

UNSTEADY MIXED CONVECTION FLOW OVER A CYLINDER OF ELLIPTIC  
CROSS SECTION NEAR FORWARD AND REAR STAGNATION POINTS

MADINA BINTI JAMALUDIN

UNIVERSITI TEKNOLOGI MALAYSIA

UNSTEADY MIXED CONVECTION FLOW OVER A CYLINDER OF ELLIPTIC  
CROSS SECTION NEAR FORWARD AND REAR STAGNATION POINTS

MADINA BINTI JAMALUDIN

A dissertation is submitted in partial fulfilment of the  
requirement for the award of the degree of  
Master of Science (Engineering Mathematics)

Faculty of Science  
Universiti Teknologi Malaysia

APRIL 2011

*To my beloved family,  
Dr. Sharidan Shafie  
Dr Anati Ali  
and friends .....*

## **ACKNOWLEDGEMENT**

The completion of this dissertation involves a lot of contributions from a number of people. Thus, I would like to use this golden opportunity to express and extend my sincere gratitude and appreciation to those who have been involved behind the development of this report.

Firstly, I would like to express my heartfelt thanks to my supervisors, Dr. Sharidan Shafie and my co-supervisor Dr. Anati Ali, for their time, willingness and patience in guiding me during my one year research on this study. I appreciate for their supervision, comments and advice.

I also wish to extend my thanks to my family, who has given me their greatest support and great motivation without fail throughout this task. Their love and encouragement had given me the spirit to complete this report successfully.

Finally, I would like to thank all my friends for all their kindly support, assistance and encouragement and also to everyone who has directly or indirectly involved in helping me to complete this dissertation.

## ABSTRACT

In this thesis, the unsteady mixed convection flow over a cylinder of elliptic cross section when the major axis are horizontal (blunt orientation) and vertical (slender orientation) have been studied. The study focused on the solution near the forward and rear stagnation points subjected to constant temperature placed in an incompressible viscous fluid. The unsteadiness is due to an impulsive motion of the free stream. The governing boundary layer equations are first reduced into a non-dimensional form, and then, transformed into a set of non similarity boundary layer equations, which are solved numerically using an efficient implicit finite-difference method known as Keller-box method. The numerical results are obtained for various values of the Prandtl numbers,  $Pr$ , the mixed convection parameter,  $\alpha$  and parameter for blunt and slender orientation,  $\omega$ . The effects of these parameter on velocity profiles, temperature profiles as well as Nusselt number are presented through graphs and tables. It is found that the increasing value of  $\omega$  leads to a decreases in the velocity profiles for both cases, blunt and slender orientation near the forward and rear stagnation point, respectively. An increased value of temperature profiles is found near the forward stagnation point while the value is decreased near the rear stagnation point for the case of slender orientation. The temperature profiles are fixed for the case of blunt orientation. Further, near both the forward and rear stagnation points, it is also found that the Nusselt number is fixed with increasing  $\omega$  for the case of blunt orientation. However, for the case of slender orientation, the Nusselt number near the forward stagnation point is decreased whereas near the rear stagnation point it is increased.

## ABSTRAK

Dalam tesis ini, masalah aliran lapisan sempadan tidak mantap berserta olakan campuran yang melepasi silinder berbentuk elip bagi kedua-dua paksi utama adalah menegak (orientasi tumpul) dan melintang (orientasi langsing) di kaji. Fokus kajian ini adalah kepada penyelesaian di sekitar titik genangan hadapan dan belakang pada suhu malar di dalam bendalir pekat yang tidak termampat. Ketidakmantapan aliran adalah disebabkan oleh gerakan dedenyut arus bebas. Persamaan-persamaan lapisan sempadan menakluk, pada mulanya diubah bentuk kepada bentuk tak bermatra, kemudian diubah kepada set persamaan lapisan sempadan tak serupa, seterusnya diselesaikan secara berangka dengan menggunakan kaedah beza terhingga tersirat yang efektif dikenali sebagai kaedah kotak-Keller. Keputusan-keputusan berangka yang diperolehi meliputi pelbagai nilai nombor Prandtl,  $Pr$ , parameter olakkan campuran,  $\alpha$  dan parameter untuk orientasi tumpul dan langsing,  $\omega$ . Kesan parameter-parameter ini terhadap profil halaju, profil suhu dan juga nombor Nusselt dipaparkan menerusi graf dan jadual. Didapati dengan meningkatnya nilai  $\omega$  menyebabkan profil halaju menurun di sekitar titik genangan hadapan dan belakang bagi kes orientasi tumpul dan langsing. Peningkatan nilai profil suhu didapati berlaku di sekitar titik genangan hadapan tetapi menurun di sekitar titik genangan belakang bagi kes orientasi langsing. Namun, bagi kes orientasi tumpul, profil suhu adalah tetap. Seterusnya, hasil kajian juga menunjukkan nilai nombor Nusselt adalah tetap dengan peningkatan  $\omega$  di sekitar titik genangan hadapan dan belakang bagi kes orientasi tumpul. Walaubagaimanapun, bagi kes orientasi langsing, nombor Nusselt menurun di sekitar titik genangan hadapan manakala meningkat di sekitar titik genangan belakang.

## TABLE OF CONTENTS

CHAPTER	TITLE	PAGE
	<b>REPORT STATUS DECLARATION</b>	
	<b>SUPERVISOR'S DECLARATION</b>	
	<b>TITLE PAGE</b>	i
	<b>DECLARATION</b>	ii
	<b>DEDICATION</b>	iii
	<b>ACKNOWLEDGEMENT</b>	iv
	<b>ABSTRACT</b>	v
	<b>ABSTRAK</b>	vi
	<b>TABLE OF CONTENTS</b>	vii
	<b>LIST OF TABLES</b>	ix
	<b>LIST OF FIGURES</b>	xi
	<b>LIST OF SYMBOLS</b>	xvii
	<b>LIST OF APPENDICES</b>	xix
<b>1</b>	<b>INTRODUCTION</b>	1
	1.1 Research background	1
	1.2 Statement of the Problem	3
	1.3 Objectives of the study	3
	1.4 Scope of the Study	4
	1.5 Significant of the Study	4
	1.6 Outline of dissertation	5
<b>2</b>	<b>LITERATURE REVIEW</b>	6
	2.1 Introduction	6
	2.2 The Stagnation Point Flow	6

2.3	Steady Boundary Layer Flow on Convection Past a Cylinder and an Elliptic Cylinder	8
2.4	Unsteady Boundary Layer Flow on Convection Past a Cylinder and an Elliptic Cylinder	12
<b>3</b>	<b>MATHEMATICAL FORMULATION</b>	<b>14</b>
3.1	Introduction	14
3.2	Basic Equations	14
3.3	Non-Similar Transformation	27
3.4	Solutions at the Stagnation Point	34
3.5	Physical Quantities	36
<b>4</b>	<b>THE KELLER-BOX METHOD</b>	<b>37</b>
4.1	Introduction	37
4.2	Finite Difference Discretization at the Forward and Rear Stagnation Points	38
4.3	Newton's Method	42
4.4	Block-elimination Method	45
4.5	Starting Conditions	52
<b>5</b>	<b>RESULT AND DISCUSSIONS</b>	<b>56</b>
5.1	Introduction	56
5.2	The Validity of the Result	56
5.3	Result and Discussion	58
<b>6</b>	<b>CONCLUSION</b>	<b>86</b>
6.1	Summary of research	86
6.2	Suggestion for Future Research	91
	<b>REFERENCES</b>	<b>92</b>
	Appendix A	97-102



## LIST OF TABLES

TABLE	TITLE	PAGE
5.0	Comparison the value of separation times at forward and rear stagnation points for some values of Pr and $\alpha$ when $\omega = 1$	57
5.1	The separation times, $t_s$ of the cylinder of the elliptic cross section near forward ( $x = 0$ ) and rear ( $x = \pi$ ) stagnation points for Pr = 1 and $\alpha = -3$ (opposing flow)	59
5.2	The separation times, $t_s$ along the cylinder of the elliptic cross section near forward ( $x = 0$ ) and rear ( $x = \pi$ ) stagnation points for Pr = 7 and $\alpha = -3$	60
5.3	The separation times, $t_s$ along the cylinder of the elliptic cross section near forward ( $x = 0$ ) and rear ( $x = \pi$ ) stagnation point for Pr = 7 and $\alpha = 1.25$ (assisting flow)	60
6.0	The behaviour of velocity and temperature profiles as the value of $\omega$ increases	86
6.1	The behaviour of Nusselt number as the value of $\omega$ increases	86

6.2	The behaviour of velocity and temperature profiles as the mixed convection parameter, $\alpha$ increases.	89
6.3	The behaviour of Nusselt number as the mixed convection parameter, $\alpha$ increases	89
6.4	The behaviour of velocity and temperature profiles as the Prandtl number, Pr increases	90
6.5	The behavior of Nusselt number as the Prandtl number, Pr increases	90

**LIST OF FIGURES**

<b>FIGURE</b>	<b>TITLE</b>	<b>PAGE</b>
3.0(a)	Physical model and coordinate system for blunt orientation	15
3.0(b)	Physical model and coordinate system when the fluid is passing near stagnation point for blunt orientation	15
3.1(a)	Physical model and coordinate system for slender orientation	16
3.1(b)	Physical model and coordinate system when the fluid is passing near stagnation point for slender orientation	16
4.0	Net rectangle for difference approximations	40
4.1(a)	Flow diagram for the Keller Box method	54
4.1(b)	Flow diagram for the Keller Box method	55
5.0(a)	Variation of the separation times with $\alpha$ near forward stagnation points when $Pr = 1$ .	57
5.0(b)	Variation of the separation times with $\alpha$ near rear stagnation points when $Pr = 1$ .	58

- 5.1 The variation of  $\frac{\partial^2 f}{\partial \eta^2}$  as a function of  $t$  at the rear stagnation point for some values of  $\omega$  when  $\text{Pr} = 1$  and  $\alpha = -3$  61
- 5.2 The variation of  $\frac{\partial^2 f}{\partial \eta^2}$  as a function of  $t$  at the Forward stagnation point for some values of  $\omega$  when  $\text{Pr} = 1$  and  $\alpha = -3$  61
- 5.3 Variation of the separation times with  $\alpha$  near forward stagnation point when  $\text{Pr} = 1$  for various value of  $\omega$ . 63
- 5.4 Variation of the separation time with  $\alpha$  near rear stagnation point when  $\text{Pr} = 1$  for various value of  $\omega$  63
- 5.5 The velocity profiles at  $x = 0$  (forward stagnation point) for some values of  $\alpha$  and  $t$  when  $\text{Pr} = 1$  and  $\omega = 0.5$  (blunt orientation) 67
- 5.6 The velocity profiles at  $x = \pi$  (rear stagnation point) for some values of  $\alpha$  and  $t$  when  $\text{Pr} = 1$  and  $\omega = 0.5$  (blunt orientation) 67
- 5.7 The velocity profiles at  $x = 0$  (forward stagnation point) for some values of  $\alpha$  and  $t$  when  $\text{Pr} = 1$  and  $\omega = 4$  (slender orientation) 68
- 5.8 The velocity profiles at  $x = \pi$  (rear stagnation point) for some values of  $\alpha$  and  $t$  when  $\text{Pr} = 1$  and  $\omega = 4$  (slender orientation) 68

- 5.9 The velocity profiles at  $x=0$  (forward stagnation point) for some values of  $\omega$  and Pr when  $t=0.15$  and  $\alpha=-3$  (blunt orientation) 69
- 5.10 The velocity profiles at  $x=\pi$  (rear stagnation point) for some values of  $\omega$  and Pr when  $t=0.15$  and  $\alpha=-3$  (blunt orientation) 69
- 5.11 The velocity profiles at  $x=0$  (forward stagnation point) for some values of  $\omega$  and Pr when  $t=0.15$  and  $\alpha=-3$  (slender orientation) 70
- 5.12 The velocity profiles at  $x=\pi$  (rear stagnation point) for some values of  $\omega$  and Pr when  $t=0.15$  and  $\alpha=-3$  (slender orientation) 70
- 5.13 The velocity profiles at  $x=0$  (forward stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=4$  (slender orientation) 71
- 5.14 The velocity profiles at  $x=\pi$  (rear stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=4$  (slender orientation) 71
- 5.15 The velocity profiles at  $x=0$  (forward stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=0.5$  (blunt orientation) 72
- 5.16 The velocity profiles at  $x=\pi$  (rear stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=0.5$  (blunt orientation) 72

- 5.17 The temperature profiles at  $x = 0$  (forward stagnation point) for some values of  $\alpha$  and  $t$  when  $Pr = 1$  and  $\omega = 0.5$  (blunt orientation) 73
- 5.18 The temperature profiles at  $x = \pi$  (rear stagnation point) for some values of  $\alpha$  and  $t$  when  $Pr = 1$  and  $\omega = 0.5$  (blunt orientation) 73
- 5.19 The temperature profiles at  $x = 0$  (forward stagnation point) for some values of  $\alpha$  and  $t$  when  $Pr = 1$  and  $\omega = 4$  (slender orientation) 74
- 5.20 The temperature profiles at  $x = \pi$  (rear stagnation point) for some values of  $\alpha$  and  $t$  when  $Pr = 1$  and  $\omega = 4$  (slender orientation) 74
- 5.21 The temperature profiles at  $x = 0$  (forward stagnation point) for some values of  $\omega$  and  $Pr$  when  $t = 0.15$  and  $\alpha = -3$  (blunt orientation) 75
- 5.22 The temperature profiles at  $x = \pi$  (rear stagnation point) for some values of  $\omega$  and  $Pr$  when  $t = 0.15$  and  $\alpha = -3$  (blunt orientation) 75
- 5.23 The temperature profiles at  $x = 0$  (forward stagnation point) for some values of  $\omega$  and  $Pr$  when  $t = 0.15$  and  $\alpha = -3$  (slender orientation) 76
- 5.24 The temperature profiles at  $x = \pi$  (rear stagnation point) for some values of  $\omega$  and  $Pr$  when  $t = 0.15$  and  $\alpha = -3$  (slender orientation) 76

- 5.25 The temperature profiles at  $x=0$  (forward stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=0.5$  (blunt orientation) 77
- 5.26 The temperature profiles at  $x=\pi$  (rear stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=0.5$  (blunt orientation) 77
- 5.27 The temperature profiles at  $x=0$  (forward stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=4$  (slender orientation) 78
- 5.28 The temperature profiles at  $x=\pi$  (rear stagnation point) for various values of Pr when  $t=0.15$  and  $\alpha=1$  and  $\omega=4$  (slender orientation) 78
- 5.29 Variation of the Nusselt number with  $t$  at  $x=0$  (forward stagnation point) for various values of  $\omega$  and Pr when  $\alpha=-3$  (blunt orientation) 80
- 5.30 Variation of the Nusselt number with  $t$  at  $x=\pi$  (rear stagnation point) for various values of  $\omega$  and Pr when  $\alpha=-3$  (blunt orientation) 80
- 5.31 Variation of the Nusselt number with  $t$  at  $x=0$  (forward stagnation point) for various values of  $\omega$  and Pr when  $\alpha=-3$  (slender orientation) 81
- 5.32 Variation of the Nusselt number with  $t$  at  $x=0$  (forward stagnation point) for various values of Pr when  $\alpha=1$  and  $\omega=0.5$  (blunt orientation) 81

5.33	Variation of the Nusselt number with $t$ at $x = \pi$ (rear stagnation point) for various values of Pr when $\alpha = 1$ and $\omega = 0.5$ (blunt orientation)	82
5.34	Variation of the Nusselt number with $t$ at $x = \pi$ (rear stagnation point) for various values of Pr when $\alpha = 1$ and $\omega = 0.5$ (blunt orientation)	82
5.35	Variation of the Nusselt number with $t$ at $x = 0$ (forward stagnation point) for various values of Pr when $\alpha = 1$ and $\omega = 4$ (slender orientation)	83
5.36	Variation of the Nusselt number with $t$ at $x = \pi$ (rear stagnation point) for various values of Pr when $\alpha = 1$ and $\omega = 4$ (slender orientation)	83
5.37	Variation of the Nusselt number with $t$ at $x = 0$ (forward stagnation point) for some values of $\alpha$ and $\omega$ when Pr = 1	84
5.38	Variation of the Nusselt number with $t$ at $x = \pi$ (rear stagnation point) for some values of $\alpha$ and $\omega$ when Pr = 1	85



## LIST OF SYMBOLS

$C_f$	-	skin friction coefficient
$C_p$	-	specific heat at constant pressure
erf	-	error function
$c$	-	thermal conductivity
$b$	-	length of the semi-minor axis
$a$	-	length of the semi-major axis
$b/a$	-	the ratio of the major and minor axis of cylinder
<b>g</b>	-	acceleration due to gravity
$Gr$	-	Grashof number
$Nu$	-	Nusselt number
$\bar{p}$	-	dimensional pressure
$p$	-	nondimensional pressure
$Pr$	-	Prandtl number
$q_w$	-	convection heat transfer coefficient
$Re$	-	Reynolds number
$\bar{t}$	-	dimensional time
$t$	-	nondimensional time
$t_s$	-	separation time
$\bar{T}$	-	dimensional fluid temperature
$T$	-	nondimensional fluid temperature
$T_w$	-	surface temperature
$T_\infty$	-	external temperature
$\bar{u}, \bar{v}$	-	dimensional velocity components along $\bar{x}$ and $\bar{y}$ axes
$u, v$	-	nondimensional velocity components along $x$ and $y$ axes

$U_\infty$	-	stream velocity
$\bar{x}, \bar{y}$	-	dimensional Cartesian coordinates measured along the surface of the cylinder and normal to it, respectively
$x, y$	-	nondimensional Cartesian coordinates measured along the surface of the cylinder and normal to it, respectively

#### Greek symbols

$\alpha$	-	mixed convection parameter
$\beta$	-	thermal expansion coefficient
$\phi$	-	angle between outward normal and downward vertical
$\gamma$	-	eccentric angle
$\kappa$	-	vortex viscosity
$\eta$	-	similarity variable
$\mu$	-	dynamic viscosity
$\tau_w$	-	wall shear stress
$\nu$	-	kinematic viscosity
$\rho$	-	density
$\psi$	-	stream function
$\omega$	-	constant

#### Superscripts symbols

$\prime$	-	differentiation with respect to $\eta$
----------	---	--

#### Subscripts symbols

$w$	-	wall condition
$\infty$	-	far field condition

**LIST OF APPENDICES**

<b>APPENDICES</b>	<b>TITLE</b>	<b>PAGE</b>
A	Matlab Program for Finding Numerical Solution of Unsteady Mixed Convection Flow over a Cylinder of Elliptic Cross Section near Forward and Rear Stagnation Points	97

## **CHAPTER 1**

### **INTRODUCTION**

#### **1.1 Research Background**

The transfer of heat through fluid (liquid or gas) caused by molecular motion is known as convection. Besides that, convection is also defined as a movement of fluids regardless of the cause in fluids mechanics field. In general, the convection type of heat transfer can be divided into two basic processes. The first process is named as free or natural convection and the second process is forced convection. Forced convection occurs when a fluids flow is induced by an external force, such as a pump, fan or a mixer, while free convection is caused by buoyancy forces due to density differences created by the temperature variations in fluids. However, when the effect in these both convections becomes significant, then the process is described combined forced and free convection, which is also known as mixed convection. The effect is particularly marked in situations where the forced fluid flow velocity is low and/or the temperature difference is large.

There are lot of problems about free convection constantly arise in engineering service. An example of free convection is the cooling process in heat exchanger components. Therefore, by understanding the properties of the convection occurring in the process, the lifespan of the heat exchanger component can be monitored and predicted.

In these recent years, unsteady flows have become significant in both different category of fluid mechanics and an area of convection heat and mass transfer. The problem of unsteady convective heat transfer has long been a major subject in the heat transfer theory because of its great importance from both a theoretical and practical viewpoint. The extra independent variables time which has been considered in the unsteady problem can increase the complexity of its solution procedure. The unsteady effects can arise in two situations. The first situation is due to self-induced motion of the body and the second situation is due to the fluctuations or nonuniformities in the surrounding fluid. Besides that, some devices are required to execute time-dependent motion in order to perform their basic functions (McCroskey, 1977).

In general, unsteady viscous phenomena play an important role in the reentry of space vehicles. Unsteady viscous flows have been studied quite widely and all the characteristic features of unsteady effects are now more or less familiar to fluids mechanicians. The problem of unsteady mixed convection boundary layer flow of Newtonian and Non-Newtonian fluid past a circular cylinder have been considered by Ingham and Merkin (1981) and Ali *et al* (2010), respectively.

In addition, the study of stagnation point flow has attracted much attention because of its capability in providing the governing equations to be much simplified besides allowing the process of bringing out all the essential features. The stagnation point solution, though it may be valid in a small region in the vicinity of stagnation point, may function as a starting solution for the solution over the entire body, as proven by Lok (2008).

Following the above studies, the present study aspires to obtain the unsteady mixed convection flow over a cylinder of elliptic cross section near forward and rear stagnation points for the case of constant wall temperature. This study considered the problem near both forward and rear stagnation point. In addition, this study also looks into the difference caused by blunt orientation and slender orientation. This boundary layer problem is solved by Keller's Box method described in Ali *et al* (2007). According to Keller (1978), we know that this method has been found to be

efficient and flexible in dealing with many type of problem, especially for free and mixed convection boundary layer flows. In fact, it is easily adaptable for solving equation of any order (Cebeci and Bradshaw, 1988)

## **1.2 Problem Statement**

The study will investigate the following questions; (i) How Prandtl number, mixed convection coefficient and time affect the results of skin friction, Nusselt number, velocity profile and temperature profile in unsteady mixed convection over a cylinder elliptic cross section near both forward and rear stagnation point? (ii) What are the effects of blunt orientation and slender orientation to the skin friction, Nusselt number, velocity profile and temperature profile in unsteady mixed convection over a cylinder elliptic cross section near both forward and rear stagnation point?

## **1.3 Objectives of the Study**

The objectives of this study are:

- i. To transform the non- dimensional governing equation of the problem into a system of non-similarity equation using stream function and similarity variables.
- ii. To solve the governing equation numerically using Keller box method and develop numerical algorithm using Matlab.
- iii. To determine the separation times of boundary layer near the forward and rear stagnation points.

- iv. To investigate the effects of Prandtl number, mixed convection coefficient and axis ratio for blunt and slender orientation on the velocity profiles, temperature profiles, skin friction, and Nusselt number.

#### **1.4 Scope of the study**

The unsteady mixed convection boundary layer flow is considered in an incompressible viscous fluid problem. The problem will be narrowed down to boundary layer flow over horizontal cylinders of elliptic cross section subjected to constant temperature. The analysis of this study is only focusing on the forward and rear stagnation point. The numerical scheme used is Keller box method and the numerical results are obtained from various values of time, Prandtl number, mixed convection coefficient and axis ratio for blunt and slender orientation. The results are discussed based on the velocity profile, temperature profile, Nusselt number and skin friction coefficient.

#### **1.5 Significant of study**

Mixed convection (combined forced and free convection) flow with and without mass transfer occurs in many technologies and industrial applications. Its applications are namely solar central receiver exposed to wind currents, nuclear reactors cooled during emergency shutdown, heat exchangers placed in low-velocity environments, boundary-layer control on airfoil, lubrication of ceramic machine parts and food processing. Mixed convection occurs during the motion of fluid that results from variety in density and heat change.

In environment and engineering services, mixed convection over cylinder is a basic and vital problem. Moreover, in manufacture industry, most of the manufacturing machine has its own heat exchanger components which are made

from tubes of elliptic cross section. The benefit of this design is it creates less resistance for cooling the fluid pass by. Thus, the study of heat transfer for an elliptic cross section cylinder is useful to create an effective and efficient heat exchanger component and design.

## **1.6 Outline of Dissertation**

This dissertation consists of six chapters including this introductory chapter, in which discuss about the background of research, the problem statement, objectives, scope and significant of the study. The literature review for the research problem is given in Chapter 2.

Chapter 3 contains a discussion on the mathematical formulation of the equations that involved in our problem of unsteady mixed convection boundary layer over a cylinder of elliptic cross section near forward and rear stagnation point.

Full explanation of the numerical method, the Keller box method are given in the Chapter 4, which are presented and described particularly for the problem in this study. Stepwise development of the method was stated. The Keller box method used in this study is programmed in Matlab. The complete program of the specific problem discussed in Chapter 4 is given the Appendix B.

Further, Chapter 5 includes the result and discussion of the problem. The numerical computation of results are presented both in the form of tables and graphs. Finally, Chapter 6 contains a summary of the dissertation and several recommendations for future research.



## REFERENCES

- Ahmad, S., Arifin, N. M., Nazar, R., and Pop, I. (2008). Free Convection Boundary Layer Flow over Cylinders of Elliptic Cross Section with Constant Surface Heat Flux. *European Journal of Scientific Research*. 23:613-625.
- Ahmad, S., Arifin, N. M., Nazar, R., and Pop, I. (2009). Mixed Convection Boundary Layer Flow Past an Isothermal Horizontal Circular Cylinder with Temperature-dependent Viscosity. *International Journal of Thermal Sciences* 48: 1943-1948.
- Ali, A., Amin, N., and Pop, I. (2010). Unsteady Mixed Convection Boundary layer from a Circular Cylinder in a Micropolar Fluid, *International Journal of Chemical Engineering*. 2010: 1-10
- Ali, A., Amin, N., and Pop, I. (2007). The Unsteady Boundary Layer Past a Circular Cylinder in a Micropolar Fluid. *International Journal of Numerical Methods for Heat and Fluids Flow*.17(7):692-714.
- Ariel, P.D. (1992). A Hybrid Method for Computing the Flow of Viscoelastic Fluids. *International Journal of Numerical Method in Fluids*. 14:757-774.
- Alessio, S. J. D., and Perera, R. N. (2009). Unsteady Free Convection from Elliptic Cylinder at Large Grashof Numbers. *International Journal of Heat and Mass Transfer*. 52: 5940-5953.
- Anati Ali (2010). *Unsteady Micropolar Boundary Layer Flow and Convective Heat Transfer*. Doctor Philosophy, Universiti Teknologi Malaysia, Skudai.
- Ali, A., Amin, N., and Pop, I. (2007). The Unsteady Boundary Layer Flow Past a Circular Cylinder in Micropolar Fluid. *International Journal of Numerical Method for Heat and Fluid Flow*. 17: 692-714.

- Bhattacharyya, S., and Pop, I. (1996). Free Convection from Cylinder of Elliptic Cross-section in Micropolar Fluid. *International Journal of Engineering Science*. 34:1301-1310.
- Bharti, R. P., Sivakumar, P., and Chhabra, R. P. (2008). Forced Convection Heat Transfer From an Elliptical Cylinder to Power-law Fluids. *International Journal of Heat and Mass Transfer*. 51.54:1838-1853.
- Ching, Y. C, (2007). Natural Convection from a Horizontal Cylinder of Elliptic Cross Section in Saturated Porous Media Using a Thermal Non-Equilibrium Model. *Proceeding of the 4<sup>th</sup> WSEAS International Conference on Heat and Mass Transfer*. January 17-19, 2007. Gold Coast, Queensland, Australia: WSEAS. 2007. 92-95.
- Ching, Y. C, (2009). Natural Convection from a Horizontal Elliptic Cylinder with Constant Heat Flux and Internal Heat Generation. *International Communications in Heat and Mass Transfer*. 36:1025-1029.
- Cebeci, T., and Bradshaw, P. (1988). *Physical and Computational Aspects of Convection Heat Transfer*. Springer-Verlag, New York.
- Devi, C. D. S., Takhar, H. S., and Nath, G. (1991). Unsteady Mixed Convection Flow in Stagnation Region Adjacent to a Vertical Surface. *Warme-und staffubertragung*. 26:71 – 79.
- Ingham, D. B., and Merkin, J. H. (1981). Unsteady Mixed Convection from an Isothermal Circular Cylinder. *Journal of Acta Mechanica*. 38: 55-69.
- Ishak, A., Nazar, R., Arifin, N. M., and Pop, I. (2008). Dual Solution in Mixed Convection Flow Near a Stagnation Point on a Vertical Porous Plate. *International Journal of Thermal Sciences*. 47: 417-422.

- Ishak, A., Nazar, R., Bachok, N., and Pop, I. (2010). MHD Mixed Convection Flow Near a Stagnation Point on a Vertical Permeable Surface. *Journal of Physica A*. 389: 40-46.
- Ishak, A. (2009). Mixed Convection Boundary Layer Flow over a Vertical Cylinder with Prescribed Surface Heat Flux. *Journal of Physica A*. 42: 1-8.
- Ibrahim, F. S., and Hamad, M. A. A. (2006). Group Method Analysis of Mixed Convection Boundary Layer Flow of a Micropolar Fluid near a Stagnation Point on a Horizontal Cylinder. *Journal of Acta Mechanica*. 181: 65-81.
- Keller, H. B., and Cebeci, T. (1971). Accurate Numerical Method for Boundary Layer Flows, I: Two-Dimensional Laminar Flows. *Proc. of the 2<sup>nd</sup> Int. Conference on Numerical Methods in Fluid Dynamics*. New York: Springer-Verlag.
- Keller, H. B., and Cebeci, T. (1972). Accurate Numerical Method for Boundary Layer Flows, II: Two-Dimensional Turbulent Flows. *AIAA Journal*. 10:1193-1199.
- Katagiri, M., and Pop, I. (1979). Unsteady Combined Convection from an Isothermal Circular Cylinder. *Journal of Applied Mathematics and Mechanics (ZAMM)*. 59: 51-60.
- Kumari, M., and Nath, G. (1989). Unsteady Mixed Convection Flow of Thermo-Micropolar Fluid on a Long Thin Vertical Cylinder. *International Journal of Engineering Science*. 27: 1507-1518.
- Lok, Y. Y., Phang, P., Amin, N., and Pop, I. (2003a). Unsteady Boundary Layer Flow of a Micropolar Fluid Near the Forward Stagnation Point of a Plane Surface. *International Journal of Engineering Science*. 41: 173–186.

- Lok, Y. Y., Amin, N., and Pop, I. (2003b). Unsteady Boundary Layer Flow of a Micropolar Fluid Near the Rear Stagnation Point of a Plane Surface. *International Journal of Thermal Sciences*. 42: 995–1001.
- Lok, Y. Y., Amin, N., and Pop, I. (2006). Unsteady Mixed Convection Flow of a Micropolar Fluid Near the Stagnation on a Vertical Surface. *International Journal of Thermal Sciences*. 45:1149-1157.
- Leal, L. G. (2007). *Advanced Transport Phenomena*. New York : Cambridge University Press.
- Lok Yian Yian. (2008). *Mathematical Modeling of a Micropolar Fluid Boundary Layer Near a Stagnation Point*. Doctor Philosophy, Universiti Teknologi Malaysia, Skudai.
- Merkin, J. H. (1977). Free Convection Boundary Layer on Cylinders of Elliptic Cross Section. *Journal of Heat Transfer*. 99: 453-457.
- Merkin, J. H. (1976). Free Convection Boundary Layer on an Isothermal Horizontal Cylinder. *Proceedings of the 1976 ASME-AIChE Heat Transfer Conference*. August 9-11, 1976. St Louis, USA.
- Mucogla, A., and Chen, T. S. (1978). Mixed Convection about a Sphere with Uniform Surface Heat Flux. *Journal of Heat Transfer*. 100: 542-544.
- Mccroskey, W., J. (1977). Some Current Research in Unsteady Fluids Dynamics, *Journal of Fluids Engineering*, 99(1): 8-39.
- Nazar, R., Amin, N., and Pop, I. (2003). Mixed Convection Boundary Layer Flow from a Horizontal Circular Cylinder with in Micropolar Fluids: Case of Constant Wall Temperature. *International Journal of Numerical Methods for Heat and Fluids Flow*. 13(1):86-109.

- Nazar, R., Amin, N., and Pop, I. (2003). Unsteady Mixed Convection Near the Forward Stagnation Point of a Two-Dimensional Symmetric Body. *Int Comm. Heat Mass Transfer*. 30:673-682.
- Nazar, R., Amin, N., and Pop, I. (2004). Mixed Convection Boundary Layer Flow from a Horizontal Circular Cylinder with a Constant Surface Heat Flux. *International Journal of Heat and Mass Transfer*. 40: 219-227.
- Nakai, S., and Okazaki, T. (1975). Heat Transfer From a Horizontal Circular Wire at Small Reynolds and Grashof Numbers – II. *International Journal of Heat and Mass Transfer*. 18: 397-413.
- Pop, I., and Na, T. Y. (1998). Darcian Mixed Convection Along Slender Vertical Cylinders with Variable Surface Heat Flux Embedded in a Porous Medium. *International Communications in Heat and Mass Transfer*. 33: 311-318.
- Seshadri, R., Sreeshylan, N., and Nath, G. (2002). Unsteady Mixed Convection Flow in the Stagnation Region of a Heated Vertical Plate due to Impulsive Motion. *International Journal of Heat and Mass Transfer*. 45: 1345-1352.
- Telionis, D. P. (1981). *Unsteady Viscous Flows*. Berlin: Springer.