



## Promoting a well-dispersion of MoO<sub>3</sub> nanoparticles on fibrous silica catalyst via one-pot synthesis for enhanced photoredox environmental pollutants efficiency

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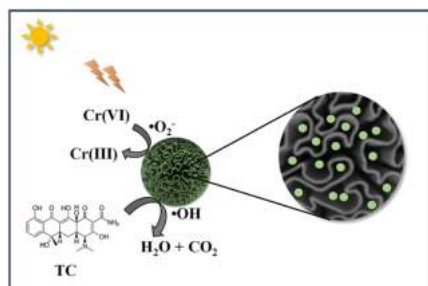
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### HIGHLIGHTS

- Nanoporous of FSMo was efficaciously synthesized via microemulsion method.
- FSMo catalyst demonstrated a preserved spherical morphology with dendrimeric silica fibre.
- The well-dispersion of Mo element in the FSMo catalyst greatly inhibits the electron-hole recombination.
- FSMo showed the 75% and 69% towards simultaneous remediation of Cr(VI) and TC, respectively.
- $h^+$ ,  $\cdot OH_{ads}$ , and  $e^-$  are noted as the reactive species that play significant role in the photoredox of Cr(VI) and TC.

### GRAPHICAL ABSTRACT



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### ABSTRACT

The coexistence of pharmaceutical compounds and heavy metals in the aquatic environment has resulted in complications in the treatment process and thus, causing uproar among the citizens. The radical-based photocatalysis technology has aroused as an excellent method to eliminate both heavy metal and pharmaceutical compounds in the water. Herein, reported the utilization of the microemulsion technique for the preparation of nanoporous fibrous silica-molybdenum oxide (FSMo) towards simultaneous photocatalytic abatement of hexavalent chromium (Cr(VI)) and tetracycline (TC). The FESEM analysis showed the spherical morphology of the FSMo catalyst with dendrimeric silica fiber. The synthesized FSMo catalyst exhibited narrowed bandgap, high crystallinity, and well Mo element dispersion for enhanced photo-redox of Cr(VI) and TC. Remarkably, simultaneous remediation of the Cr(VI) and TC over FSMo demonstrated superior photocatalytic efficiency, 69% and 75%, respectively, than in the individual system, possibly due to the effective separation of photoinduced charges. The introduction of the Mo element to the silica framework via microemulsion technique demonstrated better dispersion of Mo compared to the incipient wetness impregnation method and thus, yielded higher

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photocatalytic activity towards simultaneous removal of TC and Cr(VI). Besides, quenching experiments revealed the electrons and holes as the active species that play a dominant role in the simultaneous photo-redox of Cr(VI) and TC. Lastly, the FSMo catalyst demonstrated high stability after four continuous cycles of simultaneous photocatalysis reactions, implying its potential as a suitable material for practical wastewater treatments.

## 1. Introduction

Water is a vital source that covers around 70% of the Earth's surface. However, due to the engender of water contaminants such as pharmaceutical compounds in the hydrosphere, clean water resources have been scared significantly (Seid et al., 2022). Over the years, the growth of the human population and changes in lifestyle have instigated rapid industrialization and an extensive production of pharmaceutical products around the globe (Yaashikaa and Kumar, 2022). This phenomenon has exposed the environment and humans to great danger due to the uprising of pharmaceutical compounds in the water matrix, ascribed to the uncontrollable consumption of pharmaceutical products and the discharge of partially treated pharmaceutical effluent into the water bodies (Oluwole and Olatunji, 2022). Over the years, tetracycline compound (TC) has been determined as one of the prevalent pharmaceutical compounds in the environment and has been considered one of the global threats due to its low metabolism property which makes some proportion of the consumed TC be excreted from the human body in form of feces or urine, resulting in the accumulation of TC in the aquatic domain (Zhang et al., 2021). Moreover, TC has been related to numerous health issues such as kidney and liver failure, endocrine disruptors, hepatic and some cancers which make it hazardous to humans (di Cerbo et al., 2019). Besides, a recent study reported that some heavy metal ions such as hexavalent chromium (Cr(VI)) and divalent cadmium (Cd(II)) have also been detected in the practical pharmaceutical industrial wastewater (Girish, 2020). Cr(VI) is a non-biodegradable metal ion in which its removal is an urgent matter due to its high potential for carcinogenicity, mutagenicity, toxicity, and teratogenicity properties which can give negative consequences to humans and the environment even at trace levels (Agoro et al., 2020). In addition, National Water Quality Standard (NWQS) of Malaysia has set 0.05 mg/L as a safety limit for discharging the Cr(VI) into the water bodies (Alias et al., 2020). Nevertheless, the coexistence of TC and Cr(VI) in the pharmaceutical wastewater can be a problem to the wastewater treatment process since Cr(VI) can actively react with TC to generate a complex molecule that is difficult to treat (Izzudin et al., 2021). Hence, the effective and sustainable elimination of TC and Cr(VI) from the pharmaceutical industry has become a top priority for research directions.

Numerous traditional methods have been employed over the past year to destroy the tetracycline in the aqueous system, which includes physical processes such as adsorption and membrane separation methods (Jannat Abadi et al., 2019; Zdartar et al., 2022). But, the efficiencies of these conventional wastewater treatment methods are limited by some drawbacks including the generation of secondary pollution, the complexity of the treatment process, and the time-consuming (Keerthana et al., 2022). Additionally, some of these conventional methods are inefficient for the removal of a low concentration of pollutants, which allows some residual of pollutants to be discharged into the hydrosphere, resulting in the accumulation of the pollutants in the water matrix (Azami et al., 2020). On the other hand, the removal of Cr(VI) from water also has become quite challenging nowadays. Till date, the most efficient way for dealing with Cr(VI) pollution is by reducing the high toxicity of Cr(VI) to low toxicity of Cr(III) (Yang et al., 2022).

In this context, advanced oxidation processes (AOPs) which utilized the radical species have been identified as a feasible alternative approach to the traditional wastewater remediation methods in eliminating the heavy metals and organic pollutants in the hydrosphere (Berkani et al., 2022). Furthermore, the photocatalysis reaction is one of

the most widely investigated AOPs due to its environmentally friendly (Ma et al., 2020), can be operated at a mild process condition (Aziz et al., 2021b), no generation of secondary pollution (M.S. Azami et al., 2021), and remarkable potential in degrading the organic pollutants to non-hazardous materials such water and carbon dioxide (Hassan et al., 2020). Interestingly, this method is capable of effectively eliminating both organic pollutants and heavy metals. For instance, the modification of TiO<sub>2</sub> catalyst with activated carbon materials has shown excellent photocatalytic activity toward phenol removal (Asencios et al., 2022). Meanwhile, the fabricated g-C<sub>3</sub>N<sub>4</sub>/Cu-doped ZrO<sub>2</sub> photocatalyst also showed favorable photocatalytic activity towards Cr(VI) removal in which 90% of Cr(VI) has efficaciously been removed in this study (Reddy et al., 2022). Generally, the photocatalysis reaction is conducted for removing either heavy metal or organic pollutants at a time. Interestingly, an innovative simultaneous photocatalysis reaction has been proven to show superior photocatalytic efficiency relative to the typical photocatalysis reaction (Guo et al., 2018; Hemmati-Eslamloo et al., 2021; Jiang et al., 2021). This can be attributed to its excellent utilization of photoproduced electrons and holes, and efficient charge transferability due to the presence of the synergistic effect between oxidizable organic pollutants and reducible heavy metals.

During the last decades, numerous photocatalyst materials have been employed for photocatalysis studies. Among them, molybdenum oxide (MoO<sub>3</sub>) is one of the intriguing materials due to its non-toxicity behavior, high photon absorption (Liu et al., 2019), anisotropic crystal growth (Cai et al., 2021), and rich oxygen vacancies (Liu et al., 2021a), and has been utilized widely as a suitable photocatalyst for the remediation of distinct organic contaminants and toxic metals. Wang and his research group have successfully developed MoO<sub>3</sub>/Zn-Al LDHs composite photocatalyst and showed 90.5% removal of tetracycline in 60 min (Wang et al., 2021). On the other hand, Tahmasebi et al. reported the utilization of MoO<sub>3</sub>/Cs<sub>3</sub>PMo<sub>12</sub>O<sub>40</sub> composite photocatalyst for rhodamine B (RhB) removal. Remarkably, this photocatalyst demonstrated 93% efficiency towards the removal of RhB under visible light irradiation (Tahmasebi et al., 2021). Meanwhile, the Z-scheme ZnIn<sub>2</sub>S<sub>4</sub>@MoO<sub>3</sub> heterojunction photocatalyst synthesized by Ouyang et al. demonstrated 94.5% degradation of tetracycline hydrochloride (TC-HCl) in 90 min (Ouyang et al., 2021). Despite these outstanding performance of MoO<sub>3</sub>-based photocatalysts toward removal of various water contaminants, the utilization of commercial MoO<sub>3</sub> in the photocatalysis study is restricted by two key drawbacks; (1) low surface area and accessibility of the active site, and (2) low quantum yield.

Recently, fibrous silica (KCC-1) has captivated a lot of attention among researchers due to its unique characteristic that promotes the generation of mesopores and micropores with bi-continuous lamellar silica fibre structures (Fauzi et al., 2022). In addition, the fibrous silica material demonstrated high surface area and abundant defect sites which is favorable for high photocatalytic activity (Hitam et al., 2020a). Previously, our group successfully synthesized several fibrous silica-metal oxide photocatalysts using a modified microemulsion method for a distinct range of water pollutants removal. For instance, Fauzi and her teammates have successfully synthesized fibrous silica-titania (FST) and showed 90% efficiency towards the degradation of ibuprofen (Fauzi et al., 2018). Besides, Rahim et al. (2020) reported 70.2% efficiency towards desulphurization of dibenzothiophene over fibrous silica tantalum (FSTa). Meanwhile, Aziz et al. (2021) reported 96% and 59% removal of Cr(VI) and *p*-cresol, respectively via simultaneous photocatalysis over fibrous silica zirconia (FSZr) photocatalyst (Aziz et al., 2021b). These high photocatalytic efficiencies can be

assigned to the improvement of photocatalyst properties such as lower bandgap, large surface area, low recombination of charge carriers and abundant of defects.

Despite the extensive fabrication of fibrous silica metal oxides, there is no reported study on the development of fibrous silica molybdenum oxide (FSMo) for the removal of water pollutants. Hence, inspired by these studies, we presented a novel development of nanoporous fibrous silica-molybdenum oxide (FSMo) for simultaneous TC and Cr(VI) removal. The efficiency of the FSMo catalyst towards TC and Cr(VI) abatement was compared to the MoO<sub>3</sub>/KCC-1, KCC-1, and MoO<sub>3</sub> catalysts. Furthermore, the effect of parameters such as pollutant concentration, pH, and catalyst dosage on the visible-light-driven photocatalytic activities are also investigated. A possible mechanism of simultaneous photocatalysis reaction over FSMo is proposed and scrutinized in detail. It is believed that these findings will give significant information on the development of fibrous silica-based materials for wastewater remediation.

## 2. Experimental

### 2.1. Material synthesis

The commercial molybdenum oxide (MoO<sub>3</sub>) with 99.5% purity, was obtained from Sigma Aldrich Sdn. Bhd., Malaysia. Tetraethyl orthosilicate (TEOS) and toluene with 98% and 99.5% purity, respectively were obtained from Merck Sdn. Bhd., Malaysia. Urea was acquired from Vchem Sdn. Bhd., Malaysia. Butanol (BuOH) was acquired from QRec Sdn. Bhd., Malaysia. Potassium dichromate (K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>) and tetracycline used as pollutant precursors were bought from Emorg Sdn. Bhd. and Chem Cruz Sdn. Bhd., Malaysia with purity 98% and 99%, respectively. Cetyltrimethylammonium bromide (CTAB) with 99% purity was bought from Fisher Scientific (M) Sdn. Bhd., Malaysia. The variation of the pH system was calibrated by adding the HCl or NaOH solution dropwise.

### 2.2. Synthesis of KCC-1

As previously reported by our group, fibrous silica (KCC-1) was successfully synthesized using the microemulsion approach. (Shahul Hamid et al., 2019). In a brief, about 15 g of surfactant (CTAB) together with 6 g of hydrolyzing agent (urea) were dissolved in distilled water with vigorous stirring for 1 h under room standard room conditions. After that, a 5:2 M ratio of toluene and butanol was added to the blend solution and constantly agitated for 1 h. Next, approximately 10 mL of TEOS was mixed with this mixture and agitated for 4 h prior to the heating at 423 K. Then, the solution was transferred into the beaker before let dried overnight at 383 K. After that, the white solid obtained was ground into a fine powder before undergoing heating treatment at 823 K with a ( $q = 3 \text{ K min}^{-1}$ ,  $t = 8 \text{ h}$ ).

### 2.3. Synthesis of composite MoO<sub>3</sub>/KCC-1

The composite of molybdenum oxide (MoO<sub>3</sub>) loaded onto fibrous silica (KCC-1) was synthesized by the effortless incipient wetness impregnation method (Hitam et al., 2020a). In a typical synthesis, the pristine MoO<sub>3</sub> was used as the Mo precursor and the preparation procedure for MoO<sub>3</sub>/KCC-1 was as follows. Initially, MoO<sub>3</sub> and KCC-1 with a ratio of 0.1:1 by weight were transferred into two separate beakers containing 50 mL of distilled water and then stirred at medium speed for 30 min at 323 K. The solution containing MoO<sub>3</sub> catalyst was labelled as solution A. Meanwhile, the solution containing the KCC-1 catalyst was labelled as solution B. After 30 min of homogeneous stirring, solution A was then mixed with solution B and continuously stirred at 353 K for 2 h. Then, the temperature of the solution was rise to 373 K and let continuously stirred until the solution is completely dried. Next, the obtained catalyst was dried in the oven at 383 K to ensure the complete removal of residual moisture. Finally, the obtained greenish-white solid was ground

into a fine powder and calcined for 8 h ( $T = 823 \text{ K}$ ,  $q = 3 \text{ K min}^{-1}$ ).

### 2.4. Synthesis of FSMo

The fibrous silica-molybdenum oxide (FSMo) was prepared via in-situ microemulsion method as reported in the previous study (FSZr) (Aziz et al., 2021a). On the contrary, in this study, commercial MoO<sub>3</sub> was used as a seed instead of TiO<sub>2</sub> and the molar ratio of water to toluene was determined at 1:5. Firstly, the blend solution of mixed urea, water, and CTAB was stirred vigorously for 30 min to ensure the homogeneous mixing of the mixture. To this solution, toluene and butanol with a molar ratio of 5:2 were added and consistently stirred for 1 h. After that, the TEOS solution was added to the mixture and stirred continuously for 8 h at 423 K. Then, microwave irradiation was applied to the solution at 480 W for 2 h. A greenish-white precipitate was obtained after a centrifugation step. The greenish-white precipitate was then washed with acetone and distilled water before being dried at 383 K overnight. After that, the obtained greenish-white solid was ground into a fine powder before undergoing a calcination process under a muffle furnace at 823 K for 8 h.

### 2.5. Characterization of the catalysts

The phase and crystallinity of prepared catalysts were determined under X-ray diffraction (XRD) spectroscopy analysis using a diffractometer (Bruker Advance D8, USA) in the range of  $2\theta = 3^\circ$  to  $90^\circ$ . The microscopy of the surface morphology of the catalysts was evaluated using Field-emission scanning electron microscopy (JEOL JSM-6701F). The inner microstructure of the catalysts was studied using Transmission electron microscopy (JEM-ARM200F). The functional group present in the catalysts was evaluated using Fourier Transform Infrared spectroscopy (Agilent Cary 640) via KBr method in the region of  $1600\text{--}400 \text{ cm}^{-1}$ . The textural properties of catalysts were analyzed using N<sub>2</sub> physisorption (Thermo-Scientific Surfer). The optical and electronic properties of the catalysts were identified using ultraviolet-visible/diffuse reflectance spectra (UV-Vis/DRS, Agilent Cary 60) and Photoluminescence (PL) spectroscopy analysis (PTI QuantaMaster™ 60 Fluorescence Spectrophotometer, USA). The extrapolation of the bandgap of the prepared catalysts was determined through Kubelka-Munk (K-M) plot.

### 2.6. Synergistic photocatalytic remediation of Cr(VI) and TC

The photocatalytic activities of the synthesized catalysts towards simultaneous remediation of Cr(VI) and TC were investigated in a batch reactor. The metal halide lamp (400 W,  $\lambda \geq 400 \text{ nm}$ ) was utilized as the visible light source. The reactor is coupled with a cooling system to retain the room temperature condition throughout the reaction. The simultaneous photocatalytic redox experiments were preceded as follows:  $0.1\text{--}0.6 \text{ g L}^{-1}$  of catalyst was dispersed into a 100 mL mixed pollutants system of required initial concentration (Cr(VI) = 50 mL, TC = 50 mL). The pH of the pollutants (1–11) was adjusted using HCl or NaOH solutions. Prior to the visible light illumination, the solution was agitated for 1 h in the dark to achieve adsorption-desorption equilibrium. The photocatalytic experiment was conducted for 3 h at 293 K. About 2 mL of the solution was taken at the 30 min time interval and centrifuged at 750 rpm to separate the catalyst from the treated pollutant solution. The concentration of TC and Cr(VI) were analyzed using UV-Vis spectrophotometry (Cary 60 UV-Vis, Agilent Technologies, USA) at maximum wavelengths of 357 nm and 345 nm, respectively (Q. H. Li et al., 2021; Valério et al., 2020). The photocatalytic efficiency towards Cr(VI) and TC removal was evaluated using the equation below:

$$\text{Photocatalytic efficiency (\%)} = (1 - C_t / C_0) \times 100 \quad (1)$$

where  $C_t$  is the pollutant's concentration at time ( $t = t$ ), and the  $C_0$  is the initial concentration of the pollutant.

The stability of the optimum photocatalyst was evaluated for four cycles of simultaneous photo-redox of Cr(VI) and TC. At the end of every photocatalytic experiment, the photocatalyst was rinsed with HCl to eliminate the residual Cr and then let dry overnight at 383 K before being reused for the next cycle.

### 3. Results and discussion

#### 3.1. Photocatalytic activity

##### 3.1.1. Simultaneous photocatalytic redox of Cr(VI) and TC

The catalytic activity of the prepared FSMo catalyst was evaluated in visible-light illumination for the reduction of Cr(VI) and the oxidation of TC. Prior to the photocatalytic experiment, the photolysis of TC and Cr(VI) were conducted in a single pollutant system using visible light exposure to determine the self-degradability and reducibility of pollutants in the natural condition. As shown in Fig. S1, TC and Cr(VI) demonstrated 17.1% oxidation efficiency and 10.8% reduction efficiency, respectively, in the absence of photocatalyst, showing that the TC and Cr(VI) exhibited high stability in the natural water bodies. On the other hand, in the photocatalytic experiment, the adsorption-desorption equilibrium of Cr(VI) and TC was achieved after 1 h of agitation in the dark before illumination with visible light. The effectiveness of the FSMo towards the removal of TC and Cr(VI) in individual and mixed pollutants systems was evaluated as shown in Fig. 1. As clearly observed, both TC and Cr(VI) demonstrated an enhancement of photoredox efficiency in the mixed pollutants system. As noticed, the degradation efficiency of TC in single pollutant system is 46%. However, upon the addition of Cr(VI) into the system, the removal efficiency of TC was boosted at a tremendous rate (74%). Similarly, Cr(VI) showed a minimal reduction efficiency in the single pollutant system (55%). When an equivalent amount of TC solution was added to the pollutant system, the reduction efficiency of Cr(VI) increased significantly to 69%. The results obtained suggest that the synchronicity of oxidizable (TC) and reducible (Cr(VI)) species could more effectively exploit the photoinduced carrier (electrons and holes), resulting in high TC oxidation and Cr(VI) reduction performance (Zhao et al., 2019). A similar phenomenon was found when the  $\text{CuBi}_2\text{O}_4/\text{calcined ZnAlBi-LDHs}$  composite photocatalyst was utilized for simultaneous removal of TC and Cr(VI) (Zhang et al., 2022). The coexistence of TC and Cr(VI) induced the synergistic effect which resulted to high photocatalytic performance.

##### 3.1.2. Kinetic of simultaneous photoredox of TC and Cr(VI)

The photokinetic evaluation of the FSMo was then carried out utilizing the Langmuir-Hinshelwood (L-H) model to determine its photocatalytic performance. The pseudo-first-order was calculated using Eq. (2).

$$\ln \frac{C_t}{C_0} = k_{app} t \quad (2)$$

where  $C_t$  represents the concentration at  $t = t$ , and  $C_0$  is the initial concentration of TC or Cr(VI). Meanwhile, the  $k_{app}$  is represent the pseudo-first-order reaction rate constant. The linear plot of  $\ln(C_0/C_t)$  vs illumination time, as shown in Fig. 2, verifies that the simultaneous photocatalytic removal of TC and Cr(VI) over FSMo followed the pseudo-first-order kinetic model. The  $k_{app}$  calculated from the slope of the plot, as shown in Table S1, demonstrated that the FSMo has a positive and significant impact on the degradation of TC and reduction of Cr(VI). The  $k_{app}$  value decreased as the initial concentration was increased, indicating that the reaction is favorable at low concentrations. (Azami et al., 2020). Then, the L-H kinetic model was plotted based on the L-H Eq. (3).

$$\frac{1}{k_{app}} = \frac{1}{k_r K_{LH}} = \frac{C_0}{k_r} \quad (3)$$

where  $k_r$  is the reaction rate constant ( $\text{mg L}^{-1} \text{min}^{-1}$ ),  $K_{LH}$  is the TC or Cr(VI) adsorption coefficient onto the catalyst surface ( $\text{L mg}^{-1}$ ), and  $C_0$  refers to the initial concentration of TC or Cr(VI) ( $\text{mg L}^{-1}$ ). The obtained values of  $k_r$  0.5429  $\text{mg L}^{-1} \text{min}^{-1}$  and 0.0565  $\text{mg L}^{-1} \text{min}^{-1}$  and  $K_{LH}$  were 0.011  $\text{L mg}^{-1}$  and 0.0002  $\text{L mg}^{-1}$ , for TC degradation and Cr(VI) reduction, respectively. These values indicated that the TC and Cr(VI) on the catalyst surface were the reaction's controlling steps (Aziz et al., 2021a).

#### 3.2. Characterization

##### 3.2.1. Phase and crystallinity studies

Fig. 3a-b shows the XRD diffractogram of commercial  $\text{MoO}_3$ , KCC-1,  $\text{MoO}_3/\text{KCC-1}$ , and FSMo catalysts. The synthesized catalysts displayed a clearly defined peak at  $2\theta = 10^\circ\text{-}70^\circ$ . The KCC-1 catalyst displayed a broad peak at  $2\theta = 15^\circ\text{-}30^\circ$ , which represents the amorphous phase of silica structure (Shahul Hamid et al., 2019). The XRD analysis confirmed the orthorhombic structure of  $\alpha\text{-MoO}_3$  and this result matched well with the JCPDS data (Card no. 050508) (Prakash et al., 2019). Several crystallite peaks appeared at  $2\theta = 12.9^\circ, 23.4^\circ, 25.8^\circ, 27.4^\circ, 33.7^\circ, 39.0^\circ, 46.1^\circ$  and  $49.4^\circ$  in  $\text{MoO}_3/\text{KCC-1}$  and FSMo catalysts are corresponded to the crystal plane of (020), (110), (040), (021), (111), (041), (200) and (002). The FSMo catalyst displayed a much lower intensity of crystallite peaks than the  $\text{MoO}_3/\text{KCC-1}$  catalyst, signifying that the in-situ synthesis method (FSMo) promoted well-dispersion of Mo element on the silica framework compare to the incipient wetness impregnation method ( $\text{MoO}_3/\text{KCC-1}$ ) (Bahari et al., 2022; Hitam et al., 2020b).

##### 3.2.2. FTIR spectroscopy analysis

The analysis of Fourier Transform Infrared (FTIR) spectroscopy was conducted to explore the functional group that exists in the prepared catalysts. Fig. 4A displayed the FTIR spectra of the prepared catalysts in the range of  $400\text{-}1600 \text{ cm}^{-1}$ . The KCC-1 shows four distinct bands at 460, 797, 964, and  $1084 \text{ cm}^{-1}$ , which revealed the presents of Si-O-Si bending, Si-O-Si symmetric, Si-OH, and Si-O-Si asymmetric, respectively (M. S. Azami et al., 2021; Hitam et al., 2020b). Meanwhile, the pristine  $\text{MoO}_3$  displays 4 major bands at 484, 588, 865, 994, and  $1106 \text{ cm}^{-1}$ . The broad peak at 484 and  $588 \text{ cm}^{-1}$  are assigned to the bending and stretching vibration of the O-Mo-O functional group (Hu et al., 2015). The stretching mode of Mo=O oxygen terminal at peak  $994 \text{ cm}^{-1}$  revealed the orthorhombic layered of the  $\text{MoO}_3$  phase (Hojabri et al., 2015). The Mo-O-Mo stretching mode was represented by the peak at  $865 \text{ cm}^{-1}$ . A notable decrease in peaks intensity is observed for Si-O-Si bending Si-OH, Si-O-Si, and Si-O-Si symmetric group of  $\text{MoO}_3/\text{KCC-1}$  and FSMo catalysts, which can be assigned to the interaction between the fibrous silica framework and Mo element upon been introduced by both in-situ microemulsion and incipient wetness impregnation methods (Fatah et al., 2020).

For further study on the chemical composition of the catalysts, the bands at  $1400\text{-}1000 \text{ cm}^{-1}$ ,  $1000\text{-}900 \text{ cm}^{-1}$ , and  $600\text{-}400 \text{ cm}^{-1}$  were deconvoluted by the Gaussian curve fitting (Fig. S2) and the results were interpreted and presented in Fig. 4B-D. The deconvoluted of  $1084 \text{ cm}^{-1}$  demonstrated five major bands at 1233, 1163, 1106, 1074, and  $1045 \text{ cm}^{-1}$ , which correspond to the Si-O-Si longitudinal optical asymmetric, fewer cross-linked stretching, linear structure stretching, and transversal optical asymmetric, respectively (Hitam et al., 2020b). The intensity of these bands reduced significantly upon the introduction of Mo species, signifying that which can be assigned to the formation of Si-O-Mo interaction. It was also observed that the Si-O-H and Si-O bands at  $968 \text{ cm}^{-1}$  and  $945 \text{ cm}^{-1}$  declined at once after the addition of the Mo element. An emergence of the band at  $945 \text{ cm}^{-1}$  was also observed, which attributed to the formation of Si-O-Mo bond. On the other hand,

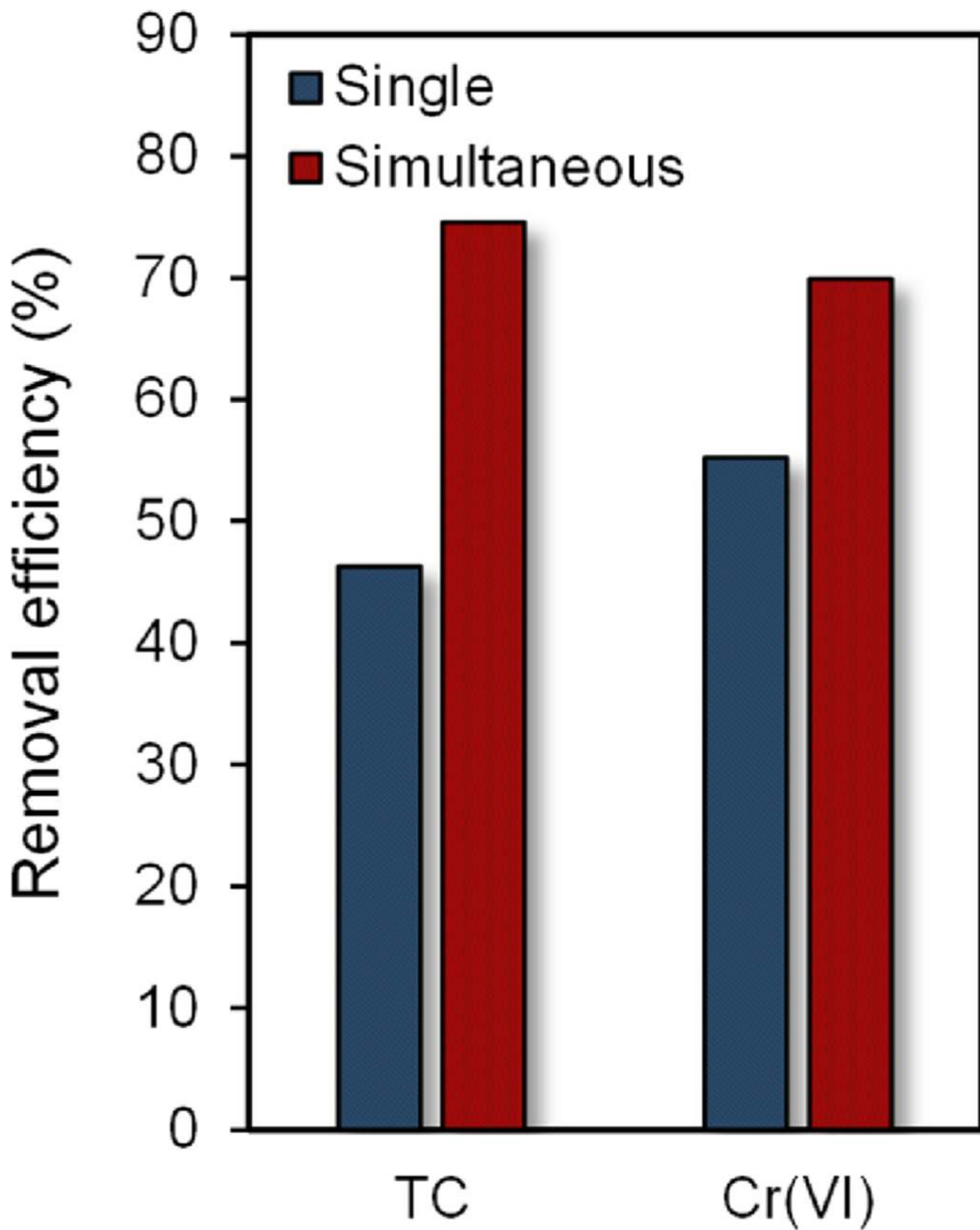


Fig. 1. Photocatalytic removal efficiency of TC and Cr(VI) in single and simultaneous system under visible light irradiation ( $W = 0.375 \text{ g L}^{-1}$ ,  $\text{TC} = 10 \text{ mg L}^{-1}$ ,  $\text{Cr(VI)} = 10 \text{ mg L}^{-1}$ ,  $\text{pH} = 9$ ,  $t = 3 \text{ h}$ ).

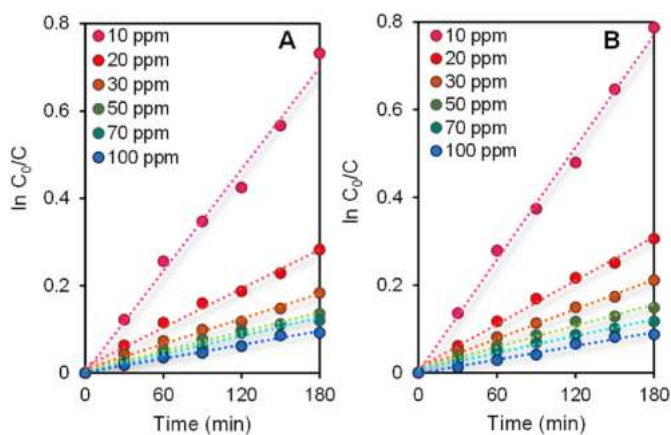


Fig. 2. Kinetic photo-redox of (A) TC and (B) Cr(VI) at different initial concentration in the simultaneous system over FSMo catalyst ( $W = 0.375 \text{ g L}^{-1}$ ,  $\text{pH} = 9$ ,  $t = 3 \text{ h}$ ).

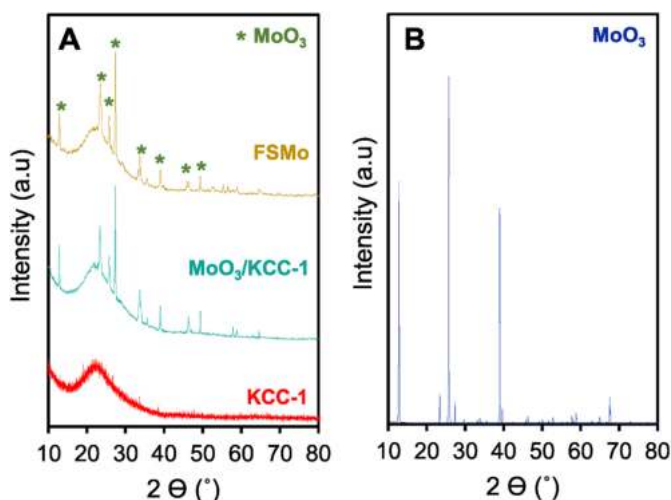


Fig. 3. XRD diffractogram of prepared catalysts.

$\text{MoO}_3/\text{KCC-1}$  demonstrated a much lower intensity of Si–O–Si at band  $467 \text{ cm}^{-1}$  compared to the FSMo, which might be due to the distortion of the fibrous silica framework when introducing the Mo element via the incipient wetness impregnation method (Hassan et al., 2022; Shahul Hamid et al., 2019).

### 3.2.3. Morphological studies

The surface morphology of the prepared catalysts ( $\text{MoO}_3$ , KCC-1,  $\text{MoO}_3/\text{KCC-1}$ , and FSMo) have been studied by FESEM and TEM analyses. As shown in Fig. 5A, the pristine  $\text{MoO}_3$  catalyst exhibited irregular and stacked flake-like morphology with a relatively smooth surface (Li et al., 2017). On the other hand, the synthesized KCC-1 presented in Fig. 5B demonstrated a spherical morphology of well-ordered dendrimeric silica fiber with particle sizes ranging from 400 to 600 nm, which is similar to those reported in the previous studies (Aziz et al., 2018; Fauzi et al., 2018). Meanwhile, upon the addition of the Mo element (Fig. 5C) onto the cockscomb-like silica surface via the incipient wetness impregnation method, the spherical morphology of fibrous silica is still retained but slightly distorted which can possibly be assigned to the interaction between Mo element and the surface of Si–O–Si framework (Hitam et al., 2020b). This finding is similar to the previously reported study on the development of metal oxide loaded/KCC-1 for carbon dioxide methanation, in which the fibrous morphology remains intact with a slight change in its sphericity upon the addition of metal element

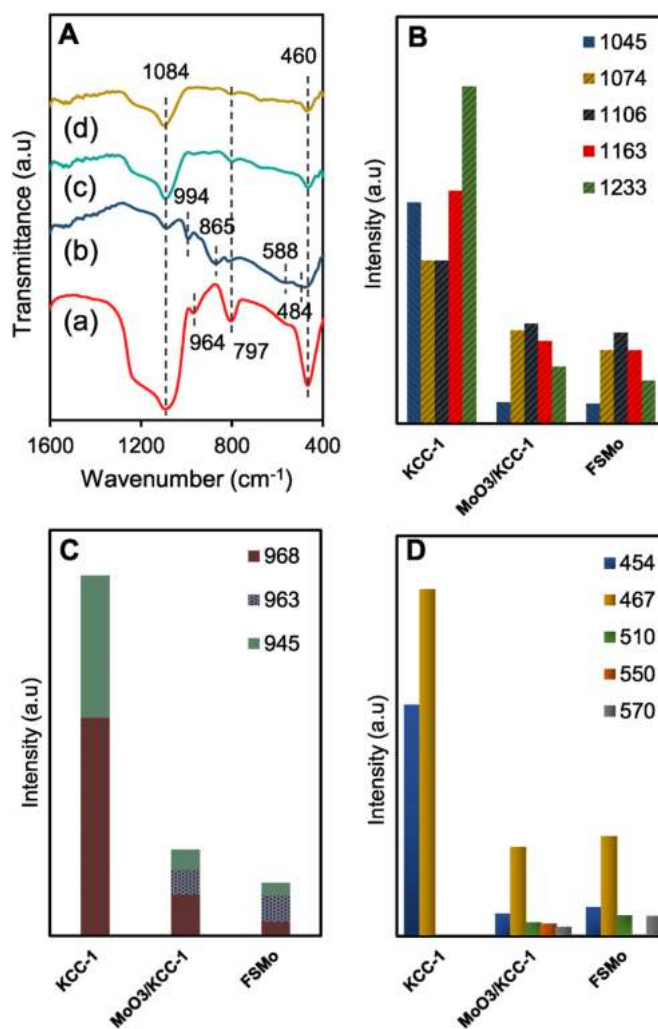


Fig. 4. (A) The FTIR spectra of (a) KCC-1, (b)  $\text{MoO}_3$ , (c)  $\text{MoO}_3/\text{KCC-1}$ , and (d) FSMo catalyst; Gaussian peak area of FTIR deconvolution peak and intensity of the bands at (B)  $1400\text{--}100 \text{ cm}^{-1}$ , (C)  $1000\text{--}900 \text{ cm}^{-1}$ , and (D)  $600\text{--}400 \text{ cm}^{-1}$ .

on the KCC-1 by the incipient wetness impregnation method (Shahul Hamid et al., 2018). For the FSMo catalyst (Fig. 5E), it is observed that the morphology of this catalyst is identical to the KCC-1 catalyst, confirming a well-preserved fibrous structure upon the addition of  $\text{MoO}_3$  seed via the in-situ method. Moreover, FSMo demonstrated highly dispersion of Mo element (Fig. 5F) compared to the  $\text{MoO}_3/\text{KCC-1}$  (Fig. 5D), describing that the FSMo shows the spatial distribution and close contact of  $\text{MoO}_3$  with dendrimeric silica fiber during the in-situ microemulsion method, which is in accordance with the result in XRD analysis.

Further study on the morphology of FSMo catalyst has been carried out by TEM analysis. Similar to the previous study, the TEM image of prepared FSMo (Fig. 6A), demonstrated a high-resolution image of preserved fibrous silica framework, which indicated the successful development of fibrous silica-molybdenum oxide photocatalyst (Fauzi et al., 2020b). Furthermore, the elemental mapping on the FSMo catalyst revealed the uniformly disperse of Si, O, and Mo elements in the FSMo catalyst, suggesting that the synthesis of silica-molybdenum oxide catalyst via the microemulsion method resulted in well-dispersion of Mo element onto the fibrous structure (M.S. Azami et al., 2021). The well-dispersion of Mo in the FSMo may play a vital role in achieving high photocatalytic activity towards simultaneous photo-redox of Cr(VI) and TC. Meanwhile, the EDX analysis (Fig. 6E) unveiled the intensity of Si, O, and Mo elements in the FSMo catalyst. As clearly shown, the Si elements

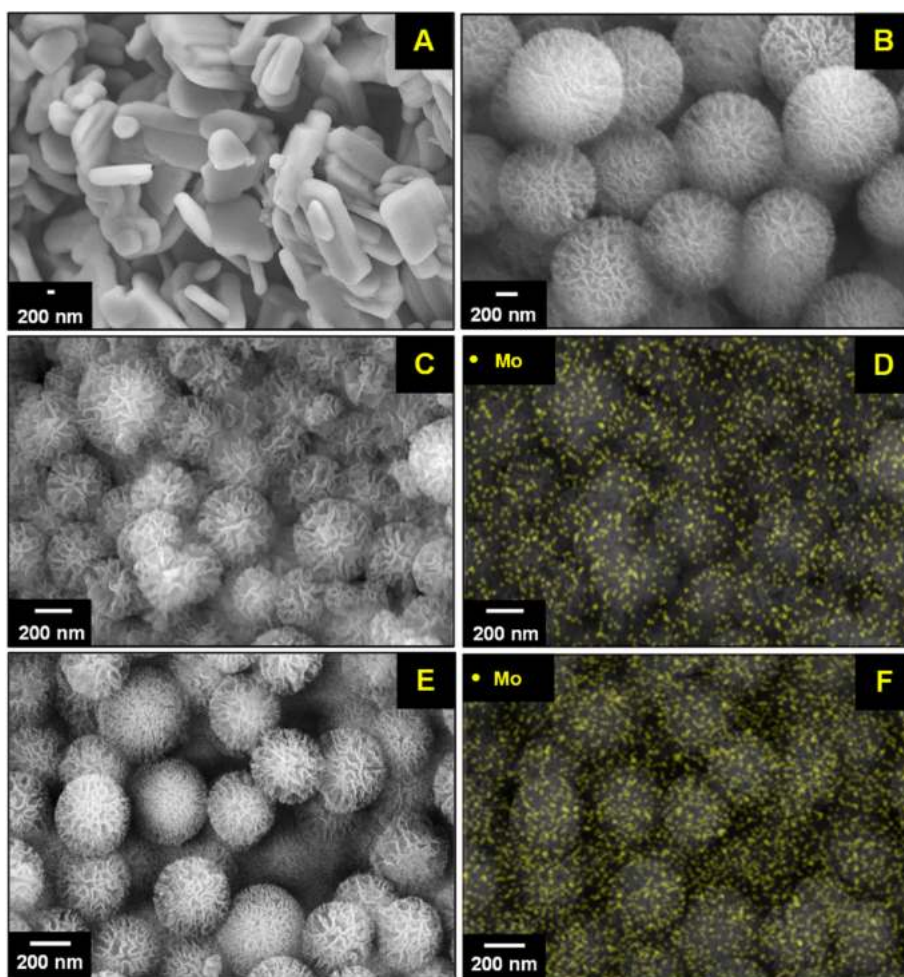


Fig. 5. FESEM images of (A)  $\text{MoO}_3$ , (B) KCC-1, (C–D)  $\text{MoO}_3/\text{KCC-1}$  with elemental mapping Mo, and (E–F) FSMo with elemental mapping Mo.

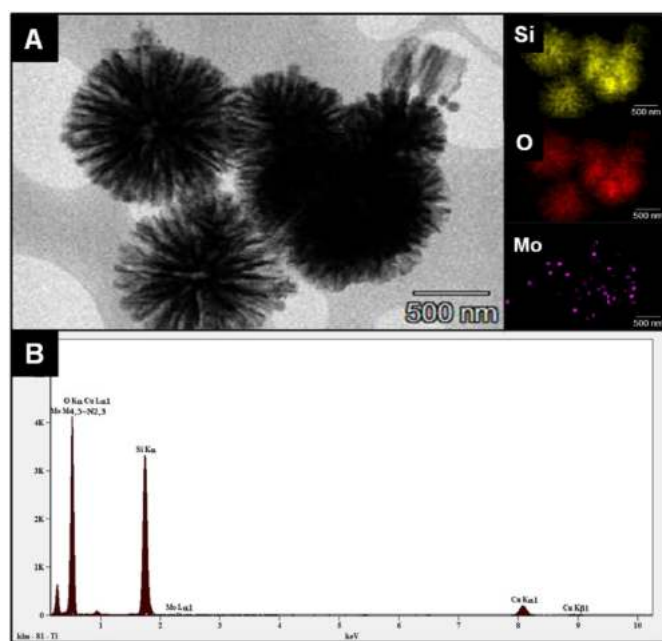


Fig. 6. (A) The TEM image of FSMo with elemental distribution of (B) O, (C) Si and (D) Mo; and (E) EDX analysis of FSMo catalyst.

demonstrated the highest intensity elements in the FSMo, attributed to the large fibrous silica framework. On the other hand, high intensity of O element was observed in the FSMo catalyst compared to the Mo element which can be reasoned to the presence of excess oxygen during the calcination process which resulted in the high concentration of surface oxygen (Fu et al., 2022).

#### 3.2.4. Textural studies

The textural properties of synthesized catalysts were studied by  $\text{N}_2$  adsorption-desorption isotherm analysis as shown in Fig. 7. According to the IUPAC, the isotherms of all catalysts can be classified as type IV, indicating that these catalysts exhibited mesoporous structures (Baca et al., 2020; Yan et al., 2020). In addition, the specific surface area and interparticle pores for the  $\text{MoO}_3$  were substantially increased after the introduction of the fibrous silica framework, suggesting that the fibrous silica provides a high surface area and accessible active sites for more contact between the targeted pollutants and photocatalyst (M. S. Azami et al., 2021). Nevertheless, the FSMo catalyst demonstrated a much lower surface area and total pore volume compared to the  $\text{MoO}_3/\text{KCC-1}$  catalyst which can possibly be due to the presence of the Mo element in the fibrous silica framework. This is in agreement with the morphological results from FESEM and XRD analysis. The  $\text{N}_2$  adsorption-desorption analysis showed an average pore diameter  $<50$  nm for all catalysts, revealing the nanoporous structure of the synthesized catalysts. Table 1 summarized the textural properties as well as the bandgap of all the catalysts.

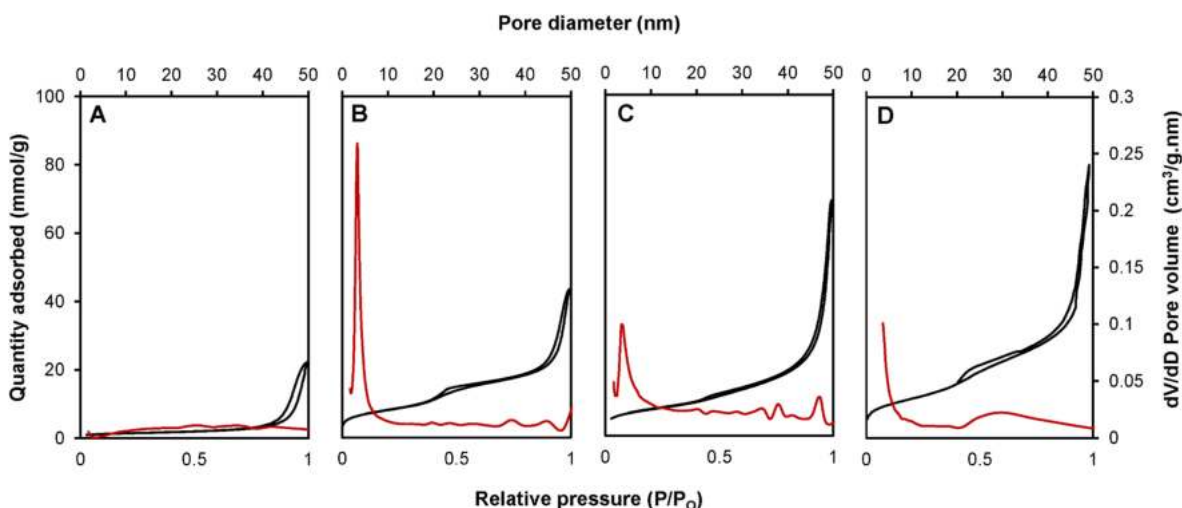


Fig. 7. BJH pore size distribution and N<sub>2</sub> adsorption-desorption isotherms of (A) KCC-1 (B) MoO<sub>3</sub> (C) MoO<sub>3</sub>/KCC-1 and (D) FSMo.

Table 1

The textural and optical properties of all catalysts.

Photocatalyst	Surface area <sup>a</sup> (m <sup>2</sup> /g)	Total pore volume (cm <sup>3</sup> /g)	Avg. pore diameter (nm)	Bandgap <sup>b</sup> (eV)
MoO <sub>3</sub>	114	0.77	27.1	2.21
KCC-1	632	1.71	9.55	3.75
MoO <sub>3</sub> /KCC-1	610	2.39	15.7	1.90
FSMo	417	1.14	17.9	2.12

<sup>a</sup> Calculated from N<sub>2</sub> adsorption measurements using the BET method.

<sup>b</sup> Calculated using Kubelka-Munk Equation.

### 3.2.5. Optical and photoluminescence spectroscopy studies

The optical property and charge separation efficiency of the catalysts were evaluated via Photoluminescence (PL) spectroscopy and Ultraviolet-Visible Diffuse Reflectance Spectra (UV-Vis/DRS) analyses, respectively. The UV-Vis/DRS analysis was conducted to determine the bandgap of all catalysts by using the Kubelka-Munk equation as follows:

$$(ah\nu)^2 = A(h\nu - E_g) \quad (4)$$

where  $E_g$  = bandgap energy,  $\nu$  = light frequency,  $A$  = absorbance (cm<sup>-1</sup>), and  $h$  = Planck constant. As shown in Fig. 8A, the KCC-1 catalyst demonstrated exceptional large bandgap energy (3.75 eV), depicting its

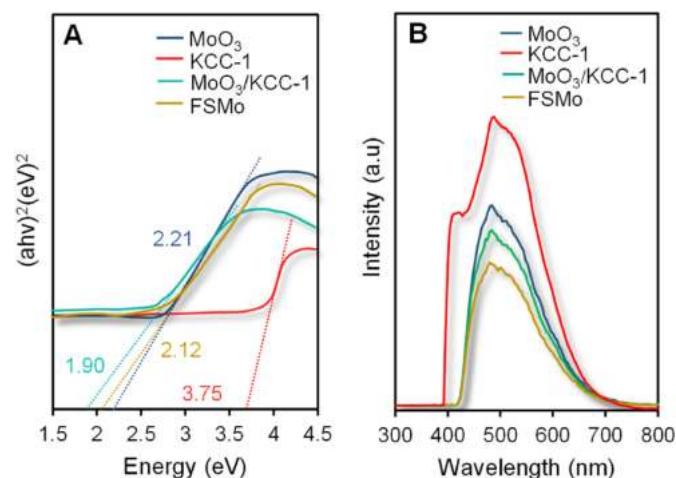


Fig. 8. (A) Plot of transformed Kubelka-Munk function versus the energy of light; and (B) Photoluminescence spectra of all catalysts.

inadequacy as photocatalyst material for the visible light region. Meanwhile, the MoO<sub>3</sub> demonstrated as a highly-photosensitivity material with relatively low bandgap energy (2.21 eV). This finding matched well with the reported study by Mafa in 2021 (2.40 eV) (Mafa et al., 2021). In addition, red-shifts in the absorption edge were observed for FSMo and MoO<sub>3</sub>/KCC-1 catalysts, possibly due to the formation of defects during the synthesis of composite catalysts which narrowed the bandgap energy level (Liu et al., 2021b). The FSMo and MoO<sub>3</sub>/KCC-1 catalysts demonstrated 2.12 eV and 1.90 eV of bandgap energy, respectively.

Besides, photoluminescence (PL) analysis is an archetypal technique used in the photocatalysis study to observe the recombination rate of photogenerated charges, revealing the effectiveness of migration, and separation of charge carriers transfer in the photocatalyst. The catalysts were excited with the laser line at 350 nm at the emission region of 300–800 nm as presented in Fig. 8B (Joya et al., 2019). The catalysts showed emission. The KCC-1 catalyst demonstrated the highest intensity of peak at 487 nm, signifying the high recombination rate of photo-produced charges. This can be assigned to the large bandgap of the KCC-1 catalyst, which provides a significant hindrance and required more energy for the excitation of the electron to the conduction band of the catalyst. Thus, the excited electrons in the KCC-1 catalyst tend to recombine back with the photogenerated holes. Likewise, the PL spectrum of pristine MoO<sub>3</sub> showed a much lower intensity peak relative to the KCC-1 catalyst which might be correlated to the high crystallinity of the MoO<sub>3</sub> catalyst which provided well dispersion of the excited electron on the conduction band (Liu et al., 2021b). On the other hand, a substantial improvement in the solar utilization efficiency and charge separation rate was observed upon the introduction of MoO<sub>3</sub> to the silica framework which can be assigned to the migration of charges in the composite catalysts, resulting in efficient charge separation and high photocatalytic efficiency (Xiao et al., 2022). However, the composite MoO<sub>3</sub>/KCC-1 catalyst demonstrated a slightly higher intensity of PL than the FSMo catalyst which might be due to the poor dispersion of Mo element on the KCC-1 catalyst, which acted as a new recombination center for electrons and holes, resulting in low charges separation efficiency (Adhikari et al., 2020). The FSMo exhibited the lowest PL intensity, demonstrating it as a potential photocatalyst material with excellent charge separation. Similar cases also have been reported by Fauzi et al. (2020) and Azami et al. (2022) where the fibrous silica metal oxides showed much lower PL intensity compared to the commercial ones which can be attributed to the suppression of recombination between photoexcited electron and hole pairs (M.S. Azami et al., 2022; Fauzi et al., 2020a).



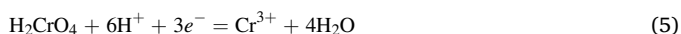
### 3.3. Effect of parameters towards simultaneous photoredox TC and Cr(VI)

#### 3.3.1. Effect of pH

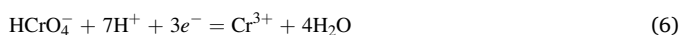
In general, TC exists in four different structures in a different range of pH, in which each structure possesses a different charge state. Interestingly, TC exists predominantly as a monovalent cation (pH < 3.0), a zwitterion (pH = 3.3–7.7), a monovalent anion (pH = 7.7–9.7) and a bivalent anion (pH > 9.7) (Bembibre et al., 2022). Based on the complication property of TC at different pH, therefore, it can be deduced that the pH of the pollutant system greatly affects the photocatalytic performance.

The effect of pH on simultaneous photocatalytic removal of TC and Cr(VI) using FSMo catalyst was inspected by adjusting the pH value from 3 to 11 at an initial concentration of 10 mg L<sup>-1</sup> for both pollutants and 0.375 g L<sup>-1</sup> dosage of catalyst as depicted in Fig. S1. Obviously, the FSMo catalyst demonstrated high photocatalytic activity towards TC degradation in medium alkaline conditions. The degradation efficiency of TC increased as the pH of the system increased up to pH 9. However, beyond pH 9, a tremendous decline in the photocatalytic efficiency toward TC removal was observed. This result can be attributed to the characteristic of the negative charges of TC at pH > 9, which reduced the adsorption of TC onto the catalyst surface, resulting in low photocatalytic activity.

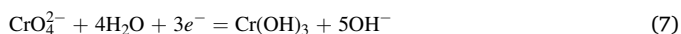
Meanwhile, the reduction of Cr(VI) to Cr(III) is typically favored in the acidic condition (pH < 3) due to the abundant presence of H<sup>+</sup> can facilitate the reduction of Cr(VI) oxyanions. The mechanism of reduction Cr(VI) in the acidic condition proceeds as follows:



or



In the alkaline condition, the presence of excessive OH<sup>-</sup> ions would suppress the reduction of Cr(VI) as follow:



The photoreduction of Cr(VI), however, showed increasing efficiency with the increased pH up to pH 7. This could be owing to a synergistic interaction between TC and Cr(VI), which allows the photoinduced charges to be separated efficiently. Consequently, increase the number of free electrons which results in better photoreduction efficiency towards Cr(VI) removal. Similarly, at alkaline pH (pH > 7), the high concentration of OH<sup>-</sup> in the aqueous system demonstrated a significant hindrance to the intimate contact between Cr(VI) ions and the catalyst surface which in turn, slowed down the reduction activity of Cr(VI).

#### 3.3.2. Effect of catalyst dosage

The effect of catalyst dosage on simultaneous photocatalytic removal of TC and Cr(VI) was investigated in this study in which the photocatalysis reaction was carried out under different amounts of catalyst dosage. As illustrated in Fig. S2, the FSMo catalyst demonstrated an increasing trend for TC and Cr(VI) removal when the catalyst dosage increased up to 0.375 g L<sup>-1</sup>. A noticeable decline in the removal efficiency for both TC and Cr(VI) was observed when the dosage of catalyst exceed 0.375 g L<sup>-1</sup> was used, suggesting that the excessive dosage of catalyst increase the turbidity of the solution and hindered the penetration of light to the catalyst surface, resulting to low photocatalytic activity (Heidarpour et al., 2020). However, the 0.625 g L<sup>-1</sup> catalyst dosage demonstrated much higher total efficiency towards simultaneous removal of TC and Cr(VI) which was mainly contributed by the high adsorption of pollutants to the catalyst surface. Yet, its efficiency on the photocatalysis reaction basis is still lower than that of 0.375 g L<sup>-1</sup> due to the blockage of active sites by adsorbed pollutants (Song et al., 2022). This finding evinces that 0.375 g L<sup>-1</sup> is the optimum dosage for this

simultaneous photocatalytic reaction.

#### 3.4. Photocatalytic efficiency of all prepared catalyst

To prove the effectiveness of the FSMo catalyst towards simultaneous remediation of TC and Cr(VI), the simultaneous photocatalysis reaction over commercial MoO<sub>3</sub>, KCC-1, and MoO<sub>3</sub>/KCC-1 catalysts were also performed (Fig. S3). The KCC-1 catalyst demonstrated the lowest photocatalytic activity towards simultaneous removal of TC (46%) and Cr(VI) (24%), possibly due to the poor visible light utilization and rapid recombination rate of the photoinduced charges (Fig. 6A and B). In contrast, FSMo and MoO<sub>3</sub>/KCC-1 catalysts exhibit high photocatalytic activity towards the removal of Cr(VI) and TC, been FSMo yields the highest efficiency towards oxidation of TC (75%) and reduction of Cr(VI) (69%). This result can be attributed to the narrow bandgap energy and efficient separation of photogenerated electron-hole pairs. Likewise, MoO<sub>3</sub>/KCC-1 showed much lower photocatalytic activity relative to the FSMo catalyst which can possibly be attributed to the low dispersion of Mo element onto fibrous silica framework, which introduced a new recombination center, in turn, facilitates the recombination of photo-generated charges, resulting in low photocatalytic activity (Zhou et al., 2022).

The simultaneous photocatalytic removal of TC and Cr(VI) was compared with various previous photocatalysts to prove the efficacy of the FSMo catalyst, as depicted in Table 2. Based on the results, it can be said that the efficiency of simultaneous photocatalytic removal of TC and Cr(VI) over FSMo was comparable with other photocatalyst materials.

#### 3.5. Photocatalytic mechanism

To expose the mechanism of simultaneous photo-redox of Cr(VI) and TC over FSMo, the dominant species that actively participate in the photocatalysis process were explored through quenching experiments. In this study, methanol (Met), potassium carbonate (PC), and potassium iodide (PI) were used as quenchers for the photogenerated hole (h<sup>+</sup>), photogenerated electron (e<sup>-</sup>), and hydroxyl radical on the surface (•OH<sub>ads</sub>), respectively (M. S. Azami et al., 2022; Hassan et al., 2021). As depicted in Fig. 9, a notable decline in the degradation efficiency of TC was observed when Met and PI were added to the pollutants system. This result concluded that the TC undergoes oxidation process at the valence band of FSMo and photogenerated h<sup>+</sup> and •OH<sub>ads</sub> are the active species in the TC degradation. On the other hand, the removal percentage of Cr(VI) declined from 69% to 14% when PC was added to the pollutants system, inferring that the photogenerated e<sup>-</sup> is the dominant species for the photoreduction of Cr(VI). Meanwhile, the reduction efficiency of Cr(VI) decrease insignificantly along with the oxidation of TC when PI was added, suggesting that the •OH<sub>ads</sub> do not actively participate in the photoreduction of Cr(VI). The high utilization of e<sup>-</sup> at the conduction band (CB) for the reduction of Cr(VI) reduced the recombination of photoinduced charges which resulted in more free h<sup>+</sup> species. However, when the e<sup>-</sup> quencher was added to the system, the oxidation of TC is not significantly affected suggesting that the e<sup>-</sup> is not actively participated in the oxidation of TC. Based on the result obtained, it is concluded that h<sup>+</sup> and •OH<sub>ads</sub> played a major role in TC photo-oxidation, while e<sup>-</sup> dominated Cr(VI) photo-reduction.

For better comprehension of the simultaneous photo-redox mechanism of TC and Cr(VI) over FSMo, the valence band (VB) and conduction band (CB) positions should be calculated. The location of CB and VB of FSMo were calculated by using the Mulliken electronegativity concept as shown in the following equation (Wei et al., 2019):

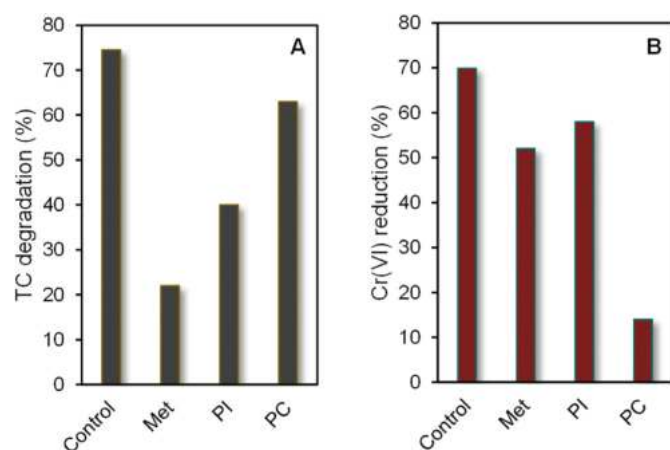
$$E_{CB} = X - E_C - 0.5E_g \quad (8)$$

$$E_{VB} = E_{CB} + E_g \quad (9)$$

**Table 2**  
Comparison of simultaneous photocatalytic removal TC and Cr(VI) over various photocatalysts.

Photocatalyst	Initial concentration (mg L <sup>-1</sup> )	Dosage (g L <sup>-1</sup> )	pH	Light source	Removal efficiency (%)	Reference
FSMo	Cr(VI): 10	0.38	9.0	Visible light	69.5	This work
	TC: 10				75.0	
MIL-125-NH <sub>2</sub> @BiOI	Cr(VI): 80	1.00	NA	Visible light	80.0	Dai et al. (2022)
	TC: 80				81.0	
CQDs/HBWO-18	Cr(VI): 5	1.00	5.4	Visible light	84.5	(C. Li et al., 2021)
	TCH: 20				83.0	
rGO@ZnAlTi-LDO	Cr(VI): 5	0.40	7.0	Visible light	52.5	Ye et al. (2019)
	TC:10				80.0	
AgI/BiVO <sub>4</sub>	Cr(VI): 15	0.40	NA	Visible light	70.0	Zhao et al., 2019
	TC: 20				88.0	
ZnO/rGO	Cr(VI): 20	0.05	NA	Visible light	84.0	Kumar et al. (2020)
	TC: 20				68.0	
Bi <sub>2</sub> MoO <sub>6</sub> @DE	Cr(VI): 60	1.00	NA	Visible light	90.1	Wan et al. (2020)
	TC: 50				74.7	
AIS/BWO	Cr(VI): 10	0.30	NA	Visible light	64.0	Zhang et al. (2019)
	TCH: 10				92.0	

\*NA: not state in the literature, Cr(VI): hexavalent chromium, TC: tetracycline, TCH: tetracycline hydrochloride.

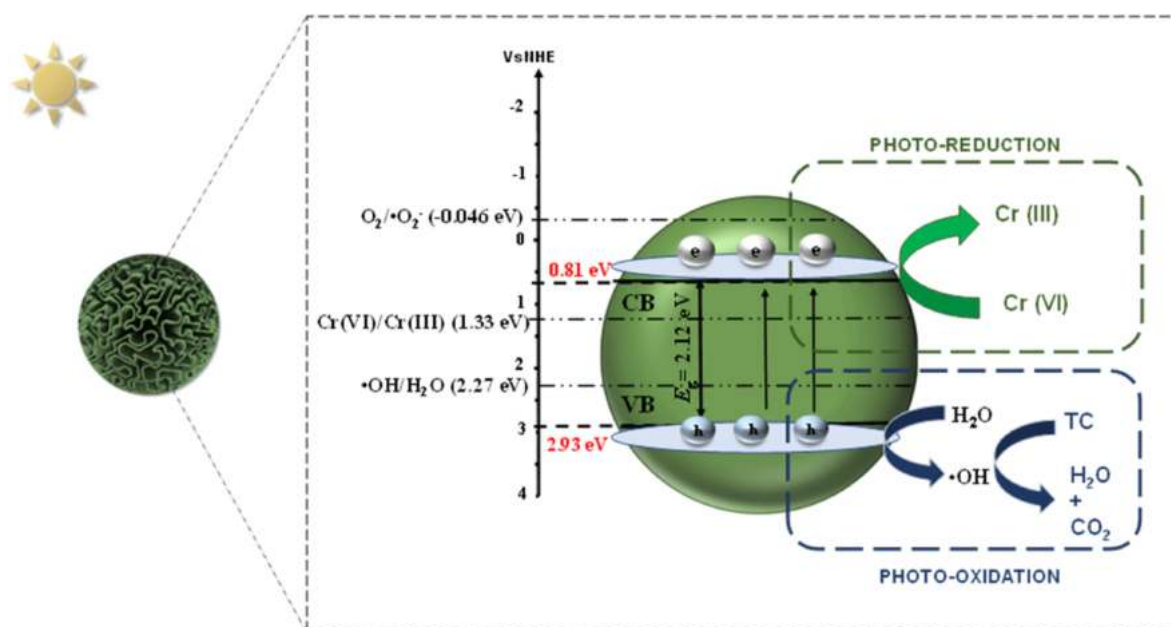


**Fig. 9.** Scavenger effect on simultaneous photoredox of (a) TC and (b) Cr(VI) over FSMo catalyst (TC = 10 mg L<sup>-1</sup>, Cr(VI) = 10 mg L<sup>-1</sup>, W = 0.375 g L<sup>-1</sup> pH = 9, t = 3 h).

where  $E_{CB}$  and  $E_{VB}$  are the conduction and valence band potentials, respectively;  $E_g$  is the bandgap energy of the semiconductor;  $X$  is the absolute electronegativity of the elements, while  $E_C$  is the energy of free electron on the hydrogen scale (4.5 eV).

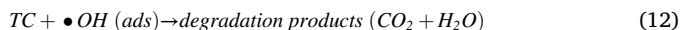
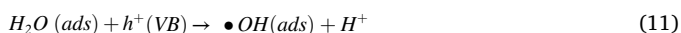
By using Eqs. (8) and (9) and the bandgap energy of FSMo from Table 1 (2.12 eV). Hence, the calculated CB and VB potentials of FSMo were 0.81 eV and 2.93 eV, respectively.

On the basis of these results, a mechanism for the simultaneous photocatalytic remediation of TC and Cr(VI) over FSMo was proposed and briefly described in Scheme 1. Briefly, the cationic TC was drawn towards highly anionic Cr(VI) which then attracted to the positively charged surface of FSMo under the dark conditions. Under the visible light illumination, the FSMo catalyst absorbed the light irradiation and spontaneously excited to the CB. Synchronously, an equivalent amount of photogenerated  $h^+$  is formed at the VB. According to the calculated band energies,  $\bullet O_2^-$  as well as the  $\bullet OH_{bulk}$  were not produced in this photocatalysis reaction due to the  $E_{CB}$  value of FSMo was higher compared to the standard redox potential of  $O_2/\bullet O_2^-$  ( $E^\ominus = -0.046$  eV vs. NHE) (Jiang et al., 2021). Likewise, the oxidation potential of  $H_2O/\bullet OH$  ( $E^\ominus = +2.40$  eV vs. NHE) is more negative than the VB potential of FSMo (Jiang et al., 2021). Hence, the photogenerated  $h^+$  can



**Scheme 1.** Proposed mechanism of FSMo over simultaneous photo-redox of TC and Cr(VI).

oxidize the water molecules ( $H_2O$ ) to hydroxyl radical ( $\bullet OH$ ) species, which is further utilized for the degradation of TC molecules. The mechanisms involved in the TC degradation are shown in the Eqs. 10 and 11 below.



Meanwhile, since the  $\bullet O_2^-$  was not produced in this reaction, hence more excited  $e^-$  are utilized for the reduction of Cr(VI) due to the CB level of FSMo is more negative than the reduction potential of Cr(VI)/Cr(III) ( $E^\ominus = +1.33$  eV vs. NHE) (Aziz et al., 2021a). In addition, owing to the high utilization of  $e^-$  for reduction of Cr(VI), the recombination rate of photogenerated  $h^+$  and  $e^-$  is reduced, resulting in high photocatalytic activity of FSMo towards simultaneous removal of TC and Cr(VI). Similarly, The mechanisms for Cr(VI) reduction to Cr(III) are shown in Eqs. 13–16 (Kumar et al., 2020). As the light penetrated the FSMo surface, the electron-hole pairs (excitons) is formed, in which the excited  $e^-$  is dispersed to the CB of FSMo. At the same time, some of the excited  $e^-$  are used to reduce the Cr(VI) to Cr(V). Then, the mechanisms of chromium reduction are continued until the Cr(VI) was successfully reduced to Cr(III). Since the  $e^-$  at CB are not been utilized for any reaction, the  $e^-$  was then recombined with the photoproduced  $h^+$  at the VB.



### 3.6. Stability and reusability of the catalyst

Photocatalyst reusability is a crucial criterion for commercial-scale uses of such materials, as well as their significant economic worth (Liu et al., 2020). The reusability of the synthesized FSMo photocatalyst was evaluated for four continuous cycles (Fig. S4). The prepared FSMo catalyst demonstrated high stability towards simultaneous remediation of Cr(VI) and TC. A minor reduction in the removal efficiency was clearly observed for Cr(VI) reduction and TC degradation after four cycles of photocatalytic experiments. The obtained reduction percentages for Cr(VI) photocatalytic reduction are 69% (1st cycle), 66% (2nd cycle), 63% (3rd cycle), and 56% (4th cycle). The obtained degradation percentages of TC at the different runs are 74% (1st cycle), 70% (2nd cycle), 67% (3rd cycle), and 59% (4th cycle). The reduction in the removal efficiency could be attributed to the aggregation of the catalyst, which led to the reduction of surface area and accessibility of the active sites (M.S. Azami et al., 2022). Moreover, the FTIR pattern (Fig. S6A) and FESEM image (Fig. S6B) of the spent FSMo, showed no emergence of new peak and preservation of the spherical fibrous structure, respectively, suggesting that the approximately chemical stable and high durability of FSMo was stable for simultaneous photoredox of Cr(VI) and TC. In addition, the intensity of FTIR for spent FSMo reduced substantially compared to the fresh FSMo which is possibly due to a slight distortion of silica matrix. These findings have proved the potential of FSMo photocatalyst as a suitable candidate for practical wastewater remediation.

### 3.7. Practicability of the FSMo

The real pharmaceutical wastewater consists of a very complex matrix of organic compounds, dissolved organic matter and inorganic ions, heavy metal ions, etc. Some of these components might affect the

photocatalytic efficiency towards the removal of water pollutants. Hence, to evaluate the real practical applicability of the FSMo catalyst, the photocatalytic experiment of multi-pollutants was carried out by adding the Ibuprofen (IBU) to the Cr(VI)-TC pollutants system. The result presented in Fig. S7 showed that the removal efficiency of Cr(VI), TC and IBU in the multi-pollutants system over FSMo catalyst is 55.2%, 63.2% and 50.2%, respectively. The decrement of photocatalytic efficiency for removal of Cr(VI) and TC in the multi-pollutants system could be ascribed to the limited reactive oxygen species (ROS) produced during the photocatalysis reaction which induced the competition between the pollutants for the reactive species. Hence, leading to low photoredox efficiency.

## 4. Conclusion

In conclusion, the FSMo catalyst was successfully synthesized via the microemulsion technique. The FESEM morphology demonstrated FSMo catalyst with molybdenum oxide as its core and encapsulated by the fibrous silica framework with particle sizes ranging from 500 to 600 nm. The  $N_2$  adsorption-desorption analysis further confirmed the nanoporous structure of the FSMo catalyst with an average pore diameter of 15.7 nm. The prepared FSMo catalyst exhibits a narrow bandgap (2.12 eV) and high surface area (417  $m^2/g$ ), which signifies the successful fabrication of fibrous silica-molybdenum oxide framework. Furthermore, under visible light irradiation, the FSMo catalyst showed remarkable performance in simultaneous photocatalytic oxidation of TC (75%) and reduction of Cr(VI) (69%) compare to the pristine  $MoO_3$ , KCC-1, and  $MoO_3/KCC-1$  catalysts which can be ascribed to its unique structure, which includes increased crystallinity, a bigger total pore volume, and a well-dispersed of Mo element. The quenching experiment revealed that the photogenerated electron was the most important species in Cr(VI) photoreduction, whereas  $h^+$  and  $\bullet OH_{ads}$  radicals were important species in TC photooxidation. Finally, it could be summarized that the modification of the  $MoO_3$  structure encapsulated by the fibrous silica framework, would provide critical information in designing a potential photocatalyst for wastewater remediation.

## Credit author statement

**N.M. Izzudin:** Conceptualization, resources, formal analysis, visualization, writing the draft. **A.A. Jalil:** writing-review and editing, supervision, project administration, funding acquisition, validation. **M.W. Ali:** writing- review and editing, validation, formal analysis, visualization. **F.F.A Aziz:** writing- review and editing, conceptualization. **M.S. Azami:** writing- review, editing, and conceptualization. **N.S. Hassan:** writing- review and editing, conceptualization. **A.A. Fauzi:** data curation, writing- review, editing, and conceptualization. **N. Ibrahim:** writing-review, editing, and conceptualization. **R. Saravanan:** data curation, and writing-review. **M.H. Hassim:** data curation and writing-review.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## Data availability

No data was used for the research described in the article.

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.chemosphere.2022.136456>.

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