# EFFECT OF VARIABLES ON THE PINEAPPLE POWDER PRODUCTION USING MICROWAVE SPRAY DRYER

SOUD ALI SOUD

UNIVERSITI TEKNOLOGI MALAYSIA

# EFFECT OF VARIABLES ON THE PINEAPPLE POWDER PRODUCTION USING MICROWAVE SPRAY DRYER

## SOUD ALI SOUD

A dissertation submitted in partial fulfillment of the requirements for the award of the degree of Master of Engineering (Chemical)

Faculty of Chemical Engineering

Universiti Teknologi Malaysia

MAY 2011

I dedicate this thesis to my parents, family and siblings

#### ACKNOWLEDGEMENT

At first, I would like to express my sincere appreciation and gratitude to my supervisor Associate Professor Adnan Ripin, for encouragement, critics, motivation, guidance, precious advice. Without his restless efforts and motivations, I might not have able to produce this thesis. I am also indebted to the laboratory technicians, Arsad Abu Hassan, Mohammad Rafiza Othman and Mohd Nur Shairray Jais for assisting me throughout this research work. Lastly, I wish to thank my parents, family and siblings. Without their patience, understanding, support and most of love, the completion of this thesis would not be possible.

#### ABSTRACT

The aim of this research is to produce pineapple powder with high qualities by using microwave rig assisted spray drying (MWSD). In previous research used (MWSD) operated at atmospheric pressure to obtain pineapple powder with high inlet air temperatures. All know the effect of high temperature on the foods product especially fruits, it make thermal degradation of powder product, so the final product lose some characteristics. In this study, the drying process carried out with low inlet air temperatures. The experiments were conducted keeping constant the nozzle size, feed flow rate and maltodextrin concentration (DE12): 1mm, 25 ml/min and 25% w/w respectively. Drying was carried out by using 1000 Watt microwave power intensity and with the different inlet air temperatures (40-100 °C). Also, drying was conducted using 80°C inlet air temperature and with the different microwave power intensities (700-1600 Watt). The product powder was analyzed for moisture content, bulk density and solubility. In two cases, moisture content and bulk density are inversely proportional to the inlet air temperature and microwave power intensity, whereas solubility proportional to the inlet air temperature and microwave power intensity. The best result when inlet air temperature 80°C and microwave power intensity 1000Watt, will produce pineapple powder with 3.91% moisture content, 0.59g/ml bulk density and 33 sec powder solubility. The results showed that the data were adequately fitted into the second order polynomial model.

## ABSTRAK

Tujuan penyelidikan ini adalah untuk menghasilkan serbuk nanas dengan kualiti yang tinggi dengan menggunakan rig gelombang mikro dibantu oleh pengering sembur (MWSD). Dalam kajian sebelumnya dengan menggunakan (MWSD), ia dikendalikan pada tekanan atmosfera untuk mendapatkan serbuk nanas dengan suhu udara masuk yang tinggi. Ramai orang mengetahui pengaruh suhu yang tinggi terhadap produk makanan terutama buah-buahan, ia menyebabkan penyusutan terma bagi produk serbuk, jadi produk akhir akan kehilangan beberapa ciri. Dalam kajian ini, proses pengeringan dilakukan dengan suhu udara masuk yang rendah. Eksperimen ini dijalankan dengan menggunakan saiz muncung, kadar aliran masuk dan kepekatan maltodextrin (DE12) tetap pada nilai masing-masing: 1mm, 25 ml/minit dan 25% w/w. Pengeringan dilakukan dengan menggunakan keamatan kuasa gelombang mikro 1000 Watt dan aliran suhu udara masuk yang berbeza (40-100 °C). Selain itu, pengeringan juga dilakukan dengan menggunakan suhu aliran masukan 80°C dan dengan tenaga gelombang mikro yang berbeza (700-1600 Watt). Serbuk produk dianalisis untuk kandungan lembapan, ketumpatan pukal dan keterlarutan. Dalam dua kes, kandungan lembapan dan ketumpatan pukal adalah berkadar songsang dengan suhu udara masukan dan keamatan gelombang mikro. Keputusan yang terbaik adalah pada suhu udara masuk 80 °C dan keamatan gelombang mikro 1000Watt akan menghasilkan serbuk nanas dengan kandungan lembapan 3.91%, ketumpatan pukal 0.59g/ml dan keterlarutan serbuk 33 saat. Keputusan menunjukkan bahawa data ujikaji adalah bersesuaian dengan model polinomial turutan kedua.

# TABLE OF CONTENTS

СНАРТЕ	CR TITLE	PAGE
	TITLE PAGE	i
	DECLARATION	ii
	DEDICATION	iii
	ACKNOWLEDGEMENT	iv
	ABSTRACT	V
	ABSTRAK	vi
	TABLE OF CONTENTS	vii
	LIST OF TABLES	Х
	LIST OF FIGURES	xii
	LIST OF SYMBOLS	xvi
	LIST OF ABBREVIATIONS	xvii
1	INTRODUCTION	1
	1.1 Research Background	1
	1.2 Problem Statement	3
	1.3 Objectives of research	3

	1.4 Scopes of research	4
2	LITERTURE REVIEW	5
	2.1 Pineapple	5
	2.2 Microwave	8
	2.3 Spray Drying Process	17
	2.4 A review on Previous Experiments	25
	2.4.1 Using maltodextrin as drying aid	25
	2.4.2 Experiment used pre-treatment and air-drying	
	to produce pineapple powder	27
	2.4.3 Experiment used Microwave alone	29
	2.4.4 Experiment used Vacuum-Microwave	31
	2.4.5 Experiment used Hot Air and Vacuum Microwave	
	Combination	33
	2.5 Produce pineapple powder using microwave assisted spray	
	Drying process (MWSD)	35

viii

41

## **3** METHODOLOGY

3.1 Preparation of Pineapple Juice 41

3.2 Microwave Oven with built-in Spray Drying	44
3.3 Analysis Method	48
3.3.1 Moisture Content	48
3.3.2 Bulk Density	48
3.3.3 Solubility	49

4	RESULTS AND DISCUSSIONS	50
	4.1 Introduction	50
	4.2 Effect of Inlet air Temperature on Pineapple Powder	51
	4.3 Effect of Microwave Power intensity on Pineapple Powder	54
5	CONCLUSION AND RECOMMENDATIONS	59
	5.1 Conclusion	59
	5.2 Recommendation	60

REFERENCES

61

іх

## LIST OF TABLES

TABLE NO.TITLE		PAGE
2.1	Pineapple % composition.	6
2.2	Standard food requirement recommended by IDF and ADMI.	24
2.3	Total time required (pre-treatment + air-drying) to reduce	
	90% and 95% of the initial water content of the fruit.	29
2.4	Time of drying required to reduce the moisture content of each	
	samples to a given level.	32
2.5	Pineapple powder properties of moisture content, bulk density	
	and solubility at constant inlet temperature, feed flow rate	
	and nozzle size.	
2.6	Summary of results obtained from experimental studies	
	with and without microwave power intensity.	40

4.1	Pineapple powder properties of moisture content, bulk	
	density and solubility with different inlet air temperatures	
	and constant microwave power intensity, feed flow rate and	
	nozzle size: 1000 watt, 25 ml/min and 1mm respectively.	51
4.2	Discouple neuronantics of maintum content hulls	
4.2	Pineapple powder properties of moisture content, bulk	
	density and solubility with different microwave power intensities	
	and constant inlet air temperature, feed flow rate and	
	nozzle size: 80 °C, 25 ml/min and 1mm respectively.	55

## LIST OF FIGURES

FIGURE NO.	TITLE	PAGE
2.1	Main pineapple producers in Asia (FAO, 2009)	7
2.2 a	The electromagnetic (EM) spectrum.	9
2.2 b	The electromagnetic (EM) spectrum and the microwave range.	
	The most commonly used frequency is 2.45 GHz with a wav	elength
	of 12.2 cm (Fawwaz, 2004).	9
2.3	Interaction of microwaves with materials (Kingston, 1997)	11
2.4	Molecular oscillations of polarisable substances under the influence	e
	of an alternating electric field.	12
2.5	Schematic of solution heating by conduction (left) and microwave	
	energy(right) (Be'atrice and Philippe, 2002).	4
2.6	Direction of the heat and mass transfer during microwave assis	ted
	and hot air drying (Araszkiewicz et al., 2007).	16
2.7	Schematic diagram of spray drying process (Patel et al. 2009)	18
2.8	Rotary type atomizer.	19
2.9	Nozzle type atomizer.	20
2.10	Different types of spray/hot air contact (Larry et al. 2008)	21

2.11	Spray dryer type co-current and open cycle layout	
	(Larry et al. 2008)	23
2.12	Spray dryer type co-current and closed cycle layout	
	(Larry et al. 2008)	23
2.13	Effect of different percentages of maltodextrin on	
	pineapple powder	27
2.14	Drying curves of parsley leaves under various microwave	
	power intensities: ×, 900 W; ▲, 810 W; ●,720 W; ■, 630 W;	
	$\square$ , 540 W; Δ, 450 W; ο, 360 W ( Soysal, 2004)	30
2.15	Diagram of vacuum-microwave drying experimental stand	
	(Markowski et al., 2007).	31
2.16	The way of transfer of energy on hot air drying and	
	microwave vacuum drying (Sutar and Suresh, 2007).	
2.17	Schematic diagram of the vacuum microwave dryer	
	(Zhang et al., 2006).	
2.18	Powder moisture content as a function of microwave power	
	intensity at constant inlet temperature, feed flow rate and nozzle	
	size(Norashikin,2010).	38

2.19	Powder bulk density as a function of microwave power	
	intensity at constant inlet temperature, feed flow rate and	
	nozzle size.	38
2.20	Powder solubility as a function of microwave power	
	intensity at constant inlet temperature, feed flow rate and	
	nozzle size.	39
3.1	The flow chart of microwave spray dryer experimental	
	procedure	43
3.2	Schematic representation of the microwave assisted spray	
	drying system	45
3.3	Conventional Spray Dryer (Separation Lab II, Faculty of	
	Chemical and Natural Resources Engineering, Universiti	
	Teknologi Malaysia, Skudai, Johor)	45
3.4	(a) Magnetron with fan cooling (b) Inside heating cavity (c)	
	cyclone coordination (d) control system of the Microwave	
	assisted Spray Drying (MWSD)	46
3.5	(a) Air compressor and (b) Electrical Heater	47
3.6	Moisture Analyzer MB25	48
3.7	Solubility test apparatus	49
4.1	Powder moisture content as a function of inlet air temperature at	•
	constant microwave power intensity, feed flow rate and nozzle	
	size.	52

xiv

4.2	Pineapple powder bulk density as a function of inlet air temperature	
	at constant microwave power intensity, feed flow rate and nozzle	
	size.	53
4.3	Pineapple powder solubility as a function of inlet air temperature at	
	constant microwave power intensity, feed flow rate and nozzle	
	size.	54
4.4	Powder moisture content as a function of microwave power intensity	
	at constant inlet air temperature, feed flow rate and nozzle size.	56
4.5	Powder bulk density as a function of microwave power intensity at	
	constant inlet air temperature, feed flow rate and nozzle size.	57
4.6	Powder solubility as a function of microwave power intensity at	
	constant inlet air temperature, feed flow rate and nozzle size.	58

# LIST OF SYMBOLS

±a	-	redness
±b	-	yellowness
db	-	dry basis
L	-	lightness
Tg	-	glass transition temperature
%v/v	-	percentage of volume
wb	-	wet basis
%w/w	-	percentage of weight

# LIST OF ABBREVIATIONS

AD	-	Air drying
ADMI	-	American Dry Milk Institute
ADVMD	-	Combination of air and vacuum microwave drying
CIE	-	Commission Internationale de L'Eclairage
DE	-	Dextrose equivalent
GA	-	Gum Arabic
IDF	-	International Dairy Federation
ISM	-	Frequencies for industrial, scientific and medical purposes
MD	-	Maltodextrin
MWSD	-	Microwave assisted Spray Drying
SD	-	Spray Drying
VMD	-	Vacuum microwave drying

#### **CHAPTER 1**

#### **INTRODUCTION**

#### 1.1 Research Background

Pineapples (Ananas Comosus) one of the most popular tropical and subtropical fruits. It has attractive flavor and refreshing sugar-acid balance. Pineapples are largely grown in several countries such as Malaysia, Thailand, Philippines, Taiwan, Hawaii, Caribbean area, Mexico, Australia, South Africa and Kenya (Fuster et al., 1995). However only a limited quantity of pineapple products such as canned juice, canned fruit and frozen juice concentrate, is produced. Furthermore misuse the right way for harvest many quantities of pineapple can be wasted (Nicoleti et al., 2001). There are many uses of pineapple. It is used in baby foods, biscuit products, flavoring agent in ice cream, salads, dessert and bakery. Also is used in paper and medicine industries and food for livestock when the pineapple canning, drying and juice extraction.

One of the establish method of food preservation is dehydration. The objective from any drying process is reduce moisture content in foods to a level low enough to prevent undesirable biochemical reactions and microbial growth (Feng et al., 2001) The most common method to produce powders is spray drying. During the last two decades intensive researches were made about spray drying to develop its work. The definition of spray drying is a technique change the feed from a fluid state to dried particulate. The feed can be liquid, slurry, emulsion, gel or paste. The final product may take the shape of a powder, granulate or agglomerate according to the physical and chemical properties of the feed, the final powder specification and drying characteristics. This technique involves spraying (atomizing) the feed into very hot air inside a large chamber (Patel et al., 2009). The disadvantages of this method are: large equipment, expensive, use high temperature and long drying time this may cause thermal degradation in the final products.

Microwaves have been used as a heat source since the 1940 (Mermelstein, 1997). Currently, microwave is applied in many food manufacturing and chemical processes for dehydration (drying) and finishing fruits, vegetables and herbs. As well as for sintering of ceramics, heating and reheating, thawing (melting), tempering of frozen food like meat and fish. Also, baking, sterilization, cooking and precooking, pasteurization of ready meals, blanching and phyto-extract.

In a microwave drying system, the microwave energy can easily penetrate into the material. The quick energy absorption causes rapid evaporation of water, creating an outward flux of rapidly escaping vapour, thus, both thermal gradient and moisture gradient are in the same direction (Hu et al., 2007). In conventional drying methods the directions of heat and mass transfer are opposite. The outer layer of the product becomes dry first, forms a poor heat conductor which hinders the dehydration process. As a result increase drying time.

According to Norashikin (2010), used a new technique to produce pineapple powder. She combined two methods for drying in one equipment, this new method called microwave assisted spray drying process (MWSD) operated at atmospheric pressure, and use high temperatures. In this research, the drying process use low temperatures at atmospheric pressure to produce pineapple powder by using same equipment.

### **1.2 Problem Statement**

In conventional and combined methods use hot drying medium (usually hot air) to dry materials. All know the effect of high temperatures on the sensitive foods especially fruits, it make thermal degradation of powder product, so the final product lose some characteristics such as vitamins, flavor and color compounds. Furthermore, the hot air cause oxidation for many sensitive components. Also, increase the consumption of energy which used on heater to heat air and as a result waste money. For all these reasons prefer to apply low temperatures.

## **1.3** Objective of research

The objectives of this study are:

- i. To study the effect of operating parameters such as inlet air temperature and microwave power intensity to the powder product.
- ii. To examined the quality of the product due to moisture content, bulk density and solubility.

## 1.4 Scopes of research

The scopes of this research consists as below:

- Sample preparation.
  Prepare pineapple juice from fresh pineapple. Add water and maltodextrin to this juice. Introduce the solution to drying process.
- ii. Study the drying process using varies inlet air temperatures (40-100 °C) for constant microwave power intensity (1000 Watt).
- Study the effect of varies microwave power intensities (700-1600 Watt) at constant inlet air temperature (80°C).

#### REFERENCES

- Abdurahman H. N. (2006). Emulsion stability and microwave demulsification of crude oil emulsion. Phd, University Technology Malaysia, Skudai.
- Adhikari B., Howes T., Bhandari, B. R. and Troung, V. (2004). Effect of addition of maltodextrin on drying kinetics and stickiness of sugar and acid-rich foods during convective drying experiments and modelling. Journal of Food Engineering, 62, 53–68.
- Alamilla-Beltran L., Chanona-Pe´rez J.J., Jime´nez-Aparicio A.R., Gutie´rrez-Lo´pez
  G.F. (2005) Description of morphological changes of particles along spray
  drying Journal of Food Engineering 67, 179–184.
- Altan, A. and Maskan, M. (2005) Microwave assisted drying of short-cut (ditalini) macaroni: Drying characteristics and effect of drying processes on starch properties, Food Research International, 38, 787–796.
- Amer A. S. (2004). Solvent extraction of essential oils from plants using microwave technique. Phd, University Technology Malaysia, Skudai.
- Ana P. Bartolomk, Pilar Rupbrez and Carmen Fuster (1995). Pineapple fruit: morphological characteristics, chemical composition and sensory analysis of Red Spanish and Smooth Cayenne cultivars. Food Chemistry, 53, 75-79.

- Araszkiewicz M., Antoni K., Anita L. and Michal L. (2007) Microwave drying of various shape particles suspended in an air stream Transp Porous Med 66, 173– 186.
- Be´atrice K. and Philippe C. (2002). Recent Extraction Techniques for Natural Products: Microwave-assisted Extraction and Pressurised Solvent Extraction. Phytochemical Analysis, 13, 105–113.
- Beaudry C., Raghavan G. S. V. and Rennie T. J. (2003), Microwave finish drying of osmotically dehydrated cranberries, Drying Technology, 21(9):1797-1810.
- Bemiller, J. N., & Whistler, R. L. (1996). Carboydrates. In O. R. Fenemma (Ed.), Food chemistry (3rd ed., pp. 157–224). New York: Marcel Dekker.
- Bruce, R. W. (1988). Microwave Processing of Materials: Mat. Res. Soc. Symp. Proc., 124, 33-43.
- Chegini R. and Ghobadian B. (2007) Spray Dryer Parameters for Fruit Juice Drying World Journal Agriculture Science. 3 (2), 230-236.
- Chomchalow, N.( 2004). Pineapple. Fruits of Vietnam. (P 57) . FAO 2004.
- Corrigan, O. I. (1995). Thermal analysis of spray dried products. Thermochimica Acta. 248, 245-258.
- Datta, A. K. (1990). Chemical Engineering Progress. Oxford: Clarendon Press, 47-53.
- El-Tinay, A.H. and Ismail, I.A., (1985). Effect of some additives and processes on the characteristics of agglomerated and granulated spray-dried Roselle powder. Acta Alimentaria Hungaricae 14 (3), 283–295.

- Erle, U. and Schubert, H. (2001). Combined osmotic and microwave– vacuum dehydration of apples and strawberries. Journal of Food Engineering, 49(2/3), 193–199.
- FAO( 2009), A case study of tropical fruits in Asia, with special reference to mangoes and pineapples. Rome, 9 11 December.
- Fawwaz, T. U. (2004) Fundamentals of Applied Electromagnetics, Pearson Prentice Hall.
- Feng H., J. Tang and R. P. Cavalieri, O. A. Plumb (2001), Heat and Mass Transport in Microwave Drying of Porous Materials in a Spouted Bed. AIChE Journal, Vol. 47, No. 7: 1499-1512.
- Goose, P.G. and Binsted, R., (1964). Allied tomato products. In: Tomato paste, puree, juice and powder (1st ed.), Food Trade Press, UK, London. 124–126.
- Goula, A.M. and Adamopoulos, K.G. (2005). Spray drying of tomato pulp in Dehumidified air: II. The effect on powder properties. Journal of Food Engineering, 66, 35-42.
- Joanna Bondaruk , Marek Markowski, Wioletta Błaszczak (2007), Effect of drying conditions on the quality of vacuum-microwave dried potato cubes, Journal of Food Engineering 81, 306–312.
- Khraisheh, M. A. M., Cooper, T. J. R. and Magee, T. R. A. (1997). Shrinkage characteristics of potatoes dehydrated under combined microwave and convective air conditions. Drying Technology, 15, 1003-1022.

- Kingston, H. M. (1997). Microwave-Enhanced Chemistry. Washington, DC. American Chemical Society, 258-267.
- Larry R. Genskow, Wayne E. Beimesch, John P. Hecht, Tim Langrish, D.Phil., Christian Schwartzbach, Lee Smith (2008), Psychrometry, Evaporative Cooling, and Solids Drying. PERRY'S CHEMICAL ENGINEERS' HANDBOOK, The McGraw-Hill Companies. 94-98.
- Lazarowych N.J. and Pekos P. (1998) Use of fingerprinting and marker compounds for identification and standardization of botanical drugs: strategies for applying pharmaceutical HPLC analysis to herbal products. Drug Information Journal, 32, 497-512.
- Lew A., Krutzik P. O., Hart M. E. and Chamberlin A. R. (2002), Increasing rates of reaction: microwave-assisted organic synthesis for combinatorial chemistry, Journal of combinatorial chemistry, 4(2):95-105.
- Marchal L.M., H.H. Beeftink and J. Tramper (1999), Towards a rational design of commercial maltodextrins. Trends in Food Science & Technology 10: 345-355.
- Masters, K. (1985). Spray drying handbook. (4<sup>th</sup>edition). New York: Halsted Press, a division of John Wiley & Sons Inc.
- Mermelstein, N. H. (1997). How food technology covered microwaves over the years. Food Technology, 51(5):82–84.
- Mohd Azizi C.Y. and Adnan R. (2001). Optimization of processing Parameter for enhanced Good Quality of Manggo Powder using Response surface Methodology". Proceedings of The 15th Symposuim of Malaysian Chemical Engineers, Somche, September 2001 Johor Bahru.

- Mohd Azizi C.Y., (2007). Extraction, identification and separation of vitamin E and djenkolic acid from Pithecellobium Jiringan (Jack) Prain seeds using super critical carbon dioxide. PhD Thesis, Universiti Sains Malaysia.
- Neas, E.D., and Collins, M.J. (1988). An Introduction to Microwave Sample Preparation-Theory and Practice. Washington, DC, American Chemical Society, chapter 2, 7-32.
- Norashikin A. Z. (2010). Production of pineapple powder using microwave assisted Spray drying process. Master, University Technology Malaysia, Skudai.
- Nicoleti, J. F., Telis-Romero, J., & Telis, V. R. N. (2001). Air-drying of fresh and osmotically pre-treated pineapple slices: Fixed air temperature versus fixed slice temperature drying kinetics. Drying Technology, 19(9), 2175–2191.
- Obon, J. M., Castellar, M. R., Alacid, M., Fernandez-Lopez, J. A.(2009). Production of a red purple food colourant from Opuntia stricta fruits by spray drying and its application in food model systems. Journal of Food Engineering. 90, 471-479.
- Patel R. P., M. P. Patel and A. M. Suthar (2009), Spray drying technology: an overview, Indian Journal of Science and Technology, Vol.2 No.10, 44-47.
- Perkins-Veazie, P., Collins, J.K., Pair, S.D. and Roberts, W. (2001). Lycopene content differs among red-fleshed watermelon cultivars. Journal Science Food Agriculture. 81, 1–5.
- Qing-guo Hu, Min Zhang, Arun S. Mujumdar, Gong-nian Xiao, Jin-cai Sun, (2006). Drying of edamames by hot air and vacuum microwave combination. Journal of Food Engineering (77), 977–982.

- Ramaswamy, H. and Marcotte, M. (2006) Food processing: Principles and Applications, Taylor & Francis Group.
- Regier M, Knorzer K. and Erle U. (2004), Microwave-and microwave vacuum-drying of food [review], Chemi Ingenier Technik, 76(4):424-432.
- Righetto, A. M. and Netto, F. M. (2005). Effect of encapsulating materials on water sorption, glass, transition and stability of juice from immature acerola. International Journal of Food Properties, 8, 337–346.
- Roos, Y.H., 1993a. Water activity and physical state effects on amorphous food stability. J. Food Process. Preserv. 16, 433–447.
- Roos, Y.H., 1993b. Melting and glass transition of low molecular weight carbohydrates. Carbohydrate Res. 238, 39–48.
- Saenz, C., Tapia, S., Chavez, J. and Robert, P. (2009). Microencapsulation by spray drying of Bioactive compounds from cactus pear (Opuntia ficus-indica). Food Chemistry. 114, 616-622.
- Schubert H. and Regier M. (2005), The microwave processing of foods, CRC Press, New York Washington, DC.
- Shivhare U. S., Raghavan G. S. V. and Bosisio R. G. (1994), Modelling the drying kinetics of maize in a microwave environment, Journal of Agricultural Engineering Research, 57: 199-205.

- Shyam S. Sablani, Ashok K. Shrestha, Bhesh R. Bhandari (2008), A new method of producing date powder granules: Physicochemical characteristics of powder, Journal of Food Engineering 87, 416–421.
- Soysal Y. (2004), Microwave Drying Characteristics of Parsley .Biosystems Engineering 89 (2), 167–173.
- Sutar P.P. and Suresh Prasad (2007). Moisture Diffusivity and Product Temperature
  Analysis of Carrot Slices in Microwave Vacuum Rotary Chamber Dryer.
  ASABE Annual International Meeting. Minneapolis, Minnesota. 17 20 June.
- Tinga, W.R., and Nelson, S.O. (1973). Dielectric Properties of Materials for Microwave Processing. J. Microwave Power. 8: 23-64.

USDA National Nutrient Database for Standard Reference, Release 22 (2009),

Pineapple, raw, traditional varieties, Agricultural Research Serrvice.

- Yu Li, Shi-Ying Xu, Da-Wen Sun (2007) Preparation of garlic powder with high allicin content by using combined microwave–vacuum and vacuum drying as well as microencapsulation. Journal of Food Engineering 83 :76–83.
- Zhengfu Wang, Junhong Sun, Fang Chen, Xiaojun Liao, Xiaosong Hu (2007) Mathematical modelling on thin layer microwave drying of apple pomace with and without hot air pre-drying. Journal of Food Engineering 80: 536–544.