

HYBRID LAPLACE TRANSFORM SOLUTION FOR COUPLED PARTIAL  
DIFFERENTIAL EQUATION OF FUMIGANT TRANSPORT IN STORED  
GRAIN

SALISU LUKUNTI

A dissertation submitted in partial fulfilment of the  
requirements for the award of the degree of  
Master of Science

Faculty of Science  
Universiti Teknologi Malaysia

OCTOBER 2019

## **DEDICATION**

My humble effort dedicates to my beloved  
FATHER: Late Alhaji.Muhammad Lukunti Koko  
MOTHER: Late Hajiya.Aisha Muhammad  
Siblings and friends.

## ACKNOWLEDGEMENT

Alhamdulillah. Thanks to Allah S.W.A., the almighty, the lord of the world for given me the strength to complete my master's degree successfully. I wish to express my sincere appreciation to my main supervisor Assoc. Prof. Dr. Yeak Su Hoe and my co-supervisor Dr. Zaiton Mat Isa for their support, encouragement and guidance throughout my research work. I am very thankful for their patience, valuable advices, motivations and kindness in giving me, that have been a major part in the success of this dissertation. Without that, I would not have been able to complete my dissertation. Thanks to all the staff in the department of mathematical science for helping me out all the time and my heartfelt Universiti Teknologi Malaysia at large for providing conducive environment for learning.

I would like to acknowledgement the Federal Polytechnic Bauchi, Nigeria and Tertiary Education Trust Fund (TETFUND), Nigeria for the financial support in pursuing this study. My sincere gratitude goes to my parents, late Alhaji Muhammad Lukunti koko and late Hajiya Aisha, for their supports, prayers, so much comfort and care me in the journey of my education and also my siblings for their concern, support and motivation. sincere appreciation also extends to all my colleagues and friends for the prayers and support on various occasion. Once again, thanks to everyone who has directly or indirectly involved for supporting me to complete this dissertation and my study.

## ABSTRACT

The research presented in this dissertation is a mathematical solution of hybrid analytical and numerical simulation approach to the model of coupled partial linear differential equations of grain stored fumigation. The model is partly adopted based on phenomena of advection-diffusion transport process of solute mass for the fumigation distribution of phosphine gas concentration in a cylindrical silo containing grain. One dimensional advection diffusion coupled of partial linear differential equation is solved using Laplace transform by applied numerical simulation of Week's method of Laplace inverse (WLI) and finite difference method (FDM) while Octave software is used in the simulation. The developed WLI algorithm results verified using Cauchy test for convergence on FDM error results. However, the FDM error shows that to have better results of FDM, need a smaller step size increment  $\Delta x$ . The error results also showed that the higher fumigant concentration ( $C_s=10$  mg/L) injected to the silo, the higher relative error in the solution of concentration of phosphine gas and concentration in the grain obtained, when compared with  $C_s=5$  mg/L. Furthermore, the investigation on efficiency of phosphine gas concentration during fumigation based on graph of the results showed that, the length of the time phosphine gas concentration could be taken for covering the silo is independent of the amount of boundary fumigant concentration (BFC) injected to the silo. While for concentration in the grain inside the silo, the time is depending on the BFC, where the higher fumigant concentration in the silo, the higher concentration received by the grain. Besides that, when the velocity of the model increase, the time taking for phosphine gas concentration during fumigation is reduced. In addition, the higher the velocity of the model and less amount of BFC, then the least amount of concentration the grain absorbs during the fumigation processes.

## ABSTRAK

Penyelidikan yang disampaikan dalam disertasi ini adalah penyelesaian matematik menggunakan analisis hibrid analitik dan simulasi berangka kepada model persamaan terbitan separa linear bagi pengasapan penyimpanan bijirin. Model ini diadaptasi berdasarkan fenomena proses pengangkutan-penyebaran jisim larut untuk pengedaran pengasapan kepekatan gas phosphine dalam silo berbentuk silinder yang mengandungi bijirin. Pengangkutan- penyebaran satu dimensi persamaan terbitan separa linear diselesaikan menggunakan transformasi Laplace dan menggunakan kaedah simulasi berangka iaitu laplace songsang Week (WLI) dan kaedah pembezaan terhingga (FDM) manakala perisian Octave digunakan untuk simulasi. Keputusan yang diperoleh menunjukkan algoritma WLI adalah menumpu di mana hasilnya telah disahkan dengan FDM melalui ujian ralat penumpuan pada FDM, dan ia menunjukkan bahawa ralat dikurangkan jika  $\Delta x$  adalah lebih kecil. Keputusan ralat juga menunjukkan bahawa kepekatan fumigant yang lebih tinggi ( $C_s=10$  mg/L) disuntik ke silo, ralat relatif juga lebih tinggi dalam penyelesaian kepekatan gas phosphine dan kepekatan dalam bijirin yang diperoleh, jika dibandingkan dengan  $C_s=5$  mg/L. Selain itu, penyiasatan terhadap tingkah laku kepekatan gas fosfin semasa pengasapan berdasarkan graf keputusan menunjukkan bahawa tempoh masa yang diambil oleh gas phosphine untuk memenuhi semua ruang adalah tidak bergantung kepada kepekatan fumigant yang disuntik ke silo manakala untuk kepekatan dalam bijirin di dalam silo, masa bergantung kepada kepekatan fumigant di dalam silo, dimana jika kepekatan yang lebih tinggi, kepekatan yang diterima oleh bijirin akan lebih meningkat. Selain itu, apabila halaju meningkat, pengambilan masa bagi kepekatan gas fosfin semasa pengasapan dikurangkan. Di samping itu, semakin tinggi halaju, jumlah kepekatan fumigant lebih rendah, maka jumlah kepekatan juga rendah yang akan diserap oleh bijirin semasa proses pengasapan.

## TABLE OF CONTENTS

	<b>TITLE</b>	<b>PAGE</b>
	<b>DECLARATION</b>	<b>i</b>
	<b>DEDICATION</b>	<b>iii</b>
	<b>ACKNOWLEDGEMENT</b>	<b>iv</b>
	<b>ABSTRACT</b>	<b>v</b>
	<b>ABSTRAK</b>	<b>vi</b>
	<b>TABLE OF CONTENTS</b>	<b>vii</b>
	<b>LIST OF TABLES</b>	<b>x</b>
	<b>LIST OF FIGURES</b>	<b>xi</b>
	<b>LIST OF ABBREVIATIONS</b>	<b>xiii</b>
	<b>LIST OF SYMBOLS</b>	<b>xiv</b>
	<b>LIST OF APPENDICES</b>	<b>xv</b>
<b>CHAPTER 1</b>	<b>INTRODUCTION</b>	<b>1</b>
	1.1 Introduction	1
	1.2 Research Background	1
	1.3 Problem Statement	4
	1.4 Research Objectives	5
	1.5 Scope and Limitation of the study	5
	1.6 Research Significance	6
	1.7 Outline Report	6
<b>CHAPTER 2</b>	<b>LITERATURE REVIEW</b>	<b>9</b>
	2.1 Introduction	9
	2.2 Grain Fumigation Processes.	9
	2.3 Types of Fumigants	10
	2.4 Transport Phenomena	12
	2.4.1 Diffusion Equation	13
	2.4.2 Advection Diffusion Equation	15

2.5	Mathematical Modelling	16
2.6	Laplace Transform	18
<b>CHAPTER 3</b>	<b>MATHEMATICAL MODEL</b>	<b>25</b>
3.1	Introduction	25
3.2	Model Equation for Fumigant Transport	25
3.3	Parameters Values of the Model	27
<b>CHAPTER 4</b>	<b>NUMERICAL SIMULATIONS</b>	<b>31</b>
4.1	Introduction	31
4.2	Weeks' Method of Laplace Inversion (WLI)	31
4.3	Solution of the Model using Laplace Transform Method	38
4.3.1	Laplace Transform of the Model	38
4.3.2	Laplace Inverse Transform of the Model using Week's Method of Inverse (WLI)	40
4.4	Solution of the Model using Finite Difference Method (FDM)	41
4.4.1	Description of Method	41
4.4.2	Finite Difference Method (FDM) to the Model	42
<b>CHAPTER 5</b>	<b>RESULT AND DISCUSSION</b>	<b>47</b>
5.1	Introduction	47
5.2	Numerical Results using Laplace Transform with Weeks' Method of Laplace Inversion (WLI)	47
5.2.1	The Results at a Constant Velocity 0.002m/s, using Boundary Fumigant Concentration (BFC) of 10 Mg/L.	48
5.2.2	The Result at a Constant Velocity 0.002m/s, using Boundary Fumigant Concentration (BFC) of 5 Mg/L.	50
5.2.3	The Results at a Constant Velocity 0.004m/s, using Boundary Fumigant Concentration (BFC) of 10 Mg/L.	52
5.2.4	The Results at a Constant Velocity 0.004m/s, using Boundary Fumigant Concentration (BFC) of 5 Mg/L.	53

5.3	Numerical Results of the Model using Finite Difference Method (FDM)	54
5.3.1	The Results at a Constant Velocity 0.002m/s using Boundary Fumigant Concentration (BFC) of 10 Mg/L, FDM.	55
5.3.2	The Results at a Constant Velocity 0.002m/s using Boundary Fumigant Concentration (BFC) of 5 Mg/L, FDM.	56
5.3.3	The Results at a Constant Velocity 0.004m/s using Boundary Fumigant Concentration (BFC) of 10 Mg/L, FDM.	58
5.3.4	The Results at a Constant Velocity 0.004m/s using Boundary Fumigant Concentration (BFC) of 5 Mg/L, FDM.	59
5.4	Error in Finite Difference Method (FDM).	60
5.4.1	The Result at a Velocity 0.002m/s and Boundary Fumigant Concentration (BFC) of 10 Mg/L.	61
5.4.2	The Results at a Velocity 0.002m/s and Boundary Fumigant Concentration BFC of 5 Mg/L.	63
5.5	Validation of Weeks' Method of Laplace Inversion (WLI)	64
<b>CHAPTER 6 SUMMARY, CONCLUSION AND RECOMMENDATIONS</b>		<b>67</b>
6.1	Introduction	67
6.2	Summary of the Work	67
6.3	Conclusion	69
6.4	Recommendation for Further Research	69
<b>REFERENCES</b>		<b>71</b>



## LIST OF TABLES

TABLE NO.	TITLE	PAGE
<b>Table 3.1:</b>	Parameters used in the model (Isa et al. 2016)	30
<b>Table 4.1:</b>	The values of the parameters used for Week's method of Laplace inverse (WLI).	48

## LIST OF FIGURES

FIGURE NO.	TITLE	PAGE
<b>Figure 1.1:</b>	Example for transport phenomena involving diffusion process.	2
<b>Figure 2.1:</b>	Shows the image Silo/harvest bags of grain (Abalone et al. 2011).	12
<b>Figure 2.2:</b>	Diffusion of a solute in tube from high concentration to low concentration.	13
<b>Figure 2.3:</b>	Illustration of procedure for Laplace transform.	18
<b>Figure 2.4:</b>	The Laplace transform as algorithm that transforms functions $u(t)$ to a functions $U(s)$ (Logan 2006).	19
<b>Figure 2.5:</b>	Discrete grid points/nodes (Chakraverty et al. 2019).	21
<b>Figure 3.1:</b>	Schematic of the model. (Abdullah 2018).	27
<b>Figure 3.2:</b>	Schematic of the mass transfer model of fumigant sorption by grain (Darby 2008).	29
<b>Figure 4.1:</b>	Isolated singularities of $F(s)$ are mapped to the exterior of the unit circle in the $w$ -plane (Brio, Kano, and Moloney 2005).	34
<b>Figure 4.2:</b>	Two steps of method for solving the given differential equation problem.	42
<b>Figure 4.3:</b>	Graphical illustration of forward, backward, and central approximations of a derivative.	42
<b>Figure 5.1:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 10$ Mg/L).	48
<b>Figure 5.2:</b>	The results of concentration in grain at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 10$ Mg/L).	49
<b>Figure 5.3:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 5$ Mg/L).	50
<b>Figure 5.4:</b>	The results of concentration in grain at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 5$ Mg/L).	51

<b>Figure 5.5:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 10$ Mg/L).	52
<b>Figure 5.6:</b>	The results of concentration in grain at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 10$ Mg/L).	52
<b>Figure 5.7:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 5$ Mg/L).	53
<b>Figure 5.8:</b>	The results of concentration in grain at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 5$ Mg/L).	54
<b>Figure 5.9:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.002$ m/s) with BFC( $cs = 10$ Mg/L) using FDM.	55
<b>Figure 5.10:</b>	The results of concentration in grain at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 10$ Mg/L) using FDM.	55
<b>Figure 5.11:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 5$ Mg/L) using FDM.	56
<b>Figure 5.12:</b>	The results of concentration in grain at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 5$ Mg/L) using FDM.	57
<b>Figure 5.13:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 10$ Mg/L) using FDM.	58
<b>Figure 5.14:</b>	The results of concentration in grain at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 10$ Mg/L) using FDM.	58
<b>Figure 5.15:</b>	The results of phosphine gas concentration in air at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 5$ Mg/L) using FDM.	59
<b>Figure 5.16:</b>	The results of concentration in grain at constant velocity ( $v = 0.004$ m/s) with BFC ( $cs = 5$ Mg/L) using FDM.	60
<b>Figure 5.17:</b>	The results of error produced by phosphine gas concentration and concentration in grain at velocity ( $v = 0.002$ m/s) with BFC ( $cs = 10$ Mg/L).	62
<b>Figure 5.18:</b>	The results of error produced by phosphine gas concentration and concentration in grain at velocity ( $v = 0.002$ m/s) with BFC ( $cs = 5$ Mg/L).	63
<b>Figure 5.19:</b>	Results of WLI and FDM of concentration of phosphine gas at constant velocity ( $v = 0.002$ m/s) with BFC ( $cs = 10$ Mg/L).	65

## LIST OF ABBREVIATIONS

BFC	-	Boundary fumigant concentration
CFD	-	Computational fluid dynamics
DE	-	Differential equation
FDS	-	Finite difference schemes
FDM	-	Finite difference method
ODE	-	Ordinary differential equation
PDE	-	Partial differential equation
WLI	-	Week's method of Laplace inverse

## LIST OF SYMBOLS

$C_s$	-	Boundary fumigant concentration
$C_p$	-	Concentration of phosphine gas in air
$C_g$	-	Concentration in grain
$J(x, t)$	-	mass flux of the solute
$\mathcal{L}$	-	Laplace transform
$\mathcal{L}^{-1}$	-	Inverse Laplace transform
$v$	-	Velocity
$t$	-	Time
$B_1, B_2, B_3, B_4$	-	Parameters
$\varepsilon$	-	Bulk porosity of the grain
$R_{filling}$	-	Filling ratio
$k_{fG}$	-	Linear mass transfer coefficient of adsorbed liquid fumigant
$k_{fA}$	-	Linear mass transfer coefficient of gaseous fumigant
$\rho_g$	-	Density of the grain
$F$	-	Partition factor
$S_{sorp}$	-	Specific surface area for sorption
$r_{fA}$	-	First order reaction coefficient of gaseous fumigant in air
$r_{fG}$	-	First order reaction coefficient of adsorbed liquid fumigant
$\sigma$	-	Exponential factor
$b$	-	Time scale factor
$E$	-	Error
$\infty$	-	Infinity
$h_1$	-	Increment in step size for time $t$
$h_2$	-	Increment in step size for space $x$
$Lt$	-	Length of the time $t$
$Lx$	-	Length of the space $x$
$Nt$	-	Number of nodes for $t$
$Nx$	-	Number of nodes for $x$

## LIST OF APPENDICES

<b>APPENDIX</b>	<b>TITLE</b>	<b>PAGE</b>
<b>Appendix A</b>	Flowchart of WLI algorithm	75
<b>Appendix B</b>	Flowchart of FDM	76

# CHAPTER 1

## INTRODUCTION

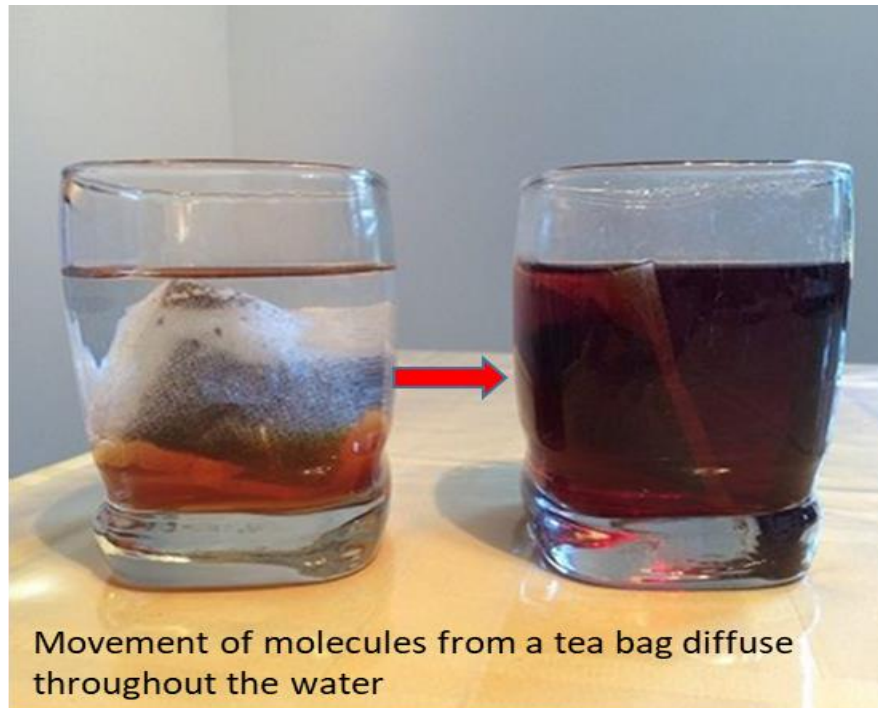
### 1.1 Introduction

The research work in this dissertation is to work out the solution to the model of coupled linear partial differential equation related to fumigation transport in stored grain. This chapter discusses the subject of the study begins with background of the research on general applications of transport phenomena and modelling, specifically on advection and diffusion, furthermore reduced to focus on the area of fumigation. The statement of the problem to conduct this research work is also presented in this introductory chapter, followed by the objectives, scope and the limitations of the study. Lastly the significant of the study and chapter by chapter dissertation structure are also presented in this chapter.

### 1.2 Research Background

Transport phenomena is the subject that deal with movement of different various entities such as mass, momentum and energy. Example of physical phenomenon, when a tea bag is place into cup of water, courses the chemicals that make a tea bag to diffuse into the water as showed in Figure 1.1. The tea bag content diffuses from it higher concentration to lower concentration. Another example is in phenomena of breathing; the diffusion in water surrounding a zebra fish embryo, the diffusion and reaction of oxygen in the fish embryo's body is an example of transport phenomena and in this process the higher concentration of oxygen in the yolk, where there is hardly metabolism taking place, only energy storage. In the daily life of human body according to Enderle, John D. and Bronzino (2012), the gas exchange in the lungs, transport across capillaries and alveoli, transport across the kidneys, and

transport across cell membranes. These mass transfer processes affect how oxygen and carbon dioxide are exchanged in your bloodstream, how metabolic waste products are removed from your blood, how nutrients are transported to tissues, and how all cells function throughout the body.



**Figure 1.1:** Example for transport phenomena involving diffusion process.

Evidently, there are many similarities in the mathematical descriptions of such transport phenomena which are essential for many processes in engineering, analytical chemistry, biology, agriculture, material science, metrology, pharmacy, physiology and other areas. According to Zoppou and Knight (1997), the transport of pollutant occurs in a large variety of environmental and industrial processes can be adequately described by the advection and diffusion equation and such pollutant is vital to the effective management of these processes. By Athayde et al (2018), burning of fossil fuels, deforestation, manufacturing and use of vehicles pollute and influences in the quality of air especially in large urban centres which due to the influence of the industrial revolution, technological advances and population growth has degraded nature over the time. However today, technology is used to study the effects of pollution and to develop appropriate physical-mathematical models of advection-diffusion equation to predict damages to the environment. Similarly, there are many



challenges in the environment of the presents insects in grain stored. With minimal changes occurring at the centre of large bulks for diurnal and seasonal, the store provides protection from the extremes of outside temperature and relative humidity fluctuations. However, in the grain bulk the presence of damaged grains, moisture and temperature gradients may act as rival attractants (Cox, P.D. and Collins 2002).

According to Darby (2008), the processes of exposure of the grain to use the gaseous chemical in order to kill all insects present is called grain fumigation and this processes refers to transport phenomena. Without harming the grain, such chemicals are usually applied as a dilute component in air that causes lethal responses in the insects. By the authors, Rajendran, S. and Sriranjini (2008) & Decker et al., (2010), fumigation plays a major role in insect pest elimination in stored products and phosphine gas is most widely used in grain fumigation, the ozone gas as fumigant used in controlling grain stored insects pests. However, modelling the behaviour of gas fumigants related to air volume of the stored grain mass is helpful in the finding out what factors may course fumigation failures and how this factors can be effected by environmental conditions due to limited information on fumigant activity within the commodity during the fumigation (Plumier, Schramm, and Maier 2018).

Today, for these multiple applications into various areas, researches conducted by many researchers experimentally to bring good management and better life to the society in general. Moreover, study grain fumigation is important roles in food commodities which is helpful to the environments. In this research work, advection and diffusion transport process is applied to the approach of mathematical modelling of grain fumigation in finding alternative techniques for the solution.

### 1.3 Problem Statement

The applications of transport phenomena play an important role to various disciplines including engineering, pharmacy, biology, agriculture, biomedical and others. Transport phenomena describes the relations and similarities among different types of transport that may occur in any system which comprising of momentum, energy and mass transports. There are uncertainties flow and transport properties on that phenomena which could be investigate through the field of experiments. The best application methods of fumigation phosphine gas distribution in grain silos are needed for fumigation to works properly so that the adequate concentration can be maintained for an adequate exposure period. However, solving such problem through the field of experiments will involve a very high cost. Hence mathematical modelling and computer simulation are alternative to that experimentation method with wide range research areas.

Advection-diffusion transport process of solute mass distribution can be studied by mathematical modelling to work out the solution by analytical or numerical approach. The couple advection-diffusion linear partial differential equations (PDEs) of solute mass transport is considered to be solved in this research work. The basic idea relies on the coupled advection-diffusion equation and linear partial differential equations (PDEs) for storage grain fumigation.

Besides that, this study will begin with a problem involving a coupled partial differential equation (PDE). This coupled equation is expected to be solved by hybrid numerical analytic and also numerically. Furthermore, this study will provide information on behaviour of gas based on available mathematical modelling, and hence the lack of understanding regarding fumigation will reduce.

## **1.4 Research Objectives**

The objectives of this research work are as follows:

- a) To get a hybrid numerical analytic solution of couple advection-diffusion of partial differential equation (PDE) related to grain fumigation problem using Laplace transform with numerical Week's method of Laplace inverse (WLI).
- b) To find the numerical solution of couple advection-diffusion partial differential equation (PDE) related to grain fumigation using finite difference method (FDM).
- c) To verify the current numerical Week's method of Laplace inverse (WLI) algorithm.
- d) To study the efficiency of phosphine gas concentration related to grain fumigation process.

## **1.5 Scope and Limitation of the study**

Transport phenomena is useful in the wide range of related application. In transport process that are consists of advection and diffusion equation, many mathematical models of differential equations (ODEs and PDEs) developed as well as grain fumigation from various researchers. The transport model partly adapted from grain fumigation in stored grain is an advection-diffusion equation which is a coupled of linear PDE were considered in this research work. However, various mathematical methods of the solution analytically or numerically applied to the problem in order to work out the solution to the models. This research work is limited to hybrid numerical analytic solution using Laplace transform with numerical Week's method of Laplace inverse (WLI) and numerical finite difference method (FDM).

## **1.6 Research Significance**

The advection and diffusion processes occur in surrounding of human life. fumigation application in a silo is among the significant transport phenomena in which there are many uncertainties about how the fumigant gas is distributed in air within the flow domain of silo. The study will show whether the gas concentration is sometimes lost due to the surrounding chemical reaction or absorb into something during the transport process and developed an understanding the behaviour of phosphine gas distribution throughout the silo. Significantly, the results obtained from this study will gives insight and enhance knowledge of the of advection-diffusion equation behaviour, particularly advection-diffusion of one-dimensional linear PDE. In addition, this study will contribute to a new theoretical knowledge in fumigation processes.

## **1.7 Outline Report**

This dissertation consists of five chapters. Firstly, chapter 1 which deal with an introduction to the whole work. This chapter contains subsections and includes all the important points such as research background, research objectives, problem statement, scope and limitation and the significance of the study. Secondly, Chapter 2 presents the literature review of this work. By different researchers, various works regarding transport phenomena, diffusion equation, advection diffusion equation, mathematical modelling of grain fumigation are discussed in details. In addition, the theory on Laplace transform as well as numerical Laplace inversion and numerical solution using FDM as it is the methodology were also presented in this dissertation.

The formulation of mathematical model as well as parameters values of the problem for this research work presented in Chapter 3. The algorithm solution to the model using Laplace transform with numerical Week's method of Laplace inverse (WLI) and numerical technique of FDM are all discussed in chapter 4. Then followed by the results in chapter 5, based on the results of FDM, verification of the numerical Week's method of Laplace inverse (WLI) algorithm and how the behaviour of a gas concentration related to grain fumigation process also briefly discusses. Lastly, the

## REFERENCES

- Abalone, R., A. Gastón, R. Bartosik, L. Cardoso, and J. Rodríguez. 2011. 'Gas Concentration in the Interstitial Atmosphere of a Wheat Silo-Bag. Part I: Model Development and Validation'. *Journal of Stored Products Research* 47(4):268–75.
- Abdullah, Norsyazleen azila binti. 2018. 'Solution for Coupled Differential Equations of Fumigant Transport in Grain Storage.' Universiti Teknologi Malaysia.
- Adamek, Vitezslav, Frantisek Vales, and Jan Cerv. 2017. 'Numerical Laplace Inversion in Problems of Elastodynamics: Comparison of Four Algorithms'. *Advance in Engineering Software* 113:120–29.
- Athayde, A. S. De, L. R. Piovesan, B. E. J. Bodmann, and M. T. M. B. De Vilhena. 2018. 'Analytical Solution of the Coupled Advection-Diffusion and Navier-Stokes Equation for Air Pollutant Emission Simulation'. 8(4):150–53.
- Bird, R. B., Stewart, W. E., Lightfoot, E. N. and Klingenberg, D. J. 2015. *Introductory Transport Phenomena*. edited by F. Sayre, Dan and Baratta. United States of America: Don Fowley.
- Brio, Moysey, Patrick O. Kano, and Jerome V. Moloney. 2005. 'Application of Weeks Method for the Numerical Inversion of the Laplace Transform to the Matrix Exponential'. *Communications in Mathematical Sciences* 3(3):335–72.
- Chakraverty, Snehashish, Rani Mahato Nisha, Perumandla Karunakar, and Tharasi Dilleswar Rao. 2019. *Advanced Numerical and Semi-Analytical Methods for Differential Equations*. first. Hoboken, NJ07030, USA: John Wiley & Sons, Inc.

- Chen, Jui Sheng, Yiu Hsuan Liu, Ching Ping Liang, Chen Wuing Liu, and Chien Wen Lin. 2011. 'Exact Analytical Solutions for Two-Dimensional Advection-Dispersion Equation in Cylindrical Coordinates Subject to Third-Type Inlet Boundary Condition'. *Advances in Water Resources* 34(3):365–74.
- Collins, P. J., G. J. Dargatzis, M. K. Nayak, P. R. Ebert, D. I. Schlipalius, W. Chen, H. Pavic, T. M. Lambkin, R. Kopittke, and B. W. Bridgeman. 2001. 'Combating Resistance to Phosphine in Australia'. *Proc. Int. Conf. Controlled Atmosphere and Fumigation in Stored Products* 593–607.
- Cox, P.D. and Collins, L. E. 2002. 'Factors Affecting the Behaviour of Beetle Pests in Stored Grain, with Particular Reference to the Development of Lures'. *Journal of Stored Products Research* 38(2):95–115.
- Darby, James; Willis, Tracy and Katherine Damcevski. 2009. 'Modelling the Kinetics of Ethyl Formate Sorption by Wheat Using Batch Experiments'. *Pest Management Science* 65(9):982–90.
- Darby, James. 2011. *Cooperative Research Centre for National Plant Biosecurity Final Report*.
- Darby, James A. 2008. 'A Kinetic Model of Fumigant Sorption by Grain Using Batch Experimental Data'. *Pest Management Scienc* 64:519–526.
- Darby, James and Peter Annis. 2003. 'Integrating Fumigation and Aeration.' *Stored Grain in Australia 2003. Proceedings of the Australian Postharvest Technical Conference* 126–33.
- Decker, S., R. L. Beeby, J. A. Hardin, C. L. Jones, D. A. Eltiste, R. T. Noyes, and E. L. Bonjour. 2010. 'Ozone Fumigation of Stored Grain; Closed-Loop Recirculation and the Rate of Ozone Consumption'. *Journal of Stored Products Research* 46(3):149–54.

Djordjevich, Alexandar and Svetislav Savovic. 2012. 'International Journal of Heat and Mass Transfer Finite Difference Solution of the One-Dimensional Advection – Diffusion Equation with Variable Coefficients in Semi-Infinite Media'. 55:4291–94.

Enderle, John D. and Bronzino, John D. 2012. *Introduction to Biomedical Engineering*. Third Edit. USA: Academic Press,30 Corporate Drive, Suite 400, Burlington, MA 01803, USA.

Fulford, Glenn R. and Philip Broadbridge. 2002. *Industrial Mathematics: Case Studies in the Diffusion of Heat and Matter*. First. CB2 2RU, UK: Press Syndicate of the University of Combigde.

Gastón, A., R. Abalone, R. E. Bartosik, and J. C. Rodríguez. 2009. 'Mathematical Modelling of Heat and Moisture Transfer of Wheat Stored in Plastic Bags (Silobags)'. *Biosystems Engineering* 104(1):72–85.

Gong, Chen, Dacheng Tao, Keren Fu, and Jie Yang. 2015. 'Fick's Law Assisted Propagation for Semisupervised Learning'. *IEEE Transactions on Neural Networks and Learning Systems*. 26(9):2148–62.

Isa, Z. M., T. W. Farrell, G. R. Fulford, and N. A. Kelson. 2016. 'Mathematical Modelling and Numerical Simulation of Phosphine Flow during Grain Fumigation in Leaky Cylindrical Silos'. *Journal of Stored Products Research* 67:28–40.

Logan, J. David. 2006. *A First Course in Differential Equations*. edited by S. & K. A. R. Axler. United States of America: Springer Science+Business Media, Inc., 233 Spring Street, New York, NY 10013, USA.

- Ndiyo, Etop. E. and Ubon A. Abasiokwere. 2018. ‘Comparative Analysis of Finite Difference Methods for Solving Second Order Linear Partial Differential Equations’. *International Journal of Mathematics Trends and Technology* 57(4):277–83.
- Pérez Guerrero, J. S. and T. H. Skaggs. 2010. ‘Analytical Solution for One-Dimensional Advection-Dispersion Transport Equation with Distance-Dependent Coefficients’. *Journal of Hydrology* 390(1–2):57–65.
- Plumier, Benjamin M., Matthew Schramm, and Dirk E. Maier. 2018. ‘Developing and Verifying a Fumigant Loss Model for Bulk Stored Grain to Predict Phosphine Concentrations by Taking into Account Fumigant Leakage and Sorption’. *Journal of Stored Products Research* 77:197–204.
- Rajendran, S. and Sriranjini, V. 2008. ‘Plant Products as Fumigants for Stored-Product Insect Control’. *Journal of Stored Products Research* 44(2):126–35.
- Rajendran, S. 2007. ‘Benchmarking - What Makes a Good Fumigation?’ *Proc. Int. Conf. Controlled Atmosphere and Fumigation in Stored Products, Gold-Coast Australia*. 345–65.
- Ridley, Andrew W., Philip R. Burrill, Christopher C. Cook, and Gregory J. Daglish. 2011. ‘Phosphine Fumigation of Silo Bags’. *Journal of Stored Products Research* 47(4):349–56.
- Smith, E. A., D. S. Jayas, and A. De Ville. 2001. ‘Modelling the Flow of Carbon Dioxide through Beds of Cereal Grains’. *Transport in Porous Media* 44(1):123–44.
- Stehfest, H. 1970. ‘Algorithm 368: Numerical Inversion of Laplace Transforms [D5]’. *Communications of the ACM* 13:47–49.
- Wang, Quanrong and Hongbin Zhan. 2015. ‘On Different Numerical Inverse Laplace Methods for Solute Transport Problems’. *Advances in Water Resources* 75:80–92.



- Xu, S., D. S. Jayas, N. D. G. White, and W. E. Muir. 2002. 'Momentum-Diffusive Model for Gas Transfer in Granular Media'. *Journal of Stored Products Research* 38(5):455–62.
- Yaghoubi, Abdulrahman. 2017. 'High-Order Finite Difference Schemes for Solving the Advection-Diffusion Equation'. *Mathematical and Computational Applications* 7(2):45–48.
- Zoppou, C. and Knight, J. .. 1997. *Analytical Solution of the Spatially Variable Coefficient Advective-Diffusion Equation in One-, Two- and Three-Dimensions*. Australia.