POLYIMIDE BASED MIXED MATRIX NANOFILTRATION MEMBRANE FOR REFINING PALM OIL

LIM KI MIN

UNIVERSITI TEKNOLOGI MALAYSIA

POLYIMIDE BASED MIXED MATRIX NANOFILTRATION MEMBRANE FOR REFINING PALM OIL

LIM KI MIN

A thesis submitted in fulfilment of the requirements for the award of the degree of Doctor of Philosophy

Malaysia-Japan International Institute of Technology Universiti Teknologi Malaysia

APRIL 2022

DEDICATION

This thesis is dedicated to my father, who taught me that the best kind of knowledge to have is that which is learned for its own sake. It is also dedicated to my mother, who taught me that even the largest task can be accomplished if it is done one step at a time.

ACKNOWLEDGEMENT

In preparing this thesis, I was in contact with many people, researchers, academicians, and practitioners. They have contributed towards my understanding and thoughts. In particular, I wish to express my sincere appreciation to my main thesis supervisor, Dr. Mohd Nazlee Faisal Md Ghazali, for encouragement, guidance, critics and friendship. I am also very thankful to my co-supervisor Dr. Tan Lian See and Dr. Mariam Firdhaus Mad Nordin for their guidance, advices and motivation. Without their continued support and interest, this thesis would not have been the same as presented here.

I am also indebted to Universiti Teknologi Malaysia (UTM) for funding my Ph.D study. Laboratory technicians in UTM also deserve a special thanks for their assistance during various unforeseen events in the laboratory.

My fellow postgraduate student should also be recognised for their support. My sincere appreciation also extends to all my colleagues and others who have provided assistance at various occasions. Their views and tips are useful indeed. Unfortunately, it is not possible to list all of them in this limited space. I am grateful to all my family member.

ABSTRACT

The purification of vegetable oil is an important process to obtain purified vegetable oil for various applications. However, conventional processes in vegetable oil purification, such as deacidification, require a huge amount of energy which is not only costly, but also contributes to a high rate of carbon footprints. To improve the current state of purification, the capability of membrane technology in purifying vegetable oil was investigated. The main objective of this study is to investigate the potential of polyimide-based mixed matrix membrane (MMM) in refining palm oil by nanofiltration. To achieve the objective, preliminary investigations on the performance of commercially available membranes were made. Subsequently, polyimide-based MMM with different additives loadings were fabricated and characterized. Additionally, membrane transport models were used to describe and predict the membrane separation process and a suitable multistage configuration was also proposed. The structural and physical characteristics of the fabricated membranes were studied. The separation performances of the fabricated membranes were investigated by using a dead-end stirred cell and ethyl acetate as the diluting solvent for palm oil. From the membrane characterization, it was found that MMM with 0.5wt% of β cyclodextrin functionalized multi-walled carbon nanotubes (BCD-fMWCNT) achieves the highest separation of palmitic acid from the feed diluted palm oil at 3.84 LMH/bar. The rejection of palmitic acid was found to be 60% and tocopherol, carotene and triglyceride at 94.43%, 98.74%, and 95.18% respectively. The membrane separation process was found to be best described by using the Solution-Diffusion model. Additionally, a theoretical study by using different multistage configurations found that the separation process can be further improved. The proposed multistage configuration was able to yield triglyceride with 99.28% purity with only 9.8% of oil loss in the purified permeate stream with a 41% of solvent recovery rate. Therefore, from this study, it is proven that membrane separation technology is a promising purification alternative and mixed matrix polyimide membrane has the potential in improving the conventional palm oil purification process.

ABSTRAK

Penulenan minyak sayuran adalah proses yang penting untuk mendapatkan minyak sayuran yang tulen untuk pelbagai aplikasi. Walau bagaimanapun, proses deasidifikasi minyak konvensional, memerlukan jumlah tenaga yang tinggi yang bukan sahaja mahal, malahan menyumbang kepada jejak karbon dalam kadar yang tinggi. Untuk menambahbaik proses penulenan pada masa kini, keupayaan teknologi membran dalam pemprosesan minyak sayuran telah dikaji. Objektif utama penyelidikan ini adalah untuk menyiasat potensi membran matriks campuran (MMM) berasaskan poliimid dalam penulenan minyak sawit. Untuk mencapai objektif utama, siasatan awal dengan menggunakan membran komersial telah dijalankan. Seterusnya, penghasilan and pencirian MMM berasaskan poliimid turut dilakukan. Pemerihalan proses pengasingan menggunakan membran telah dijalankan melalui model pengangkutan membran (MPM). Malahan, konfigurasi untuk nanofiltrasi secara bertingkat yang bersesuaian juga telah dicadangkan dalam kajian ini. Ciri-ciri struktur dan fizikal membran yang dibuat telah dikaji. Prestasi proses pengasingan melalui MMM telah dijalankan dengan menggunakan sel pengaduk hujung mati dan etil asetat sebagai bahan pelarut minyak sawit. Dari pencirian membran, adalah didapati bahawa MMM dengan 0.5% gabungan nanotiub karbon dinding-berganda berfungsikan beta siklo dekstrin (BCD-fMWCNT) mencapai kadar pengasingan asid palmitik yang tertinggi dari minyak sawit dalam kadar 3.84LMH/bar. Kajian ini juga mendapati bahawa penyingkiran asid palmitik, tokoferol, karotena, dan trigliserida adalah masing-masing pada kadar 60%, 94.43%, 98.74% dan 95.18%. Tambahan pula, dari segi perbandingan MPM, adalah didapati bahawa model resapan-larutan adalah model yang paling sesuai dalam perihalan proses nanofiltrasi minyak sawit dalam larutan etil asetat. Selain itu, dengan menggunakan nanofiltrasi secara bertingkat, pengumpulan semula bahan pelarut pada kadar 41% dan peningkatan ketulenan minyak sawit tulen (99.28%) dapat dicapai. Dari kajian ini, adalah terbukti bahawa teknologi membran adalah sesuai sebagai teknologi alternatif untuk menggantikan proses penulenan minyak sayuran yang konvensional.

TABLE OF CONTENTS

TITLE

| DECLARATION | iii |
|-----------------------|-------|
| DEDICATION | iv |
| ACKNOWLEDGEMENT | v |
| ABSTRACT | vi |
| ABSTRAK | vii |
| TABLE OF CONTENTS | viii |
| LIST OF TABLES | xii |
| LIST OF FIGURES | xiv |
| LIST OF ABBREVIATIONS | xviii |
| LIST OF SYMBOLS | XX |
| LIST OF APPENDICES | xxii |
| | |

| CHAPTER 1 | INTRODUCTION | | | |
|------------|--|----------|--|--|
| 1.1 | Background of Research | 1 | | |
| 1.2 | Problem Statement | 4 | | |
| 1.3 | Research Objectives | 5 | | |
| 1.4 | Research Scope | 5 | | |
| 1.5 | Significance to knowledge/ Contribution | 6 | | |
| 1.6 | Thesis Outline | 7 | | |
| CHAPTER 2 | LITERATURE REVIEW | 9 | | |
| 2.1 | Introduction | 9 | | |
| | | | | |
| 2.2 | Membrane Technology | 12 | | |
| 2.2 2.3 | Membrane Technology Application of Membrane Technology for Vegetable Oil Purifications | 12 14 | | |
| | Application of Membrane Technology for Vegetable | | | |
| | Application of Membrane Technology for Vegetable Oil Purifications | 14 | | |

| 2.5 | Membranes for Solvent-Resistant Nanofiltration | 26 |
|-----------|--|----|
| | 2.5.1 Nanoparticles for Mixed Matrix Membranes Fabrication | 26 |
| | 2.5.2 Polyimide Membrane Fabrications in the Literature | 29 |
| | 2.5.3 Modified Membranes for Vegetable Oil Purification | 30 |
| 2.6 | Prediction of Membrane Performance | 33 |
| | 2.6.1 Membrane Transport Model and Related Mathematical Equations | 33 |
| | 2.6.2 Akaike Information Criterion (AIC) | 40 |
| | 2.6.3 Activity Coefficient Estimation and Selectivity Figure of Merit (SFM) | 40 |
| | 2.6.4 Estimation of Transport and Process Parameters | 43 |
| | 2.6.5 Multistage Nanofiltration | 45 |
| 2.7 | Research Gaps | 46 |
| CHAPTER 3 | RESEARCH METHODOLOGY | 47 |
| 3.1 | Introduction | 47 |
| 3.2 | Materials | 48 |
| 3.3 | Preparation of Beta-Cyclodextrin Functionalized Multi-Walled Carbon Nanotube Additives (βCD- fMWCNT) | 50 |
| 3.4 | Preparation of Polymer Dope Solution | 51 |
| 3.5 | Membrane Fabrications | 51 |
| 3.6 | Membrane Characterizations | 52 |
| | 3.6.1 Fourier Transform Infrared Spectroscopy- Attenuated Total Reflectance (FTIR-ATR) | 53 |
| | 3.6.2 Thermogravimetric Analysis (TGA) | 53 |
| | 3.6.3 Field Emission Scanning Electron Microscopy (FESEM) | 53 |
| | 3.6.4 Atomic Force Microscopy (AFM) | 53 |
| | 3.6.5 Contact Angle | 54 |
| | 3.6.6 Wettability, Porosity, and Pore Size of Membrane | 54 |
| | 3.6.7 Membrane Swelling | 55 |

| | 3.6.8 Membrane Dye Rejections | 56 |
|-----------|--|----|
| 3.7 | Membrane Performance | 56 |
| 3.8 | Sample Analysis | 57 |
| 3.9 | Concentration Polarization | 58 |
| 3.10 | Modeling and Parameter Estimation | 59 |
| 3.11 | Model Development and Verification | 61 |
| 3.12 | Multistage Nanofiltration | 62 |
| CHAPTER 4 | RESULTS AND DISCUSSIONS | 63 |
| 4.1 | Nanofiltration of Commercial Membranes and Membrane Selectivity Characterization | 63 |
| | 4.1.1 Pure Solvent Permeances of Commercial OSN Membranes | 63 |
| | 4.1.2 Swelling of OSN Membrane | 65 |
| | 4.1.3 Membrane Separation Performances of Oil Constituents | 66 |
| | 4.1.4 The Effect of Concentration Polarization | 70 |
| | 4.1.5 Membrane Characterization by Robeson Plot | 73 |
| 4.2 | Fabrication of Polyimide Membranes for Nanofiltration of Vegetable Oil | 78 |
| | 4.2.1 Molecular Simulations and Interaction Studies of Solutes in Vegetable Oil and Polyimide P84 | 78 |
| | 4.2.2 Molecular Simulations of Interactions Between Solutes in Vegetable Oil and β-Cyclodextrin | 81 |
| | 4.2.3 Fabrication and Nanofiltration of PolyimideP84 Membranes with β-Cyclodextrin asAdditives | 83 |
| | 4.2.4 Fabrication of PI Membranes with βCD- fMWCNT as Additives | 86 |
| | 4.2.4.1 Morphological Studies of the Fabricated Membranes | 86 |
| | 4.2.4.2 Polymeric Membrane Material Analysis | 90 |
| | 4.2.4.3 Hydrophilicity and Porosity of the Fabricated Membranes | 94 |

| LIST OF PUBLICATIONS | | 180 |
|----------------------|--|-----|
| REFERENCES | | 125 |
| 5.2 | Recommendations | 123 |
| 5.1 | Conclusion | 121 |
| CHAPTER 5 | CONCLUSION AND RECOMMENDATIONS | 121 |
| 4.4 | Multistage Nanofiltration | 111 |
| 4.3 | Nanofiltration of Vegetable Oil by Using β CD-fMWCNT PI Membranes | 103 |
| | 4.2.4.5 Nanofiltration of Vegetable Oil by Using βCD-fMWCNT PI Membranes | 100 |
| | 4.2.4.4 Dye Rejection Investigation for Estimation of Molecular Weight Cut- Off (MWCO) | 98 |

LIST OF TABLES

| TABLE NO. | TITLE | PAGE |
|-----------|---|------|
| Table 2.1 | Summary of steps involved in conventional processing of vegetable oil (Gupta, 2008; Hamm <i>et al.</i> , 2013; O'Brien, 2008). | 11 |
| Table 2.2 | Summary of findings for deacidification and nutrient recovery/ decoloration. | 21 |
| Table 2.3 | Separation performances of recently modified membranes for the purification of vegetable oil. | 32 |
| Table 2.4 | Commonly used transport model and some of their applications. | 38 |
| Table 3.1 | Components in palm oil (Gupta, 2008). | 49 |
| Table 3.2 | Composition of synthetically prepared degummed palm oil. (Gupta, 2008). | 49 |
| Table 3.3 | Membrane specifications. | 50 |
| Table 3.4 | List of membranes fabricated in this study. | 52 |
| Table 4.1 | Pure solvent permeances of commercial OSN membranes tested at 20 bar using dead-end filtration cell at room temperature. | 65 |
| Table 4.2 | Membrane-solvent penetrant interaction parameter estimated by Flory-Huggins solution theory. | 66 |
| Table 4.3 | Molar volume and solubility parameters calculated by Hildebrand solubility parameter coupled with group contribution method by Fedors (1974). | 67 |
| Table 4.4 | Separation of palmitic acid, tocopherol, carotenoids, and triglycerides with commercial membranes of different MWCO. (Feed: 10wt% oil in the various solvents, tested with dead-end filtration cells at 20 bar and room temperature). | 68 |
| Table 4.5 | Calculated mass transfer coefficient, concentration polarization modulus and selectivity. | 71 |
| Table 4.6 | Calculated molecular weight ratio, process performance, and selectivity figure of merit. | 74 |

| Table 4.7 | Affinity parameters and interactions between receptor- ligand obtained through molecular docking and simulations. | 80 |
|------------|--|-----|
| Table 4.8 | Affinity parameters and interactions between beta- cyclodextrin and different vegetable oil solutes. | 82 |
| Table 4.9 | Solubility parameters estimated and obtained from literature (Alqarni <i>et al.</i> , 2021) at 298K. | 93 |
| Table 4.10 | The contact angles, average pore radius, effective porosity, and water contents of the fabricated polyimide membranes. | 95 |
| Table 4.11 | Solubility parameters estimated by Hildebrand solubility parameter coupled with group contribution method by Fedors. | 99 |
| Table 4.12 | Rejection data deviation from the estimated model. | 104 |
| Table 4.13 | Parameters obtained from the nonlinear model estimation of different membrane transport models. | 109 |
| Table 4.14 | Norm of residuals (<i>resnorm</i>) and Akaike Information Criterion (<i>AIC</i>) of the different models calculated in this study. | 110 |
| Table 4.15 | Calculated mass balance for configuration 1. | 113 |
| Table 4.16 | Calculated mass balance for configuration 2. | 115 |
| Table 4.17 | Calculated mass balance for configuration 3. | 117 |
| Table 4.18 | Summary of yield at retentate stream and solvent recovery after filtration. | 117 |
| Table 4.19 | Comparisons of solute compositions before and after filtrations. (oil composition in the retentate stream) | 119 |

LIST OF FIGURES

| FIGURE NO | . TITLE | PAGE |
|------------|--|------|
| Figure 1.1 | Comparison between conventional oil refining method and membrane refining method (Cheryan, 2005). | 3 |
| Figure 2.1 | Diagram showing typical chemical compounds found in palm oil: (a) alpha carotene; (b) beta carotene; (c) oleic acid; (d) palmitic acid; (e) tocopherol; (f) phospholipid; (g) triolein; (h) tripalmitin (Cheryan, 2005; Gupta, 2008). | 10 |
| Figure 2.2 | Schematic representation of (a) integrally skinned asymmetric membrane; (b) thin-film composite membrane (Vandezande <i>et al.</i> , 2008). | 14 |
| Figure 2.3 | Schematic ternary phase diagram of solvent/ non-solvent/ polymer system (Ayman <i>et al.</i> , 2012; Vandezande <i>et al.</i> , 2008). | 25 |
| Figure 2.4 | Molecular structure of a beta-cyclodextrin molecule (a) toroid structure of beta-cyclodextrin (b) seven-membered ring molecule(Haynes, 2009). | 28 |
| Figure 2.5 | Graphical model generated by molecular visualization program showing the structure of (a) SWCNT (b) MWCNT. | 29 |
| Figure 2.6 | Membrane cascades (a) without recycling (b) with recycling stream (Cui and Muralidhara, 2010; Kale <i>et al.</i> , 1999; Peeva <i>et al.</i> , 2014). | 45 |
| Figure 2.7 | Continuous purification membrane cascade according to McCabe-Thiele method (Lejeune <i>et al.</i> , 2018). | 46 |
| Figure 3.1 | Overall research flow in this study. | 48 |
| Figure 3.2 | Illustration showing the fabrication of a membrane. | 52 |
| Figure 3.3 | Membrane separation set-up by using dead-end stirred cell. | 57 |
| Figure 3.4 | Illustration showing the mechanism of concentration polarization. | 58 |
| Figure 3.5 | Calculation of permeability of different solutes and solvents by using modified UNIFAC (Dortmund) model, MATLAB, and solution-diffusion model. | 60 |

| Figure 3.6 | Data prediction by different transport models and nanofiltration (NaCl-water) experimental results by Sourirajan. | 62 |
|-------------|---|----|
| Figure 4.1 | Flux profile of pure organic solvents through different membranes: (a) acetone; (b) ethyl acetate; (c) isopropanol at 20 bar operating pressure. | |
| Figure 4.2 | Pure solvent permeances of commercial membranes tested under 20 bar using dead-end filtration cell at room temperature. | 65 |
| Figure 4.3 | Separation of palmitic acid, tocopherol, carotenoids and triglycerides with commercial membranes of different MWCO by using (a) acetone, (b) ethyl acetate, (c) isopropanol as solvent. (Feed: 10wt% oil, tested with dead end filtration cells at 20 bar and room temperature). | 69 |
| Figure 4.4 | Plot of $SFM_{A/B}$ to compare membrane experimental data in Robeson-style plot. | 77 |
| Figure 4.5 | Molecular simulations of the interactions between (a) PI1- C, (b) PI2-C, (c) PI3-C, (d) PI1-PA, (e) PI2-PA, (f) PI3-PA, (g) PI1-T, (h) PI2-T, (i) PI3-T, (j) PI1-TG, (k) PI2-TG, (l) PI3-TG (where PI is polyimide, T is tocopherol, C is carotene, PA is palmitic acid, and TG is triglyceride). | 79 |
| Figure 4.6 | Molecular simulations of the interactions between beta- cyclodextrin and (a) palmitic acid; (b) triolein; (c) beta- carotene; (d) alpha-tocopherol. | 81 |
| Figure 4.7 | Results obtained after centrifugation of oil with solutes and cyclodextrin for the different stirring duration. | 82 |
| Figure 4.8 | Investigation on the fabricated polyimide membrane with beta-cyclodextrin additives and acetone as solvent (10 bar, 1000RPM, 10wt% oil). | 84 |
| Figure 4.9 | Investigation on the fabricated polyimide membrane with beta-cyclodextrin additives and ethyl acetate as solvent (10bar, 1000RPM, 10wt% oil). | 85 |
| Figure 4.10 | The FESEM and photo images of PI membranes with different β CD-fMWCNT loadings (a) M-0, (b) M-0.25, (c) M-0.50, (d) M-1.00, (e) M-2.00. | 87 |
| Figure 4.11 | AFM images (scan size $5 \times 5 \ \mu\text{m2}$) of prepared membranes at different β CD-fMWCNT loadings: (a) M-0, (b) M-0.25, (c) M-0.50, (d) M-1.00, (e) M-2.00 | 89 |
| Figure 4.12 | Mean roughness and maximum height obtained from AFM analysis for different fabricated PI membranes. | 89 |

| Figure 4.13 | ATR-FTIR spectra of polyimide membranes before and after membrane conditioning. | 91 |
|-------------|---|-----|
| Figure 4.14 | ATR-FTIR spectra of polyimide membranes before and after β CD-fMWCNT additives addition. | 91 |
| Figure 4.15 | TGA of fabricated polyimide membranes. | 93 |
| Figure 4.16 | Flux profile of pure (a) water, (b) ethyl acetate, and (c) acetone in different fabricated polyimide membranes at 10 bar. | 96 |
| Figure 4.17 | Flux comparisons of water and ethyl acetate in different loadings of additives. | 97 |
| Figure 4.18 | Dye rejection ability of fabricated polyimide P84 membranes (10bar, 1000 RPM) | 98 |
| Figure 4.19 | Photos showing the color difference between feed, permeate, and retentate (M-0.5, 10 bar, 1000RPM). | 99 |
| Figure 4.20 | Photos showing the retention of methylene blue on the fabricated membranes after filtration. | 99 |
| Figure 4.21 | Effects of MWCNT loadings on the rejection of solutes in synthetically prepared oil diluted in ethyl acetate (10wt% oil, 10 bar, 1000RPM). | 100 |
| Figure 4.22 | Effects of pressure on the rejection of solutes and permeate flux in synthetic oil diluted with ethyl acetate (M-0.5, 10wt% oil, 1000RPM). | 101 |
| Figure 4.23 | Rejection and permeate flux comparison of solutes in synthetic oil and synthetic oil with an increased amount of palmitic acid content (1.8325g of palmitic acid in 10mL oil) (M-0.5, 10wt% oil, 10 bar, 1000RPM). | 102 |
| Figure 4.24 | Data prediction by using different nanofiltration membrane transport models for (a) palmitic acid, (b) triglyceride, (c) carotene, (d) tocopherol. | 105 |
| Figure 4.25 | Data deviation between experimental and calculated permeate fluxes by different nanofiltration membrane transport models, (a) Solution-Diffusion, (b) Spiegler- Kedem, (c) Solution-Diffusion Imperfections, (d) Finely Porous model. | 106 |
| Figure 4.26 | Data deviation between experimental and calculated rejections by different nanofiltration membrane transport models, (a) Solution-Diffusion, (b) Spiegler-Kedem, (c) Solution-Diffusion Imperfections, (d) Finely Porous model. | 107 |
| | | 107 |

| Figure 4.27 | Configuration 1 showing the illustration of multistage nanofiltration without recycling stream (M-0.5 as selected membrane). | 112 |
|-------------|---|-----|
| Figure 4.28 | Configuration 2 showing the illustration of multistage nanofiltration with recycling of permeate stream (M-0.5 as selected membrane). | 114 |
| Figure 4.29 | Configuration 3 showing the illustration of multistage nanofiltration with recycle streams (M-0.5 as selected membrane). | 116 |
| Figure 4.30 | Illustration showing configuration 1 as the first multistage unit, and configuration 3 as the second multistage unit (Config1+3). | 118 |

LIST OF ABBREVIATIONS

| ACM | - | Aspen Custom Modeler |
|--------|---|--|
| AFM | - | Atomic Force Microscopy |
| ANN | - | Artificial Neural Network |
| ATR | - | Attenuated Total Reflectance |
| βCD | - | Beta-Cyclodextrin |
| CA | - | Cellulose Acetate |
| CFSD | - | Combined Film Theory/ Solution Diffusion |
| DG | - | Diglyceride |
| EOS | - | Equation of State |
| FESEM | - | Field Emission Scanning Electron Microscopy |
| FFA | - | Free Fatty Acid |
| fMWCNT | - | Functionalized Multi-Walled Carbon Nanotubes |
| FTIR | - | Fourier-Transform Infrared Spectroscopy |
| GLCF | - | Group Contribution Lattice Fluid |
| HPLC | - | High-Pressure Liquid Chromatography |
| MB | - | Methylene Blue |
| MF | - | Microfiltration |
| MG | - | Monoglyceride |
| MWCNT | - | Multi-Walled Carbon Nanotubes |
| NF | - | Nanofiltration |
| OSN | - | Organic Solvent Nanofiltration |
| PA | - | Palmitic Acid |
| PDMS | - | Polydimethylsiloxane |
| PEEK | - | Polyether Ether Ketone |
| PEG | - | Polyethyleneglycol |
| PES | - | Polyethersulfone |
| PI | - | Polyimide |
| PI1 | - | Polyimide P84 Structure 1 |
| PI2 | - | Polyimide P84 Structure 2 |
| PI3 | - | Polyimide P84 Structure 3 |
| | | |

| - | Polysulfone |
|---|----------------------------------|
| - | Polyvinyl Alcohol |
| - | Polyvinylidene Difluoride |
| - | Rose Bengal |
| - | Reverse Osmosis |
| - | Selectivity Figure of Merit |
| - | Silicon |
| - | Solvent Resistant Nanofiltration |
| - | Single-Walled Carbon Nanotubes |
| - | Triglyceride |
| - | Thermogravimetric Analysis |
| | - |

LIST OF SYMBOLS

| $\delta_{_d}$ | - | Energy from dispersion forces between molecules [MPa ^{1/2}] |
|---------------------------------|---|---|
| ${\delta}_{_p}$ | - | Energy from the dipolar intermolecular force between |
| p | | molecules [MPa ^{1/2}] |
| $\delta_{\scriptscriptstyle h}$ | - | Energy from hydrogen bonds between molecules [MPa ^{1/2}] |
| ΔV | - | Permeate Volume [L] |
| Δt | - | Time Duration [h] |
| A | - | Surface Area of Membrane [m ²] |
| %R | - | Percentage of Rejection [%] |
| Re | - | Reynold Number [-] |
| C_P | - | Permeate Concentration [mg/L] |
| C_{R} | - | Retentate Concentration [mg/L] |
| R_0 | - | Observed Rejection [-] |
| k | - | Mass Transfer Coefficient [m/s] |
| $oldsymbol{J}_V$ | - | Solvent Flux [Lm ⁻² h ⁻¹] |
| J_{s} | - | Solute Flux [Lm ⁻² h ⁻¹] |
| $\frac{D_{AM}K}{\delta}$ | - | Solute Transport Parameter [m ² /s] |
| σ | - | Reflection Coefficient [-] |
| P_{M} | - | Permeability Coefficient [m/s] |
| D_i | - | Diffusion Coefficient [cm ² /s] |
| l | - | Thickness of Membrane [µm] |
| p_o | - | Pressure at the Retentate/Feed Side [bar] |
| p_l | - | Pressure at the Permeate Side [bar] |
| Vi | - | Molar Volume of Species i [cm ³ /mol] |
| C_O | - | Concentration at the Retentate Side [mg/L] |
| C_l | - | Concentration at the Permeate Side [mg/L] |
| d_i | - | Effective Diameter of Solute <i>i</i> [m] |
| k _B | - | Boltzmann's Constant [-] |

| μ_s | - | Dynamic Viscosity of Solvent [cP] |
|-----------------------|---|---|
| 3 | - | Membrane Porosity [nm] |
| Q | - | The volume of Pure Water Permeated Per Time [L] |
| η | - | The viscosity of Pure Water [cP] |
| $arPsi_i$ | - | Molecular Volume Fraction of Species <i>i</i> [-] |
| $	heta_i$ ' | - | Molecular Surface Area Fraction of Species <i>i</i> [-] |
| <i>r</i> _i | - | Van der Waals Volume of Species <i>i</i> [-] |
| q_i | - | Van der Waals Surface Area of Species <i>i</i> [-] |
| x_i | - | Mole Fraction of Species <i>i</i> [-] |
| $v^i{}_k$ | - | Number of Group k in Species i [-] |
| Γ_k | - | Residual Activity Coefficient in Group k in a mixture [-] |
| $\Gamma^{i}{}_{k}$ | - | Residual Activity Coefficient in Group k in a Pure Solution |
| | | of Species <i>i</i> [-] |
| Ψ_{nm} | - | Interaction Parameter of Structural Group m and n [-] |
| Φ_i | - | Volume Fraction of Solvent Penetrant <i>i</i> [-] |
| χ | - | Membrane Solvent Penetrant Interaction Parameter [-] |
| $ ho_m$ | - | The density of polymer $m [g/cm^3]$ |
| Pe | - | Peclet number [-] |

LIST OF APPENDICES

| APPENDIX | TITLE | PAGE |
|------------|---|------|
| Appendix A | Derivation of Combined Solution-Diffusion with Imperfections Model | 141 |
| Appendix B | Sample Calculation for Selectivity Figure of Merit (SFM) | 144 |
| Appendix C | Multistage Nanofiltration Mass Balances | 153 |
| Appendix D | Standard Curves | 156 |
| Appendix E | FESEM images | 165 |
| Appendix F | Membrane Certificate | 175 |

CHAPTER 1

INTRODUCTION

1.1 Background of Research

Vegetable oils such as oil palm, soybean, rapeseed, and sunflower oil have been studied widely for their production processes since the early years of this century due to their wide availability and uses. The processed oil from plants can be used in fields such as in food products, supplement and nutrition products, beauty products, and most recently biofuels (Pal and Pratap, 2017; Panchal et al., 2017). Vegetable oil processing involves the removal of undesirable components such as phospholipids, free fatty acids (FFA), sterols, trace metals, and oxidation products from edible oil which affects the taste and texture of the vegetable oil. The main stages in conventional vegetable oil processing are solvent extraction, evaporation, degumming, deacidification, bleaching, dewaxing, and deodorization (Gupta, 2008). Although these stages have been used widely in the industry, it possesses some major drawbacks which can be improved by current technology (de Morais Coutinho et al., 2009; Vaisali et al., 2015). Some of the highlighted drawbacks are high energy usage, oil losses, and contaminated effluents produced during the processes (de Morais Coutinho et al., 2009; Vaisali et al., 2015). As Malaysia and Indonesia primarily produce palm oil with approximately 84% of the world's production, the technological enhancement in the palm oil production industry would potentially bring about a significant costsaving and improved energy-efficiency in obtaining refined oil which is aligned with the current efforts of reducing carbon footprints.

Membrane technology is one of the promising alternatives for the industrial processing of vegetable oil (as can be seen in Figure 1.1) and it has been studied extensively by researchers on a lab-scale to industrial scale (Vaisali *et al.*, 2015). In the field of vegetable oil processing, this technology is capable of removing undesirable products and retrieve valuable components from crude vegetable oil

(Marchetti *et al.*, 2014; Priske *et al.*, 2016). Besides that, the solvent used during the filtration process can also be recovered. Moreover, the membrane technology is relatively energy efficient as compared to conventional approaches such as distillation. Various studies on membrane-aided vegetable oil purification have been published by researchers in the recent years (Azmi *et al.*, 2015; Firman *et al.*, 2017a; Shi *et al.*, 2019; Werth *et al.*, 2017a). From their studies, it was found that vegetable oil needs to be diluted to allow a better permeation flux and separation. As organic solvent can dissolve polymers through solvent diffusion and chain disentanglement, membrane polymer with high solvent-resistance properties is usually used in the study (Gugliuzza, 2015; Lim *et al.*, 2017). Solvent-resistant polymers such as polybenzimidazole (PBI), polyimide (PI), and poly (ether ether) ketone (PEEK) were some of the polymers used for the fabrication of membrane (Galizia and Bye, 2018). The use of solvent-resistant membranes was found to be successful in rejecting triglycerides at high rate of rejection with acceptable solvent permeation fluxes.

However, research on the separation of free fatty acids and nutritional compounds from vegetable oil are still on-going due to the difficulty of separating compounds of similar sizes with acceptable solvent permeability (Vaisali *et al.*, 2015). In the study by Shi *et al.* (2019), they had performed the separation of linoleic acid from glyceryl trilinoleate by using commercial solvent-resistant membranes. It was found the DuraMem 500 was able to reject glyceryl trilinoleate and linoleic acid at around 86% and 35% respectively at acetone permeation of 1.02 LMH/bar. In another study, Werth *et al.* (2017a) have investigated the separation between rapeseed oil and oleic acid by using PuraMem 280 membrane. They have discovered that the membrane was able to reject 97% and 34.7% of rapeseed oil and oleic acid respectively at 0.1135 kg m⁻²h⁻¹bar⁻¹ of ethanol permeation. From the investigation by the researchers, it is proven that polymeric membrane is capable of separating compounds in vegetable oil. Nevertheless, more investigations are needed to improve the permeation flux of the solvent without compensating the membrane selectivity and rejection performances.

In recent decades, nanoparticles have been employed in different fields of industry such as paint, surface coating, and polymer products (Stark *et al.*, 2015). The nano-size particles were found to enhance the properties of the materials and products

when a certain composition (of nanoparticles) was added to the base material (Nazari and Riahi, 2011; Stark *et al.*, 2015; Sun *et al.*, 2011). In the field of membrane technology, nanoparticles such as metal oxides, carbon molecular sieves, carbon nanotubes, and zeolites have been studied (Cheng *et al.*, 2018). In the research by Soroko and Livingston (2009), it was found that titanium dioxide was able to improve the structural stability of the membrane. In another study, carbon nanotubes were used as the filler which improves the permeation flux of the fabricated membrane (Farahani *et al.*, 2018). From these studies, the addition of nanoparticles was found to have positive effects on the performance of the fabricated membranes.

Conventional Membrane Technology Oil seed Oil seed Solvent extraction Seed preparation Hexane ► Lecithin Ultrafiltration Solvent extraction ┶ Hexane Nanofiltration Evaporation Water Evaporation Degumming Lecithin ╈ ► FFA Nanofiltration Crude oil Acid Alkali ► Wax Deacidification Soap Microfiltration FFA Vapor Bleaching Deodorization permeation Gas N_2 Winterization/ Dewaxing permeation ¥ Effluents Effluents Deodorization free Refined ₩ N_2 discharge packed oil Refined packed oil

Figure 1.1 Comparison between conventional oil refining method and membrane refining method (Cheryan, 2005).

The prediction of membrane separation performance on the other hand can be performed through the use of membrane transport models as proposed by researchers (Marchetti and Livingston, 2015). There are various membrane transport models available, such as the widely known solution-diffusion model, pore-flow model, and irreversible thermodynamic models. Through the correlation of experimental data to a certain membrane transport model, the mathematical description of a certain separation process can be obtained (Peshev and Livingston, 2013). The correlation of data to the model will require the estimation of model parameters which can be obtained through non-linear regression of data to the selected model. Besides that, the performance of the separation process can be further improved by employing multistage nanofiltration (Renouard *et al.*, 2018). By using a selected multistage configuration, the separation process could be more effective in separating solutes as well as enabling the recovery of solvents.

1.2 Problem Statement

The refining of vegetable oil is indeed important for the production of different consumable products in our daily life. However, the conventional refining process of vegetable oil particularly stages that involve high energy requirements such as steam distillation during the deacidification stage and winterization during the dewaxing process should be improved (Shi et al., 2019; Werth et al., 2017b). According to the researchers, the current refining process also resulted in the unnecessary loss of oil from the hydrolysis process, production of low-value soap stocks, and highly cost explosion-proof equipment (Vaisali et al., 2015). Therefore, an alternative way to remove the undesirable compounds from the vegetable oil is desired. Membrane technology is a preferable way to separate the compounds as it has low energy requirement, the ability to recover compounds in their natural state, as well as the capability to recover solvents (Marchetti et al., 2014). Although there are studies on the use of membranes to separate oil compounds, their results were either low in selectivity or low in permeation flux which makes them unsuitable for industrial applications (Shi and Chung, 2020; Werth et al., 2017a). In the recent decades, there is an emerging technology known as nanoparticle technology which can improve the overall structure and performance of materials. There are already studies on the use of nanoparticles in the fabrication of membrane, which resulted in mixed matrix membrane (MMM) or thin-film nanocomposite (TFN). However, to our best of knowledge, there is a lack of study on the fabrication of MMM for the separation of vegetable oil (Abdellah *et al.*, 2019; Ali *et al.*, 2021; Shi and Chung, 2020). Therefore, through different formulations of polymer dope solution, the fabrication of suitable MMM for vegetable oil purification can be obtained in this study.

1.3 Research Objectives

Based on the aforementioned issues, the following objectives were constructed:

- i) To formulate and fabricate integrally skinned asymmetric (ISA) membranes and mixed matrix membranes (MMM) with different additive loadings.
- ii) To perform membrane characterization on fabricated membranes and membrane performance study.
- iii) To predict the performance of selected fabricated membrane by using different membrane transport models.
- iv) To theoretically evaluate the selected membrane performance using multistage nanofiltration configuration.

1.4 Research Scope

This study focuses on the separation of palmitic acid from synthetically prepared palm oil diluted in the organic solvent. Hence, the following scopes of the study were identified and listed as follows:

• Membrane performance studies of commercial solvent-resistant membranes by solute rejections, solvent permeation fluxes, and selectivity of membranes towards different solutes (palmitic acid, tocopherol, carotene, triglyceride) in the solvent-diluted (acetone, ethyl acetate, isopropanol) synthetically prepared palm oil.

- Membrane swelling studies of the commercial solvent-resistant membrane in different solvents (acetone, ethyl acetate, isopropanol).
- Solute-solvent-polymer interaction studies by using molecular modeling.
- Membrane formulation by using polyimide P84 at different solvent/cosolvent ratios.
- Membrane fabrication by using polyimide P84 as the polymer and betacyclodextrin (β-CD) and beta-cyclodextrin functionalized multi-walled carbon nanotubes (βCD-fMWCNT) as additives.
- Membrane performance studies of fabricated membranes by using solventdiluted synthetically prepared palm oil at different additive loadings.
- Membrane characterization of fabricated membranes by using FESEM, AFM, FTIR, TGA, contact angle, pore size, wettability, and dye rejection.
- Membrane performance prediction by using different membrane transport models, where parameter estimation was performed by using MATLAB.
- Evaluation of different multistage nanofiltration configurations for improving membrane selectivity and solvent recovery.

1.5 Significance to knowledge/ Contribution

The technology for fractionating vegetable oil has been stagnant for the past 30-50 years due to the successful separation of the oil through physical and chemical refining methods (Vaisali *et al.*, 2015). However, in recent years, there is an increasing need to improve the conventional method due to its negative impact on the environment and equipment lifespan (Szekely and Zhao, 2022). The use of membrane separation technology was introduced in different industries that involve purification and separation. However, as of current, the vegetable oil refineries still rely on the conventional method due to the low permeation flux, low selectivity, and lack of studies on solvent-resistant membranes in fractionating vegetable oil components (Vaisali *et al.*, 2015). There were several studies on the use of a membrane in vegetable oil purification, but the results were either low in permeation flux or low in the selectivity of desired vegetable oil constituents (Shi and Chung, 2020; Shi *et al.*, 2019). This report is the first to describe the use of polyimide P84 nanofiltration membrane

with β CD-fMWCNT additives for the purification of palm oil. The present study found that the use of polyimide P84 membrane constructed through the use of DMF and 1,4-Dioxane as solvent was able to separate palmitic acid from triglyceride at a high selectivity and permeation flux. The addition of β CD-fMWCNT additives at certain compositions also further improves the selectivity of palmitic acid/ triglyceride and permeation flux. Furthermore, it was found that the solution-diffusion model is the best to describe the nanofiltration of ethyl acetate-diluted palm oil. By using the data from the fabricated membrane, it was also found that the selectivity and solvent recovery of the nanofiltration process can be further improved through a proposed multistage configuration. From the findings, it is demonstrated that polyimide P84 mixed matrix membrane is a promising candidate for vegetable oil deacidification applications. This work contributes to the development of membrane technology in the vegetable oil processing field, especially in the deacidification process. This work particularly provides useful data and information for the implementation of mixed matrix membrane in deacidifying vegetable oil. Besides that, through the use of different membrane transport models and multistage, this work can contribute to the future development of artificial intelligence (AI) models, in which the results from the experiments and nonlinear regressions can be used as part of the database.

1.6 Thesis Outline

This thesis consists of 5 chapters. Chapter one explains the background, objectives, scope and problem statement of this research. Chapter two provides literature review related to this research, which also includes the mathematical equations which are useful in describing and comparing the different experimental results. Chapter three outlines the methodology of the research. The methodology describes all the materials, equipment, experimental procedures, as well as process flow or description in obtaining related experimental results. Chapter four of this thesis provides explanation and discussion on the results obtained from the experiments. Finally, chapter five concludes the research and also summarizes the important findings of the study. Chapter five also include recommendations which describes the future directions of this study.

REFERENCES

- Abdellah, M., Liu, L., Scholes, C., Freeman, B., and Kentish, S. (2019). Organic solvent nanofiltration of binary vegetable oil/terpene mixtures: Experiments and modelling, *Journal of membrane science*, 573, 694-703.
- Ahmad, A., Tan, L., and Shukor, S. A. (2009). Modeling of the retention of atrazine and dimethoate with nanofiltration, *Chemical Engineering Journal*, 147, 280-286.
- Ali, N. S., Ghaffar, A., Qaiser, A. A., and Ahmad, M. (2021). Synthesis and Characterization of Polyaniline-Polyimide Thin-film Composite Membranes for Vegetable Oils/Solvent Separation, *폴리마*, 45, 68-78.
- Alqarni, M. H., Haq, N., Alam, P., Abdel-Kader, M. S., Foudah, A. I., and Shakeel, F. (2021). Solubility data, Hansen solubility parameters and thermodynamic behavior of pterostilbene in some pure solvents and different (PEG-400+ water) cosolvent compositions, *Journal of Molecular Liquids*, 331, 115700.
- Araújo, T., Bernardo, G., and Mendes, A. (2020). Cellulose-Based Carbon Molecular Sieve Membranes for Gas Separation: A Review, *Molecules*, 25, 3532.
- Arora, S., Manjula, S., Krishna, A. G., and Subramanian, R. (2006). Membrane processing of crude palm oil, *Desalination*, 191, 454-466.
- Ayman, E.-G., Heba, A., and Sahar, A. (2012). Construction of ternary phase diagram and membrane morphology evaluation for polyamide/formic acid/water system, *Australian Journal of Basic and Applied Sciences*, 6, 62-68.
- Azmi, R., Goh, P., Ismail, A., Lau, W., Ng, B., Othman, N., et al. (2015). Deacidification of crude palm oil using PVA-crosslinked PVDF membrane, *Journal of Food Engineering*, 166, 165-173.
- Benedetti, F. M., De Angelis, M. G., Degli Esposti, M., Fabbri, P., Masili, A., Orsini, A., et al. (2020). Enhancing the separation performance of glassy PPO with the addition of a molecular sieve (ZIF-8): gas transport at various temperatures, *Membranes*, 10, 56.
- Bhosle, B. M., Subramanian, R., and Ebert, K. (2005). Deacidification of model vegetable oils using polymeric membranes, *European Journal of Lipid Science* and Technology, 107, 746-753.

- Chabalala, M. B., Seshabela, B. C., Van Hulle, S., Mamba, B. B., Mhlanga, S. D., and Nxumalo, E. N. (2018). Cyclodextrin-Based Nanofibers and Membranes: Fabrication, Properties and Applications. In *Cyclodextrin-A Versatile Ingredient*: InTech.
- Chen, J., Dyer, M. J., and Yu, M.-F. (2001). Cyclodextrin-mediated soft cutting of single-walled carbon nanotubes, *Journal of the American Chemical Society*, 123, 6201-6202.
- Cheng, Y., Ying, Y., Japip, S., Jiang, S. D., Chung, T. S., Zhang, S., et al. (2018). Advanced porous materials in mixed matrix membranes, *Advanced Materials*, 30, 1802401.
- Cheryan, M. (1998). Ultrafiltration and microfiltration handbook. CRC press,
- Cheryan, M. (2005). Membrane technology in the vegetable oil industry, *Membrane Technology*, 2005, 5-7.
- Chiu, M. C., de Morais Coutinho, C., and Gonçalves, L. A. G. (2009). Carotenoids concentration of palm oil using membrane technology, *Desalination*, 245, 783-786.
- Clark, J. L., and Stezowski, J. J. (2001). Molecular recognition in cyclodextrin complexes of amino acid derivatives. 1. Crystallographic studies of βcyclodextrin complexes with N-acetyl-L-phenylalanine methyl ester and Nacetyl-L-phenylalanine amide pseudopeptides, *Journal of the American Chemical Society*, 123, 9880-9888.
- Clary, J. J. (2013). The Toxicology of Methanol. Wiley,
- Čmolík, J., and Pokorný, J. (2000). Physical refining of edible oils, *European Journal* of Lipid Science and Technology, 102, 472-486.
- Cui, Z., and Muralidhara, H. (2010). *Membrane technology: a practical guide to membrane technology and applications in food and bioprocessing.* Elsevier,
- Darnoko, D., and Cheryan, M. (2006). Carotenoids from red palm methyl esters by nanofiltration, *Journal of the American Oil Chemists' Society*, 83, 365-370.
- Darvishmanesh, S., Buekenhoudt, A., Degrève, J., and Van der Bruggen, B. (2009). General model for prediction of solvent permeation through organic and inorganic solvent resistant nanofiltration membranes, *Journal of Membrane Science*, 334, 43-49.

- Darvishmanesh, S., Degrève, J., and Van der Bruggen, B. (2010). Mechanisms of solute rejection in solvent resistant nanofiltration: the effect of solvent on solute rejection, *Physical Chemistry Chemical Physics*, 12, 13333-13342.
- Davood Abadi Farahani, M. H., Ma, D., and Nazemizadeh Ardakani, P. (2020). Nanocomposite membranes for organic solvent nanofiltration, *Separation & Purification Reviews*, 49, 177-206.
- de Morais Coutinho, C., Chiu, M. C., Basso, R. C., Ribeiro, A. P. B., Gonçalves, L. A. G., and Viotto, L. A. (2009). State of art of the application of membrane technology to vegetable oils: A review, *Food Research International*, 42, 536-550.
- De Souza, M. P., Petrus, J. C. C., Gonçalves, L. A. G., and Viotto, L. A. (2008). Degumming of corn oil/hexane miscella using a ceramic membrane, *Journal* of Food Engineering, 86, 557-564.
- Dijkstra, M., Bach, S., and Ebert, K. (2006). A transport model for organophilic nanofiltration, *J. Membr. Sci.*, 286, 60-68.
- Fang, Y., and Duranceau, S. J. (2013). Study of the effect of nanoparticles and surface morphology on reverse osmosis and nanofiltration membrane productivity, *Membranes*, 3, 196-225.
- Farahani, M. H. D. A., Hua, D., and Chung, T.-S. (2017). Cross-linked mixed matrix membranes consisting of carboxyl-functionalized multi-walled carbon nanotubes and P84 polyimide for organic solvent nanofiltration (OSN), *Separation and Purification Technology*, 186, 243-254.
- Farahani, M. H. D. A., Hua, D., and Chung, T.-S. (2018). Cross-linked mixed matrix membranes (MMMs) consisting of amine-functionalized multi-walled carbon nanotubes and P84 polyimide for organic solvent nanofiltration (OSN) with enhanced flux, *Journal of Membrane Science*, 548, 319-331.
- Fedors, R. F. (1974). A method for estimating both the solubility parameters and molar volumes of liquids, *Polym. Eng. Sci.*, 14, 147-154.
- Filip, D., and Macocinschi, D. (2002). Thermogravimetric analysis of polyurethane– polysulfone blends, *Polymer international*, 51, 699-706.
- Firman, L., Ochoa, N., Marchese, J., and Pagliero, C. (2017a). Simultaneous improvement in solvent permeability and deacidification of soybean oil by nanofiltration, *Journal of food science and technology*, 54, 398-407.

- Firman, L., Ochoa, N. A., Marchese, J., and Pagliero, C. (2017b). Simultaneous improvement in solvent permeability and deacidification of soybean oil by nanofiltration, *Journal of Food Science and Technology*, 54, 398-407.
- Firman, L. R., Ochoa, N. A., Marchese, J., and Pagliero, C. (2020). Designing of spiral wound nanofiltration multistage process for oil concentration and solvent recovery from soybean oil/n-hexane miscella, *Chemical Engineering Research* and Design, 164, 46-58.
- Firman, L. R., Ochoa, N. A., Marchese, J., and Pagliero, C. L. (2013). Deacidification and solvent recovery of soybean oil by nanofiltration membranes, *Journal of membrane science*, 431, 187-196.
- Flory, P. J. (1942). Thermodynamics of high polymer solutions, *The Journal of chemical physics*, 10, 51-61.
- Flory, P. J. (1953). Principles of polymer chemistry. Cornell University Press,
- Flory, P. J., and Rehner Jr, J. (1943). Statistical mechanics of cross-linked polymer networks I. Rubberlike elasticity, *The journal of chemical physics*, 11, 512-520.
- Fornasero, M., Marenchino, R., and Pagliero, C. L. (2013). Deacidification of soybean oil combining solvent extraction and membrane technology, *Advances in Materials Science and Engineering*, 2013.
- Galizia, M., and Bye, K. P. (2018). Advances in organic solvent nanofiltration rely on physical chemistry and polymer chemistry, *Frontiers in chemistry*, 6, 511.
- Gao, H., Sun, X., and Gao, C. (2017). Antifouling polysulfone ultrafiltration membranes with sulfobetaine polyimides as novel additive for the enhancement of both water flux and protein rejection, *Journal of Membrane Science*, 542, 81-90.
- Geens, J., Hillen, A., Bettens, B., Van der Bruggen, B., and Vandecasteele, C. (2005a). Solute transport in non-aqueous nanofiltration: effect of membrane material, *Journal of Chemical Technology & Biotechnology: International Research in Process, Environmental & Clean Technology*, 80, 1371-1377.
- Geens, J., Peeters, K., Van der Bruggen, B., and Vandecasteele, C. (2005b). Polymeric nanofiltration of binary water–alcohol mixtures: influence of feed composition and membrane properties on permeability and rejection, *Journal of Membrane Science*, 255, 255-264.

- Geens, J., Van der Bruggen, B., and Vandecasteele, C. (2006). Transport model for solvent permeation through nanofiltration membranes, *Separation and purification technology*, 48, 255-263.
- Gevers, L. E., Meyen, G., De Smet, K., Van De Velde, P., Du Prez, F., Vankelecom,
 I. F., et al. (2006). Physico-chemical interpretation of the SRNF transport mechanism for solutes through dense silicone membranes, *Journal of membrane science*, 274, 173-182.
- Ghazali, N. F., and Lim, K. M. (2020). Mass Transport Models in Organic Solvent Nanofiltration: A Review, *Journal of Advanced Research in Fluid Mechanics* and Thermal Sciences, 76, 126-138.
- Gmehling, J., Lohmann, J., Jakob, A., Li, J., and Joh, R. (1998). A modified UNIFAC (Dortmund) model. 3. Revision and extension, *Ind. Eng. Chem. Res.*, 37, 4876-4882.
- Gmehling, J., Wittig, R., Lohmann, J., and Joh, R. (2002). A modified UNIFAC (Dortmund) model. 4. Revision and extension, *Ind. Eng. Chem. Res.*, 41, 1678-1688.
- Gugliuzza, A. (2015). Membrane Swelling, Encyclopedia of Membranes1-2.
- Gunawan, F. M., Mangindaan, D., Khoiruddin, K., and Wenten, I. G. (2019). Nanofiltration membrane cross-linked by m-phenylenediamine for dye removal from textile wastewater, *Polym. Adv. Technol.*, 30, 360-367.
- Gupta, M. (2008). Basic Oil Chemistry, Practical Guide to Vegetable Oil Processing: AOCS Press, Urban, Illinos, USA.
- Hamm, W., Hamilton, R. J., and Calliauw, G. (2013). *Edible oil processing*. John Wiley & Sons,
- Han, Y., Xu, Z., and Gao, C. (2013). Ultrathin graphene nanofiltration membrane for water purification, *Advanced Functional Materials*, 23, 3693-3700.
- Haynes, R. D. (2009). Using cyclodextrin to stabilize and control colloidal microstickies to improve paper machine runnability. Paper presented at the TAPPI Engineering, Pulping and Environmental Conference, Memphis, TN.
- Holt, J. K., Park, H. G., Wang, Y., Stadermann, M., Artyukhin, A. B., Grigoropoulos, C. P., et al. (2006). Fast mass transport through sub-2-nanometer carbon nanotubes, *Science*, 312, 1034-1037.

- Hu, J., Kim, C., Halasz, P., Kim, J. F., Kim, J., and Szekely, G. (2021). Artificial intelligence for performance prediction of organic solvent nanofiltration membranes, *Journal of Membrane Science*, 619, 118513.
- Huda, W. W. N., and Ahmad, M. (2012). A Comparison of Carbon Molecular Sieve (CMS) Membranes with Polymer Blend CMS Membranes for Gas Permeation Applications, ASEAN Journal of Chemical Engineering, 12, 51-58.
- Kale, V., Katikaneni, S., and Cheryan, M. (1999). Deacidifying rice bran oil by solvent extraction and membrane technology, *Journal of the American Oil Chemists' Society*, 76, 723-727.
- Kappert, E. J., Raaijmakers, M. J., Tempelman, K., Cuperus, F. P., Ogieglo, W., and Benes, N. E. (2019). Swelling of 9 polymers commonly employed for solventresistant nanofiltration membranes: A comprehensive dataset, *Journal of membrane science*, 569, 177-199.
- Kaul, A. (2000). The phase diagram. In Aqueous Two-Phase Systems: Methods and Protocols (pp. 11-21): Springer.
- Kedem, O., and Katchalsky, A. (1961). A physical interpretation of the phenomenological coefficients of membrane permeability, *The Journal of* general physiology, 45, 143-179.
- Kim, I.-C., Kim, J.-H., Lee, K.-H., and Tak, T.-M. (2002). Phospholipids separation (degumming) from crude vegetable oil by polyimide ultrafiltration membrane, *Journal of Membrane Science*, 205, 113-123.
- Kimmerle, K., and Strathmann, H. (1990). Analysis of the structure-determining process of phase inversion membranes, *Desalination*, 79, 283-302.
- Koike, S., Subramanian, R., Nabetani, H., and Nakajima, M. (2002). Separation of oil constituents in organic solvents using polymeric membranes, *Journal of the American Oil Chemists' Society*, 79, 937-942.
- Konger, R. L. (2006). A new wrinkle on topical vitamin E and photo-inflammation: mechanistic studies of a hydrophilic γ-tocopherol derivative compared with αtocopherol, *Journal of Investigative Dermatology*, 126, 1447-1449.
- Lai, O. M., Tan, C. P., and Akoh, C. C. (2015). *Palm Oil: Production, Processing, Characterization, and Uses.* Elsevier Science,
- Lammerskötter, A., Seggert, H., Matthäus, B., Raß, M., Bart, H. J., and Jordan, V. (2017). Rapeseed hull oil as a source for phytosterols and their separation by

organic solvent nanofiltration, *European Journal of Lipid Science and Technology*, 119, 1600090.

- Lay, S., Ni, X., Yu, H., and Shen, S. (2016). State-of-the-art applications of cyclodextrins as functional monomers in molecular imprinting techniques: a review, *Journal of separation science*, 39, 2321-2331.
- Lee, B. C., and Danner, R. P. (1996). Prediction of polymer-solvent phase equilibria by a modified group-contribution EOS, *AIChE journal*, 42, 837-849.
- Lee, C. H. (1981). Synthetic membranes containing schardinger cyclodextrin additives, *Journal of Applied Polymer Science*, 26, 489-497.
- Lee, S., Kang, T., Lee, J. Y., Park, J., Choi, S. H., Yu, J.-Y., et al. (2021). Thin-Film Composite Nanofiltration Membranes for Non-Polar Solvents, *Membranes*, 11, 184.
- Lejeune, A., Rabiller-Baudry, M., and Renouard, T. (2018). Design of membrane cascades according to the method of McCabe-Thiele: An organic solvent nanofiltration case study for olefin hydroformylation in toluene, *Separation and Purification Technology*, 195, 339-357.
- Li, L., Duan, Z., Chen, J., Zhou, Y., Zhu, L., Xiang, Y., et al. (2017a). Molecular recognition with cyclodextrin polymer: a novel method for removing sulfides efficiently, *RSC Advances*, 7, 38902-38910.
- Li, X., Cai, W., Wang, T., Wu, Z., Wang, J., He, X., et al. (2017b). AF2400/PTFE composite membrane for hexane recovery during vegetable oil production, *Separation and Purification Technology*, 181, 223-229.
- Lim, K. M., and Ghazali, N. F. (2020). Nanofiltration of binary palm oil/solvent mixtures: Experimental and modeling, *Mater. Today-Proc.*
- Lim, S. K., Goh, K., Bae, T.-H., and Wang, R. (2017). Polymer-based membranes for solvent-resistant nanofiltration: A review, *Chinese journal of chemical engineering*, 25, 1653-1675.
- Lin, B., and Zhou, S. (2017). Poly (ethylene glycol)-grafted silica nanoparticles for highly hydrophilic acrylic-based polyurethane coatings, *Progress in Organic Coatings*, 106, 145-154.
- Lin, L., Rhee, K. C., and Koseoglu, S. S. (1997). Bench-scale membrane degumming of crude vegetable oil: Process optimization, *Journal of Membrane Science*, 134, 101-108.

- Liu, Y., You, C.-C., Wada, T., and Inoue, Y. (2000). Molecular Recognition of Aliphatic Alcohols and Carboxylic Acid by Chromophoric Cyclodextrins, *Supramolecular Chemistry*, 12, 243-253.
- Liu, Z., Pang, L., Li, Q., Zhang, S., Li, J., Tong, H., et al. (2018). Hydrophilic porous polyimide/β-cyclodextrin composite membranes with enhanced gas separation performance and low dielectric constant, *High Performance Polymers*, 30, 446-455.
- Livingston, A. G., and See-Toh, Y. H. (2014). Asymmetric membranes for use in nanofiltration: Google Patents.
- Lonsdale, H., Merten, U., and Riley, R. (1965). Transport properties of cellulose acetate osmotic membranes, *Journal of Applied Polymer Science*, 9, 1341-1362.
- Machado, D. o. R., Hasson, D., and Semiat, R. (2000). Effect of solvent properties on permeate flow through nanofiltration membranes: Part II. Transport model, J. *Membr. Sci.*, 166, 63-69.
- Manjula, S., and Subramanian, R. (2006). Membrane technology in degumming, dewaxing, deacidifying, and decolorizing edible oils, *Critical reviews in food science and nutrition*, 46, 569-592.
- Marchetti, P., Jimenez Solomon, M. F., Szekely, G., and Livingston, A. G. (2014). Molecular separation with organic solvent nanofiltration: a critical review, *Chemical reviews*, 114, 10735-10806.
- Marchetti, P., and Livingston, A. G. (2015). Predictive membrane transport models for Organic Solvent Nanofiltration: How complex do we need to be?, *Journal of Membrane Science*, 476, 530-553.
- Marchetti, P., Peeva, L., and Livingston, A. (2017). The selectivity challenge in organic solvent nanofiltration: membrane and process solutions, *Annual review of chemical and biomolecular engineering*, 8, 473-497.
- Marioryad, H., Ghaedi, A. M., Emadzadeh, D., Baneshi, M. M., Vafaei, A., and Lau,
 W. J. (2020). A Thin Film Nanocomposite Reverse Osmosis Membrane Incorporated with S-Beta Zeolite Nanoparticles for Water Desalination, *ChemistrySelect*, 5, 1972-1975.
- Mason, E., and Lonsdale, H. (1990). Statistical-mechanical theory of membrane transport, *Journal of Membrane Science*, 51, 1-81.

- Menczel, J. D., and Prime, R. B. (2014). *Thermal Analysis of Polymers: Fundamentals* and Applications. Wiley,
- Meyers, R. A. (2012). Encyclopedia of Analytical Chemistry. Wiley,
- Micovic, J., Werth, K., and Lutze, P. (2014). Hybrid separations combining distillation and organic solvent nanofiltration for separation of wide boiling mixtures, *Chemical Engineering Research and Design*, 92, 2131-2147.
- Miller, E. C., Hadley, C. W., Schwartz, S. J., Erdman, J. W., Boileau, T. W.-M., and Clinton, S. K. (2002). Lycopene, tomato products, and prostate cancer prevention. Have we established causality?, *Pure and Applied Chemistry*, 74, 1435-1441.
- Mulder, J. (2012). *Basic Principles of Membrane Technology*. Springer Science & Business Media, The Netherlands.
- Murthy, Z., and Chaudhari, L. B. (2009). Separation of binary heavy metals from aqueous solutions by nanofiltration and characterization of the membrane using Spiegler–Kedem model, *Chemical Engineering Journal*, 150, 181-187.
- Murthy, Z., and Gupta, S. K. (1997). Estimation of mass transfer coefficient using a combined nonlinear membrane transport and film theory model, *Desalination*, 109, 39-49.
- Nasrollahi, N., Aber, S., Vatanpour, V., and Mahmoodi, N. M. (2019). Development of hydrophilic microporous PES ultrafiltration membrane containing CuO nanoparticles with improved antifouling and separation performance, *Materials Chemistry and Physics*, 222, 338-350.
- Nazari, A., and Riahi, S. (2011). The effects of SiO2 nanoparticles on physical and mechanical properties of high strength compacting concrete, *Composites Part B: Engineering*, 42, 570-578.
- Nguyen Thi, H. Y., Nguyen, B. T. D., and Kim, J. F. (2021). Sustainable Fabrication of Organic Solvent Nanofiltration Membranes, *Membranes*, 11, 19.
- O'Brien, R. D. (2008). Fats and Oils: Formulating and Processing for Applications, Third Edition. CRC Press,
- Okarter, N., and Liu, R. H. (2010). Health Benefits of Whole Grain Phytochemicals, *Critical Reviews in Food Science and Nutrition*, 50, 193-208.
- Pagliero, C., Ochoa, N., Marchese, J., and Mattea, M. (2004). Vegetable oil degumming with polyimide and polyvinylidenefluoride ultrafiltration membranes, *Journal of Chemical Technology & Biotechnology*, 79, 148-152.

- Pal, Y. P., and Pratap, A. P. (2017). Rice Bran Oil: A Versatile Source for Edible and Industrial Applications, *Journal of Oleo Science*, 66, 551-556.
- Panchal, T. M., Patel, A., Chauhan, D., Thomas, M., and Patel, J. V. (2017). A methodological review on bio-lubricants from vegetable oil based resources, *Renewable and Sustainable Energy Reviews*, 70, 65-70.
- Peeva, L., da Silva Burgal, J., Valtcheva, I., and Livingston, A. G. (2014). Continuous purification of active pharmaceutical ingredients using multistage organic solvent nanofiltration membrane cascade, *Chemical Engineering Science*, 116, 183-194.
- Peeva, L. G., Gibbins, E., Luthra, S. S., White, L. S., Stateva, R. P., and Livingston, A. G. (2004). Effect of concentration polarisation and osmotic pressure on flux in organic solvent nanofiltration, *Journal of Membrane Science*, 236, 121-136.
- Peshev, D., and Livingston, A. G. (2013). OSN Designer, a tool for predicting organic solvent nanofiltration technology performance using Aspen One, MATLAB and CAPE OPEN, *Chemical Engineering Science*, 104, 975-987.
- Phoenix, J., Edwards, R., and Jackson, M. J. (1989). Inhibition of Ca2+-induced cytosolic enzyme efflux from skeletal muscle by vitamin E and related compounds, *Biochemical Journal*, 257, 207-213.
- Pratap, R. (2010). *Getting Started with MATLAB: A Quick Introduction for Scientists* and Engineers. Oxford University Press,
- Priske, M., Lazar, M., Schnitzer, C., and Baumgarten, G. (2016). Recent applications of organic solvent nanofiltration, *Chemie Ingenieur Technik*, 88, 39-49.
- Pusch, W. (1977). Determination of Transport Parameters of Synthetic Membranes by Hyperfiltration Experiments Part I: Derivation of Transport Relationship from the Linear Relations of Thermodynamics of Irreversible Processes, *Berichte der Bunsengesellschaft für physikalische Chemie*, 81, 269-276.
- Rahimi, Z., Zinatizadeh, A. A., Zinadini, S., and van Loosdrecht, M. (2020). βcyclodextrin functionalized MWCNTs as a promising antifouling agent in fabrication of composite nanofiltration membranes, *Separation and Purification Technology*, 247, 116979.
- Rameetse, M. S., Aberefa, O., and Daramola, M. O. (2020). Effect of loading and functionalization of carbon nanotube on the performance of blended polysulfone/polyethersulfone membrane during treatment of wastewater containing phenol and benzene, *Membranes*, 10, 54.

- Reddy, K. K., Subramanian, R., Kawakatsu, T., and Nakajima, M. (2001). Decolorization of vegetable oils by membrane processing, *European Food Research and Technology*, 213, 212-218.
- Reid, R. C., Prausnitz, J. M., and Poling, B. E. (1987). *The Properties of Gases and Liquids*. McGraw-Hill Inc., USA.
- Reiners, R. A., and Birkhaug, F. J. (1970). Glyceride oil treatment: Google Patents.
- Renouard, T., Lejeune, A., and Rabiller-Baudry, M. (2018). Separation of solutes with an organic solvent nanofiltration cascade: Designs, simulations and systematic study of all configurations, *Separation and Purification Technology*, 194, 111-122.
- Robinson, J., Tarleton, E., Millington, C., and Nijmeijer, A. (2004). Solvent flux through dense polymeric nanofiltration membranes, *Journal of membrane science*, 230, 29-37.
- Roy, B., Dey, S., Sahoo, G. C., Roy, S. N., and Bandyopadhyay, S. (2014). Degumming, dewaxing and deacidification of rice bran oil-hexane miscella using ceramic membrane: Pilot plant study, *Journal of the American Oil Chemists' Society*, 91, 1453-1460.
- Rundquist, E. M., Pink, C. J., and Livingston, A. G. (2012). Organic solvent nanofiltration: a potential alternative to distillation for solvent recovery from crystallisation mother liquors, *Green Chemistry*, 14, 2197-2205.
- Saberinasab, M., Salehzadeh, S., Maghsoud, Y., and Bayat, M. (2016). The significant effect of electron donating and electron withdrawing substituents on nature and strength of an intermolecular Se… π interaction. A theoretical study, *Computational and Theoretical Chemistry*, 1078, 9-15.
- Sablani, S., Goosen, M., Al-Belushi, R., and Wilf, M. (2001). Concentration polarization in ultrafiltration and reverse osmosis: a critical review, *Desalination*, 141, 269-289.
- Sani, N., Lau, W., and Ismail, A. (2014). Influence of polymer concentration in casting solution and solvent-solute-membrane interactions on performance of polyphenylsulfone (PPSU) nanofiltration membrane in alcohol solvents, *Journal of Polymer Engineering*, 34, 489-500.
- See-Toh, Y. H., Ferreira, F. C., and Livingston, A. G. (2006). The influence of membrane formation on functional performance of organic solvent nanofiltration membranes, *Desalination*, 199, 242-244.

- See-Toh, Y. H., Silva, M., and Livingston, A. (2008). Controlling molecular weight cut-off curves for highly solvent stable organic solvent nanofiltration (OSN) membranes, *Journal of Membrane Science*, 324, 220-232.
- Seeliger, D., and de Groot, B. L. (2010). Ligand docking and binding site analysis with PyMOL and Autodock/Vina, *Journal of computer-aided molecular design*, 24, 417-422.
- Sherwood, T., Brian, P., and Fisher, R. (1967). Desalination by reverse osmosis, Industrial & Engineering Chemistry Fundamentals, 6, 2-12.
- Shi, G. M., and Chung, T.-S. (2020). Teflon AF2400/polyethylene membranes for organic solvent nanofiltration (OSN), *Journal of Membrane Science*, 602, 117972.
- Shi, G. M., Farahani, M. H. D. A., Liu, J. Y., and Chung, T.-S. (2019). Separation of vegetable oil compounds and solvent recovery using commercial organic solvent nanofiltration membranes, *Journal of Membrane Science*, 588, 117202.
- Shiau, C.-W., Huang, J.-W., Wang, D.-S., Weng, J.-R., Yang, C.-C., Lin, C.-H., et al. (2006). α-Tocopheryl succinate induces apoptosis in prostate cancer cells in part through inhibition of Bcl-xL/Bcl-2 function, *Journal of Biological Chemistry*, 281, 11819-11825.
- Siddique, H., Rundquist, E., Bhole, Y., Peeva, L., and Livingston, A. (2014). Mixed matrix membranes for organic solvent nanofiltration, *Journal of Membrane Science*, 452, 354-366.
- Silva, P., Han, S., and Livingston, A. G. (2005). Solvent transport in organic solvent nanofiltration membranes, *Journal of Membrane Science*, 262, 49-59.
- Solomon, M. F. J., Bhole, Y., and Livingston, A. G. (2012). High flux membranes for organic solvent nanofiltration (OSN)—Interfacial polymerization with solvent activation, *Journal of membrane science*, 423, 371-382.
- Soltane, H. B., Roizard, D., and Favre, E. (2013). Effect of pressure on the swelling and fluxes of dense PDMS membranes in nanofiltration: An experimental study, *Journal of membrane science*, 435, 110-119.
- Soroko, I., and Livingston, A. (2009). Impact of TiO2 nanoparticles on morphology and performance of crosslinked polyimide organic solvent nanofiltration (OSN) membranes, *Journal of Membrane Science*, 343, 189-198.
- Spiegler, K., and Kedem, O. (1966). Thermodynamics of hyperfiltration (reverse osmosis): criteria for efficient membranes, *Desalination*, 1, 311-326.

- Stafie, N., Stamatialis, D., and Wessling, M. (2004). Insight into the transport of hexane–solute systems through tailor-made composite membranes, *Journal of Membrane Science*, 228, 103-116.
- Stark, W. J., Stoessel, P. R., Wohlleben, W., and Hafner, A. (2015). Industrial applications of nanoparticles, *Chemical Society Reviews*, 44, 5793-5805.
- Subramanian, R., Nakajima, M., and Kawakatsu, T. (1998). Processing of vegetable oils using polymeric composite membranes, *Journal of Food Engineering*, 38, 41-56.
- Subramanian, R., Nakajima, M., Raghavarao, K., and Kimura, T. (2004). Processing vegetable oils using nonporous denser polymeric composite membranes, *Journal of the American Oil Chemists' Society*, 81, 313.
- Subramanian, R., Nandini, K., Sheila, P., Gopalakrishna, A., Raghavarao, K., Nakajima, M., et al. (2000). Membrane processing of used frying oils, *Journal* of the American Oil Chemists' Society, 77, 323.
- Subramanian, R., Raghavarao, K., Nabetani, H., Nakajima, M., Kimura, T., and Maekawa, T. (2001a). Differential permeation of oil constituents in nonporous denser polymeric membranes, *Journal of Membrane Science*, 187, 57-69.
- Subramanian, R., Raghavarao, K. S. M. S., Nabetani, H., Nakajima, M., Kimura, T., and Maekawa, T. (2001b). Differential permeation of oil constituents in nonporous denser polymeric membranes, *Journal of Membrane Science*, 187, 57-69.
- Sun, J., Forster, A. M., Johnson, P. M., Eidelman, N., Quinn, G., Schumacher, G., et al. (2011). Improving performance of dental resins by adding titanium dioxide nanoparticles, *Dental Materials*, 27, 972-982.
- Szekely, G., and Zhao, D. (2022). Sustainable Separation Engineering: Materials, Techniques and Process Development. Wiley,
- Tan, S., Ladewig, K., Fu, Q., Blencowe, A., and Qiao, G. G. (2014). Cyclodextrin-Based Supramolecular Assemblies and Hydrogels: Recent Advances and Future Perspectives, *Macromolecular rapid communications*, 35, 1166-1184.
- Tarleton, E., Robinson, J., Millington, C., Nijmeijer, A., and Taylor, M. (2006). The influence of polarity on flux and rejection behaviour in solvent resistant nanofiltration—experimental observations, *Journal of membrane science*, 278, 318-327.

- Thiermeyer, Y., Blumenschein, S., and Skiborowski, M. (2018). Solvent dependent membrane-solute sensitivity of OSN membranes, *Journal of membrane science*, 567, 7-17.
- Thiermeyer, Y., Blumenschein, S., and Skiborowski, M. (2021). Fundamental insights into the rejection behavior of polyimide-based OSN membranes, *Separation and Purification Technology*, 265, 118492.
- Toh, Y. H. S. (2008). Molecular separations with organic solvent nanofiltration. Department of Chemical Engineering and Chemical Technology, Imperial College
- Toh, Y. S., Lim, F., and Livingston, A. (2007). Polymeric membranes for nanofiltration in polar aprotic solvents, *Journal of Membrane Science*, 301, 3-10.
- Tsuru, T., Izumi, S., Yoshioka, T., and Asaeda, M. (2000a). Temperature effect on transport performance by inorganic nanofiltration membranes, *AIChE journal*, 46, 565-574.
- Tsuru, T., Miyawaki, M., Yoshioka, T., and Asaeda, M. (2006). Reverse osmosis of nonaqueous solutions through porous silica-zirconia membranes, *AIChE journal*, 52, 522-531.
- Tsuru, T., Sudou, T., Kawahara, S.-i., Yoshioka, T., and Asaeda, M. (2000b). Permeation of liquids through inorganic nanofiltration membranes, *Journal of colloid and interface science*, 228, 292-296.
- Vaidya, S. Y., Simaria, A. V., and Murthy, Z. (2001). Reverse osmosis transport models evaluation: a new approach.
- Vaisali, C., Charanyaa, S., Belur, P. D., and Regupathi, I. (2015). Refining of edible oils: a critical appraisal of current and potential technologies, *International Journal of Food Science & Technology*, 50, 13-23.
- Van der Bruggen, B., Geens, J., and Vandecasteele, C. (2002). Fluxes and rejections for nanofiltration with solvent stable polymeric membranes in water, ethanol and n-hexane, *Chemical engineering science*, 57, 2511-2518.
- Vandezande, P., Gevers, L. E., and Vankelecom, I. F. (2008). Solvent resistant nanofiltration: separating on a molecular level, *Chemical Society Reviews*, 37, 365-405.

- Vanherck, K., Koeckelberghs, G., and Vankelecom, I. F. (2013). Crosslinking polyimides for membrane applications: a review, *Progress in polymer science*, 38, 874-896.
- Vankelecom, I. F., De Smet, K., Gevers, L. E., Livingston, A., Nair, D., Aerts, S., et al. (2004). Physico-chemical interpretation of the SRNF transport mechanism for solvents through dense silicone membranes, *Journal of membrane science*, 231, 99-108.
- Vatanpour, V., Esmaeili, M., and Farahani, M. H. D. A. (2014). Fouling reduction and retention increment of polyethersulfone nanofiltration membranes embedded by amine-functionalized multi-walled carbon nanotubes, *Journal of Membrane Science*, 466, 70-81.
- Wang, L., Song, X., Wang, T., Wang, S., Wang, Z., and Gao, C. (2015). Fabrication and characterization of polyethersulfone/carbon nanotubes (PES/CNTs) based mixed matrix membranes (MMMs) for nanofiltration application, *Applied Surface Science*, 330, 118-125.
- Wang, X.-L., Tsuru, T., Nakao, S.-i., and Kimura, S. (1997). The electrostatic and steric-hindrance model for the transport of charged solutes through nanofiltration membranes, *Journal of Membrane Science*, 135, 19-32.
- Wang, Z., Zhang, B., Yu, H., Li, G., and Bao, Y. (2011). Synthetic control of network topology and pore structure in microporous polyimides based on triangular triphenylbenzene and triphenylamine units, *Soft Matter*, 7, 5723-5730.
- Weidlich, U., and Gmehling, J. (1987). A modified UNIFAC model. 1. Prediction of VLE, hE, and. gamma. infin, *Ind. Eng. Chem. Res.*, 26, 1372-1381.
- Werth, K., Kaupenjohann, P., Knierbein, M., and Skiborowski, M. (2017a). Solvent recovery and deacidification by organic solvent nanofiltration: Experimental investigation and mass transfer modeling, *Journal of Membrane Science*, 528, 369-380.
- Werth, K., Kaupenjohann, P., and Skiborowski, M. (2017b). The potential of organic solvent nanofiltration processes for oleochemical industry, *Separation and purification technology*, 182, 185-196.
- White, L. S. (2002). Transport properties of a polyimide solvent resistant nanofiltration membrane, *Journal of Membrane Science*, 205, 191-202.
- Wijmans, J. G., and Baker, R. W. (1995). The solution-diffusion model: a review, J. Membr. Sci., 107, 1-21.

- Wilke, C., and Chang, P. (1955). Correlation of diffusion coefficients in dilute solutions, *AIChE journal*, 1, 264-270.
- Xie, W., Li, T., Tiraferri, A., Drioli, E., Figoli, A., Crittenden, J. C., et al. (2020). Toward the Next Generation of Sustainable Membranes from Green Chemistry Principles, ACS Sustainable Chemistry & Engineering.
- Xu, Y. M., Le, N. L., Zuo, J., and Chung, T.-S. (2016). Aromatic polyimide and crosslinked thermally rearranged poly (benzoxazole-co-imide) membranes for isopropanol dehydration via pervaporation, *Journal of Membrane Science*, 499, 317-325.
- Yamasaki, A., Iwatsubo, T., Masuoka, T., and Mizoguchi, K. (1994). Pervaporation of ethanol/water through a poly (vinyl alcohol)/cyclodextrin (PVA/CD) membrane, *Journal of membrane science*, 89, 111-117.
- Yangali-Quintanilla, V., Sadmani, A., McConville, M., Kennedy, M., and Amy, G. (2009). Rejection of pharmaceutically active compounds and endocrine disrupting compounds by clean and fouled nanofiltration membranes, *Water Research*, 43, 2349-2362.
- Yaroshchuk, A. E. (1995). Solution-diffusion-imperfection model revised, *Journal of Membrane Science*, 101, 83-87.
- Yaroshchuk, A. E. (2004). The role of imperfections in the solute transfer in nanofiltration, *Journal of membrane science*, 239, 9-15.
- Yuliwati, E., and Ismail, A. (2011). Effect of additives concentration on the surface properties and performance of PVDF ultrafiltration membranes for refinery produced wastewater treatment, *Desalination*, 273, 226-234.
- Zhou, R., Rana, D., Matsuura, T., and Lan, C. Q. (2019). Effects of multi-walled carbon nanotubes (MWCNTs) and integrated MWCNTs/SiO2 nano-additives on PVDF polymeric membranes for vacuum membrane distillation, *Separation and Purification Technology*, 217, 154-163.
- Zhou, Y., Huang, X., and Tang, X. (2009). Synthesis and characterization of novel thermoplastic poly (oligophosphazene-urethane) s, *Polymer international*, 58, 710-714.
- Zhu, L. (2015). Rejection of organic micropollutants by clean and fouled nanofiltration membranes, *Journal of Chemistry*, 2015.

LIST OF PUBLICATIONS

Indexed Journal (SCOPUS)

 Ghazali, N. F., & Lim, K. M. (2020). Mass Transport Models in Organic Solvent Nanofiltration: A Review. Journal of Advanced Research in Fluid Mechanics and Thermal Sciences, 76(3), 126-138.

Indexed conference proceedings

- Lim, K. M., & Ghazali, N. F. (2021). Nanofiltration of binary palm oil/solvent mixtures: Experimental and modeling. Materials Today: Proceedings, 39, 1010-1014. (Indexed by WOS)
- Lim, K. M., & Ghazali, N. F. (2020). Estimation of solute transport parameter and mass transfer coefficient in nanofiltration for solvent-diluted palm oil. In IOP Conference Series: Materials Science and Engineering (Vol. 736, No. 2, p. 022070). IOP Publishing. (Indexed by SCOPUS)

Non-Indexed conference proceedings

- Lim, K. M., & Ghazali, N. F. (2019). Estimation of Solute Transport Parameter and Mass Transfer Coefficient in Nanofiltration for Solvent-Diluted Palm Oil. Energy Security and Chemical Engineering Congress (ESChE 2019). 17-19 July 2019. Penang, Malaysia.
- Lim, K. M. & Ghazali, N. F. (2019). Nanofiltration of Binary Palm Oil/ Solvent Mixtures: Experimental and Modeling. Sustainable & Integrated Engineering International Conference (SIE 2019). 8-9 December 2019. Putrajaya, Malaysia.
- Ghazali, N. F. & Lim, K. M. (2019). Mass Transport Models in Organic Solvent Nanofiltration: A Review. The 4th International Symposium on Fluid Mechanics and Thermal Sciences (4th IS-FMTS 2019). 14 December 2019. Putrajaya, Malaysia.

 Lim, K. M. & Ghazali, N. F. (2019). Refining Palm Oil by Membrane Technology. UTM Graduate Seminar 2019/2020 Semester 1. 15-16 January 2020. UTM Kuala Lumpur, Malaysia.

Book Chapter

 Ghazali, N. F., & Lim, K. M. (2022). Sustainable Separations using Organic Solvent Nanofiltration. Szekely, G., and Zhao, D., Sustainable Separation Engineering: Materials, Techniques and Process Development. John Wiley and Sons Ltd. Accepted for publication.