for their generosity delivered and commitment.

I would also like to express my heartiest appreciation and gratitude to my friends and house mate, Dr. Baba Galadima, Dr Rufai Audu, Jibrin Mbaya Kawu, Abubakar Sadiq Aliyu for their endurance, support, motivation, advice and prayers.

## ABSTRACT

This study investigates the extraction of castor oil using supercritical carbon dioxide (SC-CO<sub>2</sub>). The response surface methodology (RSM) was employed to show explicitly the influence of the process parameters such as temperature, pressure and CO<sub>2</sub> flow rate on the oil yield using the Box-Behnken design. The linear terms of pressure, CO<sub>2</sub> flow rate and temperature, and the quadratic terms of temperature, pressure and CO<sub>2</sub> flow rate had a significant effect on the oil yield. The maximum oil yield obtained from the mathematical model was predicted to be 9.29% under the conditions of temperature at 63.7 °C and pressure of 29.9 MPa with CO<sub>2</sub> flow rate of 4.15 mL/min. Comparing the oil yield with the conventional soxhlet extraction, yields of 59.8%, 52.3% and 49.9% were obtained using ethanol, n-hexane and petroleum ether as solvents for optimized average particle sizes and extraction times of 1.30 mm and 2.88 h, 1.26 mm and 2.65 h and 1.25 mm and 2.55 h, respectively. In addition, the solubility of castor oil was measured at temperatures ranging from 313 to 335 K, and pressures 20 to 36 MPa, respectively. The measured solubilities ranged from  $1.00 \times 10^{-3}$  to  $4.88 \times 10^{-3}$  g of oil/g of CO<sub>2</sub>. The measurements confirmed that temperature and pressure have direct effects on solubility-enhancement factors. Five semi-empirical models were tested for correlating the experimental data from SC-CO<sub>2</sub> extraction: the Chrastil, Del Valle Aguilera (VA), Bartle, Kumar and Johnston (KJ) and Mendez-Santiago and Teja (MST) models. The solubilities from these models had the following average absolute relative deviations (AARD%) from experimental data: 0.05% (Chrastil), 0.30% (VA), 0.38% (Bartle), 5.98 % (KJ) and 28.5% (MST). Thus, the Chrastil, VA and Bartle models correlated to the castor oil solubility data with the lowest AARD%. The physico-chemical properties of the seed oil extracted using the SC-CO<sub>2</sub> and soxhlet methods were determined. Palmitic, stearic, oleic, linoleic, linolenic and ricinoleic acids were identified by gas chromatography-mass spectrometry (GC-MS) analysis after the formation of fatty acid methyl ester (FAME). For oxidation stability, castor oils derived from these extraction methods were heated in an oven at 70 °C for 0–12 weeks. The quality and oxidative stability of oil recovered by SC-CO<sub>2</sub> were generally found to be better than that recovered by the soxhlet method. In addition, the parameters considered in this study, namely peroxide value, refractive index, pH, conductivity, acid value and free fatty acid offer an appropriate tool for evaluating the quality of castor oil during storage as well as its oxidative stability; the study also sheds light on the different responses of castor oil during storage.

## ABSTRAK

Kajian ini meneliti pengekstrakan minyak kastor menggunakan karbon dioksida lampau genting (SC-CO<sub>2</sub>). Kaedah gerak balas permukaan menggunakan reka bentuk *Box-Behnken* digunakan untuk menunjukkan dengan jelas pengaruh parameter proses seperti suhu, tekanan dan kadar alir CO<sub>2</sub> ke atas hasil minyak. Pekali linear dan kuadratik bagi suhu, tekanan dan kadar alir CO<sub>2</sub> mempunyai kesan ketara ke atas hasil minyak. Hasil minyak maksimum yang diperolehi daripada model matematik dijangkakan sebanyak 9.29% pada keadaan suhu 63.7 °C dan tekanan 29.9 MPa dengan kadar alir CO<sub>2</sub> 4.15 mL/min. Membandingkan hasil minyak dengan kaedah pengekstrakan *soxhlet* menggunakan etanol, n-heksana dan petroleum eter sebagai pelarut, hasil sebanyak 59.8%, 52.3% dan 49.9% diperolehi untuk saiz zarah dan masa pengekstrakan masing-masing 1.30 mm dan 2.88 jam, 1.26 mm dan 2.65 jam, dan 1.25 mm dan 2.55 jam. Selain itu, kebolehlarutan minyak diukur pada suhu di antara 313 hingga 335 K, dan tekanan 20 hingga 36 MPa. Kebolehlarutan adalah di antara  $1.00 \times 10^{-3}$  hingga  $4.88 \times 10^{-3}$  g minyak/g CO<sub>2</sub>. Pengukuran mengesahkan bahawa suhu dan tekanan mempunyai kesan langsung ke atas faktor peningkatan kebolehlarutan. Lima model separa empirik telah diuji untuk menghubungkan data ujikaji daripada pengekstrakan SC-CO<sub>2</sub>: model *Chrastil*, *Del Valle Aguilera (VA)*, *Bartle*, *Kumar dan Johnston (KJ)*, dan *Mendez-Santiago dan Teja (MST)*. Kebolehlarutan diperolehi daripada model mempunyai sisihan relatif mutlak purata (AARD%) berikut: 0.05% (*Chrastil*), 0.30% (*VA*), 0.38% (*Bartle*), 5.98% (*KJ*) dan 28.5% (*MST*). Oleh itu, model *Chrastil*, *VA* dan *Bartle* dapat dikaitkan dengan data kebolehlarutan minyak kastor dengan AARD% terendah. Sifat fiziko-kimia minyak diekstrak menggunakan SC-CO<sub>2</sub> dan kaedah *soxhlet* ditentukan. Asid palmitik, stearik, oleik, linoleik, linolenik dan risinoleik dikenalpasti melalui analisis kromatografi gas-spektrometri jisim (GC-MS) selepas pembentukan asid lemak metil ester (FAME). Untuk kestabilan pengoksidaan, minyak kastor diperolehi daripada kaedah-kaedah pengekstrakan telah dipanaskan di dalam ketuhar pada 70 °C selama 0-12 minggu. Kualiti dan kestabilan pengoksidaan minyak yang diperolehi dengan SC-CO<sub>2</sub> secara umumnya didapati lebih baik berbanding kaedah *soxhlet*. Di samping itu, parameter yang dipertimbangkan dalam kajian ini iaitu nilai peroksida, indeks biasan, pH, kekonduksian, nilai asid dan asid lemak bebas bersesuaian untuk menilai kualiti minyak semasa penyimpanan serta kestabilan pengoksidaan; kajian ini memberikan gambaran perubahan sifat minyak kastor semasa penyimpanan.

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**LIST OF ABBREVIATIONS**

<i>a</i>	-	Solvato complex
AARD	-	Absolute relative deviation percentage
ANOVA	-	Analysis of variance
AOM	-	Active oxygen
AP	-	Adequate precision
ASTM	-	American Society for Testing and Materials
atm	-	Atmosphere
AV	-	Acid value
<i>b</i>	-	Indicates solute extraction
BHT	-	Butylated hydroxyl toluene
BHA	-	Butylated hydroxyl anisole
BS	-	British standard
<i>c</i>	-	Constant
<i>c</i>	-	Speed of light in a vacuum
°C	-	Degree Celsius
C <sub>1</sub>	-	Weight of castor seed before drying
C <sub>2</sub>	-	Weight of castor seed after drying
CCD	-	Central composite design
CE	-	Capillary electrophoresis
CO <sub>2</sub>	-	Carbon dioxide
CP	-	Critical point
cst	-	Centi stroke
CV	-	Coefficient of variance
DIN	-	Deutsche standard
DoE	-	Design of experiment
DSC	-	Differential scanning calorimetry
E <sub>a</sub>	-	Activation number
EFSA	-	European food safety authority
EoS	-	Equation of state
EtOH	-	Ethanol

FAMEs	-	Fatty acid methyl esters
FESEM	-	Field emission scanning electron microscopy
FFA	-	Free fatty acid
FTIR	-	Fourier transform infrared spectroscopy
g	-	grams
GC	-	Gas chromatography
GC-MS	-	Gas chromatography–mass spectrometry
GC	-	Gas chromatography
h	-	Hour
H <sub>2</sub> O	-	Water
$\Delta H$	-	Heat of reaction
$\Delta H_{\text{solv}}$	-	Heat of solvation
$\Delta H_{\text{vap}}$	-	Heat of vaporization
HPLC	-	High- pressure liquid chromatography
I <sub>2</sub>	-	Iodine value
IP	-	Industrial practice
K	-	Kelvin
<i>k</i>	-	Association number
KJ	-	Kumar and Johnson
KOH	-	Potassium hydroxide
m	-	Mass
Meq	-	Milliequivalents
mg	-	Milligram
mm	-	Milli meter
MPa	-	Mega Pascal
MST	-	Mendez- Santiago and Teja
n	-	Number of data points
N	-	Normality
NaOH	-	Sodium hydroxide
OSI	-	Oil stability instrument
P	-	Pressure
p	-	Probability
PG	-	Propyl gallate
P <sub>c</sub>	-	Critical pressure
pH	-	Hydrogen ion concentration
P <sub>0</sub>	-	Independent real value

$P_{\text{ref}}$	-	Standard reference pressure
$P_r$	-	Reduced pressure
$P_{\text{sub}}$	-	Sublimation pressure
PV	-	Peroxide value
R	-	Gas constant
RI	-	Refractive index
RSM	-	Response surface methodology
$S$	-	Solubility
$S_{\text{calc}}$	-	Solubility calculated using model
$S_{\text{exp}}$	-	Solubility obtained from experimental data
$S_I$	-	Volume of solution
$S_0$	-	Volume of blank
SC-CO <sub>2</sub>	-	Supercritical carbon dioxide
SCF	-	Supercritical fluid
SFE	-	Supercritical fluid extraction
T	-	Temperature
$T_i$	-	Actual independent variable
$\Delta T_i$	-	Step change
TAN	-	Total acid number
TBHQ	-	Mono-tert-butyl-hydroquinone
$T_c$	-	Critical temperature
TGA	-	Thermal gravimetric analysis
TP	-	Triple point
$T_r$	-	Reduced temperature
$v$	-	Speed of light in a substance
$\nu^1$	-	Kinematic viscosity
VA	-	Del Valle Aguilera
VI	-	Viscosity index
$X_i$	-	Independent variable
$y_1$	-	First y-value above
$y_2$	-	Second y-value below
ZDTC	-	Zinc dithiocarbomates
ZDTP	-	Zinc dithiophosphates
$\rho$	-	Density
$\rho_{\text{ref}}$	-	Reference density
%	-	Percentage

$\mu\text{L}$	-	Microlitre
$\mu$	-	Dynamic viscosity
$\mu\text{m}$	-	Microns

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## CHAPTER 1

### INTRODUCTION

#### 1.1 Background of Study

Castor oil plant (*Ricinus communis L*), a drought-resistant shrub belonging to the family *Euphorbiaceae* is extracted from castor seed. The extraction involves both mechanical and chemical separation processes (Anderson, 2005; Belgacem and Gandini, 2008; Kemper, 2005). Castor oil is viscous, pale yellow and non-drying oil with a bland taste and in most times generally used as a purgative (Mutlu and Meier, 2010). The mechanical separation process is often associated with low yields as against a chemical separation process which has (>99 weight %) of oil yield (Guoliang et al., 2011; Zhao and Zhang, 2013). Chemical extraction methods in most cases employ solvents such as *n*-hexane. However, its volatility is high and toxic in nature at low concentration. The vapors need to be monitored as uncontrolled amount could lead to an explosion during industrial oil extraction. Moreover, conventional extraction methods are time consuming, laborious, no selectivity and low extraction yields, no fractionation capabilities, solvent residue remained in the product, manipulations of limited variables, damaged the heat-sensitive components of the materials and the requirement of post-extraction process for solvent removal (Danh et al., 2009; Hossein et al., 2014; Luque de Castro and Priego, 2010; Miao et al., 2013; Rezzoug et al., 2005).

On the other hand, supercritical fluid extraction (SFE) allows the extraction of oil from seeds that are as good as, or even better than, those of conventional extraction. Thermal degradation and decomposition of labile compounds are avoided, due to the operation at reduced temperatures, whereas the absence of light and oxygen prevents the occurrence oxidation reaction (Turek and Stintzing, 2013). More also, the supercritical



fluid processed materials do not require any sterilization, since gram positive and gram negative bacteria can be inactivated at mild temperatures. The high pressure gradient during pressure release can yield extracts free of microorganisms and their spores, with a longer shelf life than standard solvent extraction (Foster et al., 2003; Perrut, 2004).

Supercritical fluid extraction (SFE) is a technique that can overcome these drawbacks of the conventional extraction process (Danlami et al., 2014). The negligible environmental impact of this process represents a prospect for changing the relative concentration of the various lipid moieties (Perretti et al., 2003). SFE is fast becoming a powerful means of extraction of solid samples especially seeds oil. It can be considered a technological revolution in the extraction industry (Sahena et al., 2009). Supercritical carbon dioxide (SC-CO<sub>2</sub>) is formed when liquids and gases are heated at a temperature and pressure higher than their critical points. Generally, substances that are heated above their critical temperature, regardless of the pressure, liquid phase cannot be recognized, as such when temperature and pressure are higher than their critical temperature and pressure, such are called supercritical fluid. Another description refers to substance in the state above its critical value. That critical value represents the temperature and pressure where it is not possible to clearly distinguish the boundary phases. That is the vapour-liquid critical point is in line and there are no separate phases of gas and liquid. Supercritical fluids effuse both solids like vapours and dissolve it like a liquid. In fact, the fluid property is neither that of a gas or liquid, but something in between. As a result, supercritical fluids provide the option for a better extraction feasibility, better products quality and efficiency. A supercritical fluid shows specific properties which are different from properties of gas and liquid states (Clifford, 1998).

The major advantages of using supercritical fluids for extraction purposes are (Baysal et al., 2002).

1. The extraction method is extremely rapid.
2. The solvent for extraction is easily removed.
3. The pressure, temperature and other variable conditions can be used to control the process
4. The solvent such as carbon dioxide, ethanol and methanol are reasonably cheap.
5. Supercritical fluid extraction does not produce any contamination.

Various studies were conducted in developing new extraction processes of increasing both quality and quantity of active natural products (Birmakr et al., 2012; Sajfrtova et al., 2010). Supercritical fluid extraction (SFE) has received great attention as a potential substitute for conventional technology for separating numerous valuable compounds from plant sources (Gomes et al., 2007; Liu et al., 2010). This is because the technique is carried out at low temperatures, at minimal extraction times and a little amount of solvent in comparison to other conventional solvent extraction methods that have been used for extracting valuable compounds for a very long time, which also involves using large amount of solvents with higher temperatures (Liza et al., 2010).

SC-CO<sub>2</sub> extraction is still receiving attention globally because carbon dioxide (CO<sub>2</sub>) is an inert, low-cost, harmless and ecologically-friendly which allows extraction at relatively low temperatures and pressures. More also, CO<sub>2</sub> evaporates easily when subjected to atmospheric conditions, as a result, the extract is freed from both chemicals and thermal degradation (Gomez et al., 1996). In fact, SC-CO<sub>2</sub> extract are by and large recognized as generally safe to be used in food industries (Gerard and May, 2002). Furthermore, CO<sub>2</sub> is also referred to be a nonpolar solvent, therefore, adding a little amount of co-solvent can improve significantly the extraction of polar compounds. Among these solvents ethanol (EtOH) is mostly used due to its miscibility with CO<sub>2</sub>, non-toxic and allowed usage in the food and pharmaceutical products (Gomez et al., 1996). Previously, SC-CO<sub>2</sub> has been used by many researchers for extracting valuable compounds from different natural sources such as hazelnut (Bernado-Gil et al., 2002), grape seed (Cao and Ito, 2003), watermelon (Vaughn et al., 2008), winter melon (Bimakr et al., 2013), orange pomace (Benelli et al., 2010), peach (*Prunus persica*) (Herrero et al., 2010), *Bidens pilosa* Linné (Kwiecinski et al., 2011) and *Mitragyna speciosa* leaves (Orio, 2012). Sanchez et al. (2009), presented an overview on some new advances and applications of SFE. In addition, SFE has been used for separating antioxidant compounds from sage, brazilian plants and some rosemary leaves (Monica et al., 2011; Ollanketo et al., 2002; Veggi et al., 2011). It is remarkable that very few reports on the extraction of castor oil using SC-CO<sub>2</sub> have been published. Turner et al. (2004) reported on the extraction of castor oil using CO<sub>2</sub> over the range of 40 – 80 °C and 20 - 40 MPa. They found that the fatty acid methyl esters (FAMES) in castor seeds were similar to those obtained using conventional methodology based on solvent extraction.

The extraction rate of seed materials with high oil is often limited by the solubility of oils in supercritical carbon dioxide (SC-CO<sub>2</sub>) (Dauksas et al., 2002; Molero et al., 2002; Marongiu, 2004; Illes et al., 2000; Leeke et al., 2002; Menaker et al., 2004). Therefore, oil solubility data are key to the development of separation processes, including feasibility evaluations, process design, scale up and establishing optimum operating conditions (Sovova et al., 2001; Abaroudi et al., 2002; Carr et al., 2011; Iwai and Yamamoto, 2013). However, experimental determination of the solubility of oil in SC-CO<sub>2</sub> is a difficult and an expensive task. Therefore, models to correlate and predict solubilities of oil in SC-CO<sub>2</sub> are very desirable; such models usually take the form of theoretical equations of state or semi-empirical equations because experimental determinations of the solubilities of oil in SC-CO<sub>2</sub> at various temperatures and pressures are time consuming. Cubic and non-cubic equations of state have been used to model the solubilities of oil in SC-CO<sub>2</sub> with and without co-solvents (Taberner et al., 2011; Ashour et al., 2000). However, these equations require robust computational methods and the knowledge of several properties such as sublimation pressures, molar volumes, critical temperatures and pressures. These properties are scarce in the literature, thus group contribution methods are usually applied, although their use introduces additional uncertainties in the use of these equations (Coimbra et al., 2006).

## **1.2 Problem Statement**

The utilization of vegetable oil in engineering is declining due to oxidative, hydrolytic and thermal stability. The greatest challenge however is the oxidative stability which has become a major concern that hinders the useful service life of the plant or vegetable oil. This is due to the presence of polar compounds which could irreversibly produce insoluble deposits throughout the whole volume, thus increasing the oil acidity and viscosity, which are not good for industrial purposes. These results from the type of extraction method used for the oil production. Valuable compounds are identified and isolated by means of extraction from plant sources (Stevigny et al., 2007). Oil extraction of plant or seed material is done using solvent extraction (Akpan et al., 2006; Salimon et al., 2010; Shridhar et al., 2010). Solvent extraction removes almost all organic phases inclusive of polar and non-polar groups and it becomes very difficult to separate compounds of interest, thereby leading to subsequent processing to improve the oxidative stability of oil is unavoidable.

Until now, attention has been mainly focussed on improving the oxidation stability of plant or seed oils obtained from solvent extraction (Akpan et al., 2006; Salimon et al., 2010; Shridhar et al., 2010) and mechanical expression with antioxidants. Examples of such antioxidant are butylated hydroxyl toluene (BHT), butylated hydroxyl anisole (BHA), mono-tert-butyl-hydroquinone (TBHQ), propyl gallate (PG), some naturally occurring tocopherols, zinc dithiophosphates (ZDTP) and zinc dithiocarbomates (ZDTC) (Fox and Stachowiak, 2007). Tocopherols are widely used as natural antioxidants, although their protective ability is not always sufficient (Milovanovi et al., 2002). However, the safety of these synthetic antioxidants has been a cause of concern because of their toxicity. They also decompose and become less effective at high temperature (Fox and Stachowiak, 2007; Akoh and Min, 2008; Gunstone, 2011; Shahidi, 2005). There is therefore need for further researches into finding a more environmentally friendly approach in improving oxidation stability. This research will therefore employ supercritical fluid extraction techniques to limit the presence of polar compounds in plant based oil from the castor oil. The castor oil has better properties than other vegetable oil due to its high content of ricinoleic acid (Scarpa and Guerci, 1982; Sorin, 2012). The main idea behind using supercritical carbon dioxide as a solvent is for selective extraction of non-polar compounds, thereby leaving behind the polar compounds that can accelerate the oxidation of the oil.

To date, there is no technical report has been published on the use of supercritical carbon dioxide extraction as a green approach to remove polar groups at the early stage of oil extraction in plant based oil processing to achieve oxidation stability improvement of the resultant oil without the addition of antioxidants. Similarly, there has been no research on the development of a mathematical model and optimization of the supercritical carbon dioxide extraction of castor oil using statistical experimental design method. Such a determination is crucial to understanding the effects of process variables such as temperature, pressure and CO<sub>2</sub> flow rate on extraction and oxidation stability.

Oil solubility data are also important at several stages in the development of SFE processes, including feasibility evaluations, process design, equipment sizing and establishing optimum operating conditions. However, experimental determination of the solubility of oils in SC-CO<sub>2</sub> is a difficult and an expensive task. Therefore, models to correlate and predict solubilities of oils in SC-CO<sub>2</sub> are very much desirable. Gupta and Shim (2007) reported the solubility data of various compounds in SC-CO<sub>2</sub> from over 1200 data. The solute including lipids, solids, polymer, food, drugs, pesticides, dyes, metal

complexes have been reported (Gupta and Shim, 2007). However, there are no studies reported on the solubility of the castor oil in SC-CO<sub>2</sub>.

### **1.3 Objectives of the Study**

The research is aimed at studying the extraction of castor oil seed using supercritical carbon dioxide.

In achieving these objectives, there are specific objectives that have to be fulfilled, which are:

1. To extract castor oil using supercritical carbon dioxide.
2. To establish the solubility profile of castor oil by supercritical carbon dioxide.
3. To characterize the physio-chemical properties of castor oil products.

### **1.4 Scope of the Thesis**

This research covers extraction of castor seed oil using supercritical carbon dioxide and also, comparing the oil yield to conventional solvent extraction. Modelling and optimization of the effect of independent variables such as average particle size, extraction time and temperature, pressure, flow rate of CO<sub>2</sub> on oil yield by employing conventional and supercritical fluid carbon dioxide were also carried out respectively, using response surface methodology (RSM) to design the experiment in order to reduce the number of experimental runs. In addition, the solubility of castor seed oil in CO<sub>2</sub> was measured and the density model was applied to determine the correlation of the solubility. Finally, the characterization of physiochemical properties of the castor oil such as the acid value, saponification value, iodine value, specific gravity, viscosity, refractive index, pH value and their fatty acid by employing supercritical carbon dioxide techniques. Moreover, oxidative stability changes of the castor oil were also studied by the schaal oven method at a temperature of 70 °C for 12 weeks.

## **1.5 Significant Contribution**

The results obtained from this research will reveal the best method for extracting castor oil to achieve enriched oil at optimum yield and this will also lead to the adoption of green approaches of supercritical CO<sub>2</sub> in improving the oxidative stability of castor oil seed. This will provide better understanding of primary oxidative compounds, which will allow the development of more effective and durable vegetable oil. In addition, this study will go long the way in understanding the fundamental aspects affecting the operating variables in achieving the desired product, so as to tailor the process to produce the desired product in a controlled manner.

The limitations of the conventional methods of oil extraction have favoured oxidation which has led to the growing interest of scientists in the development of a more efficient method. The SC-CO<sub>2</sub> is expected to serve as an alternative method in improving the oxidative stability of the oil. In terms of intellectual merit, a mathematical model showing the effect of average particle size, extraction time and temperature, pressure, flow rate of CO<sub>2</sub> was developed for both conventional and supercritical carbon dioxide extraction.

The empirical data on the solubility behavior of castor oil extraction from castor seed using supercritical carbon dioxide will provide a significant impetus for further SFE studies, especially in SC-CO<sub>2</sub>. Moreover, the use of a density model of the solubility approach will be envisioned as a simpler method for further prediction of solute solubility in supercritical carbon dioxide as an alternative and economical solvent in the extraction and improving oxidation stability.

## **1.6 Organization of the Thesis**

This thesis consists of five chapters and each chapter gives specific information about the research area as follows:

Chapter One: covers the background of the study, research aims and objectives. Moreover, the chapter highlights the scope of the research and the significance of the study.

Chapter Two: presents the literature reviews relevant to the study. The use of solvent extraction, supercritical carbon dioxide, response surface methodology (RSM) for optimization of the oil yield, solubility and oxidation stability studies were also explored.

Chapter Three: covers the raw material, description of the experimental methods and the general procedures in conducting this research work. These include oil extraction and characterization. It also explains the use of design expert in optimizing the oil yield.

Chapter Four: presents and discusses the comparisons between the physiochemical properties of conventional and supercritical fluid carbon dioxide extraction method. The effects of average particle size, extraction time, and temperature, pressure, flow rate of CO<sub>2</sub> on the optimum oil yield were also discussed. The chapter also discussed the solubility of castor oil in CO<sub>2</sub> and the application of the density model on solubility. Finally, an oxidation stability study of conventional and supercritical fluid carbon dioxide extraction were also discussed.

Chapter Five: deals with conclusions and recommendations. It presents the conclusions derived from the study and proposes several recommendations for future study for better understanding of oil solubility and oxidation stability.

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