OPTIMAL DESIGN AND SYNTHESIS OF RICE SUPPLY CHAIN

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OPTIMAL DESIGN AND SYNTHESIS OF RICE SUPPLY CHAIN

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To my dearest family:

Whose love has nourished and sustained me always.

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ABSTRACT

Continuous rise in energy cost and increased competitiveness have motivated rice enterprises to find new ways to improve productivity, reduce resource consumption, minimise waste generation, and ultimately, raise profitability. Consequently, there has been extensive research and development works in the conversion of the by-products from rice mills into value-added products. However, most of the works on the improvement of the rice mill and its downstream processes have been carried out in the piece-meal manner. There is a clear need for a systematic framework to optimise and improve the existing rice mill and its valueadded processes in an integrated, resource-efficient way. The new framework developed in this thesis includes four key components as described below. Component 1: A new cost-screening framework that is known as the resourceefficient screening (RES) method to screen the rice value chain and select the products and technologies targeted to maximise profit. Component 2: The framework for an integrated, resource-efficient (IRE) rice mill complex to synthesise the processes by evaluating the trade-off between the product revenue, capital investment and utility consumption. The model also considers the seasonality and degradation of rice resources with time. Component 3: A new framework called the integrated, resource-efficient (MSIRE) framework has also been developed for the rice enterprise that operates a cluster of rice mills at different locations. The MSIRE framework is used to determine the product portfolio for each rice mill, the location of the cogeneration system and its optimal scale, whether to expand the current processing facility or to build a new facility and the configuration of the paddy and rice husk logistic network. Component 4: A framework that combines the optimal logistic network of rice husk, with the rice mill's utility supply network has also been These frameworks were successfully implemented on several case developed. studies involving different scenarios of a national rice enterprise, and produced significant improvement in the enterprise's profitability.

ABSTRAK

Kos tenaga dan daya saing yang semakin meningkat telah mendorong pengusaha kilang beras untuk mencari alternatif bagi mengurangkan penggunaan sumber serta penghasilan sisa, dan seterusnya, meningkatkan keberuntungan. Banyak penyelidikan yang melibatkan penggunaan produk sampingan dalam proses pengilangan beras telah dilaksanakan untuk menghasilkan produk yang mempunyai nilai tambah. Namun begitu, kebanyakan penyelidikan untuk memperbaiki proses pengilangan beras telah dilaksanakan secara terpisah. Oleh itu, rangka kerja yang sistematik bagi mengintegrasi proses yang sedia ada dalam kilang beras dengan proses hiliran, dengan penggunaan sumber dengan cekap adalah amat diperlukan. Kaedah yang dipaparkan dalam tesis ini boleh dibahagikan kepada empat komponen sebagaiman yang dinyatakan di bawah. Komponen 1: Rangka kerja baru yang dikenali sebagai Resource-Efficient Screening (RES) melibatkan pemilihan rantaian nilai beras serta produk dan teknologi yang sewajarnya untuk menjana keuntungan yang maksimum. Komponen 2: Satu rangka kerja telah dibangunkan untuk sintesis proses dalam Integrated, Resource-Efficient (IRE) rice mill complex dengan menilai imbal-balik antara hasil produk, modal dan kos utiliti. Model IRE ini juga mengambil kira sifat bermusim serta potensi degradasi sumber padi dalam jangka masa yang tertentu. Komponen 3: Satu rangka kerja baru yang dipanggil Multisite Integrated, Resource-Efficient (MSIRE) juga telah dibangunkan untuk pengusaha kilang beras yang mengoperasikan sekelompok kilang padi di beberapa lokasi yang berbeza. Rangka kerja MSIRE digunakan untuk menentukan portfolio produk bagi setiap kilang beras, lokasi serta skala yang optimum untuk sistem cogeneration, keputusan sama ada meningkatkan kapasiti bagi proses yang sedia ada dalam fasiliti atau membina kilang yang baru dan konfigurasi rangkaian logistik bagi padi dan produk beras. Komponen 4: Satu rangka kerja juga dipaparkan untuk konfigurasi rangkaian logistik sekam padi yang optimum di kilang beras, dengan mengambil kira aspek jaringan bekalan utiliti di sesebuah kilang beras. Kaedah-kaedah ini telah berjaya diaplikasikan ke atas beberapa kes kajian industri beras di bawah senario yang berbeza, dan hasilnya menunjukkan peningkatan keberuntungan industri tersebut dengan ketara.

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LIST OF ABBREVIATIONS

CHF	-	Cyclonic husk furnace
FBD	-	Fluidised bed dryer
FFA	-	Free fatty acid
GAMS	-	Generalised Algebraic Modelling System
IBD	-	Inclined bed dryer
IRE	-	Integrated, resource-efficient
IRRI	-	International Rice Research Institution
LP	-	Linear programming
LP	-	Low pressure
LSU	-	Louisiana State University
MILP	-	Mixed integer linear programming
MILP	-	Mixed integer linear programming
MINLP	-	Mixed interger nonlinear programming
MP	-	Medium pressure
MPR	-	Material-Process-Resource
MSIRE	-	Multisite integrated, resource-efficient
NLP	-	Nonlinear programming
OUL	-	Optimal Utility-Logistc
PSE	-	Process systems engineering
RES	-	Resource Efficient Screening
RES	-	Resource-Efficient Screening
RM	-	Ringgit Malaysia
RPR	-	Resource-Process-Resource

LIST OF SYMBOLS

$AARHJ_i$	-	Annual available RH at internal rice mill <i>j</i>
AARHK _k	-	Annual available RH from external rice mill k
$ACCOSTB_b$	-	Annualised capital cost of biomass boiler b
ACCOSTC _c	-	Annualised capital cost of CHF c
ACRHJ _j	-	Annual transportation of rice husk from internal rice mill <i>j</i>
ACRHK _k	-	Annual transportation of rice husk from external rice mill <i>k</i>
AElecO	-	Annual electricity required from outsources
AVAIRES _{t,f,i}	-	Quantity of available resource i at location f during period t
AVRES _i	-	Amount of available external resource i
AVRES _{ivt}	-	Amount of available external resource i from location v during period t
BElecD _t	-	Basic electricity demand of drying equipment and office accessories at period <i>t</i>
B_i	-	By-product indicator of resource <i>i</i>
BYPRO _{it}	-	Amount of by-product <i>i</i> during period <i>t</i>
BYPRO _{t,pc,i}	-	Amount of by-product <i>i</i> from process complex <i>pc</i> during period <i>t</i>
BYREV	-	Revenue of by-product
CAP_{pz}	-	Capacity of process p with size z
CCAPIN _{pc,p,z}	-	Capacity index for process p at process site pc with capacity type z
CCOST	-	Capital cost of equipment
CCRH	-	Calorific value of rice husk

$CSTCOST_{pc}$	-	Construction cost of the process site at process site pc
DEMPRO _i	-	Demand of product <i>i</i>
DISFPC _{f,pc}	-	Distance between field f and process site pc
DISPC .		Distance between process site pc and another process site
DISF Cpc,pc'	-	pc'
DISPCS _{pc,s}	-	Distance between process site pc and sales centre s
DOH	-	Number of operating hours per day
DOH_p	-	Daily operating hour of process p
$EFFBB_b$	-	Efficiency of biomass boiler
$EFFCHF_c$	-	Efficiency of CHF
EFFFC	-	Efficiency of FBD coil
EFFIC	-	Efficiency of IBD coil
<i>EFFTURB</i> _b	-	Efficiency of condensing extraction turbine b
		Electricity requirement of biomass boiler and turbine b at
Elecob	-	period t
$ElecCHF_{ct}$	-	Electricity requirement of CHF c at period t (kwh)
$ElecD_t$	-	Electricity demand at period <i>t</i>
$ElecF_{ft}$	-	Electricity requirement of FBD at period t (kwh)
Elec C D.		Electricity generated from condensing extraction turbine
Liecobbt	-	b at period t
$ElecG_t$	-	Electricity generated at period t
$ElecI_{it}$	-	Electricity requirement of IBD at period t (kwh)
$ElecO_t$	-	Electricity required from outsources at period t
Electariff	-	Electricity Tariff (RM/mwh)
$ENBB_b$	-	Enthalpy change across biomass boiler
ENFBD	-	Enthalpy change of MP across FBD
ENIBD	-	Enthalpy change of LP across IBD
ENI D.		Enthalpy change between HP and LP across condensing
	-	extraction turbine b
ENMP.	_	Enthalpy change between HP and MP across condensing
LINIVII b	-	extraction turbine <i>b</i>
$EOPE_p$	-	Operation indicator of process p

		External utility indicator to allow for the intake of
LOI_u	-	external utility
EUI _u		External utility indicator to allow for the intake of
	-	external utility
FYCESSU		Excess amount of utility u at process site pc during period
EACESSU _{t,pc,u}	-	t
FYIRES		Amount of external intake resource i from venue v during
	-	period t
$EXPCOST_{p,z}$	-	Fixed cost of technology p with capacity z
$EXRES_i$	-	Amount of external intake resource <i>i</i>
EXRES _{it}	-	Amount of external intake resource <i>i</i> during period <i>t</i>
FXRFS	_	Transportation of external resource <i>i</i> between external
$LMLO_{t,f,pc,i}$	_	location f and process site pc during period t
FXII	_	Amount of external utility <i>u</i> at process site <i>pc</i> during
ЕЛО г,рс,и		period t
EXU_{ut}	-	Amount of external intake utility <i>u</i> during period <i>t</i>
FCOST	-	Total construction cost
<i>HEATCF</i> _{cft}	-	Heat supplied by CHF \underline{c} to FBD f at period t
<i>HEATCHF</i> _{ct}	-	Heat supplied by CHF c at period t
<i>HEATCI</i> _{cit}	-	Heat supplied by CHF c to IBD <i>i</i> at period t
<i>HEATF_{ft}</i>	-	Required heat of FBD at period t
<i>HEATI_{it}</i>	-	Required heat of IBD at period t
HEATLPI _{it}	-	Heat supplied by LP stream at period t
HEATMPF _{mt}	-	Heat supplied by MP stream at period t
HD		HP steam from boiler b to condensing extraction turbine
III bt	-	b at period t
		Amount of processing resource for technology p at
HRPRES _{t,pc,p}	-	process site pc for operating mode m during period t in
		one hour
HRPIL	_	Amount of processing resource at technology p at process
ин <i>О t,рс,р</i>	-	site <i>pc</i> during period <i>t</i> in one hour
ICI _{ip}	-	Indicator assigned to input material <i>i</i> to constrain the

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	-	Utility <i>u</i> feed into process <i>p</i> at process site <i>pc</i> during
$INU_{t,pc,p,u}$		period t
INV_i	-	Inventory indicator for resource <i>i</i>
NUDEC		Resource i at process site pc during period t being shifted
INVKES _{i,pc,t}	-	forward to period $t+1$ as inventory
INVRES _{it}	-	Inventory level of resource <i>i</i> during period <i>t</i>
LCOST	-	Total transportation cost
TD		LP saturated steam extracted from condensing extraction
LP_{bt}	-	turbine b period t
IDC		LP saturated steam extracted from condensing extraction
LPC_t	-	turbine b to cooling tower at period t
זמז		LP saturated steam extracted from condensing extraction
LPIit	-	turbine b to IBD coil at period t
$LWBB_b$	-	Lower bound of biomass boiler b
LWCHF _c	-	Lower bound of CHF <i>c</i>
$LWLP_b$	-	Minimum extraction rate of LP stream at turbine b
$LWMP_b$	-	Minimum extraction rate of MP stream at turbine b
MAT	-	Amount of primary material i fed into process p under
MAI ipmt		operating mode <i>m</i> during period t
MAT	-	Material i feed into process p at process site pc under
IVIAI t,pc,p,m,i		operating mode <i>m</i> during period <i>t</i>
мсм		Material composition matrix of resource i feed into
WICIW _{ipm}	-	operating mode <i>m</i> of process <i>p</i>
$MINOPE_p$	-	Minimum operating level of process p
MOD_p	-	Monthly operating day of process p
MD.		MP saturated steam extracted from condensing extraction
WIF bt	-	turbine b at period t
MDE.		MP saturated steam extracted from condensing extraction
ΙVIΓ Γ _{ft}	-	turbine b to FBD coil at period t
п	-	Life span of equipment

capacity of process p

 $IMRES_{i,pc,t}$

-

NOS	-	Number of seasons
NDE		Quantity of equipment that can be purchased for process
NF <i>Lp</i>	-	р.
OCL		Indicator assigned to system-generated resource <i>i</i> to
UCIip	-	constrain the capacity of process p
OCU		Indicator assigned to system-generated utility <i>u</i> to
OCO_{up}	-	constrain the capacity of process p
OPEINV _i	-	Amount of opening inventory for resource <i>i</i>
OPEINV _{i,pc}	-	Opening inventory of resource <i>i</i> at process site <i>pc</i>
PCOST	-	Total processing cost
$PCRHK_k$	-	Purchase cost of rice husk from external rice mill k
וחמ		Product demand indicator to denote the maximum
PDI_i	-	production level of product <i>i</i>
$Period_t$	-	Duration of period <i>t</i>
P_i	-	Product indicator for resource <i>i</i>
DDCM	-	Process-resource conversion matrix between resource <i>i</i>
PRCM _{pim}		and operating mode <i>m</i> of process <i>p</i>
DDEC	-	Amount of processing resource in operating mode m of
PKES _{pm}		process p
DDEC		Amount of processing resource in process p under
FKES pmt	-	operating mode <i>m</i> during period <i>t</i>
DDEC	-	Amount of processing resource at technology p at process
T KLSt,pc,p,m		site pc under operating mode m during period t
PRICEi	-	Unit price of product <i>i</i>
PRI_i	-	Price of resource <i>i</i>
PRODEM _{i,s}	-	Demand of product <i>i</i> at sales centre <i>s</i>
PROFIT	-	Annual profit
PRO_i	-	Amount of product <i>i</i>
PRO _{it}	-	Amount of product <i>i</i> during period <i>t</i>
$PRO_{t,s,i}$	-	Amount of product <i>i</i> at sales centre <i>s</i> during period <i>t</i>
DUCM		process-utility conversion matrix between utility <i>u</i> and
PUCM _{pum}	-	process <i>p</i> under operating mode <i>m</i>

DII	-	Amount of processing utility resource of technology p at
$\Gamma U_{t,pc,p}$		process site pc during period t in one hour
r	-	Interest rate
RCOST	-	Total resource cost
RES_i	-	Quantity of resource <i>i</i> in the system
$RES_{i,pc,t}$	-	Resource i at process site pc during period t
<i>RES_{it}</i>	-	Quantity of resource i in the system during period t
REV	-	Revenue
RHB _{bt}	-	Amount of biomass feed into boiler b at period t
<i>RHC</i> _{ct}	-	Amount of rice husk feed into CHF c at period t
ווות		Amount of rice husk transfer from internal rice mill j at
KHJ_{jt}	-	period t
		Amount of rice husk transfer from external rice mill k at
ΚΠK _{kt}	-	period t
RH_t	-	Amount of rice husk consumed at period t
SCU	-	System converted utility u by process p at process site pc
SC <i>U t,pc,p,u</i>		during period t
SCDES	-	Amount of self-generated resource <i>i</i> from the operating
SGRES _{ipm}		mode m of process p within the system
SCDES.	-	Amount of system-generated resource i from process p
SORESipmt		under operating mode m during period t
SCRES .	_	System-generated resource i by process p at process site
SORES _t ,pc,p,m,i	-	pc for operating mode m during period t
SCU	_	Utility u generated by process p under operating mode m
500 <i>t,pc,p,m,u</i>	-	at process site <i>pc</i> during period <i>t</i>
SGU	_	Amount of system-generated utility u from process p
500 upmi		under operating m during period t
TCEXRES _{t,i}	-	Transportation cost of external resource i during period t
TCIMRES	_	Transportation cost of intermediate resource <i>i</i> during
		period t
TCPRO t,i	-	Transportation cost of product <i>i</i> during period <i>t</i>
$TCRHJ_j$	-	Transportation cost of rice husk from internal rice mill j

$TCRHK_k$	-	Transportation cost of rice husk from external rice mill k
TRANSPRO _{t,i,pc,s}	-	Transportation of product i from process site pc to sales
		centre <i>s</i> during period <i>t</i>
TRANSRES _{t,i,pc,pc}		Transportation of resource i from process site pc to
	2'-	process site pc' during period t
UCM		The bonding index of input utility u and process p for
$UCM_{u,m,p}$	-	operating mode <i>m</i>
UCOST	-	Total utility cost
		Utility demand <i>u</i> of process <i>p</i> at process site <i>pc</i> during
UDEM _{t,pc,p,u}	-	period t
UDEM _{ut}	-	Demand of utility <i>u</i> during period <i>t</i>
ULCOST _{iv}	-	Unit transportation cost of resource i from venue v
$UPBB_b$	-	Upper bound of biomass boiler b
$UPCHF_c$	-	Upper bound of CHF c
$UPCOST_p$	-	Unit processing cost for process p
UPCOST _{pm}	-	Unit processing cost of process p for operating mode m
URCOST _i	-	Unit resource cost of resource <i>i</i>
UTCOST _i	-	Unit transportation cost of resource <i>i</i>
$UUCM_{p,u}$	-	Conversion yield of utility <i>u</i> via process p
<i>UUCOST</i> _u	-	Unit utility cost of utility <i>u</i>
VUD _{up}	-	Demand of utility <i>u</i> for one processing material unit <i>p</i>
Year	-	Operating hours in a year
$YEXP_{p,pc,z}$	-	Index for purchasing technology p with capacity z at
		process site pc
YOB _{bt}	-	Binary variable in operating biomass boiler b at period t
<i>YOC</i> _{ct}	-	Binary variable in operating CHF c at period t
YOEXP _{t,pc,p,z}	-	Index for determining the operation of technology p with
		capacity z at process site pc during period t
<i>YOP</i> _{tpz}	-	Number of process p equipment with capacity z being
		operated during period t
YPB_b	-	Binary variable in purchasing biomass boiler b
YPC_c	-	Binary variable in purchasing CHF c

YPC_{pc}	_	Index for constructing a process complex at process site
		pc
YP_{pz}		Number of process p equipment with capacity z being
	-	purchased

Greek Letters

Σ	-	Summation
\forall	-	All belong to

Subscripts

b	-	Index for biomass boiler and turbine
С	-	Index for CHF
f	-	Index of for paddy field and external rice mill (Chapter 6)
f	-	Index for fluidised bed dryer (Chapter 7)
i	-	Index for resource
i	-	Index for inclined bed dryer (Chapter 7)
j	-	Index for internal rice mill
k	-	Index for external rice mill
т	-	Index for operating mode
p	-	Index for process technology
pc	-	Index for process complex at process site
S	-	Index for distribution centre
t	-	Index for period

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CHAPTER 1

INTRODUCTION

1.1 Introduction

Rice industry is one of the most important food industries in the world. Three billion people across the world consume rice, as the main product of the industry. This chapter provides an outlook of the global and local rice industry, followed by an introduction of the research background and problem statement. Next, the research objectives and the scope of this work related to the development of new systematic techniques to design an integrated, resource-efficient (IRE) rice mill complex are described. Finally, this chapter highlights five key contributions of this thesis that relevant to the research field and the rice industry.

1.2 Rice Outlook

According to FAOSTAT (2010), the global rice industry produces 672.0 million tonnes of paddy (unmilled rice) in year 2010, as presented in Table 1.1. Asia region alone contributes over 90% with China and India contributing some 29.3% and 17.9% shares of the total global output, respectively. In South East Asia region, Vietnam is the main producer, as it produces 6% of global rice output.

Rice demand is expected to remain strong in the next few decades due to the economic and population growths in many countries across Africa and Asia (Mohanty, 2008). According to Timmer *et al.* (2010), the total rice consumption will be 450 million tonnes (milled basis) by year 2020, a 6.6 % growth as compared to 422 million tonnes in 2007.

Regions	Harvested Quantity	
	(million t)	
Africa	22.86	
Americas	37.17	
Asia	607.33	
China	197.21	
India	120.62	
Indonesia	66.41	
Bangladesh	49.36	
Vietnam	39.99	
Myanmar	33.20	
Thailand	31.60	
Malaysia	2.55	
Europe	4.44	
Oceania	0.22	
World	672.01	

Table 1.1 : Production quantity of paddy of year (FAOSTAT, 2009)

In Malaysia, 2.55 million tonnes of paddy is harvested from planting area of 673,745 hectares in year 2010 (FAOSTAT, 2010). However, in 2011, considering the damages caused by the flood due to the occurrence of "La Nina", the harvested area has been forecasted to decline to 667,000 hectares. Subsequently, the milled rice production is anticipated to decrease to 1.6 million tonnes. Notwithstanding, the demand for rice is expected to remain strong. Experts predict that the annual rice consumption will increase by 4.2 % to 2.7 million tonnes in year 2011, due to the influx of foreign workers and population growth, whose main staple food is also rice.

To address the demand increase in rice, the Malaysian government has highlighted this issue in Eighth Malaysian Plan (2001-2005) and the Ninth Malaysia Plan (2006-2010). In these plans, Malaysia aimed to achieve 72 % and 90 % of rice self-sufficiency level (SSL) by 2005 and 2010, respectively (Yeong-Sheng *et al.*, 2009). However, in the Tenth Malaysia Plan (2011-2015), the target has been revised to 70 % of rice SSL by 2015 (Ho, 2011). With that, several measures have been taken by the government to stabilise the rice supply, for instance, by maintaining the rice stockpile at 292,000 tonnes or sustained consumption for 45 days. Also, the government will establish a long-term contract with countries to import rice, with the agreements to export palm oil or oil products to the corresponded countries. Note that no new paddy cultivation area will be assigned, with government aim to maintain or improve the rice production rate by upgrading the infrastructure of the existing planting areas.

1.3 Rice Supply Chain in Malaysia

The rice supply chain in Malaysia can be divided into the upstream and downstream industries. Figure 1.1 shows the rice supply chain in Malaysia. The activities of upstream industry consists of paddy harvesting, drying, rice milling and packaging plant, whilst the downstream industry involves value-process industry, for instance, vermicelli plant, rice flour mill, animal feed mill, rice bran oil plant. These products will be delivered to the wholesalers, before reaching the retailers or consumers.

For the upstream industry, Wong *et al.* (2010) reported some important figures in the year 2007, including:

- a) 10 seed centres are in operation to supply seed to approximately 138,000 farmers, based on the subsidy figure.
- b) The paddy harvested by the farmer was sold to 226 mills.
- c) The products from these mills were purchased by 1239 wholesalers.
- d) Local and imported rice were supplied to 44,637 retail outlets.

e) These rice products were then sold to 27.17 million of consumers.

Note that the rice mills produce a significant quantity of by-products such as broken rice, rice bran and rice husk. In the current practice, the rice milling company only utilises a small portion of these by-products at full economic potential. Rice husk is utilised as fuel for generating thermal energy that are required by the drying facilities. However, most of the by-products will be sold directly to the downstream industries at a subsistent price.

1.4 Problem Background

Up until now, most researchers, government agencies and rice companies have focused on research related to upstream rice-processing activities, for instance, paddy yield and soil fertility improvement. Yet in a newspaper article titled "Understanding the real causes of padi crisis", Jegatheesan (2003) has stressed that the limited drying capacities of rice mills is the bottleneck of the rice industry. During the peak drying period, the delay in the drying of harvested paddy will cause the quality degradation that can adversely affect the yield and the productivity of rice mills. The loss of productivity will hamper the efforts of government in improving the upstream activities' productivity. Besides, the existing by-products from rice mills are not fully utilised by the rice company (Wong *et al.*, 2010). The aforementioned challenges, along with the continuous rise in the energy cost and stricter environment regulations, have combined to emphasise the growing importance of the optimal planning and synthesis of a resource-efficient network of processes for the rice industry, i.e., IRE rice mill complex.

The IRE rice mill complex can be defined as an optimum rice mill network design that enhances its profitability by efficiently utilising its existing by-products, to produce value-added products and energy products that includes heat and electricity. The IRE complex considers the trade-off between processes, utility system and logistic network. To date, the concept of an IRE rice mill complex is relatively new for rice industry, although there have been extensive amount of research works on process integration and supply chain integration in the conventional integrated petrochemical industry, pulp and paper industry and the bio-refinery industry. The research works in this study represents the evolution of process engineering applications beyond the domain of traditional chemical processes, into the realm of the rice industry.

Analysis of the existing literature shows that there is only one study focusing on the rice supply chain modelling (Wong, 2004). The contributions of that study were twofold. The first is to identify the bottleneck for the drying and storage capacities for the rice industry. The second is to evaluate the economic performance of the different scenarios that involves the capacity adjustments of rice drying and milling. The study, however, has not considered by-product utilisation and the utility systems. In addition, the study has also assumed that the user has predefined the technology and the equipment capacity. Clearly there is a need for a systematic approach of planning and designing an IRE rice mill that integrates the efficient utilisation of resources utilisation that includes utility systems.

In this work, a new cost-screening framework that known as Resource Efficient Screening (RES) has been introduced to screen and select the product and technology involved in rice value chain with the objective of maximising the profit. Subsequently, the concept of an IRE rice mill complex is introduced and applied for the first time in this work, by deploying a IRE framework that analyse the trade-off between product revenue, capital expenditure and utility consumption. The model is further extended into a multisite integrated, resource-efficient (MSIRE) framework that considers the supply chain management aspects of rice mill complexes at multiple sites. Finally, a framework that designs the optimal logistic network of rice husk in a rice mill that considers the utility supply network has been developed.



Figure 1.1 The rice supply chain in Malaysia

1.5 Problem Statement

Given a number of resources (materials) and a number of processes, it is desired to synthesise a resource-efficient network of processes that can preferentially utilise by-products of a process to produce energy and value-added products. Given also are the yield of each process, and its supply (inlet) composition. The flowrate of each resource is unknown and is to be determined to maximise the profit.

The flowrate of resources are bounded by their availability in the process complex and may not exceed the specified limits. On the other hand, certain resources and utilities can be purchased from sources external to the rice mill complex. The flowrates of resources are to be determined by considering the overall profit of the resource-efficient process network.

1.6 Research Objective

The main objective of this research is to develop a new systematic framework for designing an IRE process complex for the rice industry. The sub-objectives include performing

- 1) Optimal resource allocation and profit targeting for a rice value chain
- Synthesis of an integrated process-utility network for a single-site IRE rice mill complex
- Design and resource allocation planning for an integrated processutility-logistic network for a cluster of IRE rice mill complex (multiple sites)
- Design and configuration of an integrated rice husk logistic and utility network of a rice mill

1.7 Scope of the Work

The scope of this research includes:

- Analysing the state-of-the-art procedure on supply chain and process optimisation in rice industry, including its features, shortcomings and potential improvement.
- 2) Identifying the key technologies in processing the by-products.
- Developing a systematic framework for targeting the maximum profit and resource utilization planning for a set of rice resources. The developed model is then solved using Generalised Algebraic Modelling System (GAMS).
- 4) Developing a systematic framework for targeting the maximum profit and synthesing the integrated process-utility network for an IRE rice mill complex. The developed model is then solved using Generalised Algebraic Modelling System (GAMS).
- 5) Developing a systematic framework for rice supply chain planning that caters for both private rice miller and rice enterprise using mixed integer linear programming (MILP). The developed model is then solved using Generalised Algebraic Modelling System (GAMS).
- 6) Developing a systematic framework for designed the integrated rice husk logistic-utilty network for a rice mill that consist of cogeneration system and cyclonic husk furnace using mixed integer linear programming (MILP). The developed model is then solved using Generalised Algebraic Modelling System (GAMS).
- Applying the optimisation models on industry case studies to demonstrate the effectiveness of the proposed framework in solving problems.
- Comparing the economic performance of conventional rice mill and IRE rice mill complex.

1.8 Research Contributions

The key specific contributions of this work are summarised as follows:

- A new optimisation model known as *Resource-Efficient Screening* (*RES*) model for synthesising the resource-efficient network for rice value chain.
 - A generic model has been developed to obtain optimal product portfolio and process selection, along with its resource allocation strategy while maximising the profit.
- A new optimisation model known as *IRE model* to design IRE rice mill complex.
 - The concept of IRE rice mill complex is introduced. A multiperiod generic model is able to solve the complex design problem that considers resource availability, shelf-life issue, and variation of heat and electricity demand across the periods, energy supply options, trade-off of by-product selling and further processing, supply and demand constraints to achieve maximum profit.
- A new optimisation model known as *Multi-Site Integrated, Resource-Efficient (MSIRE) model* for designing IRE rice mill complexes at multiple sites.
 - A generic mixed integer linear programming (MILP) model that is capable of determining the design of IRE rice mill complex, resource allocation and logistic network at different process sites.
- 4) A new process network for an IRE rice mill complex
 - A process network that incorporates rice milling process with other value-added process.
- 5) A new optimisation model known as *Optimal Utility-Logistic (OUL) model* to design and configure rice husk logistic and utility network of a rice mill that includes a cogeneration system.
 - A MILP has been developed based on the superstructure of a rice mill that considers rice the husk logistic network and the

utility configuration to simultaneously design the cogeneration system and configure the logistic-utility network.

Appendix highlights all the publications and the corresponding key contributions of this thesis towards the new body of knowledge in designing and planning of an IRE rice mill.

This thesis consists of six chapters. Chapter 1 gives an overview of the rice industry issues, problem background, problem statement, objectives and scope of the research which aims to develop new systematic framework for designing an IRE rice mill complex using the mathematical approach. Chapter 2 of this thesis describes the fundamental theory and relevant literature related to the design of an IRE rice mill complex. Chapter 3 presents a detailed methodology of this study to achieve the targeted objectives. Chapter 4, 5, 6, 7 present the results and discussion from the application of new methods on the rice industry to showcase the effectiveness and advantages of the developed methodology. Finally, Chapter 8 summarises the key contributions of this research, prior to the recommendation of possible future work. Figure 1.2 shows the flow and linkage of the chapters.



Figure 1.2 Flow diagram illustrating the conceptual link among the chapters

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